

α-Endosulfan Removal from Water by Adsorption over Natural Clays from Burkina Faso: An Isothermal Study

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Abstract

The present study carried out the α -endosulfan removal from water by adsorption over natural clays from the western region of Burkina Faso. The adsorption experiments were performed over raw clay samples at room temperature in batch reactor and the obtained adsorption isotherms were well fitted by Fowler-Guggenheim model. It was pointed out for all samples that α -endosulfan was physisorbed in the interlayer space of the clay samples. The maximal adsorption capacities were respectively about 9.12, 6.98 and 4.13 mg/g for KO2, KO1 and KW1 samples. The differences in terms of adsorption capacity for the three samples were due to the presence of illite in the samples KO2 and KO1 when the KW1 sample contained essentially kaolinite in its structure. When the interlayer space was large enough as for samples with illite a greater amount of α -endosulfan molecules were adsorbed. It was also shown that the samples with the higher surface area were the most efficient for the removal of α -endosulfan molecules from water. Moreover, this study exhibited that the α -endosulfan adsorption depended on the crystallites size; the samples presenting largest crystallites had the greatest adsorption capacities.

Keywords

 α -Endosulfan, Removal, Water, Natural Clays, Burkina Faso

1. Introduction

Pesticides are widely used in many countries to increase the crops yield. a-endosulfan was extensively used for

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cotton farming until its prohibition in 2006 in West Africa [1]. But it remains in use because of fraudulent importation of banned pesticides in West African countries. Residues of α -endosulfan have been monitored in soils [2] [3], surface and ground waters [4] at levels exceeding the thresholds of 0.10 µg/L adopted by World health Organization (WHO). Such situation is encountered in several countries such as Burkina Faso or Spain [2]-[5]. The toxicity of α -endosulfan was clearly documented for humans and animals [6]-[8]. Both toxicological and epidemiological studies [9]-[13] were realized and many diseases such as cancers and neurological affections were identified as potential effects of the exposure to this pesticide. Because of its toxicity and its presence in groundwater, it is suitable to find methods for the removal of α -endosulfan from water.

In the literature there are a few papers dealing with low cost methods for the removal of α -endosulfan from water. Indeed, the biological treatments [14]-[16] exist, but their implementation for water treatment is difficult at the scale of African villages. The oxidative [17]-[19] and reductive [20] methods are well documented. These methods are generally expensive in the purpose of implementation in rural regions; moreover, they induce the formation of toxic or carcinogenic byproducts. An experience was performed using synthetic zeolites as adsorbents [21] with interesting removal yields of α -endosulfan from water [22]. In the purpose of valorization of local materials in Burkina Faso, we decided to investigate the removal efficiency of local clays considered as possible adsorbents for the treatment of water sources contaminated by α -endosulfan.

The aim of this paper is to study the removal performances of α -endosulfan in water over natural clays from the western region of Burkina Faso.

2. Experimental

The clay samples were collected from Kwa and Koro localities in the region of Bobo-Dioulasso (west of Burkina Faso). The Koro site is localized at 11°09' north latitude and 4°11' west longitude. Kwa is localized at 11°10' north latitude and 4°15' west longitude. According to their texture the samples from Koro site were designated by KO1 and KO2 while the sample collected in the Kwa site was designated by KW1. The samples were just sieved to collect particles with size between 0.2 and 0.4 mm; the samples have not undergone any further treatment. The analytical grade of α -endosulfan was supplied by Aldrich.

The adsorption experiments of α -endosulfan in aqueous solution by the different adsorbents were performed in batch reactor according to the protocol described by Yonli *et al.* [21] for the adsorptive removal of α -endosulfan over zeolites. The experiments were performed at room temperature and atmospheric pressure in 20 mL tanks. 200 mg of clay were used for each experiment and the initial concentrations of sorbate varied from 10 to 30 mg/L. The concentrations of the solution before adsorption were determined by Varian high performance liquid chromatograph (HPLC) coupled to Varian Prostar 340 UV-Visible detector. The analysis were performed at 1 mL/min flow rate on Lichrospher RP 18 column (length 150 mm, internal diameter 4.6 mm, 5 µm particle size). After determination of initial concentrations, 10 mL of α -endosulfan solution were put into contact with 200 mg of adsorbent and maintained under mechanical stirring until the adsorption equilibrium was achieved. 100 µL of supernatant solution were then collected and analyzed by HPLC.

The physico-chemical characteristics of clay samples were obtained by several techniques. The porous volumes and surfaces measurements were performed by nitrogen adsorption at -196° C using a Micromeritics ASAP 2010 analyzer. The surfaces and porous volumes data are reported in Table 1.

The different clay phases present in the samples were determined with a Bruker D5005 diffractometer and the diffractograms are shown in Figures 1(a)-(c) respectively for KO1, KO2, and KW1 samples.

Thermal analysis were realized with a TA instruments DTA-TGA analyzer. The experiments were performed under air flow at 60 mL·min⁻¹ with an operating temperature ranging from room temperature to 900°C. The thermograms for the different samples are presented in Figures 2(a)-(c).

| Table 1. Surface and porosity characterization of clay samples. | | | | |
|---|--|--|--|--|
| Samples | Total Volume (cm ³ ·g ⁻¹) | BET Surface (m ² ·g ⁻¹) | | |
| KO2 | 0.0034 | 42 | | |
| KO1 | 0.0037 | 24 | | |
| KW1 | 0.0021 | 7.9 | | |



Figure 1. (a) XRD pattern for KW1 sample; (b) XRD pattern for KO1 sample; (c) XRD pattern for KO2 sample.



Figure 2. (a) Thermogram for KW1 sample; (b) Thermogram for KO1 sample; (c) Thermogram for KO2 sample.

The electronic scanning microscopy was used to estimate the size of the crystallites. The measurements were performed using a high resolution Philips CM 120 microscope. The microscopy images are presented in Figures 3(a)-(c).

3. Results and Discussion

3.1. Physico-Chemical Characterization

As it can be noticed from **Table 1** the porous volume for the investigated clay samples was very week (~0.003 cm³/g). This denotes that the clay samples had no remarkable pores allowing α -endosulfan adsorption in these pores. The specific surface areas for the samples varied in the following order: KO2 > KO1 > KW1. The samples collected in Koro (KO1 and KO2) presented higher specific surface areas than the one from the KWA site (KW1). XRD scans for the same samples as presented in **Figures 1(a)-(c)** indicate that the KO1 sample consisted mainly in quartz α , feldspath, kaolinite, albite and illite; the KO2 sample contained mainly quartz α , feldspath.



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(b)



Figure 3. (a) SEM image for KW1 sample; (b) SEM image for KO1 sample; (c) SEM image for KO2 sample.

path, kaolinite and illite; and the KW1 sample was composed of quartz α and kaolinite. The DTA-TGA thermograms presented in **Figures 2(a)-(c)** confirmed the existence of some clay phases identified by XRD. Indeed, three endothermic peaks were observed for the KO1 sample. The first one towards 65°C corresponded to the lost of physisorbed and interlayer water. The second peak beginning at 441°C was characteristic of the removal of water associated to hydroxyl group degradation in illite samples [23]-[25]. The weak peak at 573°C revealed the presence of quartz. In the case of KO2 sample, three endothermic peaks were also observed. The dehydroxylation of illite starting at 449°C was responsible for the second peak. A little hook at 573°C characterizing a quartz α to quartz β transformation was observed. Likewise the same trend was observed in the case of KW1 sample. However a peak around 455°C characterizing the dehydroxylation of kaolinite [26] was also observed for this sample.

The average of crystallites sizes was estimated to be about 510 μ m, 420 μ m and 335 μ m respectively for KO2, KO1 and KW1 samples as it can be observed from Figures 3(a)-(c). In the literature the crystallite size is generally correlated to the number of silanol groups. The biggest particles have less silanol groups and therefore adsorb less water molecules on their external surface [27]. Basing upon the crystallites size the following classification in terms of water adsorption capacities was expected: KO2 > KO1 > KW1.

3.2. *α*-Endosulfan Adsorption on Clays

The α -endosulfan adsorption isotherms for KO2, KO1 and KW1 clay samples are represented in Figure 4.

According to the classification of Giles [28], these isotherms are S-type isotherms. This specific shape of isotherms indicated weak sorbate-adsorbent interactions. Moreover the adsorption isotherms were well fitted by Fowler-Guggenheim [29] model. From this modelization different parameters such as maximal adsorption capacity, sorbate-sorbate interaction energy (W) and sorbate-adsorbent interaction constant (K) could be determined. These data are reported in **Table 2** and exhibited that sorbate-adsorbent interactions were stronger for KW1 (kaolinite containing sample) and progressively lower for KO1 and KO2 (samples with illite phases).



Figure 4. Adsorption isotherms of α -endosulfan over KW1, KO1 and KO2 clay samples.

Table 2. Fowler-Guggenheim parameters for the adsorption of α -endosulfan over raw clay samples collected in western Burkina Faso.

| Samples | Maximal Adsorption Capacity (mg/g) | Sorbate-Adsorbent Interaction Constant K | Sorbate-Sorbate Interaction Energy W (KJ·mol ⁻¹) |
|---------|---------------------------------------|---|---|
| KW1 | 4.13 | 63.98 | 3.10 |
| KO1 | 6.98 | 49.92 | 2.83 |
| KO2 | 9.12 | 37.68 | 2.81 |

As reported by Yonli *et al.* [21] the diameter of α -endosulfan molecule is estimated to be about 7.2 Å. This value is close to the interlayer space of kaolinite (about 7 Å). So the physisorption of α -endosulfan in the interlayer of the KW1 sample is slightly enhanced by Van Der Waals Interactions between sorbate and solid. In the case of samples with illite phases the interlayer space is wider (10 Å) and the α -endosulfan molecules are more easily absorbed in the interlayer space with less interactions between α -endosulfan molecules and adsorbent (lower sorbate-adsorbent interactions constants for KO1 and KO2). A slight variation of sorbate-sorbate interaction energy was noticed for the three samples. Indeed the first molecules to be adsorbed in the interlayer space promote the adsorption of new molecules by lateral interactions between adsorbed molecules [30]. When the interlayer space is narrow the adsorbed molecules are cramped and confined in the interlayer inducing thus more interactions between adsorbed molecules. A ranking of maximal adsorption capacities was obtained and presented as follows: KO2 > KO1 > KW1. The higher adsorption capacities noticed for clay samples collected in the Koro site were due to the presence of illite phases in these samples. The KW1 sample had the lower adsorption capacity due to the presence of kaolinite in the structure. As the KO2 sample had a higher specific surface area than the KO1 sample the adsorption capacity for KO2 sample was more important. Indeed we had a BET surface area of about 42 m²/g for KO2, almost two times higher than the one for KO1 (24 m²/g).

Figure 5 indicates that the α -endosulfan adsorption capacities increase linearly with the crystallites size.

Indeed, the big crystallites have less terminal silanol groups than the small crystallites [31] and are consequently more hydrophobic. This hydrophobic character of samples containing big crystallites promotes the adsorption of organic molecules such as α -endosulfan in water [32] when adsorption is performed over solid samples. The KO2 sample with crystallites size of about 510 µm is thus the most efficient for the removal of α -endosulfan in water compared to KO1 and KW1 samples.



Figure 5. Evolution of α -endosulfan adsorption capacity versus crystallite average size for KW1, KO1 and KO2 clay samples.

4. Conclusion

The α -endosulfan adsorption was studied on clay samples collected from two sites in the western part of Burkina Faso. A part from mechanical sieving no further treatment was applied to the raw samples. The physico-chemical characterization showed three types of samples: the KO2 sample containing illite phases and big crystallites, the KO1 sample with illite phases and smaller crystallites and the KW1 sample with kaolinite phases and the smallest crystallites. The α -endosulfan molecules were physisorbed in the interlayer space of clay samples with Van Der Waals Interactions. The nature of clay phases, the surface BET area and the size of crystallites influenced the adsorption of α -endosulfan over natural raw clays samples. The most efficient sample for the removal of α -endosulfan in water was the KO2 sample with illite phases, the largest surface area and the biggest crystallites.

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