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The Preparation of Mn-Fe/CNTs Catalyst at the Low-Temperature Selective Catalytic Reduction of NO with NH₃

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Abstract

The metal oxide catalyst was prepared by loading MnO_x and FeO_x on carbon nano-tubes (CNTs) with impregnation method. Then the catalyst was characterized by BET and XPS, and the effect of adding FeO_x on $M_nO_x/CNTs$ catalyst at the low-temperature selective catalytic reduction of NO with NH₃ was investigated. The results showed that the active components were loaded successfully and easily on the carriers by impregnation. The Mn-Fe/CNTs catalyst was chose 10% $Fe(NO_3)_3$ solution to impregnate Mn-Fe/CNTs. The species of active components loaded on the catalyst were Fe_2O_3 . The different concentration of impregnant solution played an important role for NO conversion in SCR with NH₃. With the increase of the concentration of impregnant solution, the NO conversion of catalysts was increasing initially then decreasing.

Keywords

Carbon Nanotubes, Catalyst, Low-Temperature Selective Catalytic Reduction

1. Introduction

 $\mathrm{NO_x}$ pollutants can cause lung irritation and inhibit the body's ability to fight off diseases such as influenza and pneumonia. Long-term exposures to high concentrations of nitrogen dioxide can produce chronic damage to respiratory tract tissue that resembles the lung disease emphysema. The free radical then can react with organic compounds in the air to form nitrogenated organic compounds, some of which have been shown to be mutagenic and carcinogenic. Further high levels of $\mathrm{NO_x}$ cause a variety of environmentally harmful effects

such as acid rain and urban smog; they also contribute to the greenhouse effect. Therefore, it has become important to reduce the emission of nitrogen oxides from both stationary and mobile combustion technologies in order to keep the health of humans and protect environment.

Among various NO_x emission control techniques, selective catalytic reduction (SCR) of NO with NH₃ in the presence of excess oxygen has been proven to be the most effective which is widely used. It has been proved that the catalyst being prepared through supported metallic oxides are with good catalytic performance. Various metal oxide based catalysts have been shown to possess some potential for low temperature application, including Mn₂O₃, CeO₂, V₂O₅, etc.. As a novel carbon material, carbon nanotubes (CNTs) have attracted much attention due to their unique electric, mechanical and structural characteristics. It has been widely studied in fields of high strength carbon fiber materials [1], hydrogen storage materials [2] [3] [4], new catalytic materials [4] [5] [6] [7] [8], etc. Due to one-dimensional tubular structure of CNTs, catalytic materials with specific properties can be prepared in the cavity of tubular. So as a new catalytic material, CNTs have caused attention of many researchers [9] [10] [11].

Therefore, it can be an issue deserved intensive study to make use of CNTs to study the low-temperature selective catalytic reduction of NO with NH₃. This research prepared Mn/CNTs catalyst through supported manganese oxide, then adding iron oxide on the CNTs after purification. We have investigated the effect of adding FeO_x on MnO_x/CNTs catalyst at the low-temperature selective catalytic reduction of NO with NH₃.

2. Experimental

2.1. Preparation of Catalyst

Immerse right amount of Mn/CNTs after purification in impregnating solution for 24 hours at room temperature, meanwhile, stir them with magnetic stirrer. Then, the end product of catalyst can be obtained after drying, cooling, grinding, and roasting the immersed catalyst. In the experiment, The ferric nitrate solution was choosed to prepare the two component catalyst.

2.2. Catalysts Characterization

We analyzed the catalysts characterization TEM and XPS of catalyst. Determine the TEM of catalyst by means of JEM-1200EX made in JEOL Ltd; XPS analysis can be carried out by making use of AXIS Ultra-type X-ray photoelectron spectroscopy made in England Kratos Company.

2.3. Catalytic Activity Tests

The catalytic activity tests were carried out in a fixed bed reactor made of stainless steel in the 150° C $\sim 300^{\circ}$ C range. The gas composition was 450 ppm NO, 500 ppm NH₃, 5% O₂ balanced by N₂. The total flow rate was 500 ml·min⁻¹. The experimental apparatus of evaluation of the catalytic activity tests included

sections of gas configuration, catalytic reaction and flue gas analysis, which was shown in **Figure 1**. NO concentrations in the inlet and outlet gases were measured by flue gas analyzer (KM940, Kane). The NO conversion was calculated from the NO concentration at the inlet and outlet of the reactor.

3. Results and Discussions

3.1. Catalysts Characterization

The surface morphology and microstructures of the catalysts can be observed directly by TEM. **Figure 2** showed the TEM image of Mn/CNTs catalyst, 10% Mn-Fe/CNTs, 20% Mn-Fe/CNTs.

The photographs of Mn/CNTs catalysts loaded with manganese oxides was in (1), (2) and (3) was photographs of the catalysts impregnated with different concentrations of ferric nitrate solution on Mn/CNTs catalysts. Metal oxide particles loaded on the CNTs was evenly on the surface of the carrier. Future researches should be worthy to be carried out to reveal the effect between the catalyst activity and the metal oxide particle dispersion. In addition, it can be seen that metal oxide particles supported on Mn/CNTs catalysts were relatively uniform and the agglomeration is smaller by adding ferric oxides, which improves the dispersion of the supported metal oxide particles.

Figure 3 illustrated the surface element concentration of Mn-Fe/CNTs catalyst by XPS spectra, in which (1), (2), (3), and (4) were separately Mn-Fe/CNTs catalyst spectra, O(1s) spectra, Mn (2p) spectra, and Fe (2p) spectra. The catalyst XPS spectra showed three obvious peaks, that the bigger binding energy on the left-side was the peak of 641 eV, which was the absorption peak of manganese; the binding energy in the middle peak was 530 eV, which was the absorption peak of oxygen; peak with the biggest binding energy was 284 eV, which was the absorption peak of carbon. The surface element concentrations of Mn-Fe/CNTs catalyst sample measured by XPS were: 87.27% of C, 7.48% of O, 3.44% of Mn, 1.64% of Fe. It can be seen from **Figure 3** that there was one peak respectively at the binding energy of 641.1 eV corresponded to MnO₂, which were consistent with the report of literature [6]. There were some peaks respectively at the binding energy of 710.9 eV, this corresponded to Fe₂O₃.

3.2. Effect of Temperature on SCR Activity of Mn/CNTs Catalyst

Figure 4 presented the effects of impregnant solution concentration to the NO conversion rate under different reaction temperature conditions.

It can be indicated from **Figure 4** that the NO conversion rate of catalyst prepared with different concentrations of impregnation increased with the rise of impregnant concentration under different reaction temperature conditions. The different concentration of impregnant solution played an important role for NO conversion in SCR with NH₃. With the increase of the concentration of impregnant solution, the NO conversion of catalysts was increasing initially then

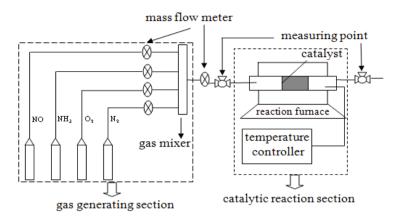


Figure 1. Experimental apparatus for activity test.

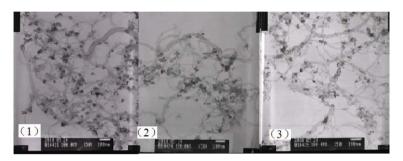


Figure 2. TEM image of samples: (1) Mn/CNTs; (2) 10%Mn-Fe/CNTs; (3) 20%Mn-Fe/CNTs.

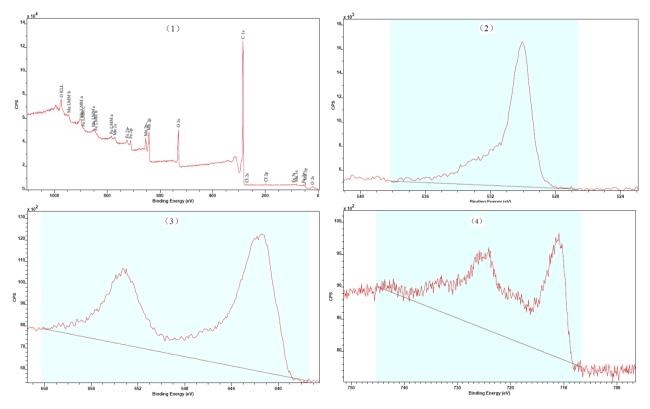


Figure 3. XPS spectra of the Mn-Fe/CNTs: (1)Mn-Fe/CNTs, (2) O(1s), (3) Mn (2p), (4) Fe(2p).

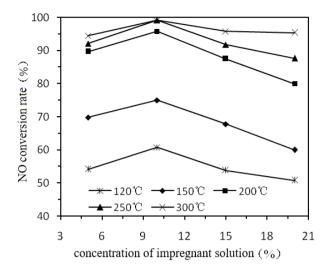


Figure 4. Effect of impregnant concentration on the activity of Mn-Fe/CNTs (Reaction conditions: 450 ppm NO, 500 ppm NH₃, $5.0\%O_2$, WHSV of $30,000 \, h^{-1}$).

decreasing. The NO conversion increased with increasing of impregnant concentration in the range of ratios from 5% to 10%. When the impregnant concentration continued to exceed 10%, the NO conversion decreased. For the impregnant concentration < 10%, the active sites provided by the catalyst surface was increased gradually. But excessive of impregnant concentration, the catalyst surface was overloaded with metal oxides, the surface area of the active substances on the catalyst surface decreased lead to the decease of the activity of the catalys.

4. Conclusions

The specific surface area of CNTs being the carrier of catalyst increased significantly after experiencing purification through nitration. Active components can load on the surface of CNTs with the augment of impregnation concentration of impregnating solution.

The species of active components loaded on the catalyst were MnO_2 and Fe_2O_3 . The different concentration of impregnant solution played an important role for NO conversion in SCR with NH₃. With the increase of the concentration of impregnant solution, the NO conversion of catalysts was increasing initially then decreasing.

Conflicts of Interest

The author declares no conflicts of interest regarding the publication of this paper.

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