

# Degradation of Aqueous 2,6-Dibromophenol Solution by In-Liquid Dielectric Barrier Microplasma

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# Abstract

Degradation of 2,6-dibromophenol (2,6-DBP) in the aqueous solution was studied using dielectric barrier discharge in micro-bubbles. Experimental comparison of working gas Ar,  $N_2$ ,  $O_2$ , and air showed that oxygen and air plasma efficiently decomposed 2,6-DBP to bromide ion, and inorganic carbon. The molecular orbital model was applied in the analysis of the degradation in electrophilic, nucleophilic, and radical reactions.

# **Keywords**

2,6-Dibromophenol, Atmospheric Pressure Plasma, Inductive Energy-Storage System

# **1. Introduction**

Today, myriad plastic materials are in use all around us: electronics boards, fire-retarding curtain, housings of household electrical appliance such as microwave ovens. Tetrabromobisphenol A (TBBPA) is a popular material and offers quality fire-retarding material, brominated poly-epoxy-phenolic resin, at low cost. Since 2007, TBBPA has been included in the OSPAR List of Chemicals for Priority Action, because anxiety about accumulation in the human body was expressed [1]. Many researchers have examined the fate of TBBPA in the environment, Ronen and Abeliovich, in 2000 [2]; Oeberg *et al.*, in 2002 [3]; Erikson *et al.*, in 2004 [4]; Greeke *et al.*, in 2006 [5]; Arbeli *et al.*, in 2006 [6] and animals, Meerts *et al.*, in 2000 [7]; Fujitani *et al.*, in 2006 [8]; Zalko *et al.*, 2006 in [9]; Antignac *et al.*, in 2009 [10], and the evidence of environmental toxicity, WHO, in 1995 [11]; Hakk *et al.*, in 2003 [12]; Ogunbayo *et al.*, in 2008 [13]. 2,6-Dibromophenol (2,6-DBP) is also a flame retardant

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in polymers and is detected as a degradation product in the slow sand filtration of TBBPA-contaminated water [14]. Similar bromine compound, 2,4,6-DBP is used as antiseptic, and 2,4-DBP shows estrogenic effect [15]. A permissible range by RoHS 2.0 in 2011 was 1000 ppm (0.1%). After the research report by the World Health Organization (WHO) about the brominated phenols such as 2-BP, 2,6-DBP, and 2,4,6-DBP in drinking water in Canada, the maximum concentration were 42, 60, and 20 ng/L, respectively, where as the normal value was less than 3 ng/L [16]. Residual material in the manufacturing industry is probably the cause of the ppb level contamination, and fire-retarding plastic materials scrap is building up in world-wide. 2,6-DBP compound hardly biodegrades, and accumulates in the environment [17]. 2,6-DBP is characterized by the odor of disinfectant at low threshold by the human sense of smell, as low as the ppt class. In this work, we aim at the remediation of water pollution, *i.e.*, to remove 2,6-DBP using small coaxial dielectric barrier discharge with multiple working gases: Ar,  $O_2$ , and  $N_2$ . The explanation for the degradation process of 2,6-DBP is studied by molecular orbital calculation.

## 2. Materials and Methods

# 2.1. Experimental Equipment

**Figure 1** shows the experimental setup and the structure of a dielectric barrier discharge plasma operated in water and a solution of dibromophenol. Discharge plasma is excited in a quartz tube by high voltage pseud-sine wave excited by a voltage inverter (Logy Electric CO., Tokyo) between a tungsten-rhenium electrode, 0.65 mm in diameter, and the liquid surface inside the tube. This plasma source is capable of generating nonthermal plasma in multiple gas, inert gas and molecular gas: oxygen, nitrogen and an arbitrary mixture.

The ground electrode is surrounding a glass test tube, 35 mm internal diameter and 100 in length. This plasma source enables processing with air, and in the experimental part, air plasma exhibits efficient degradation of di-bromophenols. Gas flow was controlled with a piezo-actuator. The dielectric barrier discharge fits for the energy-saving operation of water remediation.

## 2.2. Discharge Current, Voltage, Power

The discharge characteristics of multiple gas was compared. The discharge voltage was measure with two high voltage probes, (Type-P-300, Tektronix, USA) and discharge current was measured with a current probe and amplifier (Type-TCP-312 and TCPA-300, Tektronix, USA) The Q-V Lissajous' figure was applied to measure the power dissipation in the dielectric barrier discharge. In this measurement, a capacitor was inserted in the discharge circuit. From the Q-V Lissajous' figure, discharge voltage  $V_a$  is found as the difference between  $V_p$  and  $V_c$ . The net charge is found from the capacitance C and the voltage across the capacitor. Dissipated energy *E* 



Figure 1. Dielectric barrier plasma decomposing 2,6-DBP in solution.

is found per one cycle as in the following form. Electric power is found as the dissipated energy per cycle multiplied by the frequency.

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 $E = \int Q dV_a$ 

**Table 1** summarizes the experimental result. The discharge voltage in Ar is relatively low and the discharge current indicated good stability. In the working gas containing oxygen, the discharge voltage was especially high and large noise was observed in the discharge current. The largest discharge power 12.67 (W) was observed in  $O_2$ , and the degradation is completed in several minutes.

#### 2.3. Experimental Procedure

In this experiment, the concentration of 2,6-DBP in the solution is 20 mg/Little. 20 mg of 2,6-DBP was measured and solved in alkaline solution then the solution was neutralized to pH 7 with sulfuric acid. Individual trial was repeated for the solution of 100 mL in a test cylinder. The temporal evolution of the concentration of 2,6-DBP was determined by high-performance liquid chromatography (HPLC) with column: XBridge C18 (5 mm 4.6 mm i.d.  $\times$  250 mm , Waters, USA); eluent: methanol/water = 70/30 pH 4.0 and adjusted with phosphoric acid; flow rate: 1 mL/min; detector: Hitachi L-2455 Photo Diode Array Detector; temperature: 40°C, and UV detector (Hitachi L-4200) adjusted to 215 nm.

Concentration of organic carbon was measured with TOC analyzer (TOC-L, Shimadzu, Kyoto, Japan). Concentration of anion (Br<sup>-</sup>, NO<sub>2</sub><sup>-</sup>, and NO<sub>3</sub><sup>-</sup>) was measured with anion chromatography system (Dionex ICS-1100). The concentration of anions was determined by ion chromatography with column: IC Pack Anion HR (Waters, USA) (4.6 mm i.d.  $\times$  75 mm); eluent: 0.75 mmol/L potassium biphthalate; flow rate: 1 mL/min; detector: HITACHI L-3700 Conductivity Detector; temperature: 40°C. The concentration of dissolved organic carbon (DOC) was analyzed by a TOC analyzer (Shimadzu TOC Analyzer 5000, Japan).

The semiempirical molecular orbital calculation using a PM5 Hamiltonian was performed in MOPAC Version 6 with a CAChe package (Fujitsu Co., Tokyo, Japan).

#### 3. Results and Discussion

#### 3.1. Candidate of Reactive Species in Plasma Discharge

In the advanced oxidation processes (AOP) in weakly ionized oxygen, radicals such as OH,  ${}^{1}O_{2}$ , O, HO<sub>2</sub>, O<sub>3</sub>, O<sub>2</sub><sup>-</sup>, and hydrogen radical H play important roles in the degradation of organic compounds to inorganic components: water and carbon dioxide gas. The reaction rate given by Sugimitsu is OH >>  ${}^{1}O_{2} > O >> HO_{2} > O_{3} >> O_{2}^{-}$  [18]. The reactions with organic matter are concerned with active species in ozone and ultraviolet treatment in cleaning water. The generation processes of active species are different depending on the working gases. In this experiment, working gases Ar, oxygen, nitrogen and air are introduced to the discharge volume. A solution is given energy by working gas made into plasma in water, and it is formed active species such as OH, H and hydrated electron form in the solution [19]. For example, (1)-(3) are relatively slow reactions and incapable of forming OH radicals.

$$H_2 O \to OH + H \tag{1}$$

$$2e_{a0} \rightarrow H_2 + 2OH^- \tag{2}$$

$$H_2O \to H^+ + e_{aa} + OH \tag{3}$$

In oxygen and mixtures, ozone molecule and hydroxyl radical are generated by the following reactions: (4)-(6).

$$e + O_2 \rightarrow 2O + e \tag{4}$$

$$\mathbf{O} + \mathbf{O}_2 \to \mathbf{O}_3 \tag{5}$$

$$O_3 + H_2 O \rightarrow O_2 + 2OH \tag{6}$$

Table 1. Discharge characteristics in various working gas.							
Object	T In: t	Working gas					
Object	Ullit —	$N_2$	Ar	Air	· O <sub>2</sub>		
Applied voltage V	Frequency (kHz)	16.94	16.69	16.88	16.91		
Applied voltage $v_p$	Peak to peak voltage (kV)	7.76	4.32	7.84	7.68		
Discharge current $I_p$	Peak to peak current (mA)	480	560	920	3240		
Discharge power P	(W)	6.94	4.90	10.26	12.67		

Generally in oxygen discharges, hydroxyl radicals contribute to the advanced oxidation. The production of this species is, for example, the dissociation reaction of hydrogen peroxide. In the oxygen discharges, hydrogen peroxide is produced through (7)-(9), then hydroxyl radical is produced through the reaction of hydrogen peroxide dissociated hydrogen atom and hydrated electron,  $e_{aq}$  [19]. Thus, oxygen plasma exhibits high reactivity against organic compounds through the advanced oxidation reaction by hydroxyl radical, either by ozone or hydrogen peroxide.

$$O^- + O_3^- \to 2O_2^-$$
 (7)

$$H + O_2^- \to HO_2^- \tag{8}$$

$$\mathrm{HO}_{2}^{-} + \mathrm{H}_{2}\mathrm{O} \rightarrow \mathrm{H}_{2}\mathrm{O}_{2} + \mathrm{OH}^{-}$$

$$\tag{9}$$

$$O^- + H_2 O \to OH^- + OH \tag{10}$$

$$H + H_2O_2 \rightarrow H_2O + OH \tag{11}$$

$$e_{aa} + H_2 O_2 \rightarrow OH^- + OH \tag{12}$$

#### 3.2. Degradation of 2,6-DBP

**Figure 2** shows the temporal evolution of the residual concentration of 2,6-DBP. Efficient plasma degradation is observed in all working conditions. Apparently, the degradation process in nitrogen and Ar discharge is different from the rapid degradation by oxygen and air. **Figure 3** shows and experimental comparison of the degradation rate of 2,6-DBP. The degradation rate coefficient is determined as*k*.  $C_0$  is the initial concentration of 2,6-DBP (mg/L),  $C_t$  is the concentration after the elapsed time *t* (min.). **Table 2** shows the residual concentration of 2,6-DBP 60 minutes after the plasma degradation. In the oxygen and air discharge case, the 100% and 99.73% of degradation rate is achieved. It should be noted that in the latter case, 98.78% is achieved in 5 minutes.

The reaction rate is constant in the initial stage of the degradation reaction, then apparent slowdown occurs by the secondary reaction. Table 3 summarizes the reaction rate in the initial stage. The order of the degradation rate shows  $O_2 > Air > Ar > N_2$ . The reaction rate is calculated from the experimental result of the first 5 minutes.

Degradation ratio = 
$$\frac{\text{concentration } (2, 6\text{-DBP}) - \text{concentration } (2, 6\text{-DBP})_{t=0}}{\text{Density } (2, 6\text{-DBP})_{t=0}} \times 100$$
(13)

$$\ln\left(\frac{C_t}{C_0}\right) = -kt \tag{14}$$

In the case of oxygen, the reaction rate tends saturate in 5 minutes. This result suggests the effect of competing production of the byproduct.

#### 3.3. Degradation of Organic Carbon, TOC Density

Total Organic Carbon (TOC) concentration is an index showing the concentration of the organic compound in



Figure 2. Degradation of 2,6-DBP in aqueous solutions.



Figure 3. Degradation of 2,6-DBP: Reaction rate.

Table 2. Com	parison of t	the degradatio	n rate of 2,6-DBF	in 60 minutes.
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Working gas	2,6-DBP degradation [%]	TOC degradation [%]	Production of Br <sup>-</sup> [%]
$N_2$	48.06	48.49	30.74
Ar	85.87	76.25	77.27
Air	99.73	72.82	10.30
O <sub>2</sub>	100.00	100.00	24.96

	Τ	able	3.	Compari	son of th	e degrad	ation rate	e of 2,6-D	BP in the	initial stage.
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Working gas	$N_2$	Ar	Air	$O_2$
Reaction rate $k (\min^{-1})$	0.0041	0.0235	0.3839	(0.6029)

the water pollution control. In this experiment, TOC was evaluated as a measure for the dissociation of 2,6-DBP. **Figure 4** shows the temporal evolution of the TOC concentration. TOC concentration decreased in all workinggases. The reactivity of oxygen gas was high and the decrease in TOC was completed within 20 minutes, with time constant of 7 to 8 minutes. In air and nitrogen cases, TOC concentration is approximately constant after 30 minutes of treatment. This result suggests that the dissociation balances with the production in some kind of chemical equilibrium.



#### 3.4. Concentration of Ionic Bi-Product

In the measurement of anion product,  $BrO_3^-$  anion was identified in Ar,  $O_2$ ,  $N_2$ , and  $NO_3^-$  was identified only in the case of air plasma. **Figure 5(a)** shows the concentration of Br<sup>-</sup> anion. Br<sup>-</sup> is produced from 2,6-DBP, the dissociation from the phenol-benzene ring. Depending on the working gas, one can find two types of temporal evolution. The first pattern is the initial increase and decrease in Br<sup>-</sup> concentration, as in oxygen and air plasma. The second pattern is the continuous increase in the concentration. The production of Br<sup>-</sup> anion is 79.71% after 1 minute in oxygen plasma processing and 71.30% after 5 minutes in air plasma. Almost all Br<sup>-</sup> anion is produced in the first several minutes of the plasma processing. The decrease in Br<sup>-</sup> anion intensity suggests that Br<sup>-</sup> is consumed in the production of stable compound in the oxygen and air discharge case. In these cases, a possible explanation is the conversion to BrO<sub>3</sub><sup>-</sup> anion by the advanced oxidation of Br<sup>-</sup> anion [20] [21]. **Figure 5(b)** shows the concentration of BrO<sub>3</sub><sup>-</sup> anion, as function of the processing time. In the oxygen discharge case, the concentration of BrO<sub>3</sub><sup>-</sup> anion increases. In contrast, in the air discharge, the concentration of BrO<sub>3</sub><sup>-</sup> anion shows a maximum in the initial stage. In the air plasma discharge, one can find that the concentration of BrO<sub>3</sub><sup>-</sup> anion shows a maximum at 1 minute after the beginning of the processing, then starts to decrease, and no BrO<sub>3</sub><sup>-</sup> anion can be observed in 20 minutes. In inert gases, BrO<sub>3</sub><sup>-</sup> can be observed in 60 minutes in the Ar case. No BrO<sub>2</sub><sup>-</sup> intensity was observed in the nitrogen plasma case.

The advanced oxidation process of Br<sup>-</sup> anion is shown in **Figure 6**, following the proposal by Urs von Gunten [20] [21]. Advanced oxidation by hydroxyl radical and ozone produces  $BrO_3^-$ , through the production of HOBr and BrO<sup>-</sup> anion by ozone and BrO by hydroxyl radical. In the air plasma case in **Figure 7**, initial increase in the density of Br<sup>-</sup> and BrO<sub>3</sub><sup>-</sup> is interrupted by some competing reaction and BrO<sub>3</sub><sup>-</sup> disappears in 20 minutes after the start. The oxidation process of nitrogen produces  $NO_3^-$  anion, then  $NO_3^-$  anion react with Br<sup>-</sup> anion and produces stable compound Br<sub>2</sub>. This reaction tends to decrease in Br<sup>-</sup> and BrO<sub>3</sub><sup>-</sup> density.

$$O_3 + NO_2^- \rightarrow O_2 + NO_3^- \tag{15}$$

$$NO_3^- + 2Br^- + 3H^+ \rightarrow Br_2 + HNO_2 + H_2O$$
<sup>(16)</sup>

Identification and estimation of the resultant products remain to be examined for detailed verification of 2,6-DBP degradation.

#### 3.5. Calculation of Radical, Nucleophilic, and Electrophilic Frontier Density of 2,6-DBP

To learn the mechanism of the advanced oxidation, we used the molecular orbital theory (CAChe, Fujitsu CO., Japan). **Figure 8** shows contour plots of the radical reaction, electrophilic, and nucleophilic frontier density of 2,6-DBP. Electrophilic frontier density reveals reactive sites based on the electron distribution of active orbitals near HOMO (highest occupied molecular orbital) Radical reaction and electrophilic reaction has small area of 0.002 to 0.003 in the central area of its molecule. Molecular orbital calculation of 2,6-DBP shows that degrada-



**Figure 5.** Concentration of by-product. (a) Density of  $Br^-$  anion; (b) Concentration density of  $BrO_2^-$ .



tion is partly explained on the basis of electrophilic frontier density, where hydrogen radical contributes to various reactions. Nucleophilic frontier density is a measure of the susceptibility to a nucleophilic attack and reactive sites based on the electron distribution of active orbitals near the LUMO (lowest unoccupied molecular orbital). The counter plot of nucleophilic frontier density is at the same level around the main ring. Anion radicals such as  $OH^-$  does not contribute to the degradation. Radical reaction and the nucleophilic reaction has round area of 0.003 to 0.005 at the Br site.

**Figure 8(b)** shows the radical reaction frontier density. This result presents small area of highest susceptibility to radical reactions on the top of Br atoms of 2,6-DBP, Br atom Br(8) on the right and on the left Br atom Br(9). Br site of 2,6-DBP has high susceptibility to nucleophilic radicals. **Figure 8(c)** shows nucleophilic frontier density, where the highest susceptibility is localized on the top of Br(9) on the left and Br(10) on the right. Hydroxyl radicals in OH radical or OH ion attack these sites and contribute to the detachment of Br atoms. **Figure 8(d)** shows the electrophilic frontier density, where the highest susceptibility site is localized in the middle



Figure 7. Anionic product in the case of air plasma.





**Figure 8.** Radical, nucleophilic and electrophilic active frontier density. (a) Molecular orbital model of 2,6-DBP; (b) Radical reaction susceptibility; (c) Nucleophilic frontier density; (d) Electrophilic frontier density.

of the benzene ring, where attacked by hydrogen ion  $H^+$  contributes to the collapse of the benzene ring. Thus, the degradation of 2,6-DBP is reached by the combination of the radical, nucleophilic and electrophilic reaction. This mechanism can explain the efficient degradation of 2,6-DBP by oxygen and air plasma injection.

# 3.6. Profile of pH

**Table 4** shows the temporal evolution of pH in all settings. In the initial liquid sample, the concentration density of 2,6-DBP was 20 mg/L and pH was adjusted to 7.0. In all experiments, the decrease in pH was observed in the initial stage. In the air plasma process, the pH decrease with the degradation of 2,6-DBP may becaused by the

Table 4. Measurement of pH in the plasma degradation of 2,6-DBP.							
Processing time (min )		Workin	ng gas				
Frocessing time (initi.)	$N_2$	Ar	Air	$O_2$			
5	6.47	5.91	3.75	4.35			
10	6.42	4.66	3.55	4.40			
20	6.36	4.15	3.29	4.51			
30	6.28	4.61	3.18	5.05			
60	5.99	4.05	2.87	6.04			

formation of  $NO_3^-$  as well as the consume of OH<sup>-</sup> in the degradation process.

### 4. Conclusion

In this study, we traced the degradation of aqueous solution of 2,6-DBP by a aqueous glow discharge to inorganic carbon in a matter of several minutes. Although the identification and toxicity assessment of the resultant products remain to be examined for detailed verification of 2,6-DBP degradation, this process is an alternative choice in the degradation of TBBPA. In the fire burn destruction of such fire-retarding products, human toxicity such as the dioxin is a great concern. In the degradation of the solution, the ozone injection and the ultra violet radiation are compared. The degradation using the advanced oxidation, such as ozone injection, is employed in various water plants for sewage treatment. These reaction attacks the radical and nucleophilicreaction site. The electrophilic reaction shows higher activities in the degradation of the benzene ring, as shown in the present work.

The characteristic of decomposition of 2,6-DBP is different for molecules, ions and radicals formed in plasma of multiple working gases. The reaction rate of decomposition reaction is  $O_2 > Air > Ar > N_2$ . The treatment  $O_2$ as the working gas has the greatest reaction rate, shown after 60 minutes. Br<sup>-</sup> and BrO<sup>-</sup> anions are observed as ionic products in decomposition of 2,6-DBP. It is thought Br is formed by radical reaction and nucleophilic reaction, and  $BrO_3^-$  is formed by peroxidation.  $NO_3^-$  anion is observed also, and it is formed from chemical combination of nitrogen and oxide in air as the working gas. Radical reaction, nucleophilic and electrophilic reaction is happen at same time in dissociation process of 2,6-DBP. In the first stage, Br<sup>-</sup> anion is formed by components such as OH and OH<sup>-</sup> anion predominantly from radical and nucleophilic reaction. Finally, the benzene ring is broken by components such as H and H<sup>+</sup> ion from electrophilic reaction. It was thought that from measurements of pH by plasma of  $O_2$  as working gas, the plasma that shows the best decomposition characteristic is plasma of  $O_2$  as the working gas, because it is able to form many active species. For  $BrO_3^-$  anion toxicity, more investigations are needed to utilize as water purification.

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