

Propyl-Sulfonic Acid Functionalized Nanoparticles as Catalyst for Pretreatment of Corn Stover

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ABSTRACT

Propyl-sulfonic (PS) acid-functionalized nanoparticles were synthesized, characterized and evaluated as catalysts for pretreatment of corn stover. Silica coated nanoparticles were functionalized with 0.5% mercaptopropyltrimethoxysilane (MPTMS) at neutral pH in a mixture of water and ethanol. Sulfur contents of the acid functionalized nanoparticles, measured in a CHNS analyzer, varied from 6% - 10%, and the acid load ranged from 0.040 to 0.066 mmol H⁺/g. A Box-Behnken design was employed to calculate the minimum number experiments required to obtain an estimate of the surface response for temperature, catalyst load, and %S content of the catalyst. Pretreatment of corn stover was carried out at three temperature levels 160, 180, and 200°C for 1 h. Three levels of catalyst load were used 0.1, 0.2, and 0.3 g of catalyst per gram of biomass. Hydro-thermolysis controls were carried at each temperature level. The catalyst load did not have an effect on the glucose yield at 160°C, and the average glucose yield obtained at this temperature was 59.0%. The glucose yield was linearly correlated to the catalyst load during pretreatment at 180°C, and a maximum glucose yield of 90% was reached when using 0.2 g of PS nanoparticles that had a total sulfur content of 6.1%. Complete hydrolysis of glucose was reached at 200°C but the average xylose yield was 4.6%, and about 20.2% of the combined glucose and xylose were lost as hydroxymethylfurfural and furfural. Results showed that acid-functionalized nanoparticles can be potential catalysts for the pretreatment of biomass for its later conversion to ethanol.

KEYWORDS

Acid Functionalized Nanoparticles; Catalyst; Biomass Pretreatment; Hydrolysis

1. Introduction

One of the challenges in the production of bioethanol and chemicals from lignocellulosic biomass is breaking down the complex structure of biomass into monomeric sugars. Biomass has a complex mixture of cellulose, hemicellulose, and lignin. A pretreatment step is required to make the biomass cellulose fraction more susceptible to enzymatic hydrolysis. It has been found that the removal of lignin and the consequent solubilization of hemicelluloses favor the enzymatic digestion of cellulose [1]. The most accepted method for pretreatment of lignocellulosic biomass uses corrosive catalysts such as hydrochloric acid or sulfuric acid [2-6]. The need for corrosion resistant materials which require higher capital investment can be avoided when using less corrosive catalysts. Thermochemical pretreatment of biomass generates decomposition products such as hydroxymethylfurfural (HMF) and furfural. Pretreated biomass must be detoxified to remove these products because they could inhibit the microorganisms used during the sugar fermentation to ethanol [7]. Chemical pretreatment of lignocellulosic biomass incurs additional costs for disposal of residues from neutralization and biomass conditioning. Solid acids provide similar catalytic advantages as their liquid counterparts, with the additional benefit that solid acids can be recovered and reused [8-11]. Solid acids in the nanoscale pre-

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vent the mass transfer problems that common heterogeneous catalysts generate. Acid functionalized nanoparticles could be used to replace mineral acids during biomass pretreatment for cellulosic ethanol production. Silica-coated nanoparticles (SiMNPs) can be modified to confer them with desired chemical properties [12]. 3mercaptopropyltrimethoxysilane (MPTMS) is commonly used to graft sulfonic acid functional groups on silica materials. The acid functionalization of SiMNPs can be done using similar procedures to those reported on acid functionalization of silicas [13,14]. Acid functionalized silica materials have been used as catalyst of the α -1,4glycosidic bonds in sucrose and starch [15] and β -1,4glycosidic bonds in cellobiose [16]. Acid functionalized nanoparticles were previously used for the hydrolysis of cellobiose [17] and for the solubilization of hemicelluloses [18]. In this work, silica coated cobalt iron oxide nanoparticles functionalized with propyl-sulfonic acid groups were synthesized and used as catalyst for the pretreatment of corn stover.

2. Methods and Methods

2.1. Materials

Cobalt (II) chloride hexahydrate (99%), D-(+)-Cellobiose (98%), iron (II) chloride tetrahydrate (99.99%), MPTMS (95%), methylamine (40% w/w, 98.5%), sodium dodecyl sulfate (98.5%), and tetraethylorthosilicate (TEOS) (99.999%) were purchased from Sigma-Aldrich (St. Louis, Mo., USA). Ammonium hydroxide, toluene, and isopropanol (A.C.S. reagent) were purchased from Fisher Scientific (Pittsburgh, Pa, USA). Ethanol (95%) was purchased from Decon Laboratories (King of Prussia, Pa., USA). Corn stover was harvested from the Kansas State University Agronomy Farm in October 2011. Corn stover was ground in a cutting mill (SM2000, Retsch, Inc., Newtown, Pa.) to pass a 1 mm mesh. The chemical composition of corn stover is listed in Table 1.

2.2. Synthesis of SiMNPs

Cobalt iron oxide nanoparticles were synthesized by precipitating salts of Co^{2+} and Fe^{2+} using a microemulsion method [19,20]. In a typical experiment, a solution was prepared with 4 mmol (0.9 g) of cobalt (II) chloride hexahydrate CoCl_2 ·6H₂O, 10 mmol (1.9 g) of iron (II) tetrahydrate FeCl_2 ·4H₂O, and 45 mmol (12.9 g) of sodium dodecyl sulfate (SDS). The salts and surfactant were dissolved in distilled water, mixed and diluted to 1 L. One liter solution of 12 wt% methylamine was also prepared. After stirring the first solution for 30 min at room temperature, both solutions were heated to 55°C - 65°C and then combined. The mixture was kept at 55°C - 65°C under rigorous mechanical stirring. After three hours, the particles were magnetically separated and washed three

Table 1. Biomass	s composition	(drv	basis)*.
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Biomass constituents	Corn stover
95% ethanol extractives	21.8 ± 3.8
Glucan (%)	30.2 ± 2.6
Xylan (%)	18.4 ± 2.3
Arabinan (%)	1.9 ± 0.3
Acid-soluble lignin (%)	1.0 ± 0.1
Acid-insoluble lignin (%)	14.5 ± 0.4
Total lignin (%)	15.4 ± 0.5
Acid-insoluble ash (%)	2.1 ± 0.3

^{*}The data presented are averages of three independent analyses.

times with water and once with ethanol. Then the particles were stored in 100 mL of ethanol.

Cobalt iron oxide nanoparticles were coated with silica using the procedures reported in the literature [13,17,21]. The dispersion of $CoFe_2O_4$ in ethanol was sonicated for 1 h. About 15 ml of this solution were added to 550 ml blend isopropanol and water 9:1. This solution was sonicated and mechanically stirred for 30 min. One mL of tetraethylorthosilicate (TEOS) was diluted in 40 mL of isopropanol. After stirring, 50 mL of concentrated ammonium hydroxide were added and the dilute TEOS solution was added drop wise at a rate of 0.3 ml/min. After the addition of the TEOS solution, the mixture was sonicated for another hour. Then the silica-coated magnetic nanoparticles (SiMNPs) were magnetically separated, washed four to five times with water and dried at 40°C in a forced air convection oven.

2.3. Functionalization of SiMNPs

Propyl-sulfonic (PS) acid grafting upon silica-coated nanoparticles was done using similar procedures to those used for functionalization of silicas [13,14,22-25]. About 500 mg of dry SiMNPs and 1 ml of MPTMS were sonicated in 100 ml of ethanol for 1 h. After sonication, 100 ml of 100 mM acetate buffer at pH 4.8 was added and the mixture was heated and mechanically stirred at 75°C. After 16 h of reaction, the mercaptopropyl-functionalized nanoparticles were separated magnetically and washed three times with ethanol. Then, the nanoparticles were placed in a 60 ml solution with equal amounts of water, methanol, and hydrogen peroxide for oxidization of the mercapto groups. After 48 h in the oxidizing solution, the nanoparticles were washed three times with distilled water and left overnight in 100 mL of 0.01 N HCl. After protonation, the PS nanoparticles were separated out of the acid solution and washed multiple times with distilled water. Then, the PS nanoparticles were dried at 120°C for 3 h.

2.4. Characterization of the Nanoparticles

Fourier transform infrared (FTIR) spectra were used to confirm the presence of the propyl-sulfonic acid bonds in the synthesized nanoparticles. The measurement was carried out in the wave number range of 500 to 4000 cm⁻¹, with a resolution of 4 cm⁻¹ and 32 scans per sample. The spectra and peak positions were determined using an infrared spectrometer and its spectrum software (Spectrum 400, PerkinElmer Inc., Waltham, Mass.).

Sulfur content was used as an indicator of the silane grafting level on the nanoparticles, and it was determined in an elemental analyzer (Model 2400 Series II, Perkin-Elmer Inc., Waltham, Mass.). The concentration of hydronium ions was calculated from the percentage of sulfur dividing by the molecular weight of the sulfur atom and the working volume.

2.5. Pretreatment of Corn Stover

Compositional analysis of the corn stover before pretreatment was done following the NREL LAP TP-510-42618 [26]. PS nanoparticles were used to pretreat corn stover and evaluate their ability to increase biomass susceptibility to enzymatic hydrolysis. A scheme of the steps followed to pretreat biomass using acid functionalized nanoparticles is shown in Figure 1. A Box-Behnken design was employed to calculate the minimum number experiments required to obtain an estimate of the surface response for temperature, catalyst load, and %S content of the catalyst. A minimum of 17 experiments was calculated, and the results from 34 runs were analyzed using Design Expert (Stat-Ease, Inc., Minneapolis, Minn., USA). The pretreatment was carried out at 160, 180, and 200°C. In a typical experiment, 0.1 - 0.3 g of PS nanoparticles, and 1.0 g of corn stover both weighted to the nearest 0.1 mg, and 39 ml of distilled water were placed in 60 ml Swagelok tube (Swagelok, Kansas City Valve & Fitting Co., Kan.). Then, the tube was sonicated for 30 min to disperse the nanoparticles. After sonication, the tube was placed in a sand bath that was previously heated at the pretreatment temperature. After 60 min of reaction, the tube was cool down to room temperature in about 5 min. The control experiments had no catalyst and were carried out under the same conditions as the experiments using PS nanoparticles. After pretreatment, the solid and liquid fractions were separated via vacuum filtration using a Büchner funnel. The pretreated solids and the PS nanoparticles were retained in the paper filter and the solubilized sugars passed as filtrate. The solid material was washed with plenty of water to remove all the soluble sugars as described in [27]. Then, the solid fraction was hydrolyzed for 24 h following the NREL LAP TP-510-42629 [28]. In a typical experiment, about 2.5 g of wet biomass were placed in 30 ml of distilled water and



Figure 1. Schematic of the sugar recovery from corn stover using propyl-sulfonic acid functionalized nanoparticles during pretreatment.

30 ml of 100 mM acetate buffer at pH 4.8; after 2 ml of Accelerase[®] 1500 were added to the slurry, the samples were kept at 50°C for 24 h. After hydrolysis, the solutions were analyzed by HPLC to account for glucose and xylose using a RCM-Ca²⁺ monosaccharide column (300 \times 7.8 mm; Phemomenex[®], Torrance, CA, USA) and refractive index detector. Samples were run at 80°C at 0.6 ml/min with water as mobile phase. The PS nanoparticles were then separated from the enzymatically treated solution. A 400 mesh was used to retain the solid fraction left after enzymatic hydrolysis and then a magnet to wash the nanoparticles. The nanoparticles were then dried and analyzed by FTIR. The filtrate was passed over a filter membrane of 0.2 µm. The liquid fraction from the pretreatment was analyzed for sugars following NREL LAP TP-510-42623 [29]. The products of the decomposition of glucose and xylose, HMF, and furfural were measured using an ROA-organic acid column (300×7.8 mm; Phemomenex[®]. Torrance, CA) and an UV detector. Samples were run at 65°C at 0.6 ml/min with 5 mM H₂SO₄ for 55 min. The percentage of glucose converted to HMF was calculated multiplying the concentration of HMF by 1.429. The percentage of xylose converted to furfural was calculated multiplying the concentration of furfural by 1.562.

2.6. Recyclability Experiments

The stability of the PS nanoparticles was evaluated using cellobiose hydrolysis as model reaction of biomass pretreatment. Solutions of 4 mg/ml of cellobiose and 1% PS nanoparticles were placed in a 60 ml Swagelok tubes (Swagelok, Kansas City Valve & Fitting Co., Kan.). The tubes were kept at 175°C for 30 min in a sand bath. The sugar solution and the PS nanoparticles were separated using a neodymium magnet and dried at 105°C. PS nanoparticles were analyzed with the elemental analyzer as described above.

3. Results and Discussion

FTIR spectra taken to the acid-functionalized nanoparticles are shown in Figure 2. The peaks at 1620 cm^{-1} and 3400 cm⁻¹ observed on the spectra have been attributed to the O-H vibration and stretching vibrations of physisorbed water. These bands could also be associated to silanol groups of the SiMNPs [30,31] that did not reacted with MPTMS. It has been reported that only one hydroxyl group from silanols attaches to silica surfaces [32]. Therefore, the hydroxyl groups of the propylsilanol moieties can also generate bands at 3400 cm⁻¹. The peaks at 1950 - 1929 cm⁻¹ are associated with symmetric and asymmetric vibrations of the C-H bonds in the propyl chain, respectively [30,33,34]. Deformation vibrations bands of -CH₂ are also observed at 1457 cm⁻¹ [35]. In the fingerprint region, we can observe the bands attributed to Si-O-Si, Si-OH, and Si-O at 1078, 956, 800 cm⁻¹ [33,36-38]. The peaks at 1414 cm^{-1} in the spectra for PS nanoparticles have been assigned to the stretching vibrations of S=O from undissociated acid sulfonic groups [39,40]. The doublet at 1350 and 1310 cm⁻¹ has been attributed to stretching vibrations of -SO₃-species [40]. The peak at 2520 cm⁻¹ [41] associated to thiol groups from the mercaptopropyl groups was not observed. This means that all the groups were either oxidized to sulfonic acid groups or to other S species. Other authors have found evidence of the formation of S-S bridges when working with MPTMS: however, bands associated with S-S were not observed either. The bands at 743 and 691 cm⁻¹ may be attributed to S-OR species.

The sulfur content %S of PS nanoparticles varied from 5.01% to 9.94%. Badley *et al.* (1989) reported values of %S between 3.25% and 8.32% for propyl-sulfonic acid



Figure 2. FT-IR spectra of propyl-sulfonic acid functionalized nanoparticles.

functionalized silicas [25]. Other works reported 1.17 meq S/g (3.7%) for propyl-sulfonic modified SBA-15 [42] and 10.88 S% on thiol-MCM-41 [43]. However, it is possible that not all the sulfur was in the sulfonic acid form even though there wasn't evidence of S-S bridged or non-oxidized -SH groups in the FTIR spectra [24].

Predicted total glucose yield from corn stover is shown in Figure 3. The red dots indicate design points, and the lines represent the modeled glucose yield as a function of pretreatment temperature and catalyst loading. At 160°C, PS nanoparticles did not show a significant improvement in the digestibility of the biomass. The average glucose yield obtained at this temperature was 59.02% (±5.48) out of 11 experiments that use various catalyst load levels. Even though PS nanoparticles were effectively modified (5% - 9% S) at 160°C the sugar yield was very close to that of the hydro-thermolysis (0 mg S/g biomass). Aggregation of the particles could have caused limited availability of catalytic sites for reaction with the carbohydrate-lignin bonds in biomass. On the other hand, at 200°C complete sugar hydrolysis occurred, so it was not possible to tell the differences between the control experiments and the performance of the catalyst. At 200°C, the xylose recovery was less than 6%. This can be explained also by the fact that high temperatures catalyze the production of xylose derived products [44]. A maximum yield of xylose could be reached with a catalyst load of 6 mg S/g biomass between 165°C and 175°C (Figure 4). At low temperatures, a load of catalyst higher than 30 mg/g biomass, which is equivalent to using 24 mmol H^+/L , would be required in order to increase the xylose yield over 50%. Xylose yield increases along with the temperature; however, after 175°C the xylose yield decrease rapidly because at these temperatures the sugars can be degraded to other products such as furfural and formic acid [44]. Some works have been reported about the use of supported acids to produce carbohydrate derived products such as HMF and furfural [45,46]. The amount of glucose that was lost as HMF is shown in Figure 5. The HMF formation increased along with catalyst load and temperature. At 160°C the amount of glucose lost was less than 2% for all catalyst loadings tested. At 200°C, about 11% of the total glucose in the corn stover samples was lost at the higher catalyst load. The amount of xylose lost as furfural is shown in Figure 6. The amount of xylose lost because of furfural formation increased along with temperature. At 160°C, xylose degradation was close to zero, and at 200°C the amount of xylose lost as furfural reached 30%.

With catalyst loadings up to 30 mg S/g biomass, a temperature of 160°C did not provide an effective catalysis of the corn stover pretreatment. At 200°C, the hemicellulose sugars were thermally degraded. Therefore the



Figure 3. Contour graph of the model for total glucose yield from corn stover as a function of pretreatment temperature and catalyst loading.



Figure 4. Contour graph of the model for total xylose yield as function of pretreatment temperature and catalyst loading.

set of experiments carried out at a temperature of 180° C, were used for statistical analysis. A Bonferroni correction was applied for which a *P*-value of 0.025 was used as criteria for significance for this set. At 180° C, the total glucose yield was linearly correlated to the load of catalyst which was indicated in terms of total sulfur mass (**Figure 7**). A maximum glucose yield of 90% was reached when using 0.2 g of PS nanoparticles that had a total sulfur content of 6.1%.

PS nanoparticles could have been done a better job pretreating corn stover if they did not aggregate and form



Figure 5. Contour graph of the model for the percentage of glucose lost as HMF as a function of pretreatment temperature and catalyst loading.



Figure 6. Contour graph of the model for the percentage of xylose lost as furfural as a function of pretreatment temperature and catalyst loading.

clumps. Aggregation of the nanoparticles hides the catalytic sites and makes them unavailable for reaction. It is also possible that sulfate salts were formed with the ions derived from trace minerals in biomass. PS nanoparticles seemed to have affinity towards pretreated biomass since it was very difficult to remove biomass entirely in order to analyze the nanoparticles after pretreatment. This was evidenced by the increment in carbon content in the PS nanoparticles after pretreatment (**Table 2**). Even though the nanoparticles were present during the enzymatic hydrolysis, inhibitory character of acid-functionalized na9.00

9.59

3.13

after cellobiose hydrolysis at 175°C.						
PS nanoparticle	% C	% H	% N	% S		
Before cellobiose hydrolysis	11.86	2.39	-	9.81		

11.10

11.43

24.67

2.33

2.62

3.32

2.21

After cellobiose hydrolysis

Before corn stover pretreatment

After corn stover pretreatment

 Table 2. Elemental analysis of PS nanoparticles before and after cellobiose hydrolysis at 175°C.



Figure 7. Total glucose yield from corn stover as a function of catalyst loading at 180°C for one hour.

noparticles was not observed. Since complete glucose recovery was reached for some of the experiments we believe that PS nanoparticles did not block the access of the enzyme to the carbohydrate fraction.

Hydrolysis of cellobiose has been used as model reaction of the hydrolysis of cellulose into its constituent glucose units [16,47,48]. In this work, we used the same reaction to analyze the stability of the propyl-sulfonic acid groups in PS nanoparticles. To assess the loss of functional groups during reaction, the sulfur content of the nanoparticles was measured before and after cellobiose hydrolysis (Table 2). The PS nanoparticles lost about 1% of their sulfonic acid groups after hydrolysis of cellobiose at 175°C which is an indicator that PS nanoparticles kept most of their functional groups, and that these groups are stable during catalysis in aqueous media reactions at high temperatures. Elemental analysis was also done upon PS nanoparticles after pretreatment. However, it was difficult to separate material left after pretreatment entirely. Because the organic content of the nanoparticles increased and it was difficult to determine the real percentage of sulfonic groups after pretreatment. An FTIR spectrum was also taken after pretreatment with PS nanoparticles (Figure 8). The band at 1510 cm⁻¹, characte-



Figure 8. FTIR spectra of PS nanoparticles after pretreatment of corn stover at 180°C for 1 h.

ristic of lignin, [49] was observed, as well as an increment in the intensity of the band at 1457 cm^{-1} associated to C-H bonds. Although, the absorption of material, it is not a desired condition; it can be an indicator of the affinity of these nanoparticles towards cellulose derived materials, which it is necessary to carry out catalysis effectively.

4. Conclusion

A maximum glucose yield of 90% was reached when using 0.2 g of PS nanoparticles that had a total sulfur content of 6.1%. The average glucose yield was linearly correlated to the load of PS nanoparticles at 180°C. At 160°C, the amount of PS nanoparticles required to increase the glucose yield above the one obtained without catalyst must be higher than 30 mg S/g biomass which will be equivalent to using 24 mmol H⁺/L. At 200°C, complete cellulose hydrolysis to glucose was achieved but 96% of corn stover hemicelluloses were lost as degradation products. PS nanoparticles kept 99% of their propyl-sulfonic acid load after hydrolysis of cellobiose at 175°C.

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