

Determination of the Optimal Speed of Pultrusion for Large-Sized Composite Rods

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ABSTRACT

The paper describes a mathematical model of the stress-strain state of polymer composite materials in the pultrusion process of large-sized products. The influence of the pull speed on the stress-strain state of the products is investigated. To determine the maximum possible pull speed series of solutions at different pull speeds are obtained. Depending on the maximum strain in the cross section of the rod determined the optimal value of pulling speed.

Keywords: Composite Material; Pultrusion; Stress-Strain State; Permeability; Oversized Rod

1. Introduction

Pultrusion is one of the most common ways to manufacture large products made of polymer composites. The possibilities to improve the performance of pultruded products depending on the reinforcement scheme are well studied [1-4]. The influence of constructive and technological parameters of pultrusion process on the properties of the resulting products is no less important. The most important to choose the optimal speed at which the quality product without the main cracks and discontinuity is received. The known mathematical models considered pultrusion process in the assumption that the polymerization of the resin is completed to the exit products from the die [5,6]. This assumption reduces the productivity of the process, making it unprofitable. A complex numerical model for evaluating stress-strain state of polymer composite material is developed. This model assumes incomplete polymerization process within the die. The relation between pull speed and stress-strain state of composite product at the exit from the die is investigated. As an example the optimum value of the pull speed is determined.

2. Statement of the Problem

Figure 1 shows the process of passing the composite material through a heated die. At the same time the polymerization process takes place. If the pull speed is high enough (>60 mm/min), then polymerization process of the oversized product does not have time to finish before it exits from the die. At this, the strain occurred in a polymerized part of the rod may exceed the maximum allowable values for the material which leads to the main crack appearance. The thermal stresses, the pressure of

the liquid resin and chemical shrinkage are effects on the value of strain.

3. Stress-Strain State Model

Consider the section A-A of the rod consisting of two regions (Figure 2(a)).

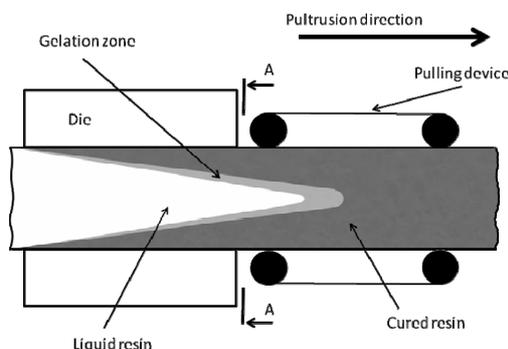


Figure 1. Scheme of pultrusion.

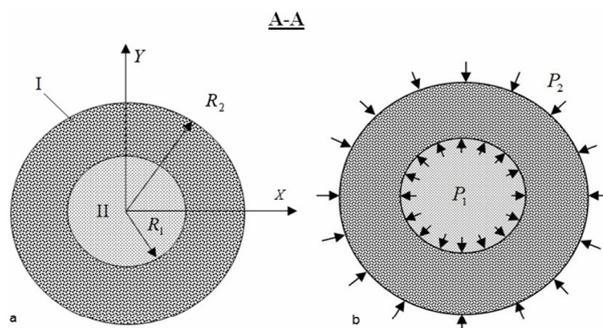


Figure 2. The rod cross-section (a) and the boundary conditions (b).

The outside Area I corresponds with cured zone. The inner Area II corresponds with zone where resin with filler is uncured.

Hooke's law for orthotropic solid in cylindrical coordinates taking into account the chemical shrinkage is given by

$$\varepsilon_r = \frac{\sigma_r}{E_r} - \mu_{r\theta} \frac{\sigma_\theta}{E_\theta} - \mu_{rz} \frac{\sigma_z}{E_z} + \alpha_r T + \chi_r, \quad (1)$$

$$\varepsilon_\theta = \frac{\sigma_\theta}{E_\theta} - \mu_{\theta r} \frac{\sigma_r}{E_r} - \mu_{\theta z} \frac{\sigma_z}{E_z} + \alpha_\theta T + \chi_\theta, \quad (2)$$

$$\varepsilon_z = \frac{\sigma_z}{E_z} - \mu_{zr} \frac{\sigma_r}{E_r} - \mu_{z\theta} \frac{\sigma_\theta}{E_\theta} + \alpha_z T + \chi_z. \quad (3)$$

where σ_r , σ_θ and σ_z —radial, circumferential and axial stress components;

ε_r , ε_θ and ε_z —radial, circumferential and axial strain components;

E_r , E_θ and E_z —modulus of elasticity of material in corresponding directions;

$\mu_{r\theta}$, $\mu_{\theta r}$, μ_{rz} , μ_{zr} , $\mu_{\theta z}$ and $\mu_{z\theta}$ —Poisson's ratios;

α_r , α_θ , α_z —linear thermal expansion coefficients in corresponding directions;

$T = T(r, z)$ —temperature function;

χ_r , χ_θ , χ_z —chemical shrinkage of material in corresponding directions.

We considered the outside Area as transversely isotropic cylindrical solid. For this solid

$$\begin{aligned} E_r = E_\theta = E, \mu_{r\theta} = \mu_{\theta r} = \mu, \mu_{z\theta} = \mu_{zr}, \\ \mu_{\theta z} = \mu_{rz}, \alpha_r = \alpha_\theta = \alpha, \chi_r = \chi_\theta = \chi \end{aligned} \quad (4)$$

Chemical shrinkage of the material along the fibers is neglected, *i.e.* $\chi_z \equiv 0$.

Also under symmetry of elastic constants the next relations are take place:

$$E_r \mu_{rz} = E_z \mu_{zr}, E_\theta \mu_{\theta z} = E_z \mu_{z\theta}, E_\theta \mu_{\theta r} = E_r \mu_{r\theta}. \quad (5)$$

For generalized plane strain state

$$\varepsilon_z = \varepsilon_\theta = \text{const} \quad (6)$$

The equilibrium equation for infinitely small element inside cylinder in local cylindrical coordinates $r\theta z$ (z direction—along fibers) for $r\theta$ plane is follow:

$$\frac{d\sigma_r}{dr} + \frac{\sigma_r - \sigma_\theta}{r} = 0 \quad (7)$$

Geometrical relations

$$\varepsilon_r = \frac{du}{dr}, \varepsilon_\theta = \frac{u}{r} \quad (8)$$

It is accepted that inner Area II of the rod is acting like incompressible liquid. The liquid resin is pressurized and acts on the walls of cured cylinder (**Figure 2(b)**). Then

boundary conditions for cylinder are following

$$\sigma_r = -P_1 \text{ for } r = R_1 \quad \sigma_r = -P_2 \text{ for } r = R_2 \quad (9)$$

Solve Equations (1)-(3) by stresses, using (4)-(8) and boundary conditions (9) the following equations for stresses can be obtained:

$$\begin{aligned} \sigma_r = \frac{P_1 R_1^2 - P_2 R_2^2}{R_2^2 - R_1^2} - \frac{1}{r^2} \frac{R_1^2 R_2^2 (P_1 - P_2)}{R_2^2 - R_1^2} - \\ \frac{1}{r^2} \frac{(\alpha + \alpha_z \mu_{rz}) E E_z}{E_z - \mu_{rz}^2 E} \left(\int_{R_1}^r T r dr - \frac{r^2 - R_1^2}{R_2^2 - R_1^2} \int_{R_1}^{R_2} T r dr \right) \end{aligned} \quad (10)$$

$$\begin{aligned} \sigma_\theta = \frac{R_1^2 P_1 - R_2^2 P_2}{R_2^2 - R_1^2} + \frac{1}{r^2} \frac{R_1^2 R_2^2 (P_1 - P_2)}{R_2^2 - R_1^2} + \\ \frac{(\alpha + \alpha_z \mu_{rz}) E E_z}{E_z - \mu_{rz}^2 E} \frac{1}{r^2} \left(\int_{R_1}^r T r dr + \frac{r^2 + R_1^2}{R_2^2 - R_1^2} \int_{R_1}^{R_2} T r dr - T r^2 \right) \end{aligned} \quad (11)$$

$$\begin{aligned} \sigma_z = \frac{N}{(R_2^2 - R_1^2) \pi} + \\ \frac{\alpha \mu_{rz} E_z E + \alpha_z E_z^2}{E_z - \mu_{rz}^2 E} \left(\frac{2}{R_2^2 - R_1^2} \int_{R_1}^{R_2} T r dr - T \right) \end{aligned} \quad (12)$$

The value of pulling force N we can find from (13):

$$N = \int f_{tot}(z) dS(z), \quad (13)$$

where $f_{tot}(z)$ is the total resisting force per unit area of the composited in contact with the die and S the internal surface area of the die. The solution for (13) is described in [7].

4. Failure Criteria

As mentioned above, at high pull speeds the strain occurred in a polymerized part of the rod may exceed the maximum allowable values for the material which leads to the main crack appearance. As a strength criterion the maximum deformation criterion is chosen which has the form [8]:

$$\varepsilon_r^\pm \leq [\varepsilon_2^\pm], \varepsilon_\theta^\pm \leq [\varepsilon_2^\pm], \varepsilon_z \leq [\varepsilon_1] \quad (14)$$

The study determined that the values of the stresses in the cross section of the rod are far from the limit values, whereas the strain exceeds the limiting values at high pull speed. Therefore, the maximum deformation criterion was chosen as the primary. The sign “+” means tension, “-” compression, $[\varepsilon_i^\pm]$ the ultimate strain obtain as

$$\varepsilon_2^\pm = \frac{\sigma_2^\pm}{E}, \varepsilon_1 = \frac{\sigma_1}{E_z}. \quad (15)$$

there σ_2^+ , σ_2^- , σ_1 —experimentally determined limiting values of stresses for a material by transverse tension,

transverse compression and tension along the fibers, respectively. The strains are defined by (1)-(3) with subject to (10)-(12) and compared with ultimate values from (15).

5. The Heat Transfer and Polymerization Model

For stress-strain state determination we need to know the temperature field distribution and location of the border between cured and liquid material. For this we should solve the non-linear heat transfer and polymerization problem which for pultrusion of the rod has a view [9]:

$$C\rho V \frac{\partial T_t(r, z)}{\partial z} = \lambda \left(\frac{\partial^2 T_t(r, z)}{\partial r^2} + \frac{1}{r} \frac{\partial T_t(r, z)}{\partial r} \right) + \chi WV \frac{\partial \psi}{\partial z}, \quad (16)$$

$$V \frac{\partial \psi}{\partial z} = K_0 \exp\left(-\frac{E_A}{RT_t(r, z)}\right) (1-\psi)^n, \quad (17)$$

$$T_t(r, z)|_{z=0} = T_0, \lambda \frac{\partial T_t(r, z)}{\partial r} \Big|_{r=R_1} = \gamma (T_t(r, z) - \mathcal{G}(z)), \quad (18)$$

$$\lambda \frac{\partial T_t(r, z)}{\partial r} \Big|_{r=0} = 0, \psi|_{z=0} = 0,$$

where C —heat capacity; ρ —density; V —pulling velocity; W —reaction heat; λ —thermal conductivity; ψ —degree of polymerization; χ —resin volume; T_r —absolute temperature; T_0 —rod temperature at inlet of die; K_0 —pre-exponential factor; E_A —active energy of process activation; R —gas constant; n —total reaction order by reacting components; γ —heat-transfer coefficient; $\mathcal{G}(z)$ —ambient temperature.

Based on the solution of (16)-(18) by the method of finite differences [11] the radius R_1 of the inner zone II is obtained. For this radius the degree of polymerization $\psi = 0.95$ (Figure 3(a)).

Using the value R_1 the interval of the temperature distribution over the cross section is determined for the calculation of integrals in the (10)-(12) (Figure 3(b)). The stress values are numerically obtained using the trapezium method.

6. Pressure Model

One of the process parameter in pultrusion is the pressure-rise inside a die. The pressure of liquid resin appears due to fiber/resin system passes through the die (Figure 4). The equation of incompressibility [5,6] for the flow of resin moving through the fibers in a cylindrical coordinate system is follow:

$$\frac{\partial}{\partial z}(\varphi \cdot u) + \frac{1}{r} \frac{\partial}{\partial r}(r \cdot \varphi \cdot v) = 0 \quad (19)$$

In the projections of the velocity vectors onto the axis

z (along the rod axis)

$$u = U - \frac{K_{11}}{\mu\varphi} \frac{\partial P}{\partial z} \quad (20)$$

In the projections of the velocity vectors onto the axis r (in radial direction)

$$v = V - \frac{K_{22}}{\mu\varphi} \frac{\partial P}{\partial r} \quad (21)$$

here K_{11} —medium permeability in axial direction; K_{22} —medium permeability in radial direction; v —component of resin velocity in radial direction; u —component of resin velocity in longitudinal direction; V —component of fiber velocity in radial direction; U —component of fiber velocity in longitudinal direction (pull speed); μ —viscosity; $\varphi = 1 - V_f$ —porosity; V_f —the function of changes in the fiber volume fraction along the length of the tapered die.

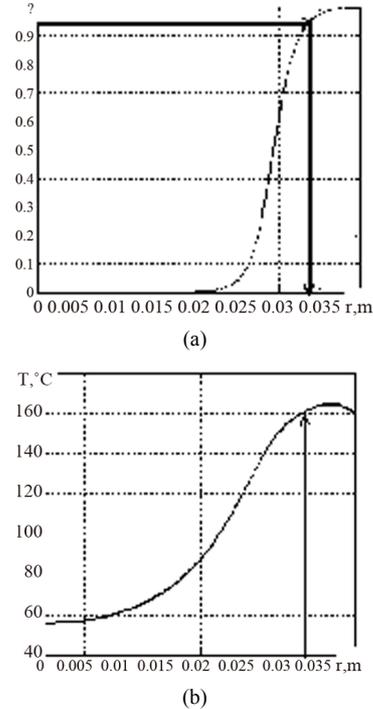


Figure 3. Defining the radius of the inner zone (a) and temperature interval (b).

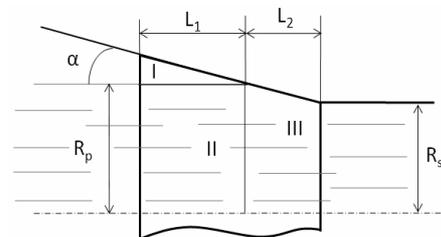


Figure 4. The input section of the die and its geometrical parameters.

Expressions (19)-(21) are based on Darcy's law for the resin flow, passing through a porous medium (fiber) at low speeds. According to Gebart's model [10] the permeability in the axial and transverse directions are given as

$$K_{11} = \frac{8R_f^2 (1-V_f)^3}{c V_f^2}, K_{22} = C_1 \left(\sqrt{\frac{V_{f\max}}{V_f}} - 1 \right)^{5/2} R_f^2 \quad (22)$$

where R_f is the fiber radius, $c = 53$, $C_1 = 0.231$ and $V_{f\max} = 0.9068$.

Taking into account (20) and (21) and that

$$V(r) = -U \frac{r \cdot \tan \alpha}{\sqrt{(R_p - z \cdot \tan \alpha)^2 + r^2 \tan^2 \alpha}},$$

where $\alpha(z)$ —geometrical parameter of the input section of the die (the taper angle), $R(z)$ is the local radius of the die wall, we can obtain the following differential equation for the pressure from (19):

$$K' \frac{\partial P}{\partial z} + K_{11} \frac{\partial^2 P}{\partial z^2} + K_{22} \frac{1}{r} \frac{\partial P}{\partial r} + K_{22} \frac{\partial^2 P}{\partial r^2} = K'' \quad (23)$$

where

$$K' = -\frac{8R_f^2 \tan \alpha}{cV_s^2 R_s^4 (R_p - z \cdot \tan \alpha)^3} \left(2R_s^6 V_s^3 + 4(R_p - z \cdot \tan \alpha)^6 \right) + \frac{48R_f^2 \tan \alpha}{cV_s R_s^2} (R_p - z \cdot \tan \alpha)$$

$$K'' = -\frac{2V \tan \alpha}{\sqrt{\left((R_p - z \cdot \tan \alpha)^2 + r^2 \cdot \tan^2 \alpha \right)}}$$

V_s —is the fiber volume fraction in the straight portion of the die (or finished products), R_p is the aperture radius of the last pre-form plate.

To solve the problem (23) by finite differences method [11], the solution region divided into four zones (**Figure 4**). In this only half die simulated due to symmetry. It was assumed that the zone I completely filled a resin (it is a resin backflow region there excess resin is squeezed out of the die due to the compression of the fiber/resin system). For this region Equation (23) has a view:

$$\frac{\partial^2 P}{\partial z^2} + \frac{1}{r} \frac{\partial P}{\partial r} + \frac{\partial^2 P}{\partial r^2} = 0 \quad (24)$$

For a region II $V_f = V_s \frac{R_s^2}{R_p^2} = const$, therefore (23)

can be written as

$$K_{11} \frac{\partial^2 P}{\partial z^2} + K_{22} \frac{1}{r} \frac{\partial P}{\partial r} + K_{22} \frac{\partial^2 P}{\partial r^2} = 0 \quad (25)$$

For a III region the Equation (23) is applied in general

form. For a IV region the Equation (25) is used taking into account that $V_f = V_s = const$.

At the computational domain inlet, the pressure is considered to be equal to atmospheric pressure P_0 (101,325 Pa). The boundary conditions on the tapered wall of the die were determined from the ratio of velocity components at the boundary: $\tan \alpha = -v/u$. The boundary condition for the grid points of the rod, where the polymerization is completed ($\psi = 0.95$): $\partial P / \partial z = 0$. At the center line ($r = 0$), and At the Top boundary (straight portion of die): $\partial P / \partial r = 0$.

7. Results and Discussion

Thus, solving the system of Equations (10)-(18), (23)-(25) we can obtain the strains for every rod cross section at the outlet of the die and, comparing them with ultimate values, prevent main crack appearance.

The following parameters were used when solving the problem. The rod radius $R_s = 38$ mm, pull speed 70 mm/min. Pre-form plate radius $R_p = 1.085R_s$. Fiber radius $R_f = 0.013$ mm, fiber volume fraction $V_s = 0.6$, taper angle $\alpha = 25^\circ$, length of the taper part of the die $L1 + L2 = 76$ mm, the resin viscosity under normal conditions $\mu = 1.5$ Pa s, $P_0 = 101325$ Pa. The Poisson's ratios $\mu_r = 0.3$; $\mu_z = 0.295$; The thermal expansion coefficients $\alpha = 15 \times 10^{-6}$ $1/C^\circ$, $\alpha_z = 3 \times 10^{-6}$ $1/C^\circ$, Modulus of elasticity $E_r = 8000$ MPa, $E_z = 40000$ MPa. The next strength data for composit material are used [8]: longitudinal tensile strength $\sigma_1 = 1800$ MPa, transverse tensile strength $\sigma_2^+ = 43$ MPa, transverse compressive strength $\sigma_2^- = 90$ MPa. Die temperature settings (the length of straight portion of the Die is 1 m): 110-150-190-160 C° . The parameters such as preexponential factor, reaction heat, active energy of process activation and total reaction order by reacting components was taken from [9].

As a result of solving the problem (23)-(25) the centerline pressure profile along the Die is obtained (**Figure 5**).

Figures 6 and 7 show the profiles of the radial (**Figure**

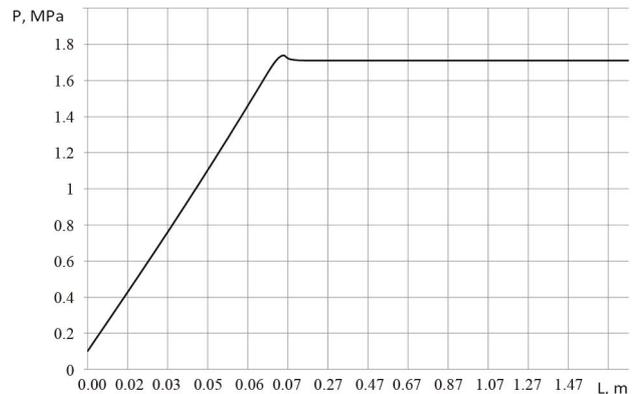


Figure 5. The centerline pressure profile ($r = 0$).

6) and circumferential (Figure 7) strains in rod section A-A (Figure 1)). It was assumed that external pressure $P_2 = 0$ (Figure 2 (b)), pulling force $N = 5000$ N. In this example the chemical shrinkage was taken as $\chi = 0.15\%$, the ultimate strain tension of composite material in according to (15) is $[\varepsilon^+] = 5.4 \times 10^{-3}$.

To determine the maximum possible pull speed series of solutions at different pull speeds are obtained. For the each of the solution the maximum strains (circumferential and radial) were determined. These values are summarized in Table 1. Figure 8 shows the maximum strain profiles as functions of pull speed.

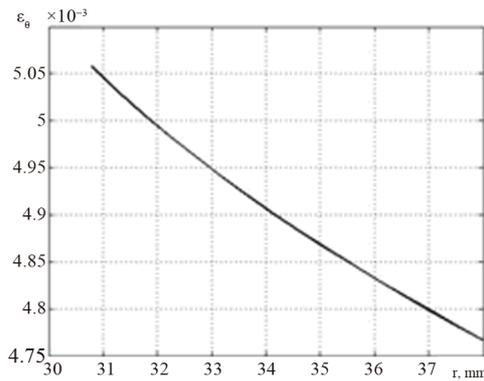


Figure 6. The distribution of radial strains in the cross section.

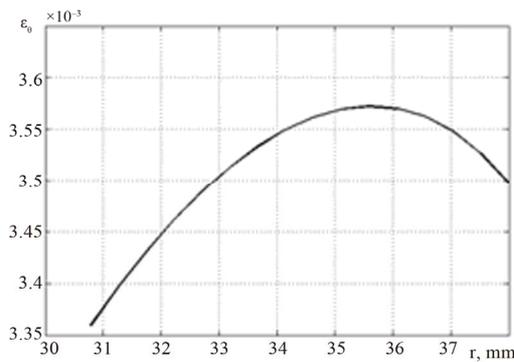


Figure 7. The distribution of circumferential strains in the cross section.

Table 1. Summary results.

Pull speed U mm/sec	Resin pressure P MPa	Inner radius R_1 mm	Strain ε_{rmax} %	Strain $\varepsilon_{\theta max}$ %
0.75	1.13	22.4	0.3911	0.4282
0.833	1.25	25.5	0.3843	0.4388
0.917	1.36	27.1	0.3789	0.4488
1	1.48	28.6	0.3722	0.4629
1.083	1.59	29.4	0.3673	0.4748
1.167	1.71	30.2	0.3613	0.4893
1.25	1.82	31.0	0.3545	0.5075
1.333	1.94	31.7	0.346	0.5304
1.417	2.05	32.5	0.3355	0.5601
1.5	2.16	32.5	0.3328	0.5694

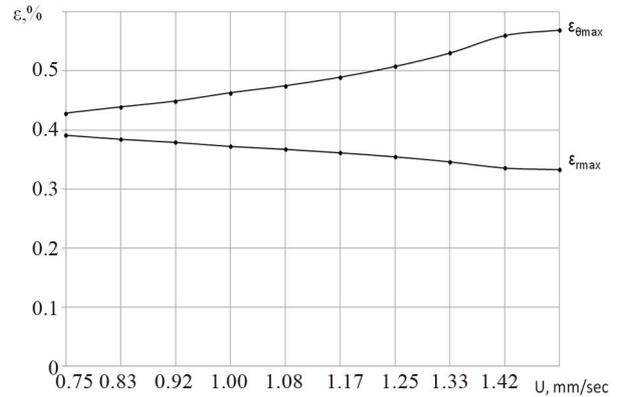


Figure 8. Profiles of the maximum strains as a functions of pull speed.

8. Conclusions

Analyzing the results, it can be concluded that for this example the optimum pull speed is up to 1.33 mm/sec.

The numerical model is a useful tool to determine the stress-strain state of polymer composite materials at the outlet of the Die through the selection of appropriate values for the different process control parameters. An appreciable stress-strain state can help to suppress crack formation, and aid in the manufacture of a quality pultruded product.

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