Enzymatic pretreatment and microwave extraction of asiaticoside from Centella asiatica

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Received 3 July 2009; revised 13 July 2009; accepted 19 July 2009.

ABSTRACT

The extraction of asiaticoside from Centella asiatica by enzymatic pretreatment and microwave extraction (EPME) was studied in this article. The effects of several important factors such as temperature of enzymatic pretreatment, liquid to solid ratio and microwave radiation time were investigated by quadric regression orthogonal design experiment and were analyzed by response surface. An extraction model with well forecast performance was then established. The results indicate that the optimum extraction condition was as follows: liquid to solid ratio was 36mL/g, temperature of enzymatic pretreatment was 45°C, enzymatic time was 30min, and microwave radiation time was 110s. On such conditions the yield was 27.10%.

Keywords: Asiaticoside; Enzymolysis; Microwave Extraction; Centella Asiatica

1. INTRODUCTION

Centella asiatica (L.) Urban, a perennial herb belonging to the umbelliferae family, is well known as a traditional Chinese herbal medicine. Its conventional efficacy is clearing away heat and toxic, inducing diuresis and reducing edema. The major active constituents of *Centella asiatica* are asiaticoside and madecassoside. It has been used for the treatment of hot and humid jaundice, traumatic injuries, infectious hepatitis and dermatosis [1]. Currently, some conventional extraction methods are mostly adopted for the extraction of asiaticoside [2,3,4], such as aqueous extraction and ethanol extraction.

In recent years, new kinds of extraction techniques appeared, including enzymolysis and microwave extraction. The former has impressive effects with characteristics of high catalytic efficiency, high specificity, mild reactive conditions and preserving the original efficacy of active compounds to the maximum [5]. The later method has many advantages, such as shorter time, less solvent, higher extraction rate and better products with lower cost [6,7]. However, the application of the combination of these two methods on plant materials was rarely reported.

For the purpose of improving the efficient of asiaticoside extraction, reducing the cost, the EPME method is employed in this article, quadric regression orthogonal design is adopted to investigate the effects of three main extraction parameters including temperature of enzymatic pretreatment, liquid to solid ratio and microwave radiation time on the yield of asiaticoside, and optimum extraction process is worked out.

2. MATERIALS AND METHODS

2.1. Equipments and Reagents

An ER-692 microwave oven (as shown in **Figure 1**) with a power output of 650W, operating at 2450MHz, was mechanically modified to fit a reflux system that enables extraction performed under atmospheric settings and permits solvent containment. The extraction vessel was a 250-mL three-necked round-bottomed flask connected to a water condenser.

Thermostat with magnetic stirrer (Model DF-101S, Yuhua Experimental Apparatus Co., Shanghai) was used as enzymolysis device. UV spectrophotometer (Model 1900PC, Yayan Electronic Co., Shanghai) was used for determination.

Dry *Centella asiatica* (fitted for the Chinese Pharmacopoeia); Asiaticoside standard (Provided by National Institute for the Control of Pharmaceutical and Biological Products, Beijing); Cellulase (≥400U/mg); Anhydrous ethanol and concentrated sulfuric acid used in the experiment were all of analytical grade.

2.2. Analytic Method of Asiaticoside

The concentration of the asiaticoside in this process was determined by ultraviolet spectrophotometry [8] and the result was expressed as extraction yield, i.e. unit extrac-



tion quantity (g asiaticoside/g Centella asiatica).

The asiaticoside standard sample solution (was diluted by anhydrous ethanol) and extraction solution were scan ed at 200-400nm respectively, there were the same absorption peak at 277nm (**Figure 2**), which was close to the literature values [9]. So 277nm was chosen for the UV wavelengths.

The asiaticoside standard sample solution (concentration: 92µg/mL) was precisely measured at 0.0, 0.5, 1.0, 1.5, 2.0, 2.5mL, and put into a 10mL volumetric flask. Firstly, volatilized out the solvent ethanol in the boiling water bath, and then added the 2mL concentrated sulfuric acid (H₂SO₄) after the flask cooling to the ambient temperature, heated for 30min in 80°C water bath. Finally, added anhydrous ethanol to the scale after the flask getting to the ambient temperature. According to the ultraviolet spectrophotometry, the prepared solution was measured at 277nm. Regression equation and correlation coefficient were y=43.40x-2.49 and r=0.9992 (n=7) respectively. The linear range was 4.6~23.0µg/mL.

The 0.5mL test sample solution was accurately measured and placed into a 10mL volumetric flask, following the preparation method of regression equation. The absorbance of test sample was determined, and the yield of asiaticoside in the test sample was calculated in accordance with the following equation:

Yield of asiaticoside (%, w/w)=

$$\frac{(43.40A - 2.49)Vn}{3 \times 10^6} \times 100\%$$
(1)

where, A, the absorbance of asiaticoside in test sample; V, volume of solvent, mL; n, diluted times.



Figure 1. Microwave equipment diagram; 1-Water condenser; 2-Air condenser; 3-Copper tube; 4-Tailored tube; 5-Air agitator; 6-Status display; 7-Microwave oven timer; 8-Microwave oven; 9-Flask; 10-Base of flask.



Figure 2. UV spectra of reference solution and extraction solution.

2.3. Enzymatic Pretreatment and Microwave Extraction

The dry *Centella asiatica* (sieved through 10 screen mesh) 3.0g was accurately weighed and placed into a threeneck flask with 3% cellulase solution (dissolved by deionized water), then the deionized water as solvent was added in according to a certain ratio (mL/g) of material to solvent volume, and the mass of system was weighed.

Three-neck flask was put into the thermostat with magnetic stirrer, setting enzymolysis time at 30min according to the pre-experiment, while the temperature of enzymatic reaction and stirring speed were set at certain values. Then the flask was taken out and placed into the microwave oven immediately. The radiation exposure was 30s for preventing the serious evaporation of solvent. At the end of each exposure, the system was brought back to ambient temperature during 2~3 min interval by cooling it with a water bath. An extraction cycle was defined as the combination of phases of radiation and phases without radiation in which the solvent cooled. The sum of radiation exposure of processing extraction cycles served as the overall intensity of microwave radiation. The extraction solution was agitated with an air pump to promote heat uniformity while exposing to microwave radiation. After the radiation, the flask was taken out to weigh the total mass again, and the lost weight was supplemented. The extract was filtered through 0.45µm millipore filter, and then abandoned the initial filtrate, added 0.5mL subsequent filtrate to a 10mL volumetric flask with anhydrous ethanol as the test sample.

3. RESULTS AND DISCUSSIONS

3.1. Effect of Temperature of Enzymatic Pretreatment on EPME

As shown in **Figure 3**, the results indicate that the yield of asiaticoside was increased with the increase of temperature of enzymatic pretreatment, reached a high point at 45 °C. Because the temperature of enzymatic pretreatment was a significant factor in the process of enzymolysis, it affected the enzyme activity as well as the rates of enzyme-catalyzed reactions. When the temperature was lower than 45 °C, the increase of temperature can improve the cellulase activity, accelerate the degradation of cytoderm. While the temperature of enzymatic pretreatment was higher than 45 °C, the cellulase activity was decreased, leading to the reduction of the yield. Therefore the temperature of enzymatic pretreatment for 45 °C was used.

3.2. Effect of Liquid to Solid Ratio on EPME

As it is known, the liquid to solid ratio is very important in the extraction. From the perspective of mass transfer, it mainly affects the concentration gradient between liquid phase and solid phase. **Figure 4** shows that the yield of asiaticoside was increased with the increase of liquid to solid ratio. After the peak, the yield of asiaticoside was decreased with the increase of liquid to solid ratio. The higher liquid to solid ratio, the longer time for the solution elevated to the same temperature was required. At the same microwave radiation, the temperature of the system with larger amount of solvent was relatively lower; the solute diffusion would be affected. So the ratio for 30mL/g was chosen.

3.3. Effect of Microwave Radiation Time on EPME

Figure 5 described that the extraction yield sharply increased before 60s and was asymptotic to a steady value during 60~120s, then falls down after 120s. At the preliminary stage of extraction, the velocity of molecular thermal motion quickened and the asiaticoside was quickly separated from the cell into solution. The extraction process had tended towards equilibrium since 60s. When



Figure 3. Effect of temperature of enzymatic pretreatment on EPME.



Figure 4. Effect of liquid to solid ratio on EPME.



Figure 5. Effect of microwave radiation time on EPME.

the microwave radiation time exceeded 120s, the system was hyperthermal, the vaporization reflux of solution increased. All of above brought about the reduction of effective contact interval of solvent and plants, and caused the decrease of the thermal effects. In addition, the extension of microwave radiation time would increase the consumption of energy. Thus the microwave radiation time for 60s was used in the experiment.

3.4. Quadratic Regression Orthogonal Design Results

The quadratic regression orthogonal design was employed to evaluate the relevance of the three main extraction factors including enzymatic temperature, liquid to solid ratio and the microwave radiation time, while other factors including grinding degree of plant material, concentration of enzyme, enzymatic pretreatment time and pH of the solvent were constant according to the pre-experiments. The multivariate study allows the identification of interactions between variables and provides a complex exploration of the experimental domain to be studied with a number of experiments optimized.

The three key variables studied were pointed at five separate coded levels [11], -1, 0, +1, + γ (=1.682) and their values were selected on the basis of previous experiments. The natural values and coded levels used in this multivariate study are presented in **Table 1**.

 Table 1. Factors of orthogonal experiment.

	X ₁ -Microwave	X ₂ -Liquid to	X ₃ -Enzymatic
-γ	9	13	28
-1	30	20	35
0	60	30	45
1	90	40	55
γ	111	47	62
Δ	30	10	10

The statistical analysis software was applied in this experiment to establish a regression **Eq.2**, in this equation, the terms of Y, X_1 , X_2 , and X_3 respectively represent the yield of asiaticoside, microwave radiation time, liquid to solid ratio and enzymatic temperature:

$$Y=25.8963+1.8150X_{1}-0.7646X_{2}+0.3464X_{3}$$

+0.9363X_{1}X_{2}+0.4688X_{1}X_{3}+0.1363X_{2}X_{3}(2)
-0.7065X_{1}^{2}-0.6852X_{2}^{2}-1.7547X_{3}^{2}

Analysis of variance was carried out in order to test the signification of the regression model. Thus, various statistical data such as sum of squares (SS), mean squares (MS), F-ratio were given in Table 2.

The F-ratio in **Table 2** was the ratio of the meansquared error to the pure error obtained from the replicates at the design center. The significance of the F-ratio depends on the number of degrees of freedom (d. f.) in the model. Thus, the effects lower than 0.05 in this column were significant.

As shown in **Table 2**, $F_{\text{Regression}}=10.866>F_{0.05}$ (9, 8)=3.388, the regression of (2) was significant, while $F_{\text{Lack of fit}}=3.478<F_{0.05}$ (5, 8) =3.687, the lack of fit was non-significant. Therefore, (2) had well predictivity under the experimental condition. In the test of regression coefficient, F-ratio for terms X₃, X_1X_3 , X_2X_3 (1.253, 1.344, 0.114) were lower than $F_{0.05}$ (1, 8) =5.318, so these terms were not significant. On the contrary, the F-ratio for other terms (X₁, X₂, X₁X₂, X₁², X₂² and X₃²) which were higher than $F_{0.05}$, indicated the significance of these terms. As the orthogonality of this experiment, the insignificant terms were cut out to simplify the (3):

$$Y=25.8963+1.8150X_{1}-0.7646X_{2}+0.9363X_{1}X_{2}$$
$$-0.7065X_{1}^{2}-0.6852X_{2}^{2}-1.7547X_{3}^{2}$$
(3)

Table 2. Variance analysis of test results.

Source	d.f.	SS	MS	F	F _{0.05}
X ₁	1	44.995	44.995	34.409	5.318
X_2	1	7.985	7.985	6.106	
X_3	1	1.639	1.639	1.253	
X_1X_2	1	7.012	7.012	5.363	
X_1X_3	1	1.758	1.758	1.344	
X_2X_3	1	0.148	0.148	0.114	
X_1^2	1	7.935	7.935	6.068	
X_{2}^{2}	1	7.463	7.463	5.707	
X_{3}^{2}	1	48.949	48.949	37.432	
Regression	9	127.885	14.209	10.866	3.388
Lack of fit	5	22.740	4.548	3.478	3.687
Pure error	8	10.461	1.308		
Total	22	161.087	7.322		

Eq.3 indicated that the microwave radiation time and liquid to solid ratio were the main factors that influence the yield because of the significance of the terms X_1 and X_2 . The significance of X_1X_2 suggested the obvious interaction between microwave radiation time and liquid to solid ratio. And the significance of all the quadratic terms demonstrated the nonlinear relationship between the three factors and the yield of extraction.

3.5. Analysis of Response Surface

The 3D surface curves were drawn to illustrate the main and interactive effects of the three factors on the yield. The response surfaces are shown in **Figures 6,7,8** with one variable kept at optimum level and the other two varied within the experimental range.

Figure 6 shows the effect of liquid to solid ratio(X2) and extraction time(X1) on the yield. A quadratic effect for both factors on the response can be observed. At a low level of X2 (-2), the system was readily hyperthermal and vaporization of the solvent could reduced the yield with the increasing of microwave time. And at a high level of X2 (2), the yield displayed an increasing curve in the experimental range of X1. It is due to the distinctly interaction between X1 and X2, which was implied in the Eq.3. The maximum yield was predicted when X1 was in the range of 1.5 to 1.7 and X2 varied from 0.4 to 0.6.

Figure 7 depicts the effect of enzymatic temperature(X3) and extraction time(X1), as both them exerting a quadratic effect. As shown in the Figure 7, an increase in yield resulted when X3 was increased in the level range from -2 to 0, then the curve started to go down, which may indicate that a level of X1 at approximate 0 is required to achieve maximum yield. Likewise, an increase in yield resulted when X1 was increased in the code range from -2 to 1.5, and then the yield was slightly reduced. In the response surface, X1 exerted a more significant effect on yield than X3, and no obvious interaction between X1 and X3 was observed, which was well in agreement with Eq.3.

In **Figure 8**, yield showed quadratic curve depending upon the liquid to solid ratio(X2), whereas no significant effect was observed in the enzymatic temperature(X3). Because the ratio was a key factor which influences the impetus in mass transfer of both enzymatic pretreatment and microwave extraction processes, it exerted a more significant effect on yield than the factor of enzymatic temperature. According to the response surface, there was no obviously interaction between X2 and X3, and it was also supported by the **Eq.3**.

3.6. Optimization of EPME Condition

Yield of extraction was employed as the evaluation objective in the optimization of the parameter to ensure it reaches the peak under constraint conditions. According



Figure 6. Response surface graph of microwave radiation time and liquid/solid ratio.



Figure 7. Response surface graph of microwave radiation time and enzymatic temperature.



Figure 8. Response surface graph of liquid/solid ratio and enzymatic temperature.

	Coded Value		Yield/%		
		Calculated Value	Esti- mated Value	Measured Value	
$X_1(s)$	1.672	110			
$X_2(mL/g)$	0.584	36	27.19	27.10	
X₃(°C)	0	45			

Table 3. Optimum values and verification results

to (3), model was then built up as described hereinafter [10]:

Objective function: $Y(X_1, X_2, X_3)$;

Constraint conditions: $-1.682 \le X_i \le 1.682$; (i=1,2,3)

The optimum parameters and maximal yield were worked out by Newton's iteration method. The results were shown in **Table 3**. To compare the predicted result (82.10%) with the practical value, the rechecking experiment was performed using this deduced optimal condition. The mean value of 27.10% (n=3), obtained from real experiments, demonstrated the validity of the model, since there was no significant differences between 27.19% and 27.10%. The strong correlation between the real and the predicted results confirmed that the extraction model was adequate to reflect the expected optimization.

4. CONCLUSIONS

The quadratic regression orthogonal design was used in this research, an extraction model which can accurately predict the yield of asiaticoside extraction under the experimental condition was established.

Through the analysis of experiment data, it can be found that the microwave radiation time and liquid to solid ratio significantly influence the yield of the extraction. Especially, there was an obvious interaction between the microwave radiation time and liquid to solid ratio.

The optimum combination of the parameters for the extraction of asiaticoside was obtained by the mathematical methology; it was microwave radiation time for 110s; liquid to solid ratio for 36mL/g, and enzymatic pretreatment temperature for 45°C . On this condition, the maximum yield of extraction was 27.10%, closed to the estimated value 27.19%.

The EPME procedure had the advantages of less time, high efficiency of extraction, and environmentally friendly. It can be applied to other extraction of plant materials. But the expansive cost of the enzyme and difficulty in industrialization of microwave extraction would limit the further application of EPME.

5. ACKNOWLEDGMENTS

The work was supported by National Natural Science Foundation of China (No. 20006003).

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