

CO₂ Capture at Room Temperature and Ambient Pressure: Isomer Effect in Room Temperature Ionic Liquid/Propanol Solutions

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Abstract

A CO₂ capture system without supercritical CO₂ was optimized for mixtures of hydrophobic room temperature ionic liquids (RTILs) and propanol. We tested RTILs using bis(trifluoromethanesulfonyl)imide, TFSI⁻, anion and four quaternary ammonium cations, two quaternary phosphonium cations, and one imidazolium cation. The addition of 2-propanol into the RTILs clearly promoted the capture of normal CO₂(*n*CO₂) at ambient temperature and pressure. When combined with 2-propanol, the most efficient RTILs for *n*CO₂ capture were *N*-butyl-*N,N,N*-trimethylammonium TFSI⁻. This enhancement of *n*CO₂ capture was not observed in RTIL mixtures with 1-propanol or in propanol mixtures containing other phosphonium- and imidazolium-based RTILs. The torsion angle of TFSI⁻, which was calculated using density functional theory, is thought to be related to high *n*CO₂ capture efficiently.

Keywords

CO₂ Capture, Room Temperature Ionic Liquids, Propanol Isomer Effect, Torsion Angle of TFSI⁻-Anion

1. Introduction

The emission of greenhouse gases, which warms the Earth's surface and atmosphere, is an urgent global problem. Room temperature ionic liquids (RTILs) have attracted considerable attention for the capture of carbon

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dioxide (CO_2) in efforts to counteract global warming. The capture of CO_2 using an RTIL was first reported by physically dissolving supercritical CO_2 (scCO_2) at high temperature and pressure into 1-butyl-3-methylimidazolium hexafluorophosphate, $[\text{C}_4\text{mim}][\text{PF}_6]$ [1], and the pressure- CO_2 molar fraction phase diagram was constructed at 40°C . Since then, various theoretical [2]–[6] and experimental [7]–[13] investigations have been conducted to further develop techniques for CO_2 capture and storage in green chemistry. Systematic studies reveal that scCO_2 is highly soluble in the bis(trifluoromethanesulfonyl)imide (TFSI $^-$) anion-based RTIL [10] and the polymerization of RTILs has been shown to allow the reversible and fast sorption and desorption of normal CO_2 ($n\text{CO}_2$) [8]. To apply RTILs in actual industrial applications, developing a cost-effective system that does not require high temperature or pressure for $n\text{CO}_2$ capture remains necessary.

As additive effect, isomer effects of alcohols in the RTILs were observed distinctly [14]–[17]. A previous study estimated the molecular interactions between RTILs and propanol on desorption time measured under vacuum [14]. The results indicated that 1-propanol interacts more strongly with RTILs than does 2-propanol. In addition, Raman spectroscopy revealed that the propanol isomer effect is related to the conformations of TFSI $^-$ anion, which can exist as two stable conformers, *cis* (C_1) and *trans* (C_2) [18] [19]. C_1 and C_2 conformers of TFSI $^-$ originate from the competition between the alkyl side-chain length of the C_nmim^+ cation and the propanol isomer effect. Recently, butanol isomer effect was reported in $[\text{C}_n\text{mim}][\text{TFSI}]$ -based systems with four types of butanol [17], owing to the different hydrophobicities of four types of butanol. The upper critical solution temperatures (UCSTs) in the phase diagrams were clearly separated with increasing alkyl side-chain length of the C_nmim^+ cation.

Systematic CO_2 solubility experiments have demonstrated that TFSI $^-$ exhibits good CO_2 capture ability in pure RTILs systems [20]. Isomer effects have been observed in TFSI $^-$ -based RTILs, including $[\text{C}_n\text{mim}][\text{TFSI}]$ ($2 \leq n \leq 10$) [15]. The established binary phase diagrams and UNIQUAC (universal quasichemical) interaction parameters indicate that the interactions of 1-propanol with RTILs differ significantly from the interactions between 2-propanol and RTILs.

In this study, we optimized physical sorption of $n\text{CO}_2$ at room temperature and ambient pressure. The dilution of RTILs with 2-propanol promoted $n\text{CO}_2$ capture, and stabilized the liquid mixing state. The amount of captured $n\text{CO}_2$ was related to the torsion angle of the TFSI $^-$ anion, which was calculated by density functional theory (DFT). The propanol isomer effect and torsion angle of TFSI $^-$ anion had critical effects on the level of $n\text{CO}_2$ absorption in the propanol-rich region, which is desirable for decreasing the cost of carbon capture operation.

2. Materials and Methods

Hydrophobic RTILs were used in this study to prevent contamination by water from atmospheric moisture. TFSI $^-$ is commonly used as the anion in hydrophobic RTILs. In this study, we tested four quaternary ammonium cations, *i.e.*, *N,N*-diethyl-*N*-methyl-*N*-(2-methoxyethyl)ammonium (DEME $^+$), ethyldimethylpropylammonium, (N1123 $^+$), *N,N,N*-trimethyl-*N*-propyl ammonium (N3111 $^+$), *N*-trimethyl-*N*-butylammonium (N4111 $^+$), *N*-tributyl-*N*-methylammonium (N4441 $^+$) and methyltrioctylammonium (N8881 $^+$), two quaternary phosphonium cations, *i.e.*, triethylpentylphosphonium (P2225 $^+$) and tributyl methyl phosphonium (P4441 $^+$), and one prototype cation, *i.e.*, 1-butyl-3-methylimidazolium (C_4mim^+). All RTILs were obtained from IoLiTecCo. 1-Propanol (99.5%) and 2-propanol (99.5%; Kanto Chemical Co.) were used as additives.

For CO_2 sorption, a CO_2 flowing system was assembled. A schematic of the CO_2 sorption system is illustrated in Figure 1. Mixtures were put into a glass-type sample bottle (30 cc).

The sample bottle was placed on a container with flowing gas. The sample container was immersed in an ethanol bath (Yamato Scientific Co., BB301) with flowing CO_2 gas (30 mL/min) for 10 min. Temperature stability was within 0.1°C ($15^\circ\text{C} \leq T \leq 30^\circ\text{C}$). Within 5 s, the sample was moved to the electric balance (HR-202i, A & D Co.), which monitored the desorption process of $n\text{CO}_2$. Gas selectivity testing was conducted using O_2 and N_2 gases.

To determine the phase diagrams of the RTIL-propanol mixtures, samples were cooled from 30°C to -50°C using an ethanol bath (Yamato Scientific Co., BE200). By visual cloud-point determinations, accuracy of the clouding temperatures was found to be within 0.5°C . A liquid N_2 pot was used as a supplement for further cooling. The minimum temperature (-50°C) is limited by viscous ethanol at low temperature. The temperature was monitored by a Pt100 temperature sensor (Netsushin Co.). The cooling rate was $1.5^\circ\text{C}/\text{min}$.

The conformational stabilities of the mixtures were examined by Raman spectroscopy using a micro-Raman spectrometer (RA-07F, Seishin-Shoji) in backscattering mode equipped with a monochromator (500M, Horiba JobinYvon) and a charge-coupled device detector (Symphony, Horiba JobinYvon). Radiation at 532 nm from a

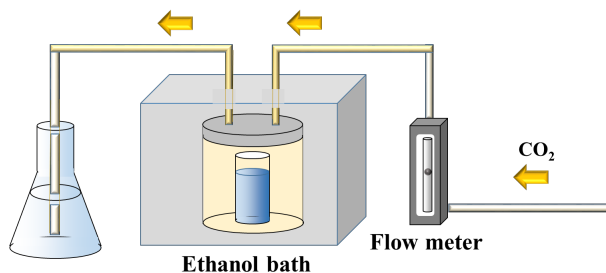


Figure 1. Schematic illustration of $n\text{CO}_2$ sorption assembly.

Nd:YAG laser (power = 50 mW) was used as the excitation source.

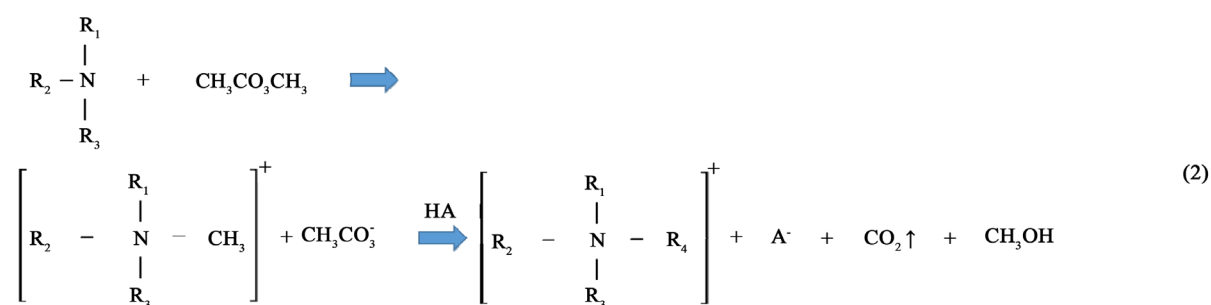
3. Results and Discussion

3.1. $n\text{CO}_2$ Capture in RTIL-Propanol Mixtures

Figure 2 shows the amount of captured $n\text{CO}_2$ as a function of propanol concentration in the [N4111][TFSI]-propanol system at a temperature of 25°C. The molar fraction of $n\text{CO}_2$ was calculated as,

$$\eta = \frac{n_{\text{CO}_2}}{n_{\text{IL}} + n_{\text{CO}_2}} \times 100(\%) \quad (1)$$

where n_{IL} and n_{CO_2} are the moles of RTILs and $n\text{CO}_2$, respectively. We did not consider the amount of propanol in this study, as propanol is relatively inexpensive compared with the RTILs. The results show that the addition of 2-propanol can promote $n\text{CO}_2$ capture in the propanol-rich region. In contrast, 1-propanol did not enhance $n\text{CO}_2$ capture. The value of η for the 1-propanol-based mixtures remained almost constant with changing propanol concentration; this is a typical isomer effect of propanol, as indicated by the phase diagrams [15]. The isomer effect of $n\text{CO}_2$ capture is discussed in the next section along with liquid stability. The above tendency is also seen in other systems. The molar fractions at the points of maximum $n\text{CO}_2$ sorption for all RTILs-propanol systems studied herein are indicated in **Figure 3**. Here, temperature was fixed at 25°C. The $n\text{CO}_2$ sorption of the 1-propanol-based mixture was larger than that of the 2-propanol one only for the [DEME][TFSI] system. Relative large values of η were obtained in the quaternary ammonium cation-based systems. In contrast, the phosphonium and imidazolium systems exhibited lower $n\text{CO}_2$ capture abilities. The high efficiency of $n\text{CO}_2$ capture in the quaternary ammonium cation-based systems can be attributed to the syntheses of these cations. An example of synthesis using the Halogen-free carbonate ester method [21] can be written as follows:



The scheme in Equation (2) leads to the coexistence of quaternary ammonium cation, alcohol and CO_2 , and provides a clue to explain the high $n\text{CO}_2$ capture obtained using quaternary ammonium cations. We predict that the cation, CO_2 and alcohol are affirmative each other. Among the RTILs used in this study, the [N4111][TFSI]-2-propanol system provided the best $n\text{CO}_2$ storage.

3.2. Thermal Properties of $n\text{CO}_2$ Capture

To investigate the thermal characteristics of $n\text{CO}_2$ capture, the η value of the [N4111][TFSI]-80 mol% 2-propanol

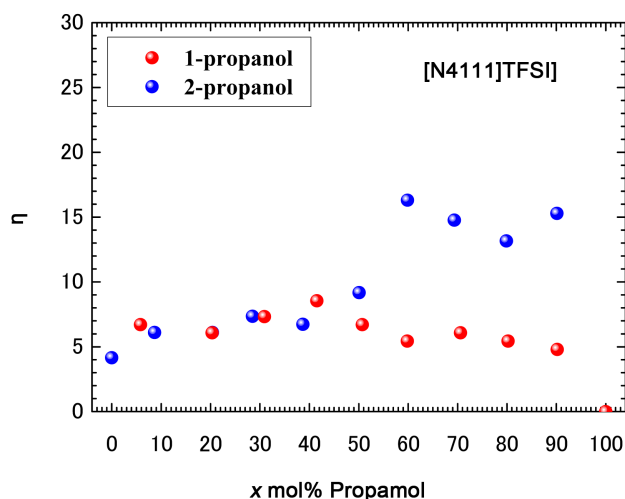


Figure 2. Dependence of $n\text{CO}_2$ molar fraction, η (%), on propanol concentration, showing the propanol isomer effect at 25°C. High $n\text{CO}_2$ sorption is observed in the propanol-rich region.

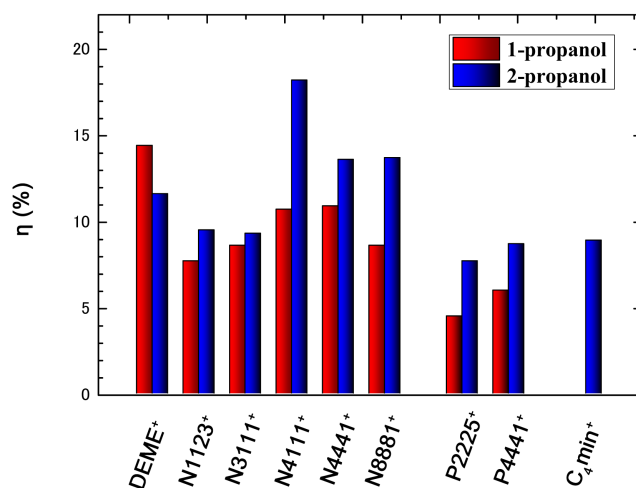


Figure 3. Maximum $n\text{CO}_2$ sorption in various RTILs-propanol systems. With the exception of the [DEME][TFSI]-propanol system, the 2-propanol-based mixtures have a preference for $n\text{CO}_2$ capture. Quaternary ammonium RTILs possess relative high abilities for $n\text{CO}_2$ capture.

system is plotted as a function of temperature in **Figure 4(a)**. Upon cooling down to 15°C, almost monotonic increase of η was observed. According to conventional thermodynamics, η decreases with increasing temperature. At lower temperature, CO_2 absorption efficiency was elevated. In [N4111][TFSI]-propanol system, however, there is a problem of phase separation in the propanol-rich region. **Figure 4(b)** reveals the phase diagram of [N4111][TFSI]-1-propanol and -2-propanol. The phase diagram of [N4111][TFSI]-propanol system was constructed based on visual cloud-point determinations [14] [15] [17]. The cloud-points of 1- and 2-based mixtures are represented by red and blue closed circles, respectively. On the phase diagrams, different molecular interactions of 1- and 2-propanol was predominant, since phase separation curves are calculated using the UNIQUAC interaction parameters [15]. The UNIQUAC model has the nearest neighbor correlation. The UCST of the [N4111][TFSI]-80 mol% 2-propanol mixture was approximately 15°C. Therefore, below 15°C, it is impossible to use $n\text{CO}_2$ capture in the [N4111][TFSI]-2-propanol system for industrial applications.

Phase diagram including phase instability is connected with $n\text{CO}_2$ capture ability in the propanol-rich region

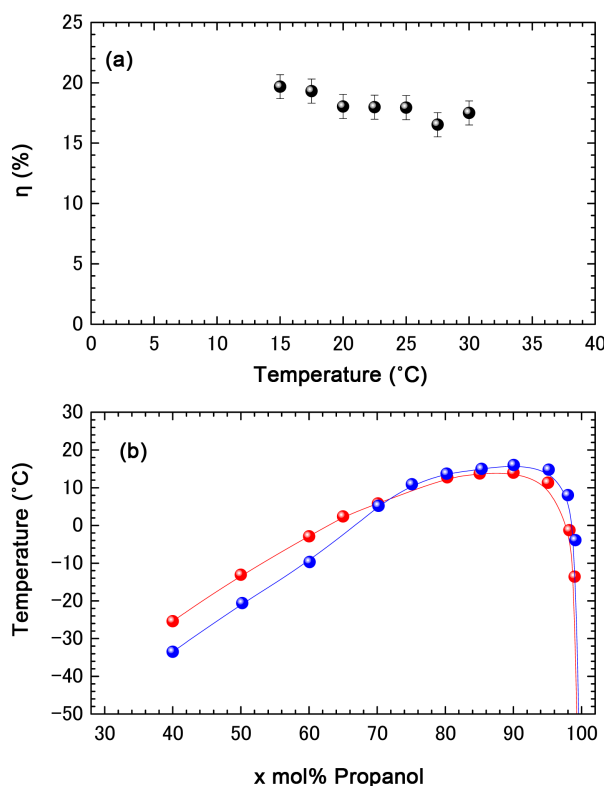


Figure 4. (a) Temperature dependence of $n\text{CO}_2$ molar fraction (η) in [N4111][TFSI]-80 mol% 2-propanol; (b) Phase diagram of the [N4111][TFSI]-propanol system.

(Figure 2). At the UCST, the phase separation behavior could significantly influence the $n\text{CO}_2$ capture. Generally, liquid becomes unstable as a precursor phenomenon close to phase separation. Fluctuations in the propanol concentration in the vicinity of the clouding point were not ignored. Furthermore, UCST and the critical concentration ($x_c = 85$ mol%) in the phase diagram have significant meaning on the UCST [15]. In thermodynamics, fluctuations are critical phenomena that are enhanced at UCST and x_c . In this study, the intrinsic instability of the liquid phase in the RTILs-propanol mixtures became distinct at around x_c . Thus, we deduce that the unstable liquid phase in the propanol-rich region was stabilized by $n\text{CO}_2$ sorption.

3.3. TFSI[−] Conformation and $n\text{CO}_2$ Capture

TFSI[−] conformation stabilities in the RTIL-propanol mixtures were estimated by Raman spectroscopy [15] [17]–[19] [22]. The observed Raman bands were assigned as C_1/C_2 conformers by DFT calculations [18] [22]. As an example, the Raman spectrum of pure [N4111][TFSI] is shown in Figure 5(a). The experimental C_2/C_1 ratio was calculated by decomposing the Raman peaks, and the asymmetric pseudo-Voigt function was used to separate peaks. The highest level of $n\text{CO}_2$ capture for [N4111][TFSI] was obtained at $C_2/C_1 = 0.539$. In contrast to [N4111][TFSI], the C_2/C_1 values of [N1123][TFSI] and [P2225][TFSI], which exhibited poor $n\text{CO}_2$ capture abilities, were 0.853 and 0.869, respectively. For instance, the Raman spectrum of [P2225][TFSI] is displayed in Figure 5(b). Despite pure systems, the C_2/C_1 ratio of TFSI[−] anion is regarded as a good indicator of $n\text{CO}_2$ capture ability, and C_2/C_1 has been used to determine the mixing states of $[\text{C}_n\text{mim}][\text{TFSI}]$ -propanol [15] and -butanol [17]. In both the pure and mixed systems, the TFSI[−] anion conformer indicates energetically stable/unstable states in the liquid state.

DFT calculations are indispensable to interpret experimental results, although DFT calculations provide the molecular-level details on the gas phase. DFT calculations were performed using the Lee-Yang-Pear correlation (B3LYP) with the 6-31++G(d,p) basis set [23] [24] in the PC-GAMESS package [25]. In the DFT simulation box, we introduced the torsion angle (α) of TFSI[−] anion (Figure 6(a)); the geometrical definition of α was provided

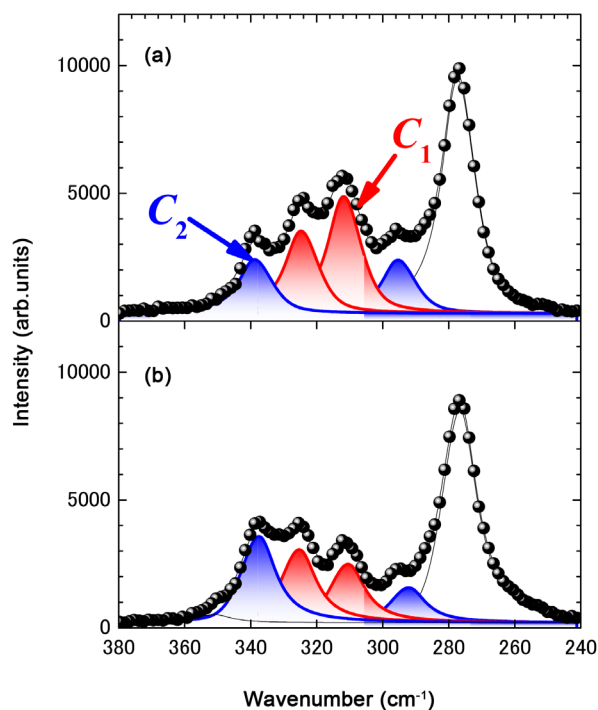


Figure 5. Raman spectrum of (a) pure [N4111][TFSI], and (b) [P2225][TFSI] at room temperature. The decomposed peaks are assigned as C_1 and C_2 conformers of TFSI $^-$.

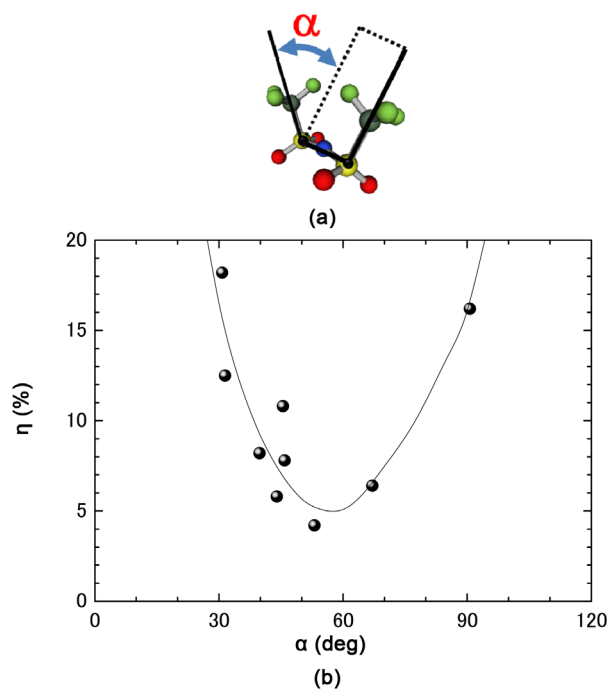


Figure 6. (a) Definition of torsional angle α , (C-S-S-C) in TFSI $^-$; (b) $n\text{CO}_2$ molar fraction (η) as a function of calculated torsion angle.

by the C-S-S-C angle. DFT calculations of the [N4111][TFSI] system were used to examine a relation between a of TFSI $^-$ and molecular configurations of propanol isomer and CO_2 additive (Table 1). The calculated torsion

angle is sensitive to the presence of propanol and its conformation. In pure [N4111][TFSI], $\alpha = 30.756^\circ$; the addition of 2-propanol increased the torsion angle to 72.517° . The effect of 2-propanol on torsion angle was larger than that of 1-propanol. These results are in agreement with previous DFT calculations. The experimentally obtained C_2/C_1 ratio of TFSI⁻ anion is known to reflect the stabilities of the liquid, glass, and solid phases [14] [15] [17] [26]. Thus, increased α in the [N4111][TFSI]-2-propanol mixture has significant implications for liquid state stabilization. The torsional potential of TFSI⁻ anion has two local minima at 80° and 280° [27]. Although the potential calculated between the two minima is relatively low, TFSI⁻ has a higher torsional barrier at approximately 0° (C_1). Hence, in case of the [N4111][TFSI]-2-propanol mixture, 2-propanol causes the TFSI⁻ anion to twist, and stabilizes energetically. In the [N4111][TFSI]-1-propanol system, α cannot reach 70° . The difference in α between the 1- and 2-propanol-based RTILs is directly connected to the propanol isomer effect on $n\text{CO}_2$ capture. To clarify the $n\text{CO}_2$ -driven stabilization in the RTIL-2-propanol systems, we replotted the observed CO_2 capture against the calculated α angle (Figure 6(b)). The most $n\text{CO}_2$ capture in the [N4111]-[TFSI]-2-propanol was observed at $\alpha = 70^\circ$. In contrast, the minimum $n\text{CO}_2$ capture in the [N1123]-[TFSI]-2-propanol system, which is fully stabilized without the addition of 2-propanol, was shifted to lower value of α . The α dependence of η in Figure 6(b) can be explained by assuming that CO_2 compensates for geometrically mismatching of TFSI⁻ conformer and additives in 2-propanol based mixtures.

3.4. Gas Selectivity of [N4111][TFSI]-2-Propanol

For actual applications, the RTIL-propanol mixtures must be gas selective. Figure 7 shows CO_2 , O_2 , and N_2 sorption in the [N4111][TFSI]-80 mol% 2-propanol system at 25°C . N_2 cannot contribute to energetic stabilization in an unstable liquid system in the propanol-rich region. N_2 mostly occupied in the air has the lowest sorption.

Table 1. Calculated torsion angle (α) of TFSI⁻ anion. α is strongly dependent on the presence of propanol and CO_2 .

[N4111][TFSI]	Number of molecules		Type of Propanol	Dipole (Debye)	α (deg)
	Propanol	CO_2			
1	0	0		15.390	30.756
1	0	1		14.983	45.338
1	1	0	1-Propanol	13.456	49.678
1	1	1	1-Propanol	13.014	36.554
1	1	0	2-Propanol	15.615	72.517
1	1	1	2-Propanol	13.589	72.736

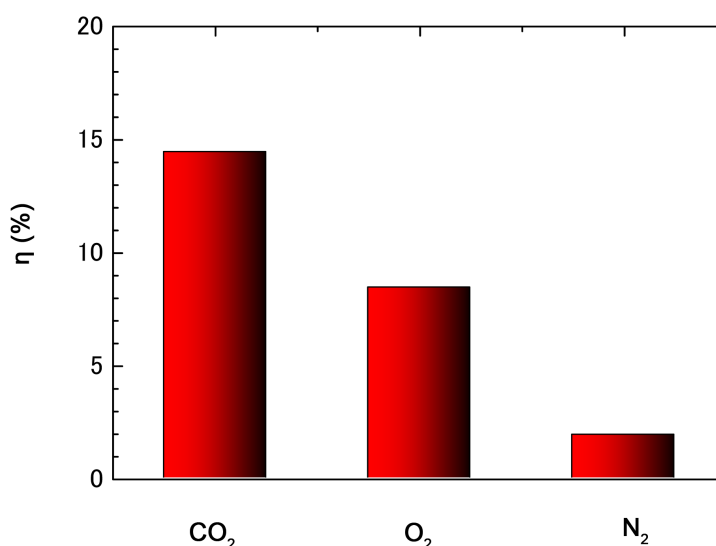


Figure 7. Gas selectivity in [N4111][TFSI]-80 mol% propanol at 25°C .

The gas selectivity in the [N4111][TFSI]-80 mol% 2-propanol system has an advantage for industrial applications. The results clearly show that CO₂ is preferred in the [N4111][TFSI]-2-propanol system. CO₂ selectivity was realized at ambient pressure. CO₂ plays an important role for the high efficient CO₂ capture system, although the mechanism remains unclear.

4. Summary

At ambient pressure and room temperature, *n*CO₂ capture in quaternary ammonium-based RTILs is promoted by the addition of 2-propanol. The propanol isomer effect associated with *n*CO₂ capture is revealed by the lack of enhancement in RTIL with added 1-propanol. The conformation of TFSI⁻ is regarded as a good indicator of *n*CO₂ capture ability, since TFSI⁻ torsion angle is strongly correlated with the amount of *n*CO₂ sorption. The increase in *n*CO₂ sorption in the propanol-rich region is consistent with liquid instability near the UCST, as shown in the phase diagram. The [N4111][TFSI]-2-propanol mixtures provide both high *n*CO₂ capture and gas selectivity.

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