

# Natural Convection and Thermal Radiation Influence on Nanofluid Flow over a Nonlinearly Stretching Sheet

#### Emad M. Abo-Eldahab<sup>1</sup>, Rasha Adel<sup>1\*</sup>, Yasmin M. Saad<sup>2</sup>

<sup>1</sup>Department of Mathematics, Faculty of Science, Helwan University, Cairo, Egypt <sup>2</sup>Basic Science Department, School of Engineering, Canadian International Collage, Giza, Egypt Email: \*roshaadel23@gmail.com

How to cite this paper: Abo-Eldahab, E.M., Adel, R. and Saad, Y.M. (2022) Natural Convection and Thermal Radiation Influence on Nanofluid Flow over a Nonlinearly Stretching Sheet. *Journal of Applied Mathematics and Physics*, **10**, 3301-3315. https://doi.org/10.4236/jamp.2022.1011219

**Received:** October 16, 2022 **Accepted:** November 20, 2022 **Published:** November 23, 2022

Copyright © 2022 by author(s) and Scientific Research Publishing Inc. This work is licensed under the Creative Commons Attribution International License (CC BY 4.0). http://creativecommons.org/licenses/by/4.0/

**Open Access** 

## Abstract

This paper studies the effects of Natural convection and Thermal radiation on nanofluid over a non-linearly stretching sheet. The governing equation of nonlinear partial differential equations of the flow is transformed to nonlinear ordinary differential equations by using similarity transformation, earlier than being solved numerically through a Rung-Kutta-Fehlberg method with shooting technique. The numerical results have been obtained for The influence of Brownian motion number (*Nb*), thermophoresis number (*Nt*), Grashof number (*Gr*), Lewis number (*Le*), stretching parameter (*n*), and thermal radiation parameter (*Ra*) on the velocity, temperature, and nanoparticles concentration profiles are shown graphically.

## **Keywords**

Nanofluid, Stretching Sheet, Thermal Radiation, Free Convection

## **1. Introduction**

The study of flow over a stretching sheet has generated a lot of interest in recent years in view of its several industrial programs along with the aerodynamic extrusion of plastic sheets, boundary layer behavior over stretching surface is crucial because it consists of several engineering processes, like, glass-fiber and paper production. Natural convection is a kind of flow motion of a liquid which includes water or a gas such as air, wherein the fluid motion isn't always generated with the aid of any external supply but with the aid of some parts of the fluid being heavier than other parts. This force of a natural Convection is gravity. However, the simultaneous impact of thermal radiation and magnetic effects on unsteady laminar viscous nanofluid flow over a shrinking sheet is given by Nandy et al. [1]. He found that the dual solutions exist for the flow over a shrinking sheet. Kuznetsov and Nield [2] have finished an analytical study on natural convective flow of a nanofluid past a vertical plate below the influence of Brownian motion and thermophoresis results. Turkyilmazoglu and Pop [3] studied the unsteady and thermal transport characteristics of different nanofluids flowing a protracted vertical plate with the consideration of a radiative effect. The study of temperature and velocity field over warm vertical plate due to natural Convection is investigated by Schmidt and Beckmann. Ostrach [5] applied method of iterative integration to research free convection over a semi-infinite isothermal flat plate. Sparrow and Gregg [6] offered a similar study on numerical solutions for laminar-free convection from a vertical plate with uniform surface heat flux. Since the pioneering work of Sakiadis, various elements of the problem were investigated through many authors, which includes Xu and Liao [8], Cortell [9], Hayat and Sajid [10] and Hayat *et al.* [11]. The effect of magnetic field in viscous flow over a stretching cylinder embedded in a porous medium has been studied by Butt. Ishak et al. [13] defined suction/injection influence on regular flow of an incompressible fluid over a permeable stretching tube, they discovered that Reynolds number ascends as mounting in the numerical values of skin friction coefficient. Alok et al. [14] study that the collective has an effect on thermal radiation and convection flow of cu-water nanofluid because of a stretching cylinder in porous medium a protracted with viscous dissipation and slip boundary conditions. The role of radiation heat transfer is superficial in lots of engineering approaches which occurs at high temperature. A large number of experimental and theoretical research had been done with the aid of numerous researchers on radiation impact [15] [16] [17] [18]. In most of the mentioned literature, radiation effect was inspected by imposing the linearized Rosseland approximation. This approximation involves the dimensionless parameter as radiation parameter and prandtl number due to the temperature difference between the plate and ambient fluid is small. However, for the large temperature difference, non linearized Rossland approximation is legitimate. M. Archana et al. [19] examined the effect of nonlinear thermal radiation on rotating flow of a casson nanofluid. Biliana et al. [20] examined the numerical solution of the boundary layer flow over an exponentially stretching sheet with thermal radiation. A. Brusly Solomon et al. [21] examined the natural convection enhancement in a porous cavity with Al<sub>2</sub>O<sub>3</sub>-Ethylene glycol/water nanofluids. And S M Sohel Murshed et al. [22] present experimental research and development on the Natural Convection of Suspensions of Nanoparticles-A Comprehensive Review. A. I. Alsabery et al. [23] research the Natural Convection Flow of a nanofluid in an inclined square enclosure partially filled with a Porous Medium. And M. Ghalambaz et al. [24] tested Natural convection of nanofluids over a convectively heated vertical plate embedded in a porous medium. In this paper, we investigated numerically and extend the work by P. Rana et al. [25]. This research is

based on a study on the effects of Natural Convection and Thermal radiation on nanofluid over a stretching sheet. The governing partial differential equations were transformed into ordinary differential equations by using similarity solution transformation. We have solved the ordinary differential equations numerically by using shooting method (Rung-Kutta-Fehlberg) and we get the result for the effects of Brownian motion number (*Nb*), thermophoresis number (*Nt*), Grashof number (*Gr*), Lewis number (*Le*), stretching parameter (*n*), and thermal radiation parameter (*Ra*) on the velocity, temperature, and nanoparticles concentration.

#### 2. Mathematical Formulation

Considering the nano fluid is steady, incompressible laminar two dimensional flow past a flat sheet coinciding with plane y=0 and the flow are confined to y>0. The flow is generated, because of non-linear stretching of the sheet caused by the simultaneous application of equal and opposite force alongside *x*-axis. Keeping the original fixed, the sheet is then stretch with a velocity  $u_w = ax^n$  wherein *a* is a constant, *n* is a nonlinear stretching parameter and *x* is the coordinate measured along the stretching surface, varying nonlinearly with the distance from the slit. The problem is within the presence of thermal radiation and free convection. The flow configuration of this problem is illustrated in **Figure 1**.

The pressure gradient and external force are neglected. The stretching surface is maintained at constant temperature and concentration,  $T_w$  and  $C_w$ , respectively, and these values are assumed to be greater than the ambient temperature and concentration,  $T_{\infty}$  and  $C_{\infty}$ , respectively. The basic steady conservation of mass, momentum, thermal energy and nanoparticles equations for nanofluids can be written in Cartesian coordinates x and y as, see Buongiorno [26], Kuznetsov and Nield [27], Niled and Kuznetsov [28], Bachok *et al.* [29] and Khan and Pop [30],

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0 \tag{1}$$

$$u\frac{\partial u}{\partial x} + v\frac{\partial u}{\partial y} = v\frac{\partial^2 u}{\partial y^2} + (1 - \varphi_{\infty})g\beta(T - T_{\infty})$$
(2)



Figure 1. Physical model and coordinate system.

$$u\frac{\partial T}{\partial x} + v\frac{\partial T}{\partial y} = \alpha_m \nabla^2 T + \tau \left[ D_B \frac{\partial C}{\partial y} \frac{\partial T}{\partial y} + \frac{D_T}{T_\infty} \left( \frac{\partial T}{\partial y} \right)^2 \right] - \frac{1}{\rho c_p} \frac{\partial q_r}{\partial y}$$
(3)

$$u\frac{\partial C}{\partial x} + v\frac{\partial C}{\partial y} = D_B \frac{\partial^2 C}{\partial y^2} + \frac{D_T}{T_{\infty}} \frac{\partial^2 T}{\partial y^2}$$
(4)

where

$$\alpha_m = \frac{k_m}{(\rho c)_p}, \ \tau = \frac{(\rho c)_p}{(\rho c)_f}$$
(5)

Here *u* and *v* are the velocity components along the axes *x* and *y*, respectively.  $\alpha_m$  is the thermal diffusivity,  $\rho_f$  is the density of the base fluid,  $D_B$  is the Brownian diffusion coefficient,  $D_T$  is the thermophoretic diffusion coefficient,  $\tau$  is the ratio between the effective heat capacity of the nanoparticle material and heat capacity of the fluid,  $\beta$  is the volumetric coefficient of the thermal expansion, *g* is the gravitational acceleration,  $\varphi_{\infty}$  is nanoparticle volume fraction,  $q_r$  is the radiative heat flux,  $C_p$  is the heat capacity at constant pressure *p*, *C* is the concentration of nanoparticles volume fraction,  $\rho_p$  is the density of the particle,  $(\rho c)_p$  effective heat capacity of the nanoparticle material,  $(\rho c)_f$ heat capacity of the fluid and  $T_{\infty}$  is the temperature of the ambient fluid.

The appropriate boundary conditions for the problem are:

$$v = 0, u_w = ax^n, T = T_w, C = C_w \text{ at } y = 0$$
  

$$u = v = 0, T = T_\infty, C = C_\infty \text{ as } y \to \infty$$
(6)

Using Roseland's approximation, the radiative heat flux  $q_r$  is modeled as

$$q_r = -\left(\frac{4\sigma}{3k_1}\right)\frac{\partial T^4}{\partial y},\tag{7}$$

where  $\sigma$  is the Stefan-Boltzmann constant and  $k_1$  is the absorption coefficient. Assuming that the difference in temperature within the flow is such that  $T^4$  can be expressed as a linear combination of temperature, we expand  $T^4$  in Taylor's series about  $T_{\infty}$  as follows:

$$T^{4} = T_{\infty}^{4} + 4T_{\infty}^{3} \left( T - T_{\infty} \right) + 6T_{\infty}^{2} \left( T - T_{\infty} \right)^{2} + \cdots$$
(8)

And neglecting higher order terms beyond the first degree in  $(T - T_{\infty})$ , we have

$$T^4 \approx 3T_{\infty}^4 + 4T_{\infty}^3 T.$$
(9)

Differentiating (7) with respect to y and using (9) we get

$$\frac{\partial q_r}{\partial y} = -\frac{16T_{\infty}^3\sigma}{3k_1}\frac{\partial^2 T}{\partial y^2}$$
(10)

Using (10) in (3) we obtain

$$u\frac{\partial T}{\partial x} + v\frac{\partial T}{\partial y} = \alpha_m \nabla^2 T + \tau \left[ D_B \frac{\partial C}{\partial y} \frac{\partial T}{\partial y} + \frac{D_T}{T_{\infty}} \left( \frac{\partial T}{\partial y} \right)^2 \right] + \frac{16\sigma T_{\infty}^3}{3k_1 \rho C_P} \frac{\partial^2 T}{\partial y^2}$$
(11)

We look for a similarity solution of Equations ((1), (2), (4), (11)) with the boundary conditions (6) of the following form:

$$\eta = y \sqrt{\frac{a(n+1)}{2\nu}} x^{\frac{n-1}{2}}, \quad u = a x^n f'(\eta), \quad v = -\sqrt{\frac{a\nu(n+1)}{2}} x^{\frac{n-1}{2}} \left( f + \left(\frac{n-1}{n+1}\right) \eta f' \right)$$
  
$$\theta(\eta) = \frac{T - T_{\infty}}{T_w - T_{\infty}}, \quad \phi(\eta) = \frac{C - C_{\infty}}{C_w - C_{\infty}}$$
(12)

The governing Equations ((1), (2), (4), (11)) then reduce to

$$f''' + ff'' - \left(\frac{2n}{n+1}\right)f'^2 + \left(\frac{2}{n+1}\right)Gr\theta = 0$$
(13)

$$\left(\frac{1}{pr} + Ra\right)\theta'' + f\theta' + Nb\theta'\phi' + Nt\theta'^2 = 0$$
(14)

$$\phi'' + Lef \,\phi' + \frac{Nt}{Nb} \,\theta'' = 0 \tag{15}$$

The transformed boundary conditions are

$$f = 0, f' = 1, \theta = 1, \phi = 1 \text{ at } \eta = 0,$$
  

$$f' = 0, \theta = 0, \phi = 0 \text{ as } \eta \to \infty$$
(16)

where

$$pr = \frac{v}{\alpha} \text{ is the Prandtl number, } Le = \frac{v}{D_B} \text{ is the Lewis number,}$$
$$Nb = \frac{(\rho c)_p D_B (C_w - C_w)}{(\rho c)_f v} \text{ is the Brownian motion parameter,}$$
$$Nt = \frac{(\rho c)_p D_T (T - T_w)}{(\rho c)_f v T_w} \text{ is the thermophoresis parameter,}$$
$$Gr = \frac{(1 - \varphi_w)g\beta_T (T_w - T_w)}{a^2 x^{2n-1}} \text{ is the Grashof number, } Ra = \frac{16\sigma T_w^3}{3k_1\rho c_p v} \text{ is the}$$

radiation parameter.

### 3. Result and Discussion

Numerical computation is carried out for several set of values of the parameters that describe the flow characteristics and the results are illustrated graphically. The partial differential Equations ((1), (2), (4), (11)) subject to the boundary condition (6) are transformed into ordinary equation by using similarity transformation method, before solved numerically by a Rung-Kutta method with shooting technique. We studied the impact of several prevailing physical parameters such as stretching parameter (*n*), Prandtl number (*Pr*), Brownian motion parameter (*Nb*), thermophoresis parameter (*Nt*), Lewis number (*Le*), radiation parameter (*Ra*), and Grashof number (*Gr*), on flow and heat transfer are elucidated through figures, the region of integration  $\eta$  is considered as 0 to  $\eta_{\infty} = 7$ , where  $\eta_{\infty}$  corresponds to  $\eta \to \infty$  which lies very well outside the momentum

and thermal boundary layers. We studied the influence of the above parameters on the velocity  $f'(\eta)$ , temperature  $\theta(\eta)$  and concentration distribution  $\phi(\eta)$ .

**Figures 2-4** we observe that  $f'(\eta), \theta(\eta)$  and  $\phi(\eta)$  with different value of *Ra*, which *Ra* = (0.2, 0.5, 1, 1.5) with *Pr* = 2, *Nt* = *Nb* = *Gr* = 0.5, *Le* = 2 and *n* = 2. It is observed reduction in concentration  $\phi(\eta)$  with increasing in thermal radiation but temperature fluid  $\theta(\eta)$  increasing with increases radiation parameter *Ra* and there is no obvious effect on velocity  $f'(\eta)$ .

**Figure 5** & **Figure 6** the effect of Brownian motion parameter *Nb* on temperature  $\theta(\eta)$  and concentration  $\phi(\eta)$ , which Nb = (0.5, 1, 1.5, 2.5) and Pr = n =Le = 2, Nt = Ra = Gr = 0.5. the temperature  $\theta(\eta)$  in the boundary layer



**Figure 2.** The effect of radiation parameter (*Ra*) on velocity distribution for Pr = Le = n = 2, Nt = Nb = Gr = 0.5.







**Figure 4.** The effect of radiation parameter (*Ra*) on concentration distribution for Pr = n = Le = 2, Nt = Nb = Gr = 0.5.



**Figure 5.** The effect of Brownian motion parameter *Nb* on temperature distribution for Pr = n = Le = 2, Nt = Ra = Gr = 0.5.





increasing with increasing in the Brownian parameter, but the nano-particle volume fraction profile  $\phi(\eta)$  decreases with the increasing in the Brownian motion parameter and there no obvious effect on velocity profiles  $f'(\eta)$  The Brownian motion of nanoparticles can enhance thermal conduction via one of two mechanism—either a direct effect owing to nanoparticles the transport heat or alternatively via an indirect contribution due to micro-convection of fluid surrounding individual nanoparticles. For small particles, Brownian motion is strong and the parameter *Nb* will have high values; the converse is the case for large particles and clearly Brownian motion does exert a significant enhancing influence on both temperature and concentration profiles.

**Figure 7 & Figure 8** with the different values of Nt = (0.5, 1, 1.5, 2) the effect of thermophretic parameter (*Nt*) with value of Pr = 2, Nb = Gr = Ra = 0.5, Le = 2



**Figure 7.** The effect of thermophoresis parameter (*Nt*) on temperature distribution for Pr = n = Le = 2, Nb = Ra = Gr = 0.5.





and n = 2, it is observed that an increasing in the thermophoretic parameter (*Nt*) leads to increase in both fluid temperature  $\theta(\eta)$  and concentration  $\phi(\eta)$  and there is no obvious effect on velocity profiles  $f'(\eta)$ .

**Figures 9-11** illustrate the effect of stretching parameter (*n*) on velocity  $f'(\eta)$ , temperature  $\theta(\eta)$  and concentration  $\phi(\eta)$  with different values of n = (0, 0.75, 3, 4) and Pr = Le = 2, Nb = Nt = Ra = Gr = 0.5., it is observed that an increasing in the stretching parameter (*n*), leads to increasing in temperature and concentration but decreases in velocity i.e. rate of heat transfer and mass transfer decreases with increasing in stretching sheet (*n*).

**Figure 12** & Figure 13 illustrate the effect of Lewis number (*Le*) which *Le* = (2, 4, 6, 10) and *Pr* = *n* = 2, *Nb* = *Ra* = *Gr* = *Nt* = 0.5. It defines as the ratio of thermal diffusivity to mass diffusivity. The increases of Lewis number it's leads to decreasing in both temperature  $\theta(\eta)$  and concentration  $\phi(\eta)$  and there is no obvious effect on velocity profiles  $f'(\eta)$ .

**Figures 14-16** depict the variation of velocity  $f'(\eta)$ , temperature  $\theta(\eta)$ 



**Figure 9.** The effect of stretching parameter (*n*)on velocity distribution for Pr = Le = 2, Nb = Ra = Gr = Nt = 0.5.







**Figure 11.** The effect of stretching parameter (*n*) on concentration distribution for Pr = Le = 2, Nb = Ra = Gr = Nt = 0.5.



**Figure 12.** The effect of Lewis number on the temperature distribution for Pr = n = 2, Nb = Ra = Gr = Nt = 0.5.







**Figure 14.** The effect of Grashof number *Gr* on velocity distribution for Pr = n = Le = 2, Nb = Ra = Nt = 0.5.



**Figure 15.** The effect of Grashof number *Gr* on temperature distribution for Pr = n = Le= 2, Nb = Ra = Nt = 0.5.





and concentration  $\phi(\eta)$  with Grashof number (*Gr*), with various values [0.5, 1, 1.5, 2] and Pr = n = Le = 2, Nb = Ra = Nt = 0.5., Grashof number (*Gr*) defined as the ratio of the buoyant to viscous force acting on a fluid in the velocity boundary layer. It is used in the correlation of heat and mass transfer due to thermally induced natural convection at a solid surface immersed in a fluid. The increasing in Grashof number (*Gr*) leads to decreases in velocity  $f'(\eta)$  but increases in both fluid temperature  $\theta(\eta)$  and nanoparticles concentration  $\phi(\eta)$ .

**Figure 17 & Figure 18** depict the variation of temperature  $\theta(\eta)$  and concentration  $\phi(\eta)$  with Prandtl number (*Pr*) = 2, 3, 6.2, 10 and n = Le = 2, Nb = Ra = Gr = Nt = 0.5, which Prandtl number (*Pr*) defined as the ratio of momentum diffusivity to thermal diffusivity. The effect of increasing in Prandtl number on temperature  $\theta(\eta)$  and concentration ( $\eta$ ), leads to decrease in temperature  $\theta(\eta)$  but increases in nanoparticle concentration  $\phi(\eta)$  and there is no obvious effect on velocity profiles  $f'(\eta)$ .



**Figure 17.** The effect of Prandtl number *Pr* on temperature distribution for Le = n = 2, *Nt* = Nb = Ra = Gr = 0.5.



**Figure 18.** The effect of Prandtl number *Pr* on concentration distribution for n = Le = 2, Nb = Ra = Gr = Nt = 0.5.

#### 4. Conclusions

In the present paper, we have examined the boundary layer flow which is the non-linear stretching of a flat surface in a nanofluid with thermal radiation and free convection with Brownian motion and thermophoresis effects. The governing partial differential equations for mass, momentum, energy and nanoparticles conservation are transformed into ordinary differential equations by using similarity transformation. Then these equations are solved numerically by using shooting method. Effects of various parameters on velocity, temperature and concentration profiles are shown graphically. The result, in summary, has shown that:

1) An analytical solution for boundary layer flow with non-linear stretching of flat surface in nanofluid with thermal radiation and free convection was obtained.

2) The velocity within the boundary layer decreases when a stretching parameter (*n*) and Grashof number (*Gr*) are increasing, and there is no effect with increasing of radiation parameter (*Ra*), Brownian motion parameter (*Nb*), thermophoresis parameter (*Nt*), Lewis number (*Le*), and Prandtl number (*Pr*).

3) The temperature  $\theta(\eta)$  within the boundary decreases when Lewis number (*Le*), and Prandtl number (*Pr*) are increasing, and increases with radiation parameter (*Ra*), Brownian motion parameter (*Nb*), thermophoresis parameter (*Nt*) and stretching parameter (*n*).

4) The concentration  $\phi(\eta)$  within the boundary decreases when radiation parameter (*Ra*), Brownian motion parameter (*Nb*) and Lewis number (*Le*) are increasing, and increasing with thermophoresis parameter (*Nt*), stretching parameter (*n*), Prandtl number (*Pr*), and radiation parameter (*Ra*).

#### **Conflicts of Interest**

The authors declare no conflicts of interest regarding the publication of this paper.

#### References

- Nandy, S.K., Sidui, S. and Mahapatra, T.R. (2014) Unsteady MHD Boundary-Layer Flow and Heat Transfer of Nanofluid over a Permeable Shrinking Sheet in the Presence of Thermal Radiation. *Alexandria Engineering Journal*, 53, 929-937. <u>https://doi.org/10.1016/j.aej.2014.09.001</u>
- [2] Kuznetsov, A.V. and Nield, D.A. (2010) Natural Convective Boundary-Layer Flow of a Nanofluid past a Vertical Plate. *International Journal of Thermal Sciences*, 49, 243-247. <u>https://doi.org/10.1016/j.ijthermalsci.2009.07.015</u>
- [3] Turkyilmazoglu, M. and Pop, I. (2013) Heat and Mass Transfer of Unsteady Natural Convection Flow of Some Nanofluids past a Vertical Infinite Flat Plate with Radiation Effect. *International Journal of Heat and Mass Transfer*, 59, 167-171. <u>https://doi.org/10.1016/j.ijheatmasstransfer.2012.12.009</u>
- [4] Schmidt, E. and Beckmann, W. (1930) Das temperatur-und geschwindigkeitsfeld vor einer warme abgebenden senkrecher platte bei naturelicher convention. *Technische Mechanik und thermodynamik*, 1, 341-349.

https://doi.org/10.1007/BF02640222

- [5] Ostrach, S. (1953) An Analysis of Laminar Free-Convection Flow and Heat Transfer about a Flat Plate Parallel to the Direction of the Generating Body Force. NACA Report, University of North Texas, Denton.
- [6] Sparrow, E.M. and Gregg, J.L. (1956) Laminar Free Convection from a Vertical Plate with Uniform Surface Heat Flux. *Transactions ASME*, 78, 435-440. <u>https://doi.org/10.1115/1.4013697</u>
- [7] Sakiadis, B.C. (1961) Boundary-Layer Behavior on Continuous Solid Surfaces: I Boundary Layer Equations for Two Dimensional and Axisymmetric Flow. AIChE Journal, 7, 26-28. <u>https://doi.org/10.1002/aic.690070108</u>
- [8] Xu, H. and Liao, S.J. (2005) Series Solutions of Unsteady Magnetohydrodynamics Flows of Non-Newtonian Fluids Caused by an Impulsively Stretching Plate. *Journal* of Non-Newtonian Fluid Mechanics, 159, 46-55. https://doi.org/10.1016/j.jnnfm.2005.05.005
- [9] Cortell, R. (2006) Effects of Viscous Dissipation and Work Done by Deformation on the MHD Flow and Heat Transfer of a Viscoelastic Fluid over a Stretching Sheet. *Physics Letters A*, 357, 298-305. <u>https://doi.org/10.1016/j.physleta.2006.04.051</u>
- [10] Hayat, T. and Sajid, M. (2007) Analytic Solution for Axisymmetric Flow and Heat Transfer of a Second Grade Fluid past a Stretching Sheet. *International Journal of Heat and Mass Transfer*, **50**, 75-84. https://doi.org/10.1016/j.ijheatmasstransfer.2006.06.045
- [11] Hayat, T., Abbas, Z. and Sajid, M. (2006) Series Solution for the Upper-Convected Maxwell Fluid over a Porous Stretching Plate. *Physics Letters A*, **358**, 396-403. <u>https://doi.org/10.1016/j.physleta.2006.04.117</u>
- [12] Butt, A.S., Ali, A. and Mehmood, A. (2016) Numerical Investigation of Magnetic Field Effects on Entropy Generation in Viscous Flow over a Stretching Cylinder Embedded in a Porous Medium. *Energy*, 99, 237-249. <u>https://doi.org/10.1016/j.energy.2016.01.067</u>
- [13] Ishak, A., Nazar, R. and Pop, I. (2008) Uniform Suction/Blowing Effect on Flow and Heat Transfer Due to a Stretching Cylinder. *Applied Mathematical Modelling*, 32, 2059-2066. <u>https://doi.org/10.1016/j.apm.2007.06.036</u>
- [14] Pandey, A.K. and Kumar, M. (2016) Natural Convection and Thermal Radiation Influence on Nanofluid Flow over a Stretching Cylinder in a Porous Medium with Viscous Dissipation. *Alexandria Engineering Journal*, 56, 55-62. https://doi.org/10.1016/j.aej.2016.08.035
- [15] Prasannakumara, B.C., Gireesha, B.J. and Manjunatha, P.T. (2015) Melting Phenomenon in MHD Stagnation Point Flow of Dusty Fluid over a Stretching Sheet in the Presence of Thermal Radiation and Non-Uniform Heat Source/Sink. *International Journal for Computational Methods in Engineering Science and Mechanics*, 16, 265-274. <u>https://doi.org/10.1080/15502287.2015.1047056</u>
- [16] Das, S., Jana, R.N. and Makinde, O.D. (2016) Magnetohydrodynamic Free Convective Flow of Nanofluids Past an Oscillating Porous Flat Plate in a Rotating System with Thermal Radiation and Hall Effects. *Journal of Mechanics*, **32**, 197-210. https://doi.org/10.1017/jmech.2015.49
- [17] Sheikholeslami, M. and Shehzad, S.A. (2017) Thermal Radiation of Ferrofluid in Existence of Lorentz Forces Considering Variable Viscosity. *International Journal of Heat and Mass Transfer*, **109**, 82-92. https://doi.org/10.1016/j.ijheatmasstransfer.2017.01.096
- [18] Makinde, O.D. and Eegunjobi, A.S. (2016) Entropy Analysis of Thermally Radiating

Magnetohydrodynamic Slip Flow of Casson Fluid in a Microchannel Filled with Saturated Porous Media. *Journal of Porous Media*, **19**, 799-810. <u>https://doi.org/10.1615/JPorMedia.v19.i9.40</u>

- [19] Archana, M., et al. (2018) Influence of Nonlinear Thermal Radiation on Rotating Flow of Casson Nanofluid. Nonlinear Engineering, 7, 91-101. <u>https://doi.org/10.1515/nleng-2017-0041</u>
- [20] Bidin, B. and Nazar, R. (2009) Numerical Solution of the Boundary Layer Flow Over an Exponentially Stretching Sheet with Thermal Radiation. *European Journal* of Scientific Research, 33, 710-717.
- [21] Brusly Solomon, A., et al. (2017) Natural Convection Enhancement in a Porous Cavity with Al<sub>2</sub>O<sub>3</sub>-Ethylene Glycol/Water Nanofluids. International Journal of Heat and Mass Transfer, 108, 1324-1334. https://doi.org/10.1016/j.ijheatmasstransfer.2017.01.009
- [22] Sohel Murshed, S.M., et al. (2020) Experimental Research and Development on the Natural Convection of Suspensions of Nanoparticles—A Comprehensive Review. Nanomaterials, 10, Article No. 1855. <u>https://doi.org/10.3390/nano10091855</u>
- [23] Alsabery, A.I., et al. (2017) Natural Convection Flow of a Nanofluid in an Inclined Square Enclosure Partially Filled with a Porous Medium. Scientific Reports, 7, Article No. 2357. <u>https://doi.org/10.1038/s41598-017-02241-x</u>
- [24] Ghalambaz, M., Noghrehabadi, A. and Ghanbarzadeh, A. (2014) Natural Convection of Nanofluids over a Convectively Heated Vertical Plate Embedded in a Porous Medium, Fluid Dynamics, Heat and Mass Transfer and Other Topics. *Brazilian Journal of Chemical Engineering*, **31**, 413-427. https://doi.org/10.1590/0104-6632.20140312s00001956
- [25] Rana, P. and Bhargava, R. (2012) Flow and Heat Transfer of a Nanofluid over a Nonlinearly Stretching Sheet: A Numerical Study. *Communications in Nonlinear Science and Numerical Simulation*, **17**, 212-226. https://doi.org/10.1016/j.cnsns.2011.05.009
- [26] Buongiorno, J. (2006) Convective Transport in Nanofluids. Journal of Heat Transfer, 128, 240-250. <u>https://doi.org/10.1115/1.2150834</u>
- [27] Kuznetsov, A.V. and Nield, D.A. (2010) Natural Convection Boundary-Layer of a Nanofluid Past a Vertical Plate. *International Journal of Thermal Sciences*, 49, 243-247. <u>https://doi.org/10.1016/j.ijthermalsci.2009.07.015</u>
- [28] Nield, D.A. and Kuznetsov, A.V. (2009) The Cheng-Minkowycz Problem for Natural Convection Boundary-Layer Flow in a Porous Medium Saturated by a Nanofluids. *International Journal of Heat and Mass Transfer*, **52**, 5792-5795. <u>https://doi.org/10.1016/j.ijheatmasstransfer.2009.07.024</u>
- [29] Bachok, N., Ishak, A. and Pop, I. (2010) Boundary Layer Flow of Nanofluid over a Moving Surface in a Flowing Fluid. *International Journal of Thermal Sciences*, 49, 1663-1668. <u>https://doi.org/10.1016/j.ijthermalsci.2010.01.026</u>
- [30] Khan, W.A. and Pop, I. (2010) Boundary-Layer Flow of a Nanofluid past a Stretching Sheet. *International Journal of Heat and Mass Transfer*, 53, 2477-2483. <u>https://doi.org/10.1016/j.ijheatmasstransfer.2010.01.032</u>