

Thermochemical Assessment of Solid and Liquid Fuels Used for Domestic Space Heating in Jordan

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Abstract

The gross calorific values of crude and exhausted olive pomace, oak, almond, olive wood, olive oil, kerosene, and diesel are reported in this article. Conversion of crude olive pomace into exhausted olive pomace resulted in 10% reduction in calorific value. The net calorific value of crude olive pomace amounts to 92% of its gross calorific value. The ultimate and proximate analyses of crude olive pomace representing the 2006-2008 olive harvest seasons were determined and compared with analyses pertaining to the 2009-2011 olive harvest seasons in Jordan. Controlled charring of crude olive pomace reduced its mass down to about 20%. Pyrolysis thermogravimetric (TG) and differential thermogravimetric (DTG) curves were recorded under nitrogen atmosphere for crude olive pomace and wood samples. Quantitative data on three DTG major peaks are reported for wood samples and crude olive pomace. A comparison based on market price and calorific value of a fuel showed that olive pomace is the most rewarding fuel for domestic space heating in Jordan.

Keywords

Olive Pomace, Fire Wood, Kerosene, Diesel, Gross Calorific Value, Net Calorific Value, Biomass, Charring

1. Introduction

The olive pomace is the solid byproduct that results from the olive oil industry. Until very recently, the accumulation of olive pomace in the premises of the olive mills in Jordan constituted a very heavy burden on the environment due to the lack of large-scale useful uses for such material. However, since the turn of the twenty-first century, the olive pomace in Jordan has become a precious asset for olive mills owners due to the heavy demand

on its use as a solid fuel useful for heat generation during winter time especially in residential space heating. Unlike exhausted olive pomace, which is practically oil-free pomace, the olive pomace in Jordan is a crude pomace that retains its residual oil. The available statistics on olive pomace production in Jordan over the period 2000-2008 [1] indicate that the annual production fluctuates between a minimum of about 25,000 metric ton in 2001 and a maximum of about 50,000 metric ton in 2006. However, the current amounts of sun-dried crude olive pomace are expected to be much larger than the ones included in this statistics because of the growing interest in planting olives in Jordan. The relevant literature information concerning olive pomace in Jordan has focused on its co-firing with liquid diesel fuel in a slurry form [2], exploring briquettes of olive pomace as a potential source of thermal energy [3], drying characteristics [4], characterization of activated carbon produced from olive pomace [5], use of partially pyrolyzed olive pomace as sorbent for preconcentration of environmental waters [6], and characterization of crude and exhausted olive pomace [7].

The aim of the present work is to provide thermochemical data for the local liquid and solid fuels, namely: kerosene, diesel, local fire wood and olive pomace which represent the types of fuels used for space heating in Jordan. Such data can be combined with fuel price and availability to assess its suitability for domestic space heating.

2. Materials and Experimental Procedures

A brief description of the samples used in the present study is given in **Table 1**. All the reported measurements concerning the wood and pomace samples were carried out on powder samples. A hand-held drill was used to get samples from the wood chunks; further grinding was achieved by using a laboratory grinder. The bark of wood samples was excluded. The grinder was also used for preparing the powder of the olive pomace samples. Care was taken to avoid formation of oil droplets due to heat generated during the grinding step of the pomace samples. The liquid samples of olive oil, kerosene, and diesel were used as received. The sulfur and nitrogen content of these liquid samples was determined by X-ray fluorescence. The nitrogen content of the wood and olive pomace samples was estimated from the acid wash at the end of the oxygen bomb calorimetric measurement. NaOH with molarity of 0.0866 M was used for titrating the acid wash with phenolphthalein as indicator. The moisture content of the solid samples was determined by drying at 110°C for about 15 hours in a conventional drying oven. The ash content of the solid samples was determined by burning the test sample in a muffle furnace at 600°C for three hours. The reported results of moisture and ash content are averages of two runs. Percentages of carbon and hydrogen of wood and olive pomace were determined by using an elemental analyzer. The thermogravimetric analysis of the wood and olive pomace samples was carried out by using a TGA-50 Shimadzu Thermogravimetric Analyzer stationed at the Research Laboratories Division, Jordan University of Science and Technology (JUST). The pyrolysis thermograms were recorded under the following conditions: An inert atmosphere of nitrogen at a flow rate of 50 ml per min, a heating rate of 25°C per min from room temperature up to about 600°C, and the use of aluminum crucibles with pierced lids. The heat of combustion (gross calorific value, GCV) measurements were carried out by using an adiabatic oxygen bomb calorimeter (IKA C 2000 Calorimeter System) stationed at the Royal Scientific Society (RSS). The reported data of the GCV are averages of two runs.

The sieving experiment, which aimed at finding the particle size distribution of the as-received loose sun-dried olive pomace sample, was carried out by using a set of ASTM standard sieves and a laboratory shaker. Five sieves with mesh designations of 10, 18, 35, 60, and 100 were used. Sample KT26, with initial mass of 2.5 kg, is the source of the pomace material used in the sieving experiment. Prior to sieving, several batches of the sample have their lumps crushed for one min. The cumulative mass of the ground batches is 533.6 g which amounts to 21.3% of the original sample mass. In order to find the mass percentage of the sieved fractions, the amount of pomace powder retained by each one of the five sieves was weighed. The mass of the fine powder that passed through the 100-mesh sieve was also determined.

Charring of crude olive pomace was carried out on samples KT25 and KT26 which represent sun-dried compact fire logs and loose olive pomace, respectively. About one kg of each sample was charred in a grill placed in an outdoor environment. Few sprays of kerosene were used to start the charring process and every care was taken to avoid ash formation. The char yield of sample KT25 is 20.71%, and that of sample KT26 is 21.32%. About 11% of the char of these two samples was used for ash determination. Twelve replicates of ash determinations were carried out for each one of these two samples.

Table 1. Brief description of olive pomace, fire wood, and liquid samples used in the present study.

Sample identity	Acquisition time	Sample physical state	Sample source	Remarks
KT7	October 2006	Slurry	^a Sa'doon new olive mill	Virgin pomace collected from mill operation line
KT8	September 2007	Wood chunks	Al-Huson wood shop	Oak wood, bark neglected
KT9	September 2007	Wood chunks	Al-Huson wood shop	Almond wood, bark neglected
KT12	May 2006	Briquettes	^b Sa'doon old mill	Pomace collected from mill drying yard
KT13	December 2006	Briquettes	Pomace shop (Amman)	Sample of pomace used for solid-fired residential boiler
KT14	October 2007	Wood chunks	Al-Huson wood shop	Olive wood, bark neglected
KT23	May 2008	Dry olive pulp	Sa'doon old mill	Pulp of KT25
KT24	May 2008	Dry olive pits	Sa'doon old mill	Pits of KT25
KT25	May 2008	Briquettes	Sa'doon old mill	Pomace collected from mill drying yard
KT26	June 2008	Loose pomace	Sa'doon old mill	Pomace collected from mill drying yard
KT27	June 2008	Powder of KT26	Sa'doon old mill	Mesh: +10
KT28	June 2008	Powder of KT26	Sa'doon old mill	Mesh: -10, +18
KT29	June 2008	Powder of KT26	Sa'doon old mill	Mesh: -18, +35
KT30	June 2008	Powder of KT26	Sa'doon old mill	Mesh: -35, +60
KT31	June 2008	Powder of KT26	Sa'doon old mill	Mesh: -60, +100
KT32	June 2008	Powder of KT26	Sa'doon old mill	Mesh: -100
KT33	December 2008	Liquid olive oil	Al-Kfarat, Irbid Governorate	Extra virgin olive oil
KT34	May 2009	Liquid kerosene	Gas station, Irbid	Local grade
KT35	May 2009	Liquid diesel	Gas station, Amman	Local grade

^{a,b}: Two neighboring olive mills located near Al-Nuaymeh intersection, Amman-Irbid highway.

The exhausted olive pomace samples were prepared from the crude olive pomace samples, namely: KT7, KT12, KT13, KT25, KT26, KT27, and KT32. Extraction of the fat material present in the crude olive pomace was achieved by using n-hexane with purity of 95%. A Soxhlet extractor and cellulose extraction thimbles were used in the extraction experiments. About five grams of the test sample and 200 ml of hexane were used in each extraction experiment. Exhaustive extraction lasted for about 48 hours. In naming the extractives-free residue, the letter “h” is added as a suffix to the symbol of the crude pomace sample used in the hexane extraction experiment.

3. Results and Discussions

3.1. Fluctuations in Olive Pomace Production

The olive tree exhibits an alternate bearing phenomenon (biennial bearing cycle) where the amount of the annual yield for two successive years is quite different. Consequently, fluctuations in the amount of the olive mill solid residue occur for a certain period of time. **Figure 1** shows a graph of such fluctuations in the period 2000-2008 olive harvest seasons in Jordan. The graph is based on numerical data given as part of an annual agricultural statistics report [1]. The fluctuations in the annual yield of olive pomace have serious consequences on the end users who buy olive pomace for space heating in winter times.

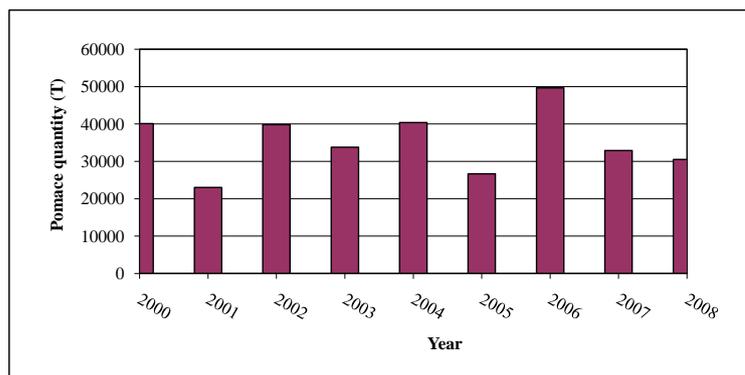


Figure 1. A bar graph of the annual production of sun-dried crude olive pomace in Jordan in the period 2000-2008.

3.2. Moisture and Ash Content

3.2.1. Moisture Content

The results of moisture content are given in **Table 2**. All of the samples have moisture content less than 10%. The differences in the moisture content among the samples reflect variations in sample history. With the exception of sample KT7 which received special treatment of not being exposed to direct sun light, the moisture content of KT26 and its sieved fractions seems to be higher than that of the other olive pomace samples. Samples KT26-KT32 had not been stored for long and presumably contained appreciable volatile matter to be lost in the moisture determination experiments. Being the one with smallest particle size, sample KT32 is a fine powder which is expected to have the highest surface area. Fine powder samples usually retain much water and other volatiles which necessarily lead to higher moisture loss upon heating.

3.2.2. Ash Content

Examination of the ash percentages given in **Table 2** indicates that the percentages fall in the range 0.5% to 6%. It should be mentioned that samples KT23 and KT24 are hand-separated pulp and pits fractions of a batch of sample KT25 with mass proportions equal to 55% pulp and 45% crushed pits. Based on this information and the ash percentages of samples KT23 and KT24, the calculated ash percentage of sample KT25 is 3.081% which is less than the actual value by 7.6%. Within the limits of experimental error, this result is an indication of self-consistency in the results of these three samples. However, such self-consistency was not observed for sample KT26 and its sieved fractions given in Section 3.2.3; presumably due to the fact that each sieved fraction is a mix of variable proportions of both pits and pulp fractions. The gradual increase in the ash content as the particle size diminishes is quite evident in **Table 2** for the sieved fractions. Based on differences in physical hardness of pits and pulp, it is quite reasonable to assume that samples KT27, KT28, and KT29 are fractions rich in mill-crushed pits. The average ash% of these three samples is 1.064%, which is close to the ash% of the pure pits of sample KT24. On the other hand, samples KT30, KT31, and KT32 can be assumed to be rich in crushed pulp. Among these samples, sample KT32 with ash% equal to 88% of that of the pure pulp of sample KT23 seems to be the fraction with highest pulp content. The ash content of the pit sample reported in the present study falls in a literature range of 0.35% - 1.55% [8]. As with regard to the other pomace samples, we note that samples KT25 and KT26 have nearly the same history and their ash percentages are within $\pm 3.2\%$ from their average. Sample KT7, which is a virgin olive pomace, gave the lowest % ash among the non-fractioned pomace samples. This sample was air-dried at home for few months; then drying was completed for one year in the laboratory environment. The % ash of this sample is very close to that of several pomace samples representing the 2010 and 2011 harvest seasons in Jordan [7]. The remaining samples, KT12 and KT13, were obtained from different locations in the same harvest season; sample KT13 gave % ash close to that of samples KT25 and KT26 while the ash % of sample KT12 is within the range of ash percentages of samples taken in the 2010 and 2011 olive harvest seasons [7]. The ash content of the wood samples given in the present study is lower than those given in the literature, especially the almond and olive wood samples. For pellets of almond, holm oak, and olive trees, the literature values are 3.5%, 4.5%, and 5.9%, respectively [9].

Table 2. Moisture and ash content of olive pomace and fire wood samples.

Sample	Moisture %	Ash %	Sample	Moisture %	Ash %
KT7	6.775	2.215	KT25	5.965	3.335
KT8	5.601	5.882	KT26	7.298	3.558
KT9	4.865	0.628	KT27	6.940	0.757
KT12	5.351	5.397	KT28	6.921	0.835
KT13	5.250	3.282	KT29	7.118	1.600
KT14	4.806	0.577	KT30	7.807	3.500
KT23	5.662	4.613	KT31	6.570	3.680
KT24	5.811	1.208	KT32	8.745	4.056

3.2.3. Distribution of Particle Size of Sun-Dried Crude Olive Pomace

The distribution of particle size of an olive mill solid waste is governed by several factors. These factors include the type of olive mill, the mill operational parameters, the size distribution of the olive drupes, and the pits/pulp ratio of ripe olives. Visual inspection of sun-dried olive pomace has shown appreciable amounts of tiny uncrushed pits. Relatively small olives have small pits that might escape crushing during the olive oil extraction stages. It is also known that olive mills generate sizable amounts of fine solids in their waste water. In this case the yield of marketable olive pomace may be reduced. For space heating purposes, marketable olive pomace is usually sold in the form of cylindrical pieces (fire logs) with mass of about 1 kg and a height of about 20 cm. If the freshly prepared cylindrical pieces have high content of fine particles and moisture, they might develop cracks during their sun-drying stage due to excessive expulsion of moisture content. This is a disadvantage for the end user in terms of transportation and storage. Therefore, it is preferable to have a balance between coarse and fine portions in order to have manageable dry fire logs. Because of these remarks, frequent check on the olive mill operational adjustments has to be carried out during the olive harvest season which is stretched over a period of about 10 weeks, starting at middle of October and ending at the end of December of each year. The data shown in **Table 3** are results of a sieve analysis of an olive mill-crushed sun-dried olive pomace (sample KT26). If we consider mesh No. 35 as the border line between the coarse and fine fractions of the test sample, we notice that these fractions are nearly close to a 1:1 ratio. The handling loss in the sieving experiment is 1.92%.

3.2.4. Charred Olive Pomace

In essence, the charring of the olive pomace samples as we did it is a controlled burning of the volatiles accompanied by the escape of the sample moisture. By doing that, the mass of the olive pomace sample was reduced to about 20% of its initial value. The char of the test sample was then burned in a muffle furnace at 600°C for three hours and the mineral content is left as ash. A more rigorous two-step procedure for preparing a low temperature ash begins with a pyrolysis step carried out in a tube furnace at about 500°C followed by burning the char at about 350°C for several hours [10]. The results of ash percentages relative to char mass and relative to the initial mass of the pomace sample are given in **Table 4** and **Table 5** for samples KT25 and KT26, respectively. The relation defined by Equation (1) was used for calculating the values of the % ash relative to the initial mass of the pomace sample. The results are given in the last columns of **Table 4** and **Table 5**.

$$\% \text{ Ash in olive pomace} = (\% \text{ Ash in char}) \left(\frac{y}{100} \right) \quad (1)$$

In Equation (1), y is the % of char yield; $y = 20.71\%$ for sample KT25 and 21.32% for sample KT26. By comparing the ash percentages given in **Table 2**, and the averages given at the bottom of the last columns of **Table 4**, and **Table 5** on dry basis, we find differences of 0.12% and 0.10% from the mean for samples KT25 and KT26, respectively. This excellent agreement implies that the charring process was properly done. Knowing the char yield and the moisture percentage, we can estimate the % of volatile matter (VM) for the tested samples as will be shown in a later section. For sample KT25 the values of the standard deviation (based on “N-1” aver-

Table 3. Distribution of particle size of sun-dried crude olive pomace.

Fraction identity	Mesh No.	Aperture/mm	Fraction mass/g	Fraction %
KT27	10	2	114.16	21.39
KT28	18	1	114.25	21.41
KT29	35	0.51	42.29	7.93
KT30	60	0.25	90.64	16.99
KT31	100	0.15	83.41	15.63
KT32	<100	<0.15	78.59	14.73
Sum			523.34	98.08%

Table 4. The ash content of crude olive pomace and char of sample KT25.

Trial No.	Char mass/g	Ash mass/g	% of Char ash	% of Pomace ash
1	2.1834	0.3357	15.3751	3.1842
2	2.2452	0.3954	17.6109	3.6472
3	2.5284	0.6050	23.9282	4.9555
4	2.4900	0.4215	16.9277	3.5057
5	2.3013	0.3791	16.4733	3.4116
6	2.3816	0.3156	13.2516	2.7444
7	2.3270	0.3664	15.7456	3.2609
8	2.4923	0.4594	18.4328	3.8174
9	2.2637	0.3603	15.9164	3.2963
10	2.5009	0.3727	14.9026	3.0863
11	2.2895	0.2807	12.2603	2.5391
12	2.2320	0.2873	12.8719	2.6658
Average ash %			16.1414	3.3429

Table 5. The ash content of crude olive pomace and char of sample KT26.

Trial No.	Char mass/g	Ash mass/g	% of Char ash	% of Pomace ash
1	2.2054	0.3206	14.5370	3.0993
2	2.2423	0.3073	13.7047	2.9218
3	2.3886	0.5027	21.0458	4.4870
4	2.0952	0.3757	17.9315	3.8230
5	2.3317	0.4271	18.3171	3.9052
6	2.4435	0.3451	14.1232	3.0111
7	2.3700	0.4295	18.1224	3.8637
8	2.3969	0.3774	15.7453	3.3569
9	2.6724	0.5025	18.8033	4.0089
10	2.2996	0.4228	18.3858	3.9199
11	2.2188	0.4018	18.1089	3.8608
12	2.2348	0.2649	11.8534	2.5271
Average ash %			16.7232	3.5654

age), are: 3.092 for % ash relative to char mass and 0.640 for % ash relative to pomace mass. The corresponding values for sample KT26 are 2.679 for % ash relative to char mass and 0.571 for % ash relative to pomace mass. The values of the percentage relative deviation, % R.D (% R.D = mean of absolute deviations \times 100/average) are 13.1% and 13.6% for ash data given in **Table 4** and **Table 5** of samples KT25 and KT26, respectively.

3.2.5. Proximate Analysis of Crude Olive Pomace

Knowledge of the proximate analysis of a fuel is necessary for evaluating its potential for energy production. The proximate analysis is a list of the percentages of moisture, ash, fixed carbon (FC), and volatile matter. The non-automated ASTM method [11] is usually used for finding the percentages of fixed carbon and volatile matter. Nowadays, the TG technique is considered as a reliable and time-saving technique for finding proximate analysis [12]. In connection to this matter, a comparison of traditional ASTM methods and TG determined volatile matter and ash content of various animal manures has been reported [13]. In a previous publication [7], we reported the proximate analysis of several olive pomace samples (samples belong to the 2009-2011 olive harvest seasons in Jordan) based on locating certain temperatures and residual masses on the TG curve of the test sample. The proximate analysis data obtained by this procedure were tested by a correlation formula suggested by Parikh *et al.* [14]. The formula predicts the higher heat value (HHV, $\text{HHV} = \text{GCV}$) of a fuel from its proximate analysis. The calculated GCV values were found to be in excellent agreement with the values obtained calorimetrically. For comparison purposes, we have calculated average proximate analysis for the previously reported results [7]. The calculated averages are: % ash = 5.2, % FC = 25.8 and % VM = 69.9%. In the present study we have chosen a procedure for deriving the percentages of fixed carbon and volatile matter from char-based data of samples KT25 and KT26. In this case the mass of the char is assumed to be the sum of the masses of fixed carbon and ash, while the mass loss accompanying the char formation is assumed to be the sum of the masses of volatile matter and the sample moisture. Based on these assumptions we calculated the proximate analysis of samples KT25 and KT26 as given in **Table 6**. Comparison on dry basis of the average proximate analysis given in this table with the above mentioned average proximate analysis of the data reported previously [7] indicated that the differences in percentages as reported in the present study are: % VM is 7.6 percentage points higher while the % FC and % ash are 7 and 1.5 percentage points lower, respectively. From other literature data related to the present study, we cite: (a) % VM of 80.94, 79.10, 77.77; % FC of 18.50, 15.30, 17.92; % ash of 0.56, 5.6, and 4.31 on dry basis for pits, pulp, and residue of olive pomace, respectively [15]; (b) % VM of 76.3%, % FC of 19.2%, and % ash of 4.5% for olive pomace [16]; (c) % VM of 86.51%, % FC of 10.7%, and % ash of 2.76% for olive pomace briquettes [3]. With the exception of the data reported in ref. [3], our results are in good agreement with the other cited literature data.

3.2.6. Ultimate Analysis of Crude Olive Pomace

The results of the ultimate analysis of crude olive pomace are given in **Table 7**. The real crude olive pomace samples in this table are KT7, KT12, KT25, and KT26. Their average ultimate analysis is given as follows: % ash = 3.868, % C = 54.792, % H = 7.605, % N = 0.788 and % O = 32.948. Certain observations can be pointed out from the data given in this table. For example samples having the same history such as KT25 and KT26, have nearly the same ultimate analysis while fractions of the same olive pomace such as the pairs KT23/KT24 and KT27/KT32 have significant differences in the contents of their mineral and nitrogen-containing compounds. Being pulp/or pulp rich, samples KT23 and KT32 indicate that the nitrogen-containing compounds and the minerals are largely contained in the pulp fraction of the olive pomace. The elemental analysis of an olive pomace sample taken from Ajloun Governorate (northern part of Jordan) has shown that the C, H, and N contents are 54.4%, 7.7%, and 0.90%, respectively [6]. These percentages are comparable with our data given in **Table 7**.

Table 6. Proximate analysis of some crude olive pomace samples. Percentages of ash, fixed carbon, and volatile matter are given on dry basis.

Sample identity	% Moisture	% Ash	% FC	% VM	FC/VM
KT25	5.965	3.555	18.469	77.976	0.24
KT26	7.298	3.846	19.153	77.002	0.25
Average	-	3.701	18.811	77.489	0.25

An attempt was made for comparing the proximate and ultimate analyses reported in the present study with their counterparts reported previously [7]. The results of this comparison are given in **Table 8**. Set 1 represents the present study while Set 2 represents the previous study. For proximate analysis, Set 1 is based on two samples, namely: KT25 and KT26 whose R.D value for % ash is 3.9% on dry basis. On the other hand Set 2 is based on six samples two of them have ash % nearly 4 times the average of the other four samples. Set 2 has % R.D of 6.6% for ash content. As with regard to ultimate analysis, Set 1 has four samples (fraction samples in **Table 7** are excluded) while Set 2 has six samples. With the exception of % R.D of the volatile matter, large deviations exist in the other values of the proximate analysis. In the case of ultimate analysis, there are also large deviations in the % R.D values of ash and nitrogen. A reasonable explanation for the variations in the proximate and ultimate analyses of the two data sets can be presented on the basis of the fact that the data were collected over a period of six harvest seasons (2006-2011). Fluctuations in rain fall, inconsistent procedures in collecting and drying of olive pomace on the premises of olive mills, differences in olive cultivar and age of olive trees, and differences in the degree of ripeness of the olive fruits when brought to the olive mills are believed to be the cause of such variations. Despite all these remarks, the averages given in **Table 8** can be used for specifications purposes of olive pomace in Jordan.

3.2.7. Oxygen Bomb Calorimetric Measurements

1) The Gross and Net Calorific Values of Crude Olive Pomace and Its Fractions

Table 7. Ultimate analysis of olive pomace and its fractions on dry basis.

Sample identity	% Ash	% C	% H	% N	% O
KT7	2.38	53.89	7.40	0.63	35.70
KT12	5.70	55.02	7.62	0.62	31.04
KT25	3.55	55.13	7.70	0.97	32.65
KT26	3.84	55.13	7.70	0.93	32.40
KT23	4.89	57.45	7.80	1.06	28.80
KT24	1.28	51.30	6.88	0.80	39.74
KT27	0.81	51.04	6.75	0.81	40.59
KT32	4.45	51.14	6.90	1.39	36.12

^a: % Oxygen determined by difference.

Table 8. Comparison of proximate and ultimate analyses of olive pomace for two data sets.

Comparison of proximate analyses					
Data set	% Ash	% FC	% VM	FC/VM	-
Set 1	3.701	18.811	77.489	0.25	-
Set 2	5.183	25.8	69.9	0.37	-
Two-set average	4.442	22.306	73.694	0.31	-
% R.D	16.7	15.7	5.1	19.4	-
Comparison of ultimate analyses					
Data set	% Ash	% C	% H	% N	% O
Set 1	3.868	54.792	7.605	0.788	32.948
Set 2	5.17	51.36	6.42	1.16	35.90
Two-set average	4.52	53.08	7.01	0.97	34.42
% R.D	14.4	3.2	8.4	19.1	4.3

When a sample of a fuel is burned in an oxygen bomb calorimeter, the resulting amount of heat energy is known as GCV. However, burning the fuel in an industrial or domestic facility generates a different amount of energy known as the net calorific value (NCV). The magnitude of NCV is generally less than that of GCV. This difference is due to the fact that certain chemical and physical processes that take place under the oxygen bomb conditions cannot proceed when the fuel is burned under normal conditions of real life applications. In the case of a solid biomass fuel, such as olive pomace, the major corrections needed for getting the NCV value from the GCV value are the heat resulting from condensation of water coming from sample moisture and oxidation of sample hydrogen. Other corrections involve the heat of hydration of acids such as HNO₃, H₂SO₄, HCl, and any heat resulting from possible interaction of water vapor with the remaining inorganic constituent of the biomass material.

In the case of acid correction, the current information regarding the thermochemical corrections for oxygen bomb calorimetry [17] [18] only the heat resulting from the combination of water vapor with HNO₃ and H₂SO₄ can be accounted for. The corrections are 59.7 and 297.2 kJ per mole for HNO₃ and H₂SO₄, respectively. In terms of % N and % S, the corrections become 42.6 and 92.7 J per gram of sample for each percentage point of N and S, respectively [7]. The corrections due to condensation of water vapor in the oxygen bomb enclosure are (2.442) (% moisture/100) and (2.442) (% H/100) (9.01) (1-% moisture/100) kJ per gram of wet sample for sample contents of moisture and hydrogen, respectively [7]. The factor 2.442 is the heat of condensation of water vapor in units of kJ per gram of condensed water based on a value of 43.990 kJ/mol of condensed water at 25°C [19]. Based on this information, the value of NCV can be calculated on dry basis in units of Joule per gram of dry sample according to the following equation:

$$\text{NCV} = \text{GCV} - (2442) \left(\frac{\% \text{H}}{100} \right) (9.01) + (92.7)(\% \text{S}) + (42.6)(\% \text{N}) \quad (2)$$

The values of the GCV reported in the second column of **Table 9** are the data obtained from the oxygen bomb calorimeter while the values of NCV given in the table were calculated according to Equation (2). On the average, NCV amounts to 92% of GCV. Correction due to condensation of water resulting from oxidation of hydrogen amounts to 7% of GCV. The remaining 1% of GCV corrections is the sum of corrections due to the hydration of HNO₃ and H₂SO₄ and any other unaccounted for corrections. We have neglected H₂SO₄ correction since the % S is usually less than 0.1% [3] [20] and the correction is within the margin of uncertainty in the GCV measurements. The average value of GCV reported in **Table 9** on dry basis is in fair agreement with literature values of 21.2 [7], 23 [3], 22.24 kJ/g [20] and 22.63 - 22.92 kJ/g [21]. The results of the GCV of the pomace fractions are given in **Table 10**. The variations in GCV reflect the fact that the samples have variable proportions of pits and pulp. It is quite reasonable to assume that samples rich in pulp have higher heating value because pulp is the part of the olive fruit where the residual oil exists. This explains the high GCV value of sample KT23 (pure pulp) compared with the low value of sample KT24 (pure pits). The same argument applies for samples KT27-KT32 where samples KT30-KT32 are believed to have higher pulp content compared with grainy KT27-KT29 samples. The value of GCV on dry basis of the pit sample (KT24) is within the range given in the literature, 19.9 - 21.1 [8]. The calculation procedure of NCV of the pomace fractions is the same as the one used for crude olive pomace samples. In addition to these calculations, we carried out a calculation check on the

Table 9. Gross and net calorific values of crude olive pomace.

Sample identity	GCV (kJ/g), wet basis	GCV (kJ/g), dry basis	NCV (kJ/g), dry basis	NCV/GCV, dry basis
KT7	20.891	22.409	20.754	0.926
KT12	20.548	21.709	20.007	0.922
^a KT13	19.836	20.935	19.219	0.918
KT25	21.589	22.959	21.223	0.924
KT26	20.878	22.522	20.788	0.923
Average	20.748	22.107	20.398	0.923

^a: % H for this sample is taken as average % H of samples KT7, KT12, KT25, and KT26.

Table 10. Calorific values of sieve-fractions of crude olive pomace.

Sample identity	GCV (kJ/g), wet basis	GCV (kJ/g), dry basis	NCV (kJ/g), dry basis	NCV/GCV, dry basis
KT23	23.368	24.771	23.013	0.924
KT24	19.129	20.309	18.762	0.924
KT27	18.832	20.236	18.717	0.925
KT28	18.585	19.967	n.d	n.d
KT29	20.226	21.776	n.d	n.d
KT30	23.121	25.079	n.d	n.d
KT31	22.451	24.030	n.d	n.d
KT32	21.987	24.094	22.516	0.934

n.d: not determined.

GCV of samples KT25 and KT26. In the case of sample KT25, we used GCV of KT23 and KT24 and the mass fractions of 0.45 for pits (sample KT24) and 0.55 for pulp (sample KT23). The calculated value of GCV of sample KT25 is 22.763 kJ/g which amounts to 99.2% of the calorimetric result on dry basis. Likewise, by using the mass fractions of KT26 given in **Table 3** and the GCV given in **Table 10** for six fractions (samples KT27-KT32), the calculated GCV of sample KT 26 is 21.896 kJ/g on dry basis. This value is 97.2% of the calorimetrically obtained value given in **Table 9**. It should be mentioned that the sum of percentages in **Table 3** is 98.08% and the remaining 1.92% is considered as handling loss during the sieving experiment. The average value of the NCV/GCV ratio in **Table 10** is 0.93 which is practically the same as the average given in **Table 9**. The calculations we made so far in this section imply that our calorimetric data have high level of precision and consistency.

2) The Gross Calorific Values of Exhausted Olive Pomace

The exhausted olive pomace samples that we prepared and studied in the present work are listed in the first column of **Table 11**. The first five samples (samples KT7h, KT12h, KT13h, KT25h, and KT26h) were prepared from their parent samples of crude olive pomace, while samples KT27h and KT32h are exhausted olive pomace fractions prepared from KT27 and KT32 which are fractions of the crude olive pomace of sample KT26. As a comment on the data given in **Table 11**, we notice that sample KT7 (collected from the olive mill operation line) has the highest % extractives because it was not exposed to weather conditions as the other samples; therefore it retained an appreciable amount of residual olive oil and other volatiles that can be extracted by hexane. As a manifestation of this fact, KT7h (which is an extractives-free version of KT7) has the lowest GCV among the other non-fractionated samples. On classification basis, sample KT7 is a virgin pomace as contrasted to crude and exhausted olive pomace types. Samples KT27 and KT32 are fraction samples; the first is assumed to be rich in pits but lean in fat material while the second is assumed to be rich in pulp and rich in fatty matter. These considerations are in accord with % extractives and GCV ratio shown in the last column of **Table 11**. Also, samples having the same % extractives have nearly the same reduction in their GCV as indicated by samples KT13h and KT27h. In all cases the GCV of an exhausted pomace is less than the GCV of the parent sample as seen in the last column of **Table 11**. When samples KT7h, KT27h, and KT32h are excluded, the remaining samples in **Table 11** represent realistic exhausted olive pomace samples originated from sun-dried crude olive pomace. In this case, the average GCV of the four exhausted olive pomace samples is 20.169 kJ/g. The corresponding literature values are 20.07 [7] and 19.596 [23] kJ/g. The ratios given in the last column of **Table 11** indicate the extent by which the value of GCV of a crude pomace is lowered by hexane extraction. The acid correction presented as HNO₃ correction in **Table 11** was obtained from the number of moles of NaOH consumed in the titration of the acid wash obtained after the combustion of the sample in the oxygen bomb and the factor 42.6 J per gram sample per percentage point of nitrogen. H₂SO₄ correction was neglected due to the low sulfur content of olive pomace. The moisture correction was calculated according to the factor 2.442 (% moisture/100) kJ per gram of wet sample. Correction due to condensation of water vapor resulting from oxidation of sample hydrogen was not calculated due to the unavailability of hydrogen analysis. The average value of the sum of HNO₃ and moisture

corrections for data given in **Table 11** amounts to 0.8% of the GCV.

3) The Gross Calorific Values of Local Fire Wood

Table 12 shows the GCV of oak, almond, and olive wood usually used for domestic space heating in Jordan. The calculated values on dry basis are in reasonable agreement with literature values [9] given in the last column of **Table 12**. Although sources of wood are very limited in Jordan, local fire wood is still in use for fire places despite its high prices. As indicated in **Table 9**, **Table 11**, and **Table 12**, the values of GCV of wood samples are a little lower than those of crude and exhausted olive pomace. In terms of market prices in Jordan, wood is more expensive than olive pomace, especially oak wood. Co-firing of wood and crude olive pomace is becoming a routine practice for firing fire places in Jordan. In this case crude olive pomace is considered as a starter in the co-firing process in addition to its participation in heat generation.

Based on personal observations of the present author, most of the wood sold during the 2014 winter season has high moisture content especially olive wood and the assorted wood mixture of almond and other related wood types; this high moisture content caused difficulties in maintaining a stable combustion in a fire place even in the presence of olive pomace. It is clear that in the absence of official specifications for the use and trade of solid fuels in Jordan, there will be health and environmental hazards. On terms of abundance and availability in the market, local wood can be considered as a non-renewable biomass in Jordan because of the scarcity of forests. This fact is the reason for marketing fire wood with high moisture content; the demand is high in winter time but wood drying is practiced at the low level by most owners of wood shops.

4) The Gross Calorific Values of Olive Oil and Local Liquid Fuels

The traditional liquid fuels used for residential space heating in Jordan are kerosene and diesel. Despite the fact that their current prices are nearly four times the prices a decade ago, these two liquid fuels are still used for diesel-fired central heating boilers and kerosene-fired space heating stoves. They are included in the present study for the purpose of determining the GCV of non-renewable fossil fuels. Therefore, their thermal capacity can be compared with the thermal capacity of a renewable biomass fuel. Although olive oil is intended for human consumption, it is also included in the present study to represent a renewable liquid fatty material. The values of GCV for olive oil, kerosene, and diesel are reported in **Table 13** along with some literature values for olive oil [24] and for kerosene and diesel [25]. The % S and % N were determined by X-ray fluorescence and were used to calculate the H_2SO_4 and HNO_3 corrections. When the sum of these acid corrections is calculated as % of GCV for each liquid, the results are 0.15%, 0.28%, and 0.32% for olive oil, kerosene, and diesel, respectively.

Table 11. Calorimetric data for exhausted olive pomace.

Sample No.	% Extractives ^a (d. b)	% Moisture	GCV (kJ/g), ^b (w. b)	GCV (kJ/g), (d. b)	HNO ₃ Correction, J/g (d. b)	Moisture Correction, J/g	^c GCV _{exh} / ^d GCV _{cr} (d. b)
KT7h	24.5	7.108	17.063	18.369	55	174	0.82
KT12h	10.5	4.426	19.098	19.982	27	108	0.92
KT13h	7.9	4.248	19.261	20.116	42	104	0.96
KT25h	14.5	4.507	19.623	20.549	41	110	0.90
KT26h	9.8	7.825	18.462	20.029	40	191	0.89
KT27h	8.0	2.974	19.017	19.600	33	73	0.97
KT32h	22.3	3.036	18.784	19.372	45	74	0.80

^a: Dry basis; ^b: Wet basis; ^c: GCV_{exh} of exhausted pomace; ^d: GCV_{cr} of crude pomace.

Table 12. Calorimetric data for local fire wood samples.

Sample identity	% Moisture	GCV (kJ/g), (wet basis)	GCV (kJ/g), (dry basis)	Literature GCV, kJ/g [9]
KT8	5.601	16.952	17.958	18.82
KT9	4.865	18.556	19.505	18.01
KT14	4.806	18.230	19.150	18.47

As mentioned earlier in the discussion, these acid corrections are quite insignificant when compared with corrections of water condensation.

With gross calorific values, on wet basis, of 20.748, 16.952, and 44.942 kJ/g for crude olive pomace, oak wood, and diesel, a comparison based on fuel price and calorific value is given in **Table 14**. It is evident from the values given in the last column of the table that olive pomace is the right choice as a fuel for space heating purposes in Jordan. In addition to its low nitrogen and sulfur content, olive pomace is abundant, carbon neutral, and a valuable renewable energy source in Jordan. With all these facts, olive pomace in Jordan deserves greater attention from the government since it contributes significantly to the energy demand in winter time.

3.2.8. Results of Thermogravimetric Measurements

1) TG and DTG Curves of Oak, Almond, and Olive Fire Wood Samples

The TG pyrolysis curves of oak, almond, and olive wood samples are shown in **Figure 2**. According to this figure, the major mass loss takes place in the temperature range 200°C - 425°C. More quantitative information about the pyrolysis of these wood samples can be obtained from their DTG curves shown in **Figure 3**. There are three peaks in this figure that correspond, in principle, to several mass loss processes. The low temperature peak is explained to be a physical process involving evolution of sample moisture and other light volatiles with peak temperature of about 90°C. The other two peaks that appear at higher temperatures are explained to be due to overlapping chemical processes involving fragmentation of lignocelluloses. The reported DTG curves of xylan (a substitute for hemicellulose in lignocellulosic studies), lignin, and cellulose [26] indicate that xylan and lignin start decomposition at temperatures lower than cellulose and decomposition of lignin extends over a wide range of temperature. Moreover, the reported DTG peak temperatures, at a heating rate of 20°C/min, of xylan, lignin, and cellulose are 298°C, 350°C, 350°C, respectively. It has also been reported that the main degradation peak of all wood species is due to the decomposition of cellulose and the shoulder on its left is due to decomposition of hemicellulose [27] [28]. It is worth mentioning that the characteristics of a DTG peak depend on heating rate [29], an observation to be considered when comparing peak value and peak temperature.

Guided with this literature information, the data given in **Table 15** were collected by careful analysis of the DTG curves of **Figure 3**. Among the three wood samples investigated in the present study, only oak wood showed a lignin hump at 525°C. There are slight differences in wood pyrolysis characteristics. For example olive wood starts decomposition at 200°C while almond and oak start at 250°C. It is also evident that almond has the lowest cellulose peak temperature while oak and olive has nearly the same peak temperature. As with regard to the rate of maximum mass loss, the three wood types have nearly the same values for cellulose decomposition and loss of water, but different values are observed for decomposition of hemicellulose. At the end of the TG run, the three wood samples have nearly the same residual mass fraction at 600°C.

2) TG and DTG Curves of Crude Olive Pomace Samples

Table 13. Calorimetric data for olive oil, kerosene, and diesel.

Sample identity	% S	% N	GCV (kJ/g), (wet basis)	H ₂ SO ₄ correction, J/g (wet basis)	HNO ₃ correction, J/g (wet basis)	Literature GCV, kJ/g
KT33	0.0251	1.352	39.838	2	58	39.675 [24]
KT34	0.1703	2.622	46.143	16	112	46.20 [25]
KT35	1.0168	1.143	44.942	94	49	44.80 [25]

Table 14. Energy and price comparison of solid and liquid fuels.

Fuel type	Reference mass/ton	^a Cost/\$ per ton	Heat energy/ 10 ¹⁰ J per ton	MJ/\$
Olive pomace	1	170	2.075	122.1
Oak wood	1	255	1.695	66.5
^b Diesel	1	1170	4.494	38.4

^a: USD; ^b: Price per metric ton was calculated from the price per liter and a density of 0.85 g/cm³.

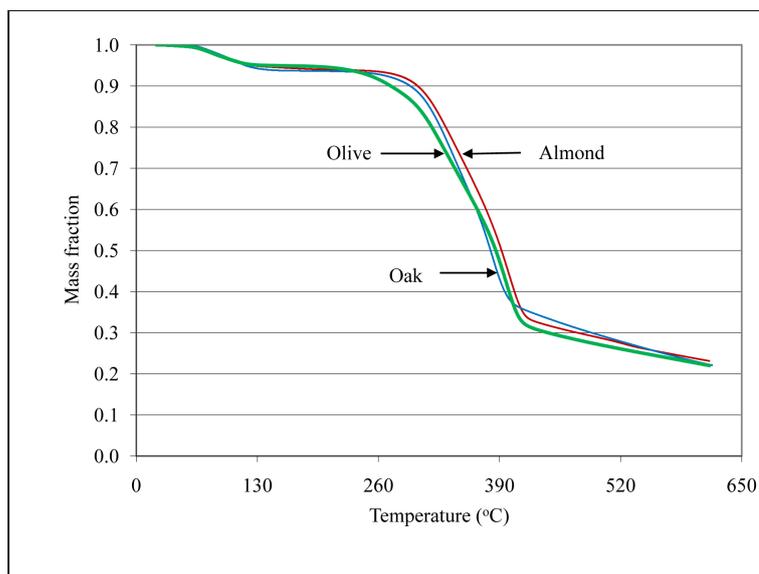


Figure 2. TG pyrolysis curves of oak, almond, and olive fire wood samples.

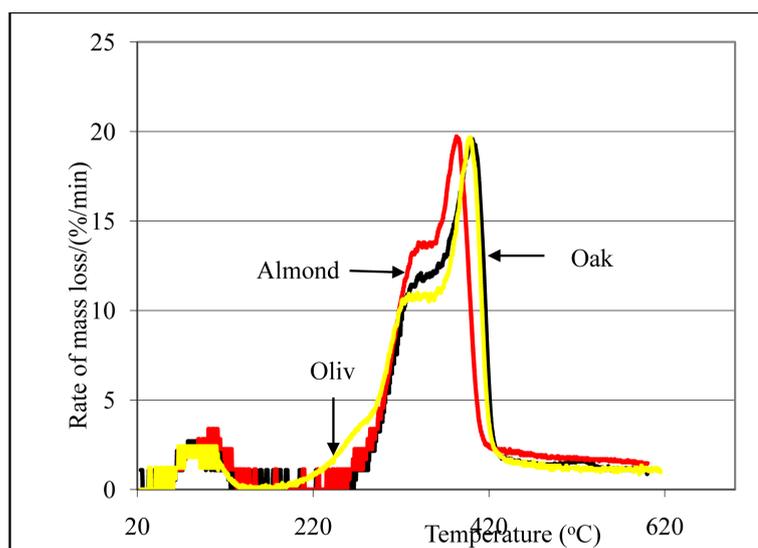


Figure 3. Plot of DTG curves of oak, almond, and olive fire wood samples.

The pyrolysis curves of three crude olive pomace samples are shown in **Figure 4**. Comparison of these TG curves with the TG curves of wood samples given in **Figure 2** shows that the decomposition of the lignocellulosic matter of olive pomace starts and ends at temperatures lower than those of the wood samples. For olive pomace, major decomposition of its lignocelluloses takes place in the temperature range 180°C - 400°C. The TG curves depicted in **Figure 4** show appreciable differences in the extent of lignocellulosic decomposition. These differences are also evident in the DTG curves in **Figure 5**. The same observations were noticed for samples KT23, KT24, KT25, KT27, and KT32. The DTG curves of sample KT25 and its pulp and pit fractions are given in **Figure 6** while the DTG curves of samples KT27 and KT32 (sieve fractions of KT26) are given in **Figure 7**. In most cases, these DTG curves maintain the two-peak feature of the lignocelluloses decomposition of a biomass, which is largely attributed to hemicellulose/cellulose decomposition. However, lignin peaks were not detected except the high temperature humps in **Figure 7**. As with regard to peak value, all DTG curves shown in the present study have cellulose as the component with highest peak value; an exception is sample KT27 which has hemicellulose as the one with highest peak value. The DTG curves shown in **Figure 6** indicate that the

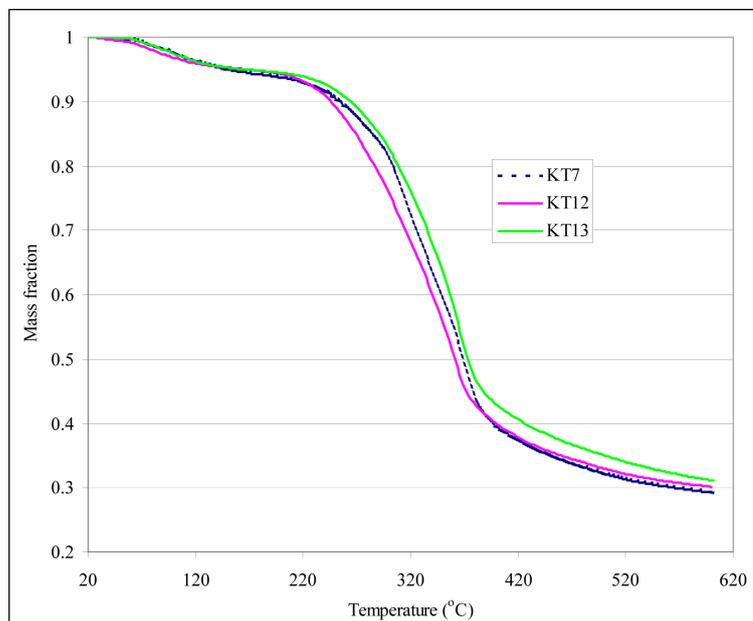


Figure 4. TG curves of crude olive pomace samples.

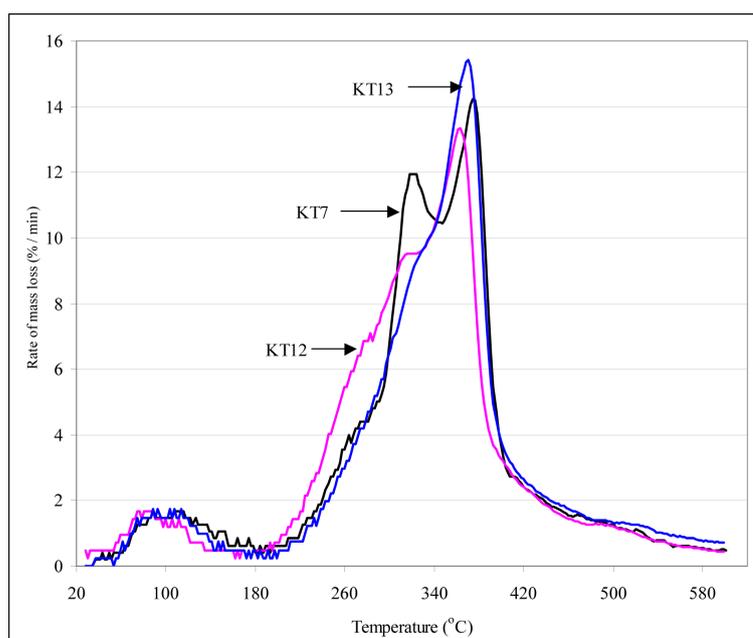


Figure 5. DTG curves of crude olive pomace samples.

maximum rates of mass loss for cellulose and hemicellulose are highest for pit fraction (sample KT24) and lowest for pulp fraction (sample KT23). The DTG curves shown in Figures 5-7 were analyzed to get quantitative information of the type given in Table 15. The results are collected in Table 16. It is seen in this table that samples KT23 (pulp of KT25) and KT32 (pulp-rich fraction of sample KT26) have hemicellulose peak temperatures appreciably lower than those of the other samples. In addition, the residual mass fraction given in the bottom row of Table 16 for sample KT32 seems unrealistic when compared with residual mass fractions of samples KT23 (pure pulp) and KT24 (pure pits). The cause of this result is very likely to be an equipment-related error such as a sudden high pulse of the flowing nitrogen gas. The detailed information given in Table 16 is transformed into concise form of ranges and averages as shown in Table 17. Whether we include or exclude sample

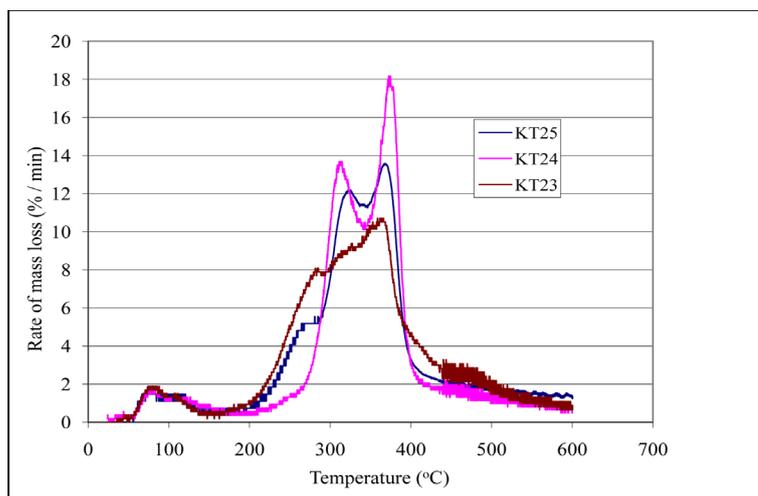


Figure 6. DTG plot of crude olive pomace and its pit and pulp fractions.

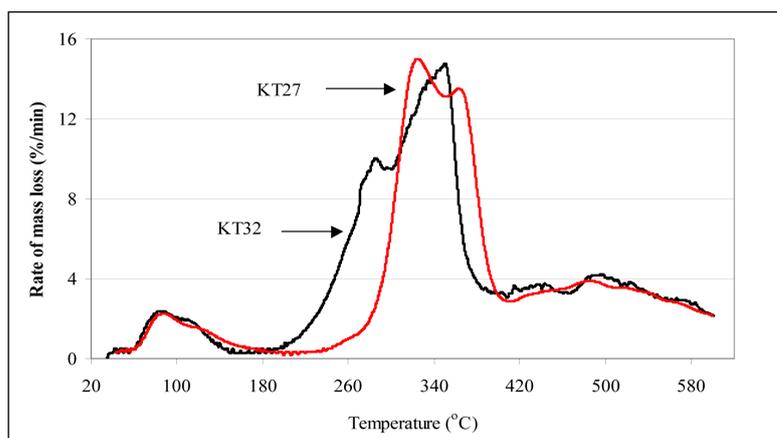


Figure 7. DTG plot of coarse and fine powder fractions of crude olive pomace.

Table 15. Maximum rate of mass loss and peak temperature of major derivatives on the DTG curves of oak, almond, and olive fire wood samples. Rates are given on dry basis.

Sample identity	KT8	KT9	KT14
Sample mass (mg)	11.78	13.43	10.44
Sample moisture (%)	5.60	4.86	4.81
Moisture peak temperature (°C)	90	93	90
Moisture maximum rate of mass loss (%/min)	2.2	2.5	2.4
Hemicellulose peak temperature (°C)	342	342	340
Hemicellulose maximum rate of mass loss (%/min)	11.7	13.5	10.8
Cellulose peak temperature (°C)	400	386	398
Cellulose maximum rate of mass loss (%/min)	19.2	19.4	19.3
Lignin peak temperature (°C)	525	^a n.d	n.d
Lignin maximum rate of mass loss (%/min)	1.6	n.d	n.d
Residual mass fraction at 600°C	0.24	0.23	0.23

^a: Not determined.

Table 16. Maximum rate of mass loss and peak temperature of major derivatives on the DTG curves of olive pomace samples.

Sample identity	KT7	KT12	KT13	KT23	KT24	KT25	KT27	KT32
Sample mass (mg)	14.33	12.66	12.13	9.13	9.30	12.00	12.61	11.29
Sample moisture (%)	6.78	5.35	5.25	6.00	6.00	6.00	6.94	8.74
Moisture peak temperature (°C)	80	82	80	74	68	80	89	88
Moisture maximum rate of mass loss (%/min)	1.3	1.8	1.5	2.0	1.5	1.2	2.2	2.1
Hemicellulose peak temperature (°C)	318	315	316	273	312	319	328	286
Hemicellulose maximum rate of mass loss (%/min)	12.6	9.4	8.9	7.9	14.2	12.3	14.8	10.0
Cellulose peak temperature (°C)	360	358	364	358	368	363	367	350
Cellulose maximum rate of mass loss (%/min)	14.4	14.0	15.3	10.5	18.1	13.8	13.1	14.7
Lignin peak temperature (°C)	^a n.o.	n.o.	n.o.	n.o.	n.o.	n.o.	486	500
Lignin maximum rate of mass loss (%/min)	n.o.	n.o.	n.o.	n.o.	n.o.	n.o.	3.9	4.1
Residual mass at 600°C	0.29	0.30	0.31	0.25	0.28	0.23	0.17	0.07

^an.o.: not observed.

Table 17. Ranges and averages of DTG peak values and peak temperatures for moisture and lignocellulosic components of crude olive pomace.

Parameter	Range	Average
Moisture peak temperature (°C)	68 - 89	80
Moisture ^a R max (%/min)	1.3 - 2.2	1.7
Hemicellulose peak temperature (°C)	273 - 328	308
Hemicellulose R max (%/min)	7.9 - 14.8	11.3
Cellulose peak temperature (°C)	350 - 368	361
Cellulose R max (%/min)	10.5 - 18.1	14.2
Residual mass fraction at 600 (°C)	0.07 - 0.31	0.24
^b Residual mass fraction at 600 (°C)	0.17 - 0.31	0.26

^a: Maximum rate of mass loss; ^b: If residual mass fraction at 600°C for sample KT32 is excluded.

KT32 from the average residual mass fraction in **Table 17**, the value of the average for olive pomace is a little bit higher than that of wood samples.

4. Conclusion

When properly dried at the premises of olive mills, sun-dried crude olive pomace can be marketed with moisture content of 10% or less; therefore much of its heat content is densified. Removal of extractives by solvent extraction reduces the calorific value of crude olive pomace by a factor of about 10%. Marketing crude olive pomace in loose or compact form has no significant effect on its gross calorific value. The loose form of crude olive pomace has about 21% of its mass in the form of grains with diameter >2 mm and about 47% of fine particles of diameter <0.5 mm. The remaining 32% fall within the range of these size limits. These fractions have different calorific values. Although the calorific value of olive pomace is substantially lower than that of kerosene and diesel, its low market price and its abundance and renewability pave the way for its use as an affordable substitute for space heating in Jordan. Because of its scarcity and high prices, local fire wood cannot compete with olive pomace for space heating in Jordan. The crude olive pomace of Jordan is relatively rich in volatiles with

mass percentage of 77.5%. Because of their low moisture content and low nitrogen and sulfur contents, the net calorific values of the studied crude olive pomace samples amount to about 92% of their gross calorific values. The results of the TG and DTG measurements indicate the conformity of the pyrolysis of the lignocellulosic matter of the crude olive pomace samples to the pyrolysis behavior of other agrocellulosic biomass residues. The data on proximate and ultimate analyses as well as the calorimetric data can be reliably considered for specification purposes of olive pomace in Jordan.

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References

- [1] Al-Shdeifat, S.M. and Al-Bdoor, H.A. (2009) Annual Report. National Center for Scientific Research and Agricultural Extension, Jordan.
- [2] Abu-Qudais, M. and Okasha, G. (1996) Diesel Fuel and Olive-Cake Slurry: Atomization and Combustion Performance. *Applied Energy*, **54**, 315-326. [http://dx.doi.org/10.1016/0306-2619\(95\)00077-1](http://dx.doi.org/10.1016/0306-2619(95)00077-1)
- [3] Al-Widyan, M.I., Tashtoush, G. and Khadair, A.I. (2002) Briquettes of Olive Cake as a Potential Source of Thermal Energy. *Journal of Solid Waste Technology and Management*, **28**, 51-59.
- [4] Jumah, R., Al-Kteimat, E., Al-Hamad, A. and Telfah, E. (2007) Constant and Intermittent Drying Characteristics of Olive Cake. *Drying Technology*, **25**, 1421-1426. <http://dx.doi.org/10.1080/07373930701536668>
- [5] Aljundi, I.H. and Jarrah, N.A. (2008) A Study of Characteristics of Activated Carbon Produced from Jordanian Olive Cake. *Journal of Analytical and Applied Pyrolysis*, **81**, 33-36. <http://dx.doi.org/10.1016/j.jaap.2007.07.006>
- [6] El-Sheikh, A.H., Sweileh, J.A. and Saleh, M.I. (2009) Partially Pyrolyzed Olive Pomace Sorbent of High Permeability for Pre-Concentration of Environmental Waters. *Journal of Hazardous Materials*, **169**, 58-64. <http://dx.doi.org/10.1016/j.jhazmat.2009.03.061>
- [7] Tawarah, K.M. and Rababah, R.A. (2013) Characteristics of Some Jordanian Crude and Exhausted Olive Pomace Samples. *Green and Sustainable Chemistry*, **3**, 146-162. <http://dx.doi.org/10.4236/gsc.2013.34018>
- [8] Mata-Sánchez, J., Pérez-Jiménez, J.A., Díaz-Villanueva, M.J., Serrano, A., Núñez-Sánchez, N. and López-Giménez, F.J. (2014) Development of Olive Stone Quality System Based on Biofuel Energetic Parameters Study. *Renewable Energy*, **66**, 251-256. <http://dx.doi.org/10.1016/j.renene.2013.12.009>
- [9] Garcia-Maraver, A., Terron, L.C., Zambrano, M. and Ramos-Ridao, A.F. (2013) Thermal Events during the Combustion of Agricultural and Forestry Lopping Residues. In: Mendez-Vilas, A., Ed., *Materials and Processes for Energy: Communicating Current Research and Technological Developments*, Formatex, 407-411.
- [10] Misra, M.K., Ragland, K.W. and Baker, A.J. (1993) Wood Ash Composition as a Function of Furnace Temperature. *Biomass and Bioenergy*, **4**, 103-116. [http://dx.doi.org/10.1016/0961-9534\(93\)90032-Y](http://dx.doi.org/10.1016/0961-9534(93)90032-Y)
- [11] ASTM Standard D3172 (2007) Standard Practice for Proximate Analysis of Coal and Coke. ASTM International.
- [12] Mayoral, M.C., Izquierdo, M.T., Andrés, J.M. and Rubio, B. (2001) Different Approaches to Proximate Analysis by Thermogravimetry Analysis. *Thermochemica Acta*, **370**, 91-97. [http://dx.doi.org/10.1016/S0040-6031\(00\)00789-9](http://dx.doi.org/10.1016/S0040-6031(00)00789-9)
- [13] Cantrell, K.B., Martin II, J.H. and Kyoung, S.R. (2010) Application of Thermogravimetric Analysis for the Proximate Analysis of Livestock Wastes. *Journal of ASTM International*, **7**, 1-13.
- [14] Parikha, J., Channiwalab, S.A. and Ghosal, J.K. (2005) A Correlation for Calculating HHV from Proximate Analysis of Solid Fuels. *Fuel*, **84**, 487-494. <http://dx.doi.org/10.1016/j.fuel.2004.10.010>
- [15] Gaur, S. and Reed, T.B. (1998) Thermal Data for Natural and Synthetic Fuels. Marcel Dekker, New York, 259.
- [16] Varol, M. (2006) Combustion and Co-Combustion of Olive Cake and Coalina Fluidized Bed. Thesis, Middle East Technical University, Ankara.
- [17] Parr 587 M-6400 (2011) Oxygen Bomb Calorimeter Operating Instruction Manual. Chapter 7, Parr Instruments Company, Moline.
- [18] ASTM Standard D5865-11A (2011) Standard Test Method for Gross Calorific Value of Coal and Cock. ASTM International, Appendix XI.
- [19] Marsh, K.N. (1987) Recommended Reference Materials for the Realization of Physicochemical Properties. Blackwell,

Oxford.

- [20] Meraz, L., Dominguez, A., Kornhauser, I. and Roja, F. (2003) A Thermochemical Concept-Based Equation to Estimate Waste Combustion Enthalpy from Elemental Composition. *Fuel*, **82**, 1499-1507. [http://dx.doi.org/10.1016/S0016-2361\(03\)00075-9](http://dx.doi.org/10.1016/S0016-2361(03)00075-9)
- [21] Brlek, T., Voca, N., Kricka, T., Levic, J., Vukmirovic, D. and Čolovic, R. (2012) Quality of Pelleted Olive Cake for Energy Generation. *Agriculturae Conspectus Scientificus*, **77**, 31-35.
- [22] Miranda, T., Esteban, A., Rojas, S., Montero, I. and Ruiz, A. (2008) Combustion Analysis of Different Olive Residues. *International Journal of Molecular Science*, **9**, 512-525. <http://dx.doi.org/10.3390/ijms9040512>
- [23] Integra Fuels. Typical Specifications of Olive Cake. <http://www.integra-fuels.com/olive-cake-pellets.html>
- [24] Gravalos, I., Gialamas, T., Koutsofotis, Z., Kateris, D., Tsiropoulos, Z., Xyradakis, P. and Georgiades, A. (2008) Energetic Study on Animal Fats and Vegetable Oils Using Combustion Bomb Calorimeter. *Journal of Agricultural Machinery Science*, **4**, 69-74.
- [25] NIST Chemistry Web Book, NIST Standard Reference Database Number 69. http://www.en.wikipedia.org/wiki/Heat_of_combustion
- [26] Heikkinen, J.M., Hordijk, J.C., de Jong, W. and Spliethoff, H. (2004) Thermogravimetry as a Tool to Classify Waste Components to Be Used for Energy Generation. *Journal of Analytical and Applied Pyrolysis*, **71**, 883-900. <http://dx.doi.org/10.1016/j.jaap.2003.12.001>
- [27] Sørum, L., Grønli, M.G. and Hustad, J.E. (2001) Pyrolysis Characteristics and Kinetics of Municipal Solid Wastes. *Fuel*, **80**, 1217-1227. [http://dx.doi.org/10.1016/S0016-2361\(00\)00218-0](http://dx.doi.org/10.1016/S0016-2361(00)00218-0)
- [28] Wu, C.H., Chang, C.Y. and Lin, J.P. (1997) Pyrolysis Kinetics of Paper Mixtures in Municipal Solid Waste. *Journal of Chemical Technology and Biotechnology*, **68**, 65-67. [http://dx.doi.org/10.1002/\(SICI\)1097-4660\(199701\)68:1<65::AID-JCTB610>3.0.CO;2-T](http://dx.doi.org/10.1002/(SICI)1097-4660(199701)68:1<65::AID-JCTB610>3.0.CO;2-T)
- [29] Yang, H., Yan, R., Chin, T., Liang, D.T., Chen, H. and Zheng, C. (2004) Thermogravimetric Analysis-Fourier Transform Infrared Analysis of Palm Oil Waste Pyrolysis. *Energy & Fuels*, **18**, 1814-1821. <http://dx.doi.org/10.1021/ef030193m>

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