# Halloysite Nanotubes Supported Gold Catalyst for Cyclohexene Oxidation with Molecular Oxygen

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#### Abstract

The selective oxidation of cyclohexene to 2-cyclohexene-1-ol and 2-cyclohexene-1-one has been investigated over Au/HNTs (HNTs: halloysite nanotubes) catalysts with molecular oxygen in a solvent-free system. The catalysts were prepared by deposition precipitation method and characterized by ICP-AES, TEM and XRD. The results show that the catalytic performance of Au/HNTs is quite well and the catalytic activity over recycled catalyst remains highly. Moreover, the nano-size effect of gold is also reported for the reaction.

Keywords: Gold Catalyst, HNTs, Cyclohexene Oxidation, Oxygen

# 1. Introduction

The catalytic oxidation of hydrocarbons into value-added oxygenated derivatives is still a challenge in modern chemistry and industry world [1-3]. In particular, the oxidation of cyclohexene is often inefficient as there is a C = C bound and four  $\alpha$ -H atoms in the cyclohexene molecule. Oxidation of cyclohexene is an important method for the synthesis of chemical intermediates like 2-cyclohexene-1-ol and 2-cyclohexene-1-one in the manufacture of high-value pharmaceuticals [4]. A greater demand for these oxidation products and increased enviromental concerns warrant the introduction of catalytic systems using heterogeneous catalyst and the environmentally friendly oxidants such as molecular oxygen or hydrogen peroxide [5]. The use of  $H_2O_2$  is atom efficient and the only by-product is water, but the relatively high cost of H<sub>2</sub>O<sub>2</sub> severely hinders its wide application in catalytic oxidation [6]. On the other hand, catalytic systems using oxygen as the oxidant instead resulted in three important advantages: the facility to separate the catalyst after the reaction, lower energy costs and a higher stability of the irreversible reaction of overoxidantion products [7,8]. Therefore, oxidation of cyclohexene with oxygen under solvent-free condition would be valuable.

In recent years, an increasing interest has been directed to the catalytic potential of gold catalysts [9-12]. Supported gold catalysts have been extensively studied for a wide range of oxidation reactions including CO oxidation [13], propylene epoxidation [14], the direct synthesis of hydrogen peroxide from oxygen and hydrogen [15,16], oxidation of cyclohexane to KA oil [17-19], etc.. Particularly, the partial liquid-phase cyclohexene oxidation using gold catalysts including Au/C and Au/CNTs makes gold even more attractive [20,21]. Unfortunately, as for the Au/C catalyst, it has good catalytic performance only with the addition of special organic solvent [20]. The performance of Au/CNTs catalyst is influenced by the amount of TBHP [21]. Compared Au/C and Au/CNTs, we can see that the structure of the carrier has great effect on the catalytic performance of supported gold. As silica and Al<sub>2</sub>O<sub>3</sub> are quite common industrial materials as catalysts support material because of their relative stability, high surface area and low price. Au/Al<sub>2</sub>O<sub>3</sub> and Au/SiO<sub>2</sub> are quite effective in cyclohexane oxidation [8,22], but there is little report about aluminosilicate-supported Au catalyst. HNTs (halloysite nanotubes) is a special kind of aluminosilicate. The objective of this work is to report catalyst Au/HNTs of very low metal loadings and the effect of nano-size of gold on catalytic performance for the selective oxidation of cyclohexene using molecular oxygen in a solvent-free system.

## 2. Experimental

Au/HNTs catalysts with varied gold loadings were pre-



pared by the deposition-precipitation procedure. 2.0 g HNTs support was stirred in 0.5 mmol·L<sup>-1</sup> HAuCl<sub>4</sub> aqueous solution for 1 h at 60°C. The pH of the slurry was kept at 10 adjusted with 4.0 mol·L<sup>-1</sup> ammonia solution. After filtration, the resulting solid was washed twice using 20 mL of deionized water for each wash to remove Cl<sup>-</sup> ion. Finally, the resulting solid was dried at 80°C overnight and calcined at 300°C for 3 h, Au/HNTs was obtained.

The chemical compositions of the samples were determined by ICP-AES (IRIS Intrepid II XPS). 0.1 g of the solid samples was leached by 4 mL of aqua regia for 4 h and the leaching liquid was collected for determining gold. The specific surface areas were obtained by the Brunauer-Emmett-Teller (BET) method using an Autosorb-1-C instrument. A D/max-RA instrument with CuK $\alpha$  radiation with a beam voltage of 40 kV and a beam current of 40 mA was used to collect the X-ray data. Transmission electron microscopy (TEM) images were obtained on a JEM-1230 at 80 kV. The samples were dispersed in ethanol and then dropped on copper-coated grid. The gold particle size distribution was obtained by measuring the diameter of metal particles.

The catalytic experiments for cyclohexene oxidation were carried out in a PTFE-lined autoclave (Capacity = 30mL, pressure maximum 6 MPa). In a typical oxidation reaction, 20 ml cyclohexene and 0.20 g catalyst were placed into the autoclave. The reactor was then heated to the desired reaction temperature in oil bath under constant stirring with a magnetic stirrer. After the reaction was over, the reactor was cooled to room temperature and the liquid phase was separated from the reaction slurry. The solid catalyst was washed by acetone and dried at 80°C for 3 h. Reactants and products were identified by gas chromatography-mass spectroscopy (GC-MS) as well as by comparing retention time to respective standards in GC traces. GC analyses were done using a GC 1690 instrument with a flame ionization detector (FID). The column used was an SE-54 capillary column (30 m  $\times$  0.32 mm  $\times$  0.5  $\mu$ m). N-Heptane was used as an internal standard for product analysis.

### 3. Results and Discussion

#### 3.1. Catalyst Characterization

The actual gold contents and specific surface areas of samples were shown in **Table 1**. With the increase of gold loadings, the specific surface area of Au/HNTs catalysts differs only slightly, which means loading gold has little effect on that.

Figure 1 gives the XRD patterns of the HNTs, Au(0.37%)/HNTs, Au(0.80%)/HNTs and Au(1.35%)

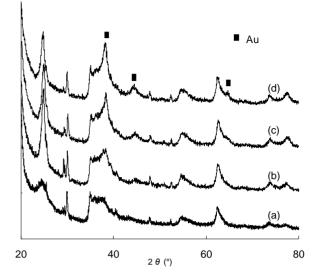


Figure 1 XRD patterns of HNTs (a), Au(0.37%)/HNTs (b), Au(0.80%)/HNTs (c), Au(1.35%)/HNTs (d).

Table 1. Au content, specific surface area of HNTs and supported gold catalysts.

Samples	Au content	SBET	
Samples	Theoretical	Actual	$(m^2 \cdot g^{-1})$
HNTs	—	—	60
Au/HNTs	0.5	0.37	57
Au/HNTs	1.0	0.80	58
Au/HNTs	1.5	1.35	58

/HNTs, respectively. The typical signals of gold at 38.19°, 44.42° and 64.57° were observed and became more obvious in steps from **Figure 1 (b-d)**, which indicated that the particle size of gold increased according to the increasing of gold content of the catalyst.

**Figure 2** shows the typical TEM images of supported Au/HNTs catalysts and the black round dots in the images are gold particles. Although gold is unevenly distributed and the particle size is discrepancy in the same sample, it is easy to see that as the gold loading changes from 0.37% to 1.35%, the gold particles become bigger, agreeing well with the results of **Figure 1**, which means the gold loading greatly affects the particle size.

#### 3.2. Catalytic Oxidation of Cyclohexene

In preliminary experiments, an uncatalyzed oxidation reaction was carried out under the typical reaction conditions as shown in **Table 2** (Entry 1). There were four main products could be obtained: cyclohexene oxide, 2-cyclohexene-1-ol, 2-cyclohexene-1-one and cyclohexane-1, 2-diol, and their selectivity was 8.1%, 15.4%, 21.7% and 23.1% respectively. Moreover, the activity of pure HNTs support was also studied under the same conditions (**Table 2**, Entry 2). Compared with uncata-

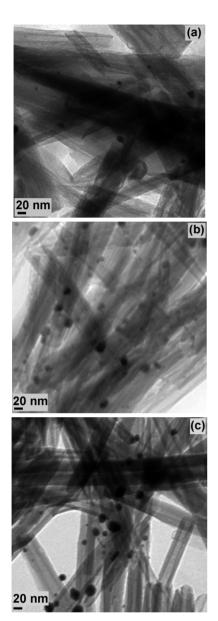


Figure 2. TEM images of Au/HNTs catalysts of (a) 0.37%, (b) 0.80%, (c) 1.35% Au.

Table 2. Effect of Au loadings on catalytic performance in cyclohexene oxidation<sup>a</sup>.

Catalyst	Conver- sion (%)	Selectivity (%)			
(wt.% Au)		Cy-oxide	Cy-ol	Cy-one	Cy-ol + Cy-one
No <sup>b</sup>	12.1	8.1	15.4	21.7	37.1
HNTs	16.9	6.5	29.8	43.4	73.2
Au/HNTs (0.37% Au)	25.9	4.0	32.5	46.9	79.3
Au/HNTs (0.80% Au)	29.5	3.5	35.5	49.0	84.5
Au/HNTs (1.35% Au)	21.2	4.1	34.3	48.0	82.3

<sup>*a*</sup> All reactions were done with 0.20 g of catalyst, 20 mL cyclohexene, at 80°C, 12 h, and the pressure of oxygen is 0.4 MPa. <sup>*b*</sup> The selectivity of cyclohexane-1,2-diol is 23.1%.

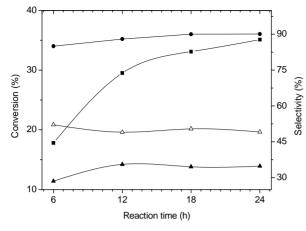
lyzed reaction, conversion of cyclohexene increased 4.8% over HNTs while the distribution of product changed a lot. No cyclohexane-1,2-diol was detected in the product as the selectivity of 2-cyclohexene-1-ol and 2-cyclohexene-1-one increased to 29.8% and 43.4% respectively.

The catalytic performance of Au/HNTs catalysts with different gold loadings was investigated for cyclohexene oxidation using molecular oxygen as an oxidant in a solvent-free system (Table 2). In this work, the best catalytic performance is Au(0.80%)/HNTs, which presents a conversion of 29.5%, a little better than Au(0.37%)/HNTs. As gold content increased from 0.80% to 1.35%, a sharp decrease of cyclohexene conversion is evident. This phenomenon may result from the different quantities of active sites of the catalysts. There existed an apparent nano-size effect of gold in cyclohexene oxidation. From the TEM images, we can see that the gold particles grow bigger as the gold content increasing. The particle sizes of Au(0.37%)/HNTs are <10nm, Au(0.80%)/ HNTs are < 20nm, Au(1.35%)/HNTs are 20~40 nm. There are much more gold particles smaller than 10 nm of Au(0.80%)/HNTs comparing with Au(0.37%)/HNTs and Au(1.35%)/HNTs, and the Au(0.80%)/HNTs has better catalytic performance. Therefore, we infer that the gold particles < 10nm could be more active.

As Au/HNTs (0.80% Au) shows the best results with respect to the conversion and the selectivity to the two desired oxygenates, it is employed to investigate the progress of the reaction with time under the typical conditions. As shown in **Figure 3**, the oxidation of cyclohexene make a large progress from 6 h to 12 h, affording a conversion of 29.5% and 84.5% selectivity to the two desired oxygenates at 12 h. It is also evident that the oxidation reaction gradually slowdowns with time, suggesting a gradual loss of catalytic activity of the catalyst. We believe this could be ascribed to a strong affinity of HNTs with the products formed increasing in the reaction, through which the adsorption of apolar cyclohexene on the catalyst can be suppressed.

Recycling tests were performed using Au/HNTs (0.80% Au) under the typical reaction conditions for 12h, and the results are given in **Figure 4.** Both the conversion and the overall selectivity to two oxygenates are well retained with a slightly enhanced selectivity to 2-cyclohexene-1-one and a little decreased selectivity to 2-cyclohexene-ol, suggesting a high stability of the catalyst.

In order to explain how the oxidation was occurred, and how the major products were formed, we also speculated the oxidation mechanism. The oxidation of cyclohexene with molecular oxygen initially formed 2-cyclohexene-1-hydroperoxide [23,24]. 2-Cyclohexene-



18

Figure 3. Cyclohexene oxidation over Au/HNTs (0.80% Au) with different reaction time. ( $\Box$ Cyclohexene,  $\bullet \sum C_6$ ,  $\triangle 2$ -cyclohexene-1-ol,  $\triangle 2$ -cyclohexene-1-one).

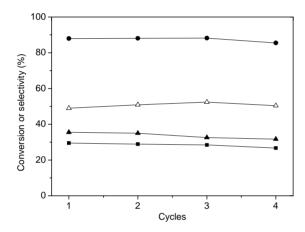


Figure 4. Results of recycling test over Au/HNTs (0.80% Au). ( $\square$ Cyclohexene,  $\bullet \sum C_6$ ,  $\triangle 2$ -cyclohexene-1-ol,  $\triangle 2$ -cyclohexene-1-one).

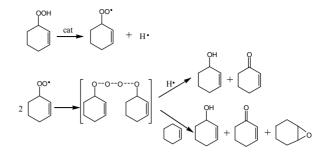
1-hydroperoxide was unstable and easily formed other products as shown in **Scheme 1**.

## 4. Conclusions

In summary, halloysite nanotubes supported gold catalysts have been prepared successfully by the deposition-precipitation procedure. The nano-size effect of gold was found in the reaction. The results show that Au/HNTs catalysts with the gold particles smaller than 10 nm are highly active for the selective cyclohexene oxidation to 2-cyclohexene-ol and 2-cyclohexene-one under relatively mild conditions.

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Scheme 1. Radical-chain sequence mechanism of 2-Cyclohexene-1-hydroperoxide to form other products.

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