

Conversion of Isopropylbenzene over AISBA-15 Nanostructured Materials

Francine Mota Ribeiro¹, Anne Michelle Garrido Pedrosa², Marcelo José Barros de Souza^{1*}

¹Department of Chemical Engineering, Federal University of Sergipe, São Cristovão, Brazil

²Department of Chemistry, Federal University of Sergipe, São Cristovão, Brazil

Email: *marcelojbs@ufs.br

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Abstract

In this paper we studied the application of a series of AISBA-15 catalysts with different Si/Al ratios on the reaction of conversion of isopropylbenzene. The catalysts were synthesized via hydrothermal method and characterized by nitrogen adsorption at 77 K and Small Angle X-ray Scattering (SAXS). Catalytic tests were accomplished in a continuous flow fixed bed microreactor. The obtained results showed catalytic activity for all AISBA-15 catalysts producing benzene and propene as main products.

Keywords

AISBA-15, Si/Al Ratio, Isopropylbenzene

1. Introduction

Several technological changes have occurred in the petroleum refining industry with the aim of improving the performance of these processes, which highlights the development of catalysts that provide higher activity and selectivity in the conversion of oil derived products with high aggregate value. Mesoporous catalysts of AISBA-15 type show a high degree of accessibility [1], so it has been studied in cracking applications. The catalytic cracking process occurs in the presence of a catalyst which promotes the breaking of a carbon chain from long to smaller molecules, and increases the selectivity to desired products.

AISBA-15 is a mesoporous material derived from SBA-15 (Santa Barbara Amorphous). SBA-15 is a mesoporous silicate which was discovered in the 90s by Zhao and collaborators [1]. These materials have well-defined pore diameter which can be adjusted between 2 and 30 nm, and have very high BET surface area (>500 m²/g), mesopores with hexagonally arranged, large pore wall thicknesses that result in high thermal and hydro-

*Corresponding author.

thermal stability, greater than MCM-41 materials [2] [3]. These characteristics have involved many research fields such as adsorption, catalysis, separation, nanoscience, solid templates for other materials, among others [4].

Catalytic tests in laboratory units are typically carried out using reagent model molecules. In this paper, the isopropylbenzene was selected as model molecule, also known as cumene. This compound, an aromatic hydrocarbon (C₉H₁₂) represents oil fractions. In the catalytic, cracking of cumene typically is expected to obtain an olefin (propylene) and an aromatic (benzene) but depending on the type of catalyst and on the reaction scheme, other side reactions can occur with the obtaining of other products, which may be verified experimentally.

2. Experiment

The AISBA-15 was synthesized by hydrothermal method with different atomic ratios of Si/Al (25, 50 and 75), using as structural template the Pluronic P123, tetraethyl orthosilicate as silica source, pseudoboehmite as aluminum source, hydrochloric acid and distilled water as solvents. These reagents were mixed in order to obtain a hydrogel reactive with the following molar composition: 1.0 TEOS: 0.017 P123: x Al₂O₃: 5.7 HCl: 193 H₂O. Where x is 0.007 (AISBA-15, Si/Al = 75), 0.01 (AISBA-15, Si/Al = 50) and 0.02 (AISBA-15, Si/Al = 25).

The reagents were mixed in order to obtain a hydrogel reactive. First, the template was dissolved on the solvents under stirring and heating at 35°C. Then there was added the required amount of pseudoboehmite (AlOOH) to obtain a Si/Al ratio desired. The silica source was added for last and the mixture was stirred and heated at 35°C for 24 hours to obtain a homogeneous gel. The resultant gel was transferred to an autoclave and conditioned on the oven for 48 hours at 100°C. The resulting products were vacuum filtered and washed with water, after this procedure the material has been placed to dry at room temperature for 24 hours.

The SAXS of the samples were obtained at a scan angle 0° - 5° in an equipment SAXS1 of scattering X-ray small angle of the LNLS—National Laboratory Light Cyclotron in Campinas/SP/Brazil. The experiments were conducted using CuK α radiation. The survey of N₂ adsorption-desorption isotherms of the samples calcined AISBA-15 was performed in a Quantachrome equipment NOVA1200 by nitrogen adsorption at a temperature of 77 K.

The catalytic test was carried out in a fixed bed continuous flow reactor manufactured by Altamira Instruments (BENCHCAT 4000 HP). The tests were conducted using a mass of 200.0 mg of catalyst. Before the start of the reaction the catalysts were activated *in situ* under heating in nitrogen flow of 50 mL/min starting from ambient temperature to the temperature of reaction (350°C or 400°C) under a rate heating of 5°C/min. After reaching the reaction temperature, the reactor was isolated by diverting the flow through the bypass and at that moment the syringe liquid pump was thrown which drove a syringe containing liquid isopropylbenzene by capillary flow lines of the unit. The liquid injected through the syringe (at 50 μ L/min) was continuously vaporized, and being transported by the flow lines in a continuous which were heated at temperature of 200°C. This were mixing with the stream of inert gas (nitrogen) for 10 minutes until the lines could be entirely filled from the mixture, after which time being directed to the reactor in a down flow in a WHSV (Weight Hourly Space Velocity) of 3 h⁻¹. During the catalytic reactions, the reactor effluent gases are injected at time intervals of approximately 3.5 minutes, through a sampling valve Valco 6 pathways in a gas chromatograph equipped with a 6890N Agilent HP-5 column -5% Methyl Phenyl siloxane 30 m. Analysis of the products was performed using a FID detector.

3. Results and Discussion

3.1. Catalyst Characterization

The SAXS analysis of the materials obtained showed the diffraction patterns with reflection peaks in the interval of low Bragg angle (less than 5). According to Zhao [1], three diffraction peaks are observed for SBA-15 materials which are related to the crystal planes, whose Miller indices are (100), (110) and (200). These diffraction lines are associated with a two-dimensional hexagonal symmetry *P6mm* typical of SBA-15 materials [2] [5]. **Figure 1(a)** show the SAXS patterns obtained for AISBA-15 samples with different Si/Al ratios and in the calcined form.

For the AISBA 15 with Si/Al ratio of 25 and 50 were observed a set of diffraction peak in the region of 2θ of 0.5° to 3° which are related to(100) plane and two less intense peaks related to (110) and (200) planes, which indicating a highly ordered hexagonal material. The diffraction intensity of reflection (100) the samples mentioned above indicates that the unit cell dimensions are the same as in material SBA-15 [6]. The sample with

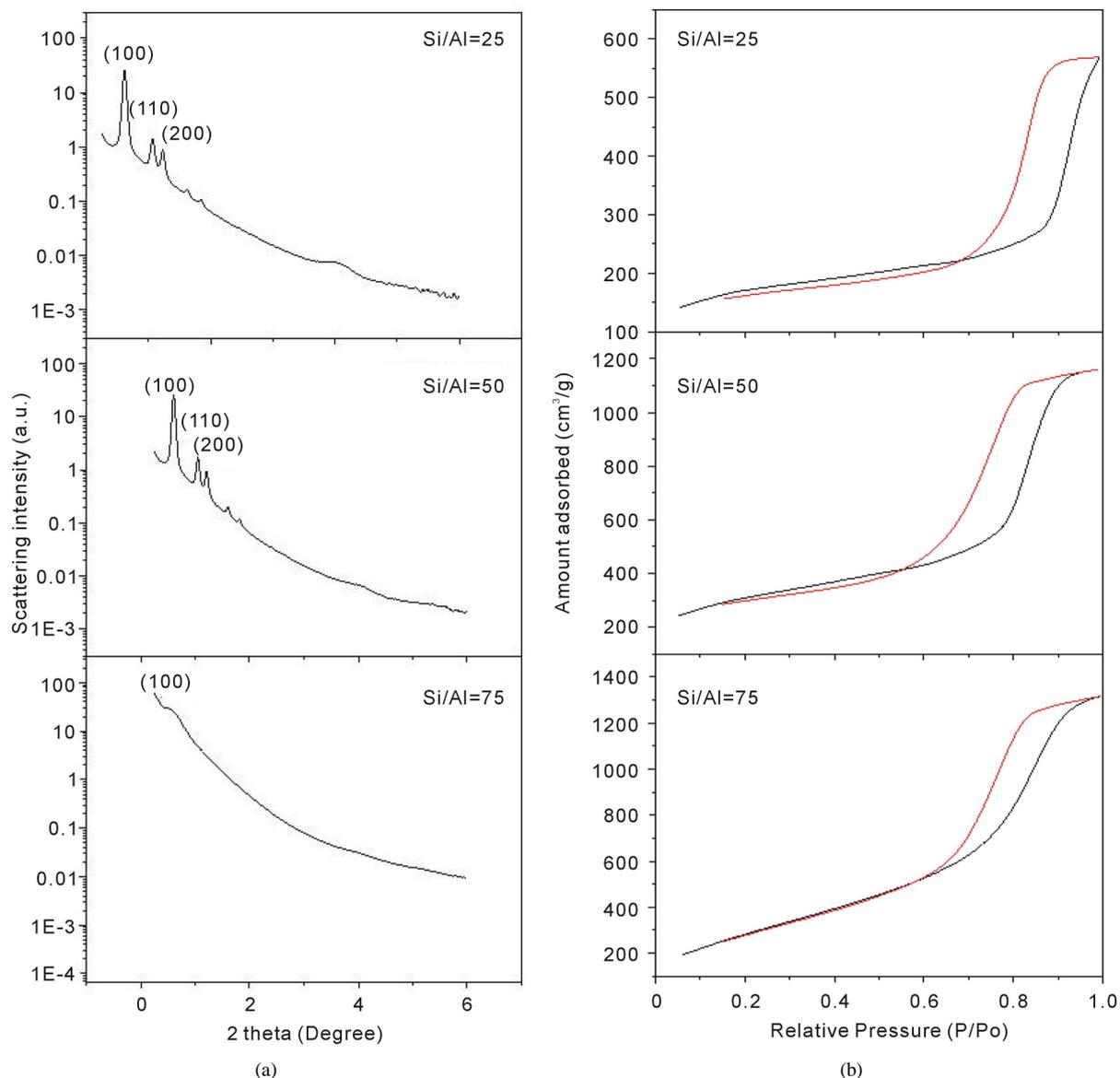


Figure 1. (a) SAXS analysis to the AISBA-15 with different Si/Al ratios and (b) Adsorption-desorption isotherms of N₂ to the AISBA-15 with different Si/Al ratios, where: black line = adsorption and red line = desorption.

Si/Al ratio = 75 no showed no characteristic peak to this material, this means that there was no formation of the structure.

The N₂ adsorption-desorption isotherms obtained for the AISBA-15 with Si/Al ratios of 25, 50 and 75 are shown in **Figure 1(b)**. It can be observed that all samples exhibit adsorption/desorption isothermal of IV type in according to the IUPAC classification. The AISBA-15 samples with Si/Al = 25 and 50 showed a “loop” of hysteresis of type I, which is associated with the porous pellets consisting of hard spherical particles of uniform size ordered regularly [7]. Hysteresis of type I are typical of mesoporous materials, thus showing that the samples AISBA-15 with ratios Si/Al = 25 and 50 have mesoporous structure [4] [8]. The profiles of adsorption of each isotherm show a sharp increasing of the N₂ adsorbed in the range of relative pressure of 0.6 to 1.0. This suggests that the materials are very regular mesoporous channels with a narrow pore size distribution of gaussian [4] [8]. The position of the inflection points of P/Po is related to the pore size [4]. The hysteresis loop at a P/Po > 0.8 is corresponding to the inter particle capillary condensation in the pores and due to the presence of certain phases of impurities [8]. **Table 1** shows the results of the textural characterization of the AISBA-15 samples with ratios

Si/Al = 25 and 50.

3.2. Catalytic Properties

The catalytic conversion of isopropyl benzene was performed at two temperatures (350°C and 400°C) in order to verify the effect of the temperature in the reactions. **Figure 2(a)** and **Figure 2(b)** shows the values of conversion as function of reaction time for different Si/Al ratios at 350°C and 400°C, respectively. At all reaction times it was observed that the conversion it was higher in temperature of 400°C than in the temperature of 350°C in the sample with Si/Al = 25. At 400°C the conversion increased slightly as a function of reaction time and after 10 minutes the conversion stabilizes. This may be related to the deposition of coke on the surface of the material. At 350°C the conversion is maintained stabilized during the reaction time studied. Deactivation at high temperatures is common for this type of reaction where the continuous deposition of coke can inhibit the reaction. The influence of catalyst to oil ratio (C/O) in the conversion shows a similar behavior, where by analyzing the initial five minutes of reaction, it is observed that by increasing the catalyst mass, reach a maximum conversion of C/O of 2.5 and 1.3, at temperatures of 400°C to 350°C, respectively. The same is observed with temperature, and as expected for this endothermic reaction that at low pressure, in the ideal gas state, increasing the temperature favors the conversion. The parameter C/O becomes very important, because although it estimated at fixed bed conditions, is one of the commonly measured parameters during the catalytic cracking in fluidized bed reactors, where the load in a given C/O ratio is cracked in the “riser” of FCC unit, giving the idea of the proportions of catalyst and oil used for the maximization of the conversion in each fluidized bed catalytic cycle.

For AISBA-15 catalyst with Si/Al = 50, conversion to 350°C remained relatively constant with flow time, indicating no apparent deactivation in the range examined. In this sample, the conversion at 400°C was low compared to the conversion at temperature of 350°C. The drastic reduction of the conversion seen during the initial phase of the reaction indicated rapid coke formation, which occurs on the catalyst surface. Thus, in this reaction, the decrease in conversion to the long reaction time may be due to fast blockage of acid sites by the coke formed during the reaction. The same also occurred with respect to C/O ratio, which show the conversion profile as a function of the C/O ratio to the catalyst AISBA-15 with Si/Al = 50 with opposite behavior in comparison with AISBA-15 with Si/Al = 25. The temperature of 350°C showed higher conversion rates in function of C/O ratio. But this data is consistent to that found in relation to the greater catalytic activity of the AISBA-15 sample with Si/Al = 50 at 350°C. For this sample, in both cases (temperatures of 350°C to 400°C), the best C/O ratio was about 2. For the AISBA-15 catalysts, through gas chromatography was observed the formation of benzene and propene as reaction products.

To the catalyst AISBA-15 with Si/Al = 75 the conversion of ca. 1% to 5% were observed in the studied expe-

Table 1. Textural properties of the AISBA-15 samples.

Samples	$S_{A_{BET}}$ ($m^2 g^{-1}$)	V_p ($cm^3 g^{-1}$)	$D_{p_{BET}}$ (nm)	Wt (nm)
AISBA-15 (25)	555	0.9	12.5	4.3
AISBA-15 (50)	1046	1.8	8.8	7.9

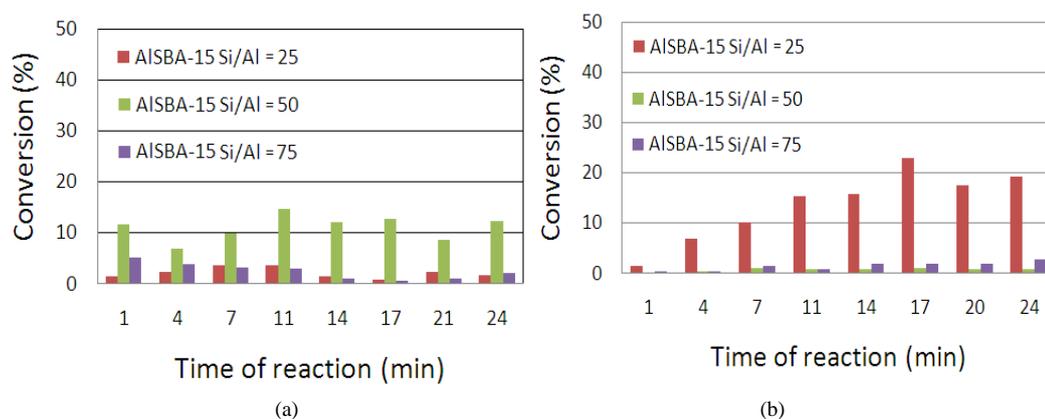


Figure 2. Conversion as function of reaction time for different Si/Al ratios: (a) at 350°C and (b) at 400°C.

perimental conditions. This is attributed to the high Si/Al ratio, thus making the material potentially less acidic to cracking. In this sample was not observed too the SBA-15 structure, as evidenced by SAXS analysis (**Figure 1(a)**). According Trejo [9], silica-alumina prepared by sol-gel method can produce a larger quantity of Brönsted acid sites most likely due to the homogeneity of Al atoms in the silica network by which is PEO the ability to generate more Brönsted acid sites on the surface of silica-alumina by forming hydrogen bonds with the silica during the sol-gel reactions. It has been reported that the oxygen atoms in the PEO can be coordinated with cations Al^{3+} and probably coordination affects the homogeneity on silica-alumina and the local structure of aluminum networks silica which promote the generation of a greater number of Brönsted acid sites. Thus, the method of preparation of the catalyst directly influences the amount of acidic sites present in the catalyst and its catalytic behavior consecutively.

4. Conclusion

AlSBA-15 catalysts were satisfactorily synthesized via hydrothermal method. The characterizations via nitrogen adsorption and SAXS evidenced that samples with Si/Al of 25 and 50 presented highly ordered structure with surface area in the range of 555 to 1046 m²/g. Catalytic cracking of isopropyl benzene was studied on nanostructured materials such AlSBA-15 at different Si/Al ratios. During the reactions the formation of benzene and propene from direct cracking of isopropyl benzene model molecule was observed.

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