

# Analysis of a Coffee Husk Fired Cogeneration Plant in South Western Ethiopia Coffee Processing Industries

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## Abstract

Nowadays our energy needs have grown exponentially corresponding with human population growth and technological advancement. Energy consumption linked to non-renewable resources contributes to greenhouse gas emissions and enhances resource depletion. Most of the researchers were proven that the worldwide concern about CO<sub>2</sub> emissions and the reduction in the use of coal fuels have increased the interest in using biomass fuel for electricity production, because there is no net increase in CO<sub>2</sub> emissions from biomass (agricultural residues such as straw, bagasse, coffee husk, and rice husks) combustion. Furthermore, coffee husk which has high energy potential was not taken into account for the generation of energy. However, this paper investigates the energy generation in coffee husk, and suggests coffee husk is an energy source. The datum was collected from the south western region of Ethiopia (Tepi town), and its equipment was selected. Coffee husk was tested experimentally in Addis Ababa University with Eager 300 software for running the equipment, storing the data and analyzing. The results obtained that calorific values were 18.98 MJ/kg. Overall the result demonstrates that the proposed coffee husk has high energy potential for the generation of energy.

## Keywords

Coffee Husk, Cogeneration, South Western Ethiopia

## 1. Introduction

Cogeneration or Combined Heat and Power (CHP) is the production of two different forms of useful energy from a single primary energy source, typically mechanical energy and thermal energy. The mechanical energy may be used to

drive an alternator for producing electricity or rotate equipment such as motor, compressor, pump or fan for delivering various services. Thermal energy can be used either for direct process applications or for indirectly producing steam, hot water, hot air for the dryer or chilled water for process cooling. According to the Second Law of Thermodynamics, the plant gives back heat to a cold sink before rejecting the remaining heat to the environment at the reference temperature ( $T_0$ ). A cogeneration plant system can operate at efficiencies greater than those achieved when heat and power are produced in separate or distinct processes (Wakui & Yokoyama, 2011; Bapat, Kulkarni, & Bhandarkar, 1997; Hall, Rosillo-Calle, & Woods, 1991). Cogeneration plant may use different forms of primary energy sources (renewable or non-renewable), among these energy sources biomass is the one. It is the third largest renewable primary energy resource in the world, after coal and oil (Werthera, Saengera, Hartgea, Ogadab, & Siagib, 2000). In all its forms, biomass currently provides about 1250 million TOE (Tons of Oil Equivalence) which is about 14% of the world's annual energy consumption. Biomass is a major source of energy in developing countries, where it provides 35% of all the energy requirements (Strehler & Stuetzle, 1987; Gemechu, 2009; Wiersum, Gole, Gatzweiler, Volkmann, Bognetteau, & Wirtu, 2008). The worldwide concern about CO<sub>2</sub> emissions and the reduction in the use of coal fuels have increased the interest in using biomass fuel for electricity production, because there is no net increase in CO<sub>2</sub> emissions from biomass combustion (Pandey, Soccol, Nigan, Brand, Mohan, & Rovossos, 2000). Biomass materials with high energy potential include agricultural residues such as straw, bagasse, coffee husk, rice husks, as well as residues from forest related activities such as wood chips, sawdust, bark and so forth (Murthy & Naidu, 2012; FAU-14, 1986; Franca & Oliveira, 2009).

From the above papers, we can infer that the presented paper considered the generation of energy based on different types of renewable or non-renewable energy sources. The paper's results were shown good for different types of renewable or non-renewable energy sources. However, coffee husk which has high energy potential was not taken into account for the generation of energy. In the end the results obtained that calorific values were 18.98 MJ/kg, maximum temperature of the furnace attained from the energy balance, based on this value inside the combustion chamber was 1489°C, and the amount of air required per kg of coffee husk was 5.45 kg. The remaining part of this paper is organized as follows: Section 2 describes data collection and interpretation of coffee husk. The experimental analysis of coffee husk and its equipment selection is carried out in Section 3. Section 4 presents the result and discussion. The conclusion of the work will be presented in Section 5.

## 2. Data Collection and Interpretation

From the data shown in Figures 1-3 and Table 1 & Table 2, the average annual collected coffee and provide to the industries will be as follows (World Bank, 1986):

average annual collected coffee

$$= \frac{(29039.72 + 18949.29 + 24159.79 + 38641.65 + 16981.08 + 29742.31 + 32037.29 + 30795.86)}{8}$$
$$= \frac{220346.99}{8} = 27543.37 \text{ Ton}$$

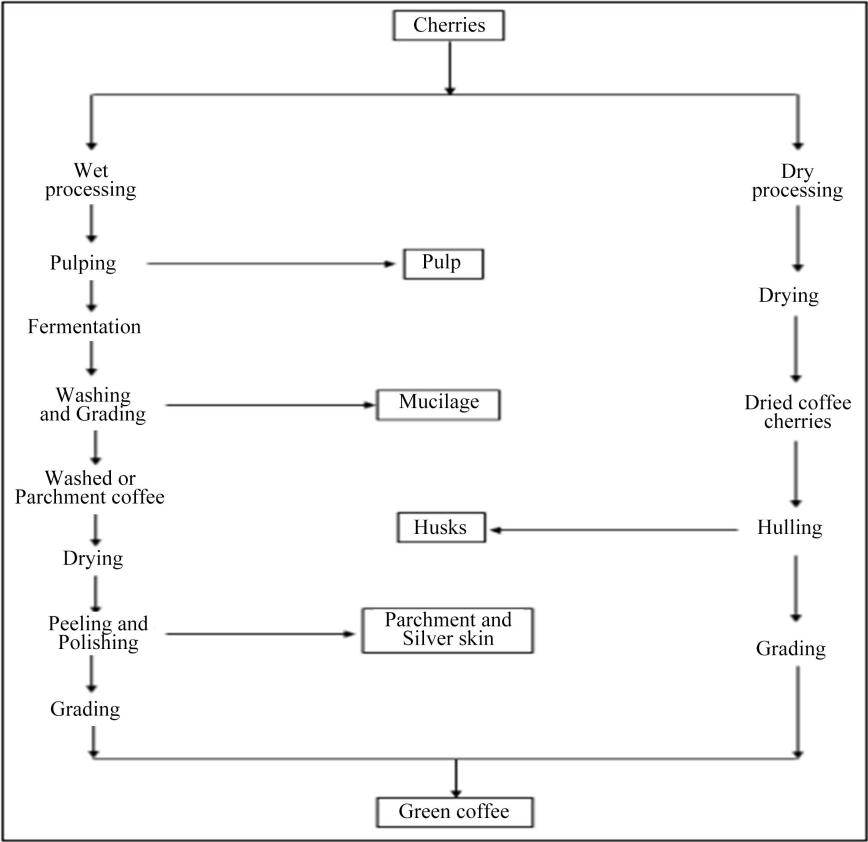


Figure 1. Flowchart of coffee processing.

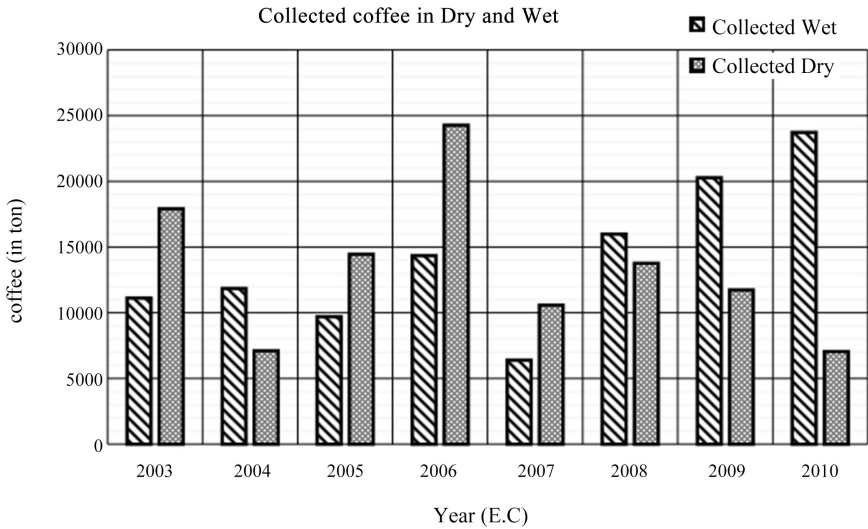
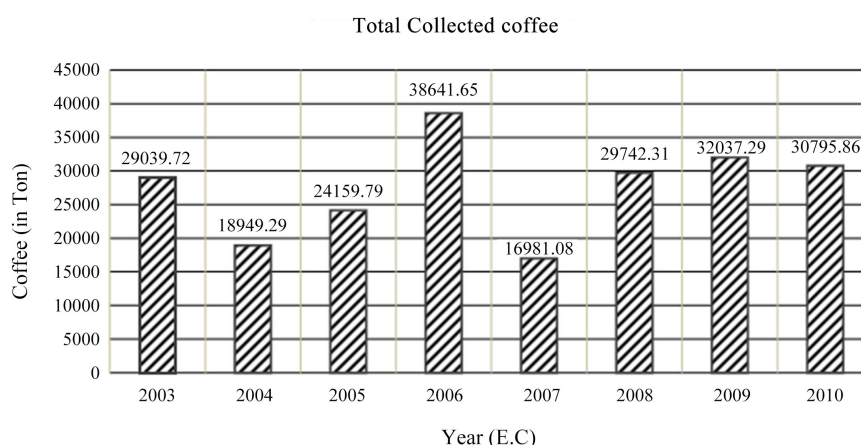


Figure 2. Coffee collected in dry and wet.



**Figure 3.** Total collected coffee in the Zone.

**Table 1.** Coffee collected and generated from the factories from 2003-2010 (E.C) [in Ton].

Year Kind	2003	2004	2005	2006	2007	2008	2009	2010
Washed coffee	2225.55	2369.28	1941.09	2870.33	1600.33	2714.56	2649.64	3637.36
Unwashed coffee	5970.74	5100.03	7127.17	10,742.58	6167	8760.59	5728.03	4380.75
Collected wet	11,127.50	11,846.45	9705.45	14,351.65	6401.32	15,978	20,298.09	2340.63
Collected dry	17,912.22	7102.84	14,454.34	24,290	10,579.76	13,764.31	11,739.20	7055.23

**Table 2.** Total collected coffee in the Zone [in Ton].

Year Kind	2003	2004	2005	2006	2007	2008	2009	2010
Collected Wet coffee	11,127.5	11,846.45	9705.45	14,351.65	6401.32	15,978	20,298.09	23,740.63
Collected dry coffee	17,912.22	7102.84	14,454.34	24,290	10,579.76	13,764.31	11,739.2	7055.23
Total	29,039.72	18,949.29	24,159.79	38,641.65	16,981.08	29,742.31	32,037.29	30,795.86

To know the average coffee husk generated in this region, we face difficult problems, since there was no information about the coffee husk that generated as waste from the industries. We manually tried to know the amount of husk out of one quintal of dry coffee by measuring each product (pure coffee, husk, outer skin of the coffee and other foreign bodies) of the machine with help experienced worker, dry coffee processing industry for 10 working days.

From **Table 3**, it is possible to estimate the average amount of coffee husk per 100 Kg (Adams & Dougan, 1987).

$$\frac{(37 + 35 + 42 + 33 + 36 + 34 + 40 + 37 + 31 + 41)}{10} = \frac{366}{10} = 36.6 \text{ kg}$$

**Table 3.** Estimation of average coffee husk generated from 100 kg of dry coffee.

Weight [kg] Item	Day 1	Day 2	Day 3	Day 4	Day 5	Day 6	Day 7	Day 8	Day 9	Day 10
pure coffee	42	44	39	44	40	40	37	41	45	37
Coffee Husk	37	35	42	33	36	34	40	37	31	41
outer skin	14	12	8	10	15	16	18	15	13	14
Others	7	9	11	13	9	10	5	7	11	8

Therefore, during coffee process ~36.8% will be coffee husk the rest 63.2% will be pure coffee and other byproducts.

So the coffee husk generated from the industries per year will be:

$$\frac{(27543.37 \times 36.8)}{100} = 10135.96 \text{ Ton/Year}$$

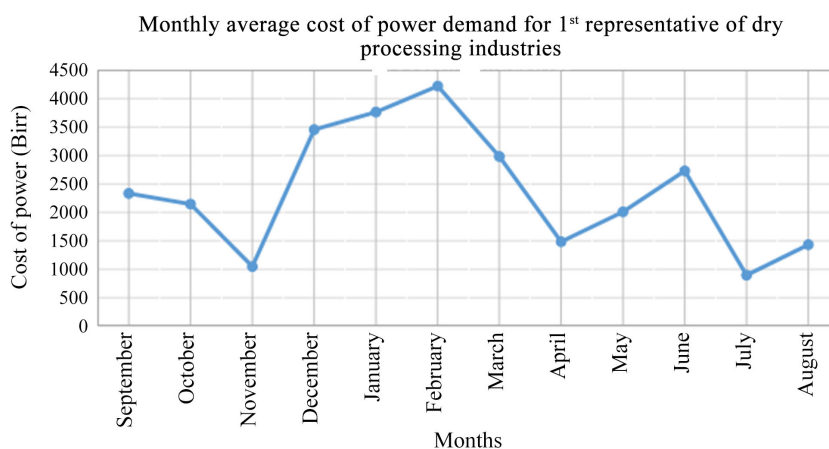
There are 44 wet and 27 dry coffee processing industries are founded in the region, these dry coffee processing industries use electric power for their respective pulping machines. The power estimations were depicted as in **Figures 4-9**.

### 3. Experimental Analysis of Coffee Husk and Its Equipment Selection

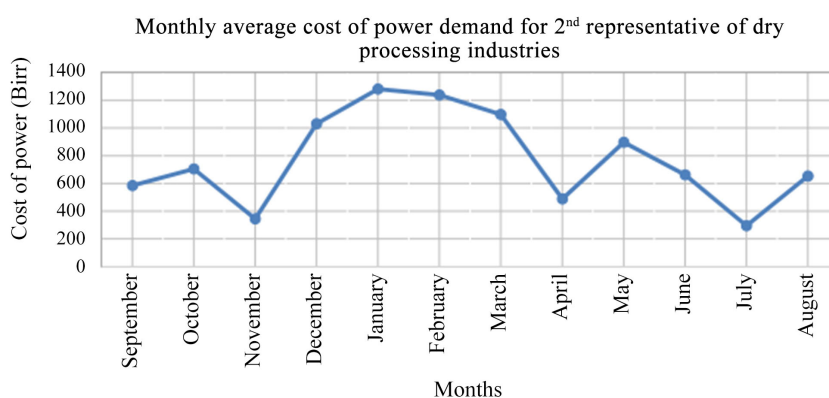
The experiments were conducted using the facilities in Addis Ababa University and Geological Survey of Ethiopian using some sample of coffee husks which came from one coffee processing factory available in the region. The proximate and ultimate analyses of the husk were done using standard ex-periodontal procedures. In order to obtain information about the combustion mechanisms of the coffee husks. Proximate analysis is used to characterize the coffee husk in order to measure its moisture, volatile matter, fixed carbon, and ash contents. Ultimate analysis gives the actual chemical composition (usually C, H, N, S and O by difference) (Musebe, Agwenanda, & Mitiku, 2007) (**Figure 10**).

During sample preparation for the CHNS analysis 5 mg dried and crushed sample is mixed with an oxidizer (vanadium pentoxide [ $V_2O_5$ ]) catalyst in a tin capsule, which is then combusted in a furnace temperature of 900°C and oven temperature of 75°C with a condition of carried gas flow rate of 120 ml/min, reference flow rate 100 ml/min and oxygen flow rate 250 ml/min. The addition of the  $V_2O_5$  ensures complete conversion of inorganic sulfur in the sample to sulfur dioxide. Then combustion products  $CO_2$ ,  $SO_2$ ,  $H_2O$  and  $NO_2$  are carried by a constant flow of carrier gas (helium) that passes through a glass column packed with an oxidation catalyst of tungsten trioxide ( $WO_3$ ) and a copper reducer both kept at 900°C. At this temperature, the nitrogen oxide is reduced to  $N_2$  and oxidation is completed. The gas mixture  $N_2$ ,  $CO_2$ ,  $H_2O$  and  $SO_2$  are then transported by the helium to chromatography column, where separation takes

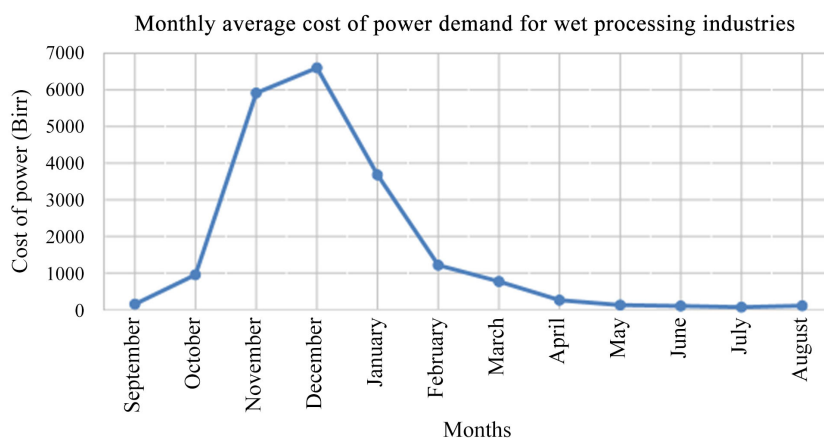
place. After separation eluted gases are sent to the thermal conductivity detector (TCD) (set at 290°C.) where electrical signals processed by the Eager 300 software provide percentages of nitrogen, carbon, hydrogen, and sulfur contained in the sample. Eager 300 software is used for running the equipment, storing the data and analyzing (Kumar, Baah, Pozo, Kufa, Zeleke, & Okwadi, 2002).



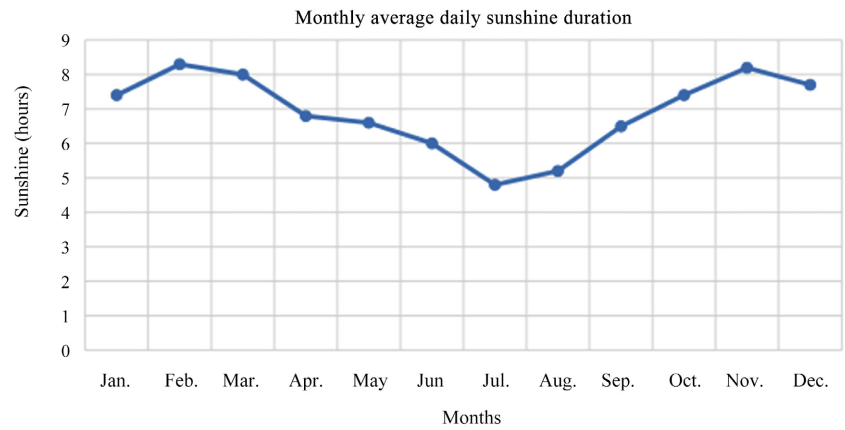
**Figure 4.** Average cost of power for dry processing 1.



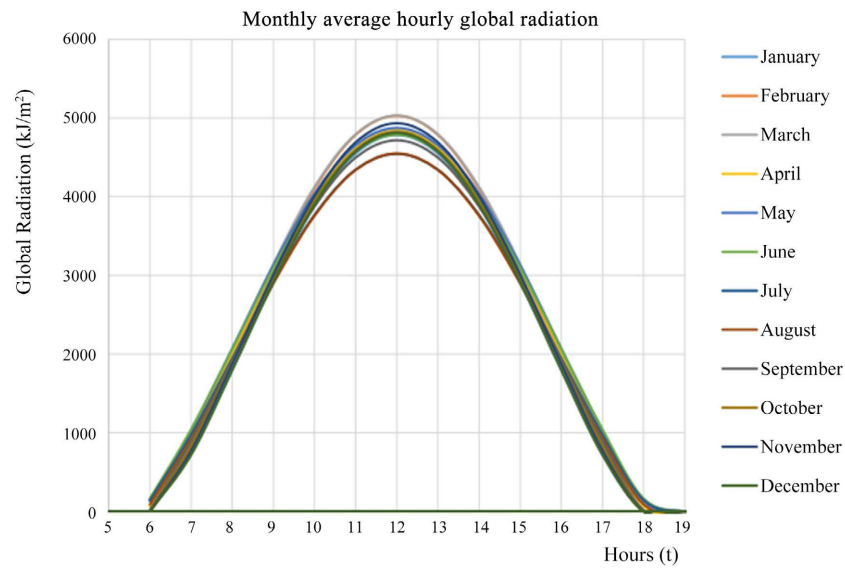
**Figure 5.** Average cost of power for dry processing 2.



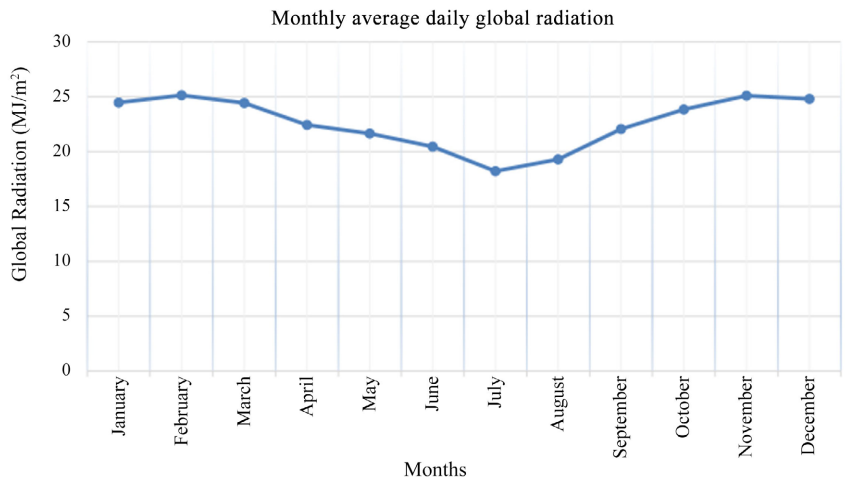
**Figure 6.** Average cost of power for wet processing.



**Figure 7.** Monthly average daily sunshine duration for Tepi.



**Figure 8.** Monthly average hourly global radiation on the horizontal surface for Tepi town.



**Figure 9.** Monthly averages of daily global radiation on the horizontal surface for Tepi town.



**Figure 10.** Flash CHNS/O-analyzer.

### 3.1. For Laboratory Elemental Analysis of the Coffee Husk (CTA, 1999)

$$\text{for carbon } C_d = C_{ad} \left( \frac{100}{100 - M_{ad}} \right)$$

$$\text{for Nitrogen } N_d = N_{ad} \left( \frac{100}{100 - M_{ad}} \right)$$

$$\text{for Hydrogen } H_d = H_{ad} \left( \frac{100}{100 - M_{ad}} \right)$$

where:  $d$  = the dry basis;

$ad$  = as determined basis;

$M_{ad}$  = the moisture content of the general analysis sample when analyzed. During the calibration process six points for every component are taken and the sample was run in duplicate finally the average values to be taken are as in **Table 4**.

### 3.2. For Proximate Analysis of the Coffee Husk

Proximate analysis helps to assess the percentage of volatile matter, fixed carbon, moisture and ash contents. This analysis is very important to study the combustion phenomenon of the coffee husk. Therefore, to know the proximate analysis and calorific value of the coffee husk different laboratory equipment is used in Geological Survey of Ethiopian. The experiment is conducted by international standard test method using three main apparatus, these are CARBOLITE furnace, Carbolite oven and Adiabatic Calorimeter. 200 GM of coffee husk sample which came from the study area is taken from this analysis (Fan, Soccol, Pandey, & Soccol, 2003) (**Figure 11**).

The experiment started from the sample preparation room. In this room, giving a code for the sample was the primary task and Y-M-001 was the sample code number. Next, removal of unwanted moisture from the sample is done in a Retsch model RS 200 (Fiori & Florio, 2010). Then grinding of the sample using



an electrical milling machine is done. Sieving the crushed sample with the help of 0.60 mesh sieve and packing the prepared sample with plastic sheet was the last work in the sample preparation room. After this the sample is sent to the hydrocarbon laboratory where the analysis of the prepared sample is conducted (Figure 12).

Proximate analysis indicates the behavior of the husk when it is heated. Therefore the following tasks are conducted in the hydrocarbon laboratory.

1) When 1 gram sample of husk is subjected to a temperature of about  $110^{\circ}\text{C}$  in the oven for a period of 1 hour, the loss in weight of the sample gives the moisture content of the husk.

2) When 1 gram sample of husk is placed in covered crucible and heated to  $950^{\circ}\text{C}$  inside Carbolite Furnace and maintained at that temperature for about 6 minutes. There is a loss in weight due to the eliminating of moisture and volatile matter. So present of volatile matter is calculated here.

3) When 1 gram sample of husk is placed on uncovering crucible and heated to  $750^{\circ}\text{C}$  until the husk is completely burned, a constant weight reached, which indicates that there is only ash remaining in the crucible. Complete combustion of husk is determined by repeated weighing of the sample.

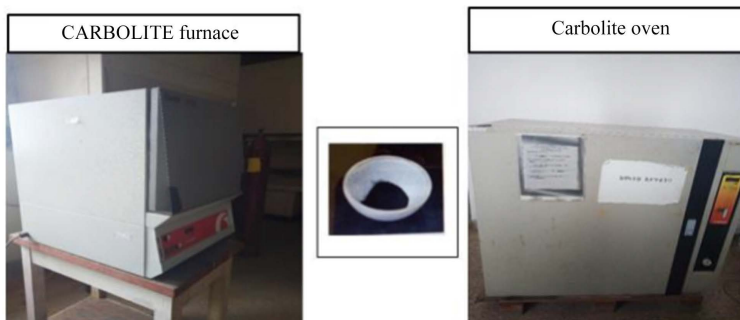
4) The amount of fixed carbon is determined as follows, using subtraction of percentage by mass.

**Table 4.** Laboratory elemental analysis report of coffee husk.

Sample Type	C (%)	H (%)	N (%)	S (%)	O (%)
Coffee Husk	46.8314	4.8132	0.4454	0.0500	~47.860



**Figure 11.** Equipment in sample preparation room.



**Figure 12.** Equipment used in hydrocarbon laboratory.

### 3.3. Calorific Value Analysis of the Coffee Husk

The calorific value (heat of combustion) of a sample may be broadly defined as the number of heat units liberated by a unit mass of a sample when burned with oxygen in an enclosure of constant volume (Wilen, Stahlberg, Sipila, & Ahokas, 1987; Ogada, 1995; Nussbaumer & Hustad, 1997). In this research to determine the calorific value of the coffee husk, the oxygen bomb adiabatic calorimeter is used, which is the standard instrument for measuring calorific values of solid and liquid combustible samples in Geological Survey of Ethiopian shown in **Figure 13**.

The amount of heat obtained from the sample was then determined by multiplying the observed temperature rise by a previously determined energy equivalent of the calorimeter. Then, by dividing this value by the weight of the sample, we obtain the calorific value (heat of combustion) of the sample on a unit weight basis. Corrections must be applied to adjust these values for any heat transfer occurring in the calorimeter, as well as for any side reactions which are unique to the bomb combustion process in **Table 5** which were obtained (Kreith, 2000).

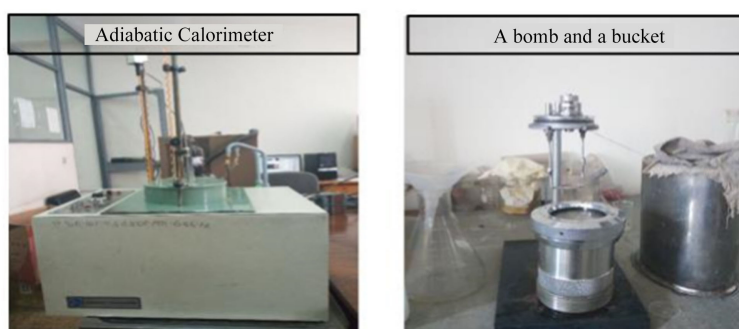
Formulas used for Post processing

The energy equivalent (W)

$$= \frac{(\text{Wight of Standard material} * \text{Heat of combustion of standard material})}{(\text{Temperature rise produced in the test})}$$

$$\text{The gross heat of combustion (Hg)} = \frac{(\text{temperature rise} * \text{energy equivalent})}{\text{weight of the sample}}$$

From the results of experiments, it can be concluded that Coffee husk is characterized by low moisture contents. The low moisture content is an important factor in the combustion of coffee husks, since the problems associated with the combustion of high moisture content of fuels are avoided. One such problem is the effect of moisture on the heating values of fuels. It is seen that husk has a



**Figure 13.** Oxygen bomb adiabatic calorimeter.

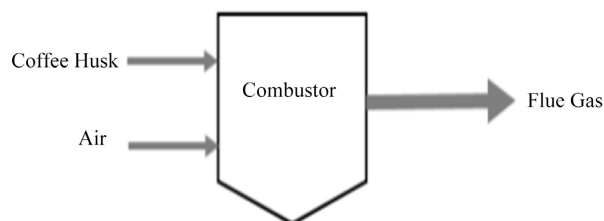
**Table 5.** Laboratory proximate analyses and calorific value report of coffee husk.

Sample Code	Volatile Matters (%)	Fixed carbon in %	Moisture in %	Ash in %	Dry in %	Calorific Value cal/gm
Y-M-001	71.63	16.9	7.92	3.54	0.8	4533.1

higher heating value when we compare it with other agricultural residues (Mendez, Dominguez, Fernandez, & Pis, 2007). The ash contents of the husk are also low and are within acceptable range. This gives a great advantage during furnace design. Because for the combustion of agricultural residues with high ash contents, such as rice husks, consideration must be given to incorporate an efficient ash removal equipment from the flue gas to eliminate or reduce particulate pollution. Due to the low contents of sulfur,  $\text{SO}_2$  emission problems would not be expected during coffee husks combustion (Wilson, John, Mhilu, Yang, & Blasiak, 2010). The high volatile matter content indicates easy ignition of fuel, although it has a significant effect on the combustion mechanisms and consequently on the design and operation of the combustion systems for this fuel. The coffee husk is lighter and smaller than wood chips and coals burned. Thus, there may be a tendency of the particles to be carried out of the furnace with the flue gas. Furthermore, without proper design of the furnace, part of the combustible volatile gases may leave the furnace unbound. The bulk density of the coffee husks is low, raising the costs of transportation and storage. Furthermore, coffee briquettes are fragile and not suitable for long distance transportation. Coffee husks are therefore more suitable for firing within the production region.

### 3.4. Combustion Analysis of Coffee Husk

Combustion chamber of boiler is designed to use the chemical energy in the coffee husk to raise the energy content of fluid in the steam generators (Boiler), so that it can be used for power and heating applications. During the combustion process, oxygen reacts with carbon, hydrogen, and other elements in the husk to produce a flame and hot combustion gases (Flue gas). As these gases are drawn through the boiler it cools as heat is transferred to the working fluid. Eventually the gases flow through a stack and into the atmosphere. As long as husks and air are both available to continue the combustion process, heat will be generated. The combustion chamber is the most important part of the boiler. It is constructed of bricks that causes to minimize heat dissipation to the surrounding. It also has no involvement to do any kind of work. In addition, the kinetic and potential energies of the fluid streams are usually negligible. Then only total energies of the incoming streams and the outgoing mixture remained same for analysis. The conservation of mass and energy principle requires that these two equal each other that is shown in Figure 14 which was obtained from (Nag, 2008).



**Figure 14.** Schematic mass and energy balance diagram of combustion chamber (Nag, 2008).

Considering the theoretical combustion reaction for the organic component of the husk, such as carbon, hydrogen and sulfur (Raja, Srivastava, & Dwivedi, 2006) for mass of air required. The combustion process is assumed as the ideal case (stoichiometry). So, nitrogen is not considered to react with oxygen during combustion reaction. It limits the intimacy between the fuel molecules and  $O_2$ . When the fuel composition is known, the carbon balance method is quite accurate for mass balance calculation (Werthera, Saengera, Hartgea, Ogadab, & Siagib, 2001). In this work, combustion takes place with excess air and when free carbon is not present in the products. The products of combustion are mainly gaseous. When a sample is taken for analysis it is usually cooled down to a temperature which is below the saturation temperature of the steam present. The steam content is therefore not included in the analysis, which is then quoted as the analysis of the dry product. Since the products are gaseous, it is usual to quote the analysis by volume. An analysis, which includes the steam in the exhaust is called a wet analysis (Coskun, Oktay, & Ilten, 2009). To obtain the maximum temperature attained in the furnace, the analysis of heat balance is necessary (Harry, 1998).

### 3.5. Steam Generators (Boiler) Selection

A steam generator generates steam at the desired rate, at the desired pressure and temperature by burning the coffee husk in its furnace. It is a complex integration of combustor, economizer, evaporator and super heater. Steam generator is a closed vessel in which the heat produced by the combustion of fuel is transferred to water for its conversion into steam at the desired temperature and pressure. While selecting a boiler the factors should be considered: the working pressure and quality of steam required, which is whether wet or dry or superheated, Steam generation rate, Floor area available, Accessibility for repair and inspection, Comparative initial cost, Erection facilities, The probable load available, The fuel and water available, Operating and maintenance cost and etc. Heat exchangers (Steam generators) are devices where two moving fluid streams exchange heat without mixing. A heat exchangers typically involve no work interactions ( $w = 0$ ) and negligible kinetic and potential energy changes for each fluid streams (Frank, Peter de, Sarah, & Jeremy, 2007). Depending upon whether the pressure of steam is below or above the critical pressure (221.2 bar), steam generators can be either subcritical or supercritical units. The subcritical steam generators are water tube drum type and they usually operate at between 130 and 180 bar steam pressure. Which produce superheated steam at about  $540^\circ\text{C}$  -  $560^\circ\text{C}$  (Rajput, 2008). But here, for this specific case a subcritical steam generator which operates at 10 bar is used, for this, satisfies the main goal of this paper that is developing a CHP steam plant with minimum cost and maximum efficiency. The increase in steam pressure is limited by the consideration of mechanical stresses and the ensuing higher cost of equipment. And the increase in steam temperature is limited by the properties of the construction materials of boiler and turbine. Increasing the steam temperature above  $540^\circ\text{C}$ , increases the

metallurgical quality of the nozzle and steam turbine blades by 30%. Very high pressures at the maximum temperature are undesirable because they create material strength problems (Aljundi, 2009). Heat transfer to water in the steam generators takes place in the three different regimes (Kenya Planters Cooperation Union (KPCU), 1996). Water is first heated sensibly in the economizer till it becomes saturated liquid. In the evaporator there is phase change from by absorbing the latent heat of vaporization at 10 bar the saturated vapor is farther heated at constant pressure in the superheated (Eastop & McConkey, 1993).

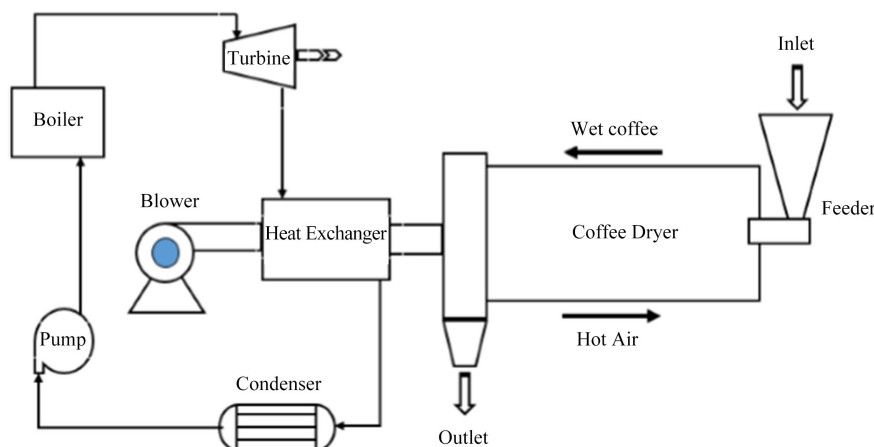
An economizer is a feed water heater which raises the temperature of feed water to about the saturated liquid temperature at the boiler pressure using the flue gases discharged from the boiler. The justifiable cost for an economizer depends on the total gain in efficiency (Bbergman, Lavine, Incropera, & Dewitt, 2011). In turn, this depends on the gas temperature out of the boiler and feed water temperature to the boiler. Economizer tubes are commonly 45 - 70 mm in diameter. And also the coils are installed at 45 - 50 mm spacing between them as obtained from Table 6 (Treybal, 1981).

### 3.6. Selection of Coffee Dryer

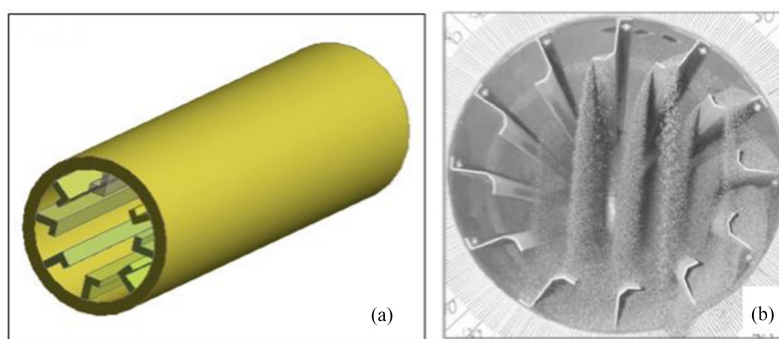
As shown in Figure 15, first the air is impelled by a blower and passed through a duct and it is heated by a set of heat exchanger and then it entered the dryer in countercurrent flow with the coffee. The air outlet is opposite to the coffee inlet. The solid coffee is fed by a container and is removed on the side opposite to the coffee inlet. The dryer cylinder is 9.46 m long with a diameter of 1.54 m. Rotary dryer is a class of dryer commonly used in industry to dry particulate solids. It is made of a long cylindrical shell that is rotated. The shell is usually slightly inclined to the horizontal to induce solids flow from one end of the dryer to the other. Indirect heat rotary dryers, a hot gas flowing through the dryer provides the heat required for vaporization of the water. To promote gas-solid contact, most direct heat dryers have flights placed parallel along the length of the shell, which lifts solids and make them rain across the dryer section. The transport of solids through the drum takes place by the action of the solids cascading from the flights, each cascade comprising the cycle of lifting on a flight and falling through the air stream as shown in Figure 16 which was obtained from Rigassa, Sundaraa, and Seboka (2011).

**Table 6.** Summary of the balance sheet of the boiler.

Heat type	Value (in kJ/kg)	Value (in %)
QSte	10,720.7382	56.48
Q(CO <sub>2</sub> + SO <sub>2</sub> )	256.8709	1.3534
QH <sub>2</sub> O	310.0369	1.6335
Q(O <sub>2</sub> + N <sub>2</sub> )	1387.4815	7.3102
QAPH	1193.672	6.2891
Sum	13,868.7995	73.0662



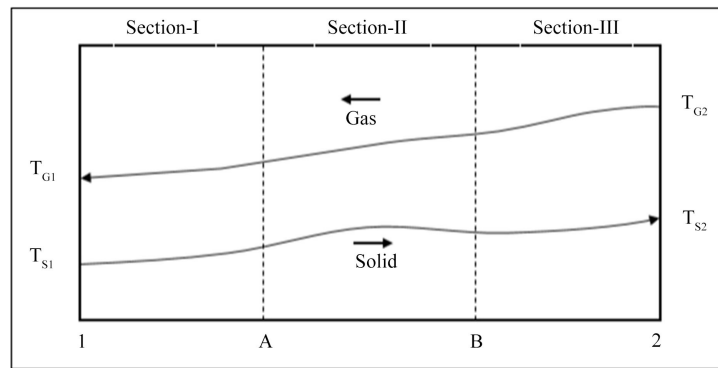
**Figure 15.** Schematic of an integrated counter rotary coffee dryer with main plant components (Dutta, 2010).



**Figure 16.** (a) Rotary dryer; (b) Solids cascading inside the dryer (Kyle, 1984).

Dryer and drying process selection for a specific operation is a complex problem and many factors have to be taken into account. Though, the overall selection and design of a drying system for a particular material is dictated by the desire to achieve a favorable combination of a product quality and process economics. In general with respect to the rate and total drying time in dryer performance is dependent on the factors such as air characteristics, product characteristics, equipment characteristics etc. As a consequence of dryer specialization the selection of the type of dryer appropriate to the specific product to be dried becomes a critical step in the specification and design of the processing plant. The choice of the wrong type of dryer can lead to inefficient operation, reduced product quality, and loss of profit. In the wet solid drying process three sub processes take place. Therefore the dryer is divided into three zones and the section wise calculation of temperature and humidity of the stream can be obtained by material and energy balance as demonstrated in Figure 17 mentioned by Chattopadhyay (2006).

The basis of calculation is 1 hour operation and the initial and final moisture values of the solid (Cherry, Parchment, and Washed coffee) are taken from literature data (Dry coffee processing handbook) which tabulate data conducted in



**Figure 17.** Temperature profile for solid and gas in a counter rotary dryer (Chattopadhyay, 2006).

the laboratory of Panama research (Geankoplis, 1993). In Sheka Zone there are two types of dry coffee processing machineries (local and foreign) with a working capacity of 700 - 1000 and 1200 - 1500 kg/h respectively (Ginzburg & Savina, 1982; Kinch, 1967; Walas, 1990). Since the dryer is the supplier for the processing machineries so, as much as possible, it must be work with the same working capacity of the pulping machine. Therefore, to make the design safe the minimum working capacity 700 kg/h is taken for this work.

### 3.7. Energy Analysis of the Cogeneration Power Plant

The cogeneration thermal power plant analysis is based on a simple Rankine-cycle, steam generated from saturated liquid water (feed water) is used as the working fluid. The super saturated steam flows through the turbine, where its internal energy is converted into mechanical work to run an electricity generating system. And the steam comes out from the turbine supplies heat to the dry process. Not all the energy from steam can be utilized for running the generating system because of losses due to friction, viscosity, bend on blades, heat losses from boilers i.e. hot flue gas losses, radiation losses and blow down losses etc. (Hewitt & Barbosa, 2008; Kreith, Manglik, & Bohn, 2003). Rankine cycle is the theoretical cycle constructed from four main processes on which the generation steam power plant works. The main processes in the Rankine cycle are:

Process 1-2: Reversible adiabatic expansion in the turbine.

Process 2-3 (2'-3'): Constant pressure transfer of heat in the condenser (Drying processes).

Process 3-4: Reversible adiabatic pumping processes in the feed pump.

Process 4-1: Constant pressure transfer of heat in the boiler.

Then, I am going to analyze energy of the cogeneration plant considering 1 kg of fluid and applying steady flow energy equation (SFEE) to Steam generators (boiler), Turbine, Condenser and Pump (Figure 18).

The power plant itself consumes a part of the electricity produced. This is due to the various auxiliary equipment required like feed water pumps, circulation pumps and air/flue gas blowers. In forced circulation boilers the share of elec-

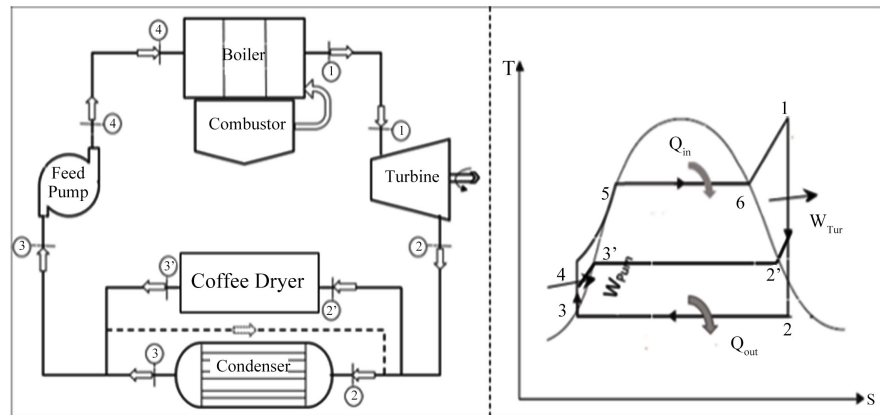


tricity consumed by the circulation pump is about 0.5% of the electricity produced by the plant. Normally the internal power consumption is about 5% of the electricity produced by the power plant. In this context, since the power used is electrical (and taken from the grid), the internal power consumption share is reduced from the final boiler efficiency in boiler calculations (Rajput, 1990; Saidur, Ahamed, & Masjuki, 2010; Duffie & Beckman, 1991; Glikin, 1978).

#### 4. Results and Discussion

The results of the calculated parameters for analysis of a coffee husk fired cogeneration plant analysis equations from the previous sections are shown in Table 7.

The results of the coffee husk generation as we compared with (Glikin, 1978), the deviations of each energy generation were presented. The numerical and experimental results were carried out to observe the deviation. From Table 7, numerical results, more than the experimental value this is because the numerical values are more related to ideal whereas experimental values indicate the actual nature of the coffee husk.



**Figure 18.** Schematic and T-S diagram of the cogeneration plant (Kreith, Manglik, & Bohn, 2003).

**Table 7.** Summary of results.

Description	Units	Formulas Used	Result of numerical	Result of experiments	Deviations
Mass of air	$m_{Air} [kg]$	$m_{Air,sto} + \left( \frac{m_{Air,Exc}}{100} * m_{Air,sto} \right)$	7.497	7.400	0.097
Mass of flue gas	$m_{FG} [kg]$	$m_{DFG} + m_{WFG} + m_{Ash}$	6.3672	6.0072	0.36
Mass of coffee husk	$m_{CH} [kg]$	-	-	-	-
Flue gas temperature	$m_{FG} [^{\circ}C]$	$\frac{m_{CH} * CV_{CH}}{m_{FG} * CP_{FG}} - \frac{m_{ste} * (h_1 - h_4)}{m_{FG} * CP_{FG}} - \frac{m_{UF} * CV_{CH}}{m_{FG} * CP_{FG}} + T_0$	1489	1486.6098	2.3902
Heat of economizer	$Q_{Eco} [kW]$	$\dot{m}_{FG} C_{pFG} (T_{FG1} - T_{FG2})$	825.061	824.003	1.058



## Continued

Heat transfer surface of the economizer	$A_s [\text{m}^2]$	$\frac{Q_{Eco}}{U * F_c * \Delta T_{lm}}$	23.46	22.98	0.48
Total length of tubes of the economizer	$L [\text{m}]$	$\frac{A_s}{\pi * d}$	149.377	149.377	0
Heat of evaporator	$Q_{Eva} [\text{kW}]$	$\dot{m}_{st} * h_{fg}$	8716.2764	8644.76	71.5164
Heat transfer surface of evaporator	$A_s [\text{m}^2]$	$\frac{N_{Tu} * C_{min}}{h}$	33.281	30.678	2.603
Total length of evaporator	$L [\text{m}]$	$\frac{A_s}{\pi * d}$	211.87	211.87	0
Rate of steam	$\dot{m}_s [\text{kg/s}]$	$\frac{\dot{m}_{FG} C_{pFG} (T_{FG1} - T_{FG2})}{h_{fg}}$	0.7701	0.6302	0.1399
Heat rate of super	$Q_{SH} [\text{kW}]$	$\varepsilon * C_{min} * (TF_{G1} - T_{S12})$	1179.4	1169.98	9.42
Transfer surface of superheater			142.04	139.86	2.18
Mass of dry cherry	$\dot{m}_s [\text{kg/h}]$	$\dot{m}_{che} (100\% - X\%)$	1350	1290.87	59.13
Moisture in the wet cherry	$X_1 [\%]$	$\frac{IM}{100 - IM}$	2.3333	1.98	0.3533
Moisture in the dry cherry	$X_2 [\%]$	$\frac{FM}{100\% FM}$	0.1111	0.08956	0.02154
Water evaporated	$m [\text{kg}]$	$\dot{m}_s (X_1 - X_2)$	3000	2909.89	90.11
Inlet gas thermal energy	$H_{G2} [\text{kJ/kg}]$	$C_s (T_{G2} - T_0) + Y_2 H_L$	176.982	170.68	6.302
Rate of mass of gas	$\dot{m}_G [\text{kg/h}]$	$\dot{m}_G (Y_1 - Y_2) = \dot{m}_P (X_1 - X_2)$	98,684.21	98,590.58	93.63
Heat transfer units in section-III	$N_{TU,III}$	$\frac{T_{G2} - T_{GB}}{\Delta T_{m,III}}$	0.022	0.002	0.020
heat transfer units in section-II	$N_{TU,II}$	$\frac{T_{GB} - T_{GA}}{\Delta T_{m,II}}$	0.2636	0.2333	0.0303
Total transfer units	$N_{TU}$	$N_{TU,I} + N_{TU,II} + N_{TU,III}$	1.84	1.09	0.75
Diameter of the dryer	$D [\text{m}]$	$\left( \frac{4 * S}{\pi} \right)^{0.5}$	1.54	1.54	0
Length of dryer	$L [\text{m}]$	$N_{TU} * L_{TU}$	9.46	9.46	0
Revolution per min	RPM	peripheral speed / diameter	4.44	4.44	0
Flue gas loss	$L_{FG} [\%]$	$L(c_{o2} + s_{o2}) + L_{H2O} + L(O_2 + N_2)$	10.297	10.099	0.198
Other losses	$W_{Oh} [\%]$	By subtraction	26.9338	25.09778	1.83602
Total heat absorbed in boiler	$W_{in} [\text{kJ/kg}]$	$h_1 - h_4$	3286.301	3198.898	87.403
Work of feed pump	$W_{FP} [\text{kJ/kg}]$	$V_3 (P_5 - P_3)$	0.9999	0.9999	0
Work of turbine	$W_{TU} [\text{kJ/kg}]$	$h_1 - h_2$	1116.7421	1116.7421	0
Net work	$W_{net} [\text{kJ/kg}]$	$W_{TU} - W_{PU}$	1115.742	1110.987	4.7551
Net power output	$P_{Out} [\text{Mw}]$	$\dot{m}_{ste} * w_{net}$	11.2	10.97	0.23
Overall CHP plant efficiency	$\eta_{Overall} [\%]$	$\frac{W_{net} + Q_{pro}}{Q_{in}}$	84.15	83.957	0.193

## 5. Conclusion

In this work, the coffee husk fired cogeneration plant has been investigated using the designed water tube boiler and rotary type cherry coffee dryer with the selected pump and condensate steam turbine components after the detailed analysis of the combustion of coffee husk using its chemical properties resulted from the laboratory. The following conclusions have been drawn from the work: Coffee husk is characterized by a high content of volatile matter and low contents of fixed carbon and ash. Due to the low contents of sulfur, SO<sub>2</sub> emission problems would not be expected during coffee husks combustion. The calorific value of the coffee husk has been carried out in the laboratory. The result was obtained as 18 KJ/kg. With this heating value, maximum temperature of the flue gas was calculated from the heat balance equation in the furnace. Thermal analysis of the coffee husk fired CHP has done with the operating conditions, taken into account, hence, for an efficient use of coffee husk as a fuel for the generation of steam in the boiler, the design calculation dimension results of different components of the plant should be used. The designed CHP plant configuration and its evaluation based on the identified potential in a coffee processing industry result in 11.2 MW of electrical output from the waste coffee husk. Among this 1.05 MW is used to meet the total demand of the factories, but the rest 10.15 MW is supplied to the national grid of community service. The work also suggested doing a detailed thermodynamic analysis of the plant as it could cover the thermal demand of the factories from the combustion of coffee husk which shifts their drying method to the advanced one. Shifting the industries mode from natural drying to thermal drying mode using the steam generated during cogeneration power plant process increases the quality of coffee with a low usage of man power and less drying space besides transfer of technology of waste to energy conversion. The work also enables us to see the power consumed by the coffee processing industries is very small. Therefore, planting a coffee husk fired cogeneration plant in Sheka zone plays a great role in supporting the community and the government beyond covering their power and heat demand.

## Conflicts of Interest

The authors declare no conflicts of interest regarding the publication of this paper.

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