

Consideration on the Flow Velocity in the Experimental Analysis of the Flame Displacement Speed Using DNS Data of Turbulent Premixed Flames with Different Lewis Numbers

Kazuya Tsuboi, Shingo Morishita, Eiji Tomita

Graduate School of Natural Science and Technology, Okayama University, Okayama, Japan

Email: tsuboi@okayama-u.ac.jp

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Abstract

The flame displacement speed is one of the major characteristics in turbulent premixed flames. The flame displacement speed is experimentally obtained from the displacement normal to the flame surface, while it is numerically evaluated by the transport equation of the flame surface. The flame displacement speeds obtained both experimentally and numerically cannot be compared directly because their definitions are different. In this study, two kinds of experimental flame displacement speeds—involving the mean inflow velocity and the local flow velocity—were simulated using the DNS data with the different Lewis numbers, and were compared with the numerical flame displacement speed. The simulated experimental flame displacement speed involving the mean inflow velocity had no correlation with the numerical flame displacement speed, while the simulated displacement speed involving the local flow velocity had a clear correlation with the numerical displacement speed in the cases of higher Lewis number than unity. The correlation coefficient of the simulated displacement speed involving the local flow velocity with the numerical displacement speed had a maximum value on the isosurface of the reaction progress variable with the maximum temperature gradient where the dilation effect of the flame is strongest.

Keywords

Flame Displacement Speed, Simulating Experimental Measurement and Analysis, Lewis Number, Dilation Effect, Turbulent Premixed Flame, Direct Numerical Simulation

1. Introduction

Turbulent flames are the configuration to have been widely used for actual combustors for automobiles, ships, aircraft, power generations, and industrial furnaces. To achieve further high efficiency and low emission of the actual combustors, it is necessary to investigate the detailed mechanism of turbulent combustion. Burning velocity is one of the major characteristics in turbulent premixed flames. In the various definitions of the burning velocity, turbulent burning velocity is a global quantity and is related to combustion efficiency, while the local burning velocity and the flame displacement speed are the dominant factors in the discussion of the local structure of turbulent premixed flames. The local burning velocity is the quantity based on the local consumption rate of the unburned mixture by the chemical reaction, while the flame displacement speed is the quantity based on the flame normal component of the speed, which a flame surface, defined as the isosurface of temperature or mass fraction of the unburned mixture, moves relatively to a flow [1]. It is not straightforward to measure the local chemical reaction rate using the current measurement technology, thus the local burning velocity can be obtained numerically only. Therefore, the flame displacement speed has been used for experiments instead of the local burning velocity. The flame displacement speed is experimentally obtained from the displacement normal to the flame surface, while it is numerically evaluated by the transport equation of the flame surface which is defined as the isosurface of the reaction progress variable. These flame displacement speeds obtained both experimentally and numerically cannot be compared directly because their definitions are different. Thus, it is necessary to investigate the relationship between the experimental and the numerical flame displacement speeds. The flame displacement speed involves flow velocity. In this relationship, the consideration of the flow velocity in the experimental flame displacement speed is also important.

Hartung *et al.* [2] developed the new experimental analysis and formulation of the flame displacement speed in turbulent premixed flames using stereoscopic particle image velocimetry (PIV) and time-sequenced OH-planar laser-induced fluorescence (PLIF). The two-dimensional flame displacement speed was measured as the projection of the three-dimensional flame displacement speed onto the plane defined by the laser sheets intersecting a flame. Chakraborty *et al.* [3] performed the DNS analysis on the flame displacement speed using the experimental definition of the two-dimensional flame displacement speed by Hartung *et al.* [2]. The flame displacement speed is essentially a three-dimensional quantity. Because it is difficult to measure the three-dimensional flame displacement speed experimentally, the flame displacement speed is measured as a two-dimensional quantity. They evaluated the correlation between the two-dimensional flame displacement speed, which was obtained from the experimental formulation by Hartung *et al.* [2], and the three-dimensional flame displacement speed, which was evaluated by the transport equation. They reported that the correlation was positive.

In our previous study [4], the experimental measurement and analysis on the two-dimensional flame displacement speed were simulated and analyzed using the DNS data with the different density ratios of the unburned mixture to the burned product. In the simulated analysis on the experimental flame displacement speed, the treatment of the local flow on the flame surface was discussed, and it was found that the correlation between the experimental and numerical flame displacement speeds was affected by the density ratio and the isosurface of the reaction progress variable due to the dilation effect of the flame.

In this study, the experimental measurement and analysis on the two-dimensional flame displacement speed were simulated using the DNS data with the different Lewis numbers. The two-dimensional flame displacement speed obtained with simulating the experimental measurement and analysis was compared with the two-dimensional flame displacement speed numerically evaluated by the transport equation, and subsequently the correlation between the both flame displacement speeds was shown. In the simulation of the experimental measurement and analysis, the flow velocity involved in the simulated experimental flame displacement speed was considered as the mean flow or the local flow, and the impact of their flows on the correlation between the simulated experimental and the numerical flame displacement speeds was also shown. The experimental measurement and analysis on the flame displacement speed were assessed on the basis of the results simulated them using the DNS data.

2. Numerical Analysis Method

2.1. DNS Database

The DNS database used for the numerical simulated analysis of the experimental measurement and analysis was

constructed with different Lewis numbers. These were $Le = 0.8$, termed case MI; $Le = 1.0$, termed case Mm; and $Le = 1.2$, termed case Mh. The simulations were carried out using the PRIMEPOWER HPC2500 installed at Nagoya University [5]. Details of the database are given in **Table 1**, and the computational domain is shown in **Figure 1**. The governing equations for constructing the database were the conservation of mass, chemical species, energy, and momentum (compressible Navier-Stokes equations), and the equation of state for an ideal gas. The database was constructed using a sixth-order central finite difference scheme in the mean flow direction and a spectral collocation method in the directions perpendicular to the mean flow for spatial discretization. A third-order three-step Runge-Kutta method was used for the time evolution and an overall single-step irreversible reaction was used to describe the chemical kinetics. The inflow and outflow boundaries were described on the basis of Navier-Stokes characteristic boundary conditions (NSCBC) [6] [7], and the lateral boundaries were periodic. The computational domain was 8 mm in the mean flow direction and 4 mm in the directions perpendicular to the mean flow; 512 and 128 grid points were used in the respective directions. At the inflow boundary, preliminary calculated homogeneous isotropic turbulence with a cycle of several milliseconds was used, with a mean inflow velocity assuming Taylor's hypothesis of frozen turbulence with a phase shift. Initially, a laminar premixed flame was formed, which grew to form a turbulent premixed flame. The inflow velocity of the unburned mixture was adjusted while monitoring the turbulent burning velocity until the turbulent premixed flame became fully developed and stabilised. The instantaneous turbulent burning velocity varied temporally; however, the time-averaged turbulent burning velocity, which can be measured experimentally, was steady. The database was constructed without changing the inflow velocity. Each case in the database consisted of almost 200 sampled data points at 51.68- μ s intervals (which was longer than the DNS time step). The conditions described in the database correspond to the boundary between wrinkled flamelets and corrugated flamelets in the turbulent combustion regime diagram [8]. Further details of the calculation method to construct the DNS database can be found in Nishiki *et al.* [9] [10] and Nishiki [11].

Table 1. The DNS database.

case	MI	Mm	Mh
ρ_u/ρ_b	5.00	5.00	5.00
Le	0.8	1.0	1.2
u_L^0 (m/s)	0.523	0.523	0.523
δ_f^0 (mm)	0.191	0.191	0.191
\bar{u}_{in} (m/s)	1.406	0.992	0.840
u'/u_L^0	1.01	1.01	1.01
λ/δ_f^0	10.7	10.7	10.7
l_i/δ_f^0	18.0	18.0	18.0
Re_λ	56.7	56.7	56.7
Re_t	95.5	95.5	95.5

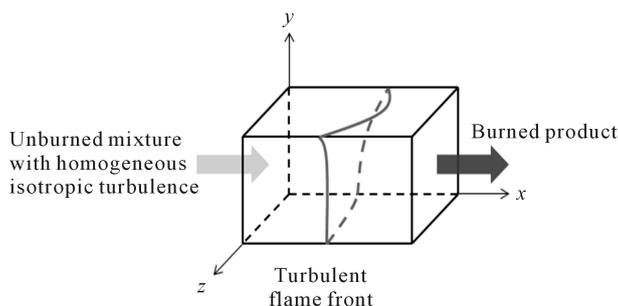


Figure 1. Computational domain.

2.2. Numerical Analysis Simulating Experimental Measurement

In this study, the DNS analysis simulated the experimental measurement and analysis of the flame displacement speed was performed in accordance with Renou *et al.* [12] [13]. The flame surface is experimentally measured as the two-dimensional cross section of a flame on a laser sheet using laser tomography. The analysis in this study was performed by simulating the experimental measurement and analysis using the data on the two-dimensional cross section parallel to the mean propagation direction of a flame in the three-dimensional DNS data of turbulent premixed combustion. The flame surface was identified as the isosurface of the reaction progress variable:

$$c_T = \frac{T - T_u}{T_a - T_u}, \quad (1)$$

where T is the temperature, T_a is the adiabatic flame temperature, and T_u is the temperature of the unburned mixture (300 K). Three isosurfaces of the reaction progress variable in all the cases were considered as follows: $c_T = 0.167$, the isosurface corresponding to 500 K where silicon oil droplets seeded in the unburned mixture evaporate [12] [13]; $c_T = 0.690$, the isosurface where the temperature gradient indicates a maximum value; $c_T = 0.900$, the isosurface where the reaction rate in the planar flame reaches a maximum value. Two-dimensional flame displacement speed simulating the experimental measurement and analysis was defined by two kinds of equations dependent on the treatment of the flow velocity involving in the flame displacement speed: u_d^{gi} using the mean inflow velocity on the upstream boundary as shown in **Figure 2(a)**,

$$u_d^{gi} = \frac{\rho}{\rho_u} \left(\left| \frac{\Delta \mathbf{x}}{\Delta t} \right| + \bar{u}_{in} \right); \quad (2)$$

u_d^{gn} using the local flow velocity defined as the normal component of the local flow velocity at each point on the flame surface as shown in **Figure 2(b)**,

$$u_d^{gn} = \frac{\rho}{\rho_u} \left(\left| \frac{\Delta \mathbf{x}}{\Delta t} \right| + \mathbf{u}^t \cdot \mathbf{n} \cos \alpha \right), \quad (3)$$

where ρ is the density, ρ_u is the density of the unburned mixture, $\Delta \mathbf{x}$ is the displacement vector of a flame, Δt is the time interval of measurement, \bar{u}_{in} is the mean inflow velocity, \mathbf{u}^t is the flow velocity vector at the time, t , and α is the angle between \mathbf{u} and unit normal vector to a flame surface, \mathbf{n} . The flame surfaces were measured experimentally every 0.167 ms in Renou *et al.* [12] [13], whereas the DNS data were sampled every 0.0517 ms. For the similar simulating analysis using the DNS data to the experimental measurement and analysis in Renou *et al.* [12] [13], Δt was 0.1551 ms as three times of the interval sampled the DNS data. The two-dimensional flame displacement speed evaluated by the transport equation of c_T ,

$$\frac{\partial c_T}{\partial t} + (\mathbf{u} + u_d^b \mathbf{n}) \cdot \nabla c_T = 0 \quad (4)$$

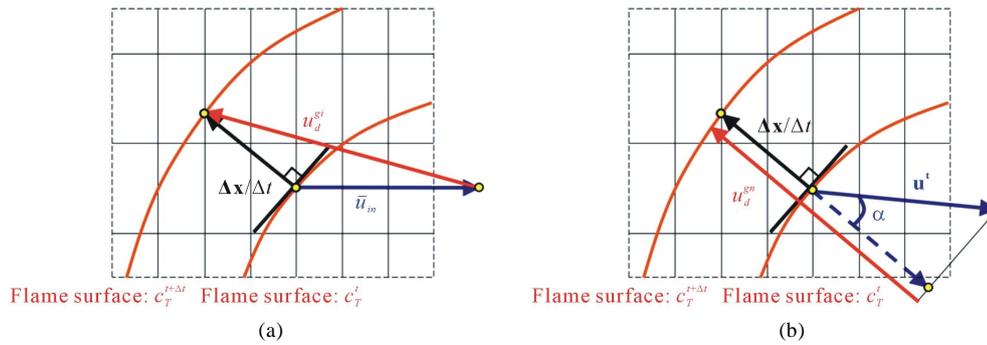


Figure 2. Schematic of simulating experimental analyses on the flame displacement speed. (a) u_d^{gi} obtained in consideration of the mean inflow velocity on the upstream boundary, (b) u_d^{gn} obtained in consideration of the normal component of the local flow velocity.

is defined as:

$$u_d^b = -\frac{1}{|\nabla c_T|} \left(\frac{\partial c_T}{\partial t} + \mathbf{u} \cdot \nabla c_T \right). \quad (5)$$

Note that u_d^{gi} , u_d^{gn} , and u_d^b were non-dimensionalised by the laminar burning velocity without flame stretch in each case after the next section.

3. Results and Discussion

3.1. Flame Displacement Speed Involving the Mean Inflow Velocity

The probability density functions (pdfs) of both u_d^{gi} as the simulated experimental flame displacement speed involving the mean inflow velocity and u_d^b evaluated by the transport equation on each isosurface of c_T in the different Lewis number cases are shown in **Figure 3**. In all Lewis number cases, the pdfs of u_d^{gi} disagreed with those of u_d^b . In each Lewis number case, however, the difference of the mode location between u_d^{gi} and u_d^b decreased with c_T , and the mode locations of both u_d^{gi} and u_d^b were very close especially in $c_T = 0.167$. c_T becomes larger in average in the downstream direction and smaller in average in the upstream direction. The flow velocity on the isosurface of $c_T = 0.167$ where is less affected by the flame than the isosurfaces of $c_T = 0.690$, 0.900 is close to the mean inflow velocity on the upstream boundary. Therefore, the pdf of u_d^{gi} involving the mean inflow velocity was similar to the pdf of u_d^b involving the local flow velocity in the isosurface of $c_T = 0.167$. The joint pdfs of u_d^{gi} with u_d^b on each isosurface of c_T in the different Lewis number cases are shown in **Figure 4**. The joint pdfs of u_d^{gi} with u_d^b in the isosurface of $c_T = 0.690$ had the largest probability density of the mode in the isosurfaces of c_T in each Lewis number case. However, the joint pdf of u_d^{gi} with u_d^b had almost no correlation in all cases. The correlation coefficients of u_d^{gi} with u_d^b on each isosurface of c_T in the different Lewis number cases are shown in **Figure 5**. The correlation coefficients were low values in all cases, even the largest coefficient on the isosurface of $c_T = 0.690$ in case Mh did not reach 0.3. This implies that the mean inflow velocity is not appropriate to the flow velocity involved in the flame displacement speed.

3.2. Flame Displacement Speed Involving the Local Flow Velocity

The pdfs of both u_d^{gn} as the simulated experimental flame displacement speed involving the normal component of the local flow velocity at each point on the flame surface and u_d^b in the different Lewis number cases are shown in **Figure 6**. The mode locations of u_d^{gn} and u_d^b in each isosurface of c_T were almost constant independent of the Lewis number. The shapes and the mode locations of the pdfs of u_d^{gn} in the isosurface of $c_T = 0.690$ were similar to those of u_d^b in case Mm, Mh. This indicates the possibility that u_d^{gn} is more appropriate definition of the experimental flame displacement speed than u_d^{gi} . The joint pdfs of u_d^{gn} with u_d^b on

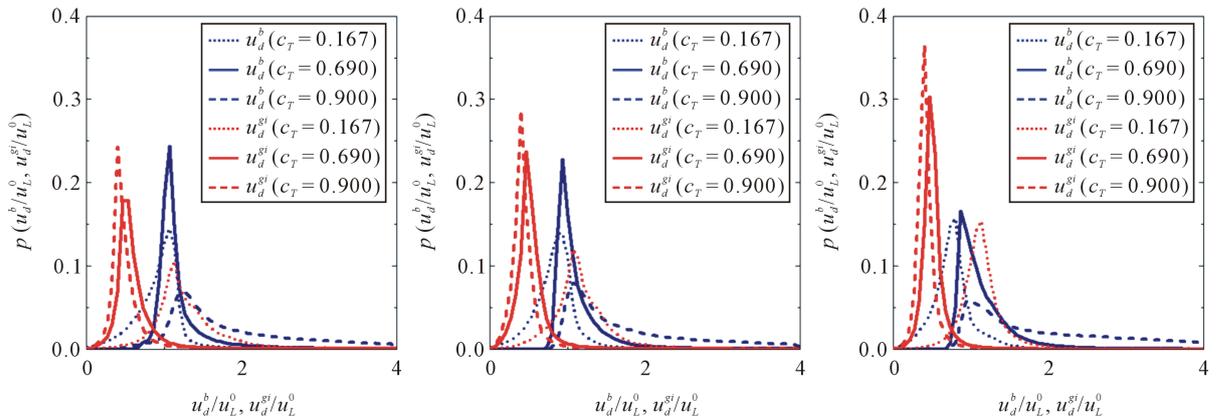


Figure 3. Probability density functions (pdfs) of non-dimensionalised u_d^{gi} and u_d^b on some isosurfaces of c_T with different Lewis numbers. From the left, case MI, case Mm, and case Mh.

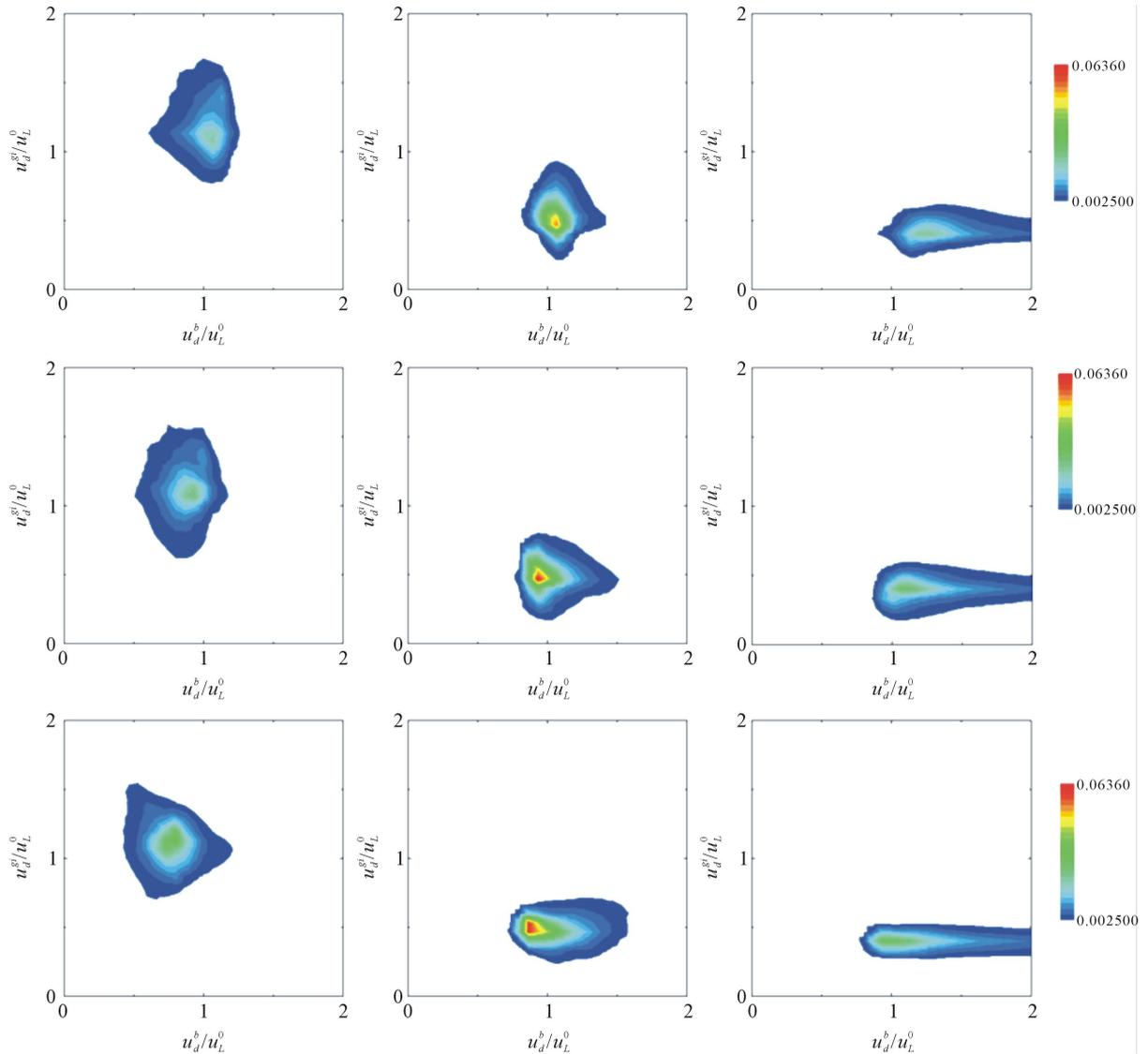


Figure 4. Joint pdfs between non-dimensionalised u_d^{gi} and u_d^b on some isosurfaces of c_T with different Lewis numbers. From the top, case Ml, case Mm, and case Mh, and from the left, $c_T = 0.167, 0.690, 0.900$.

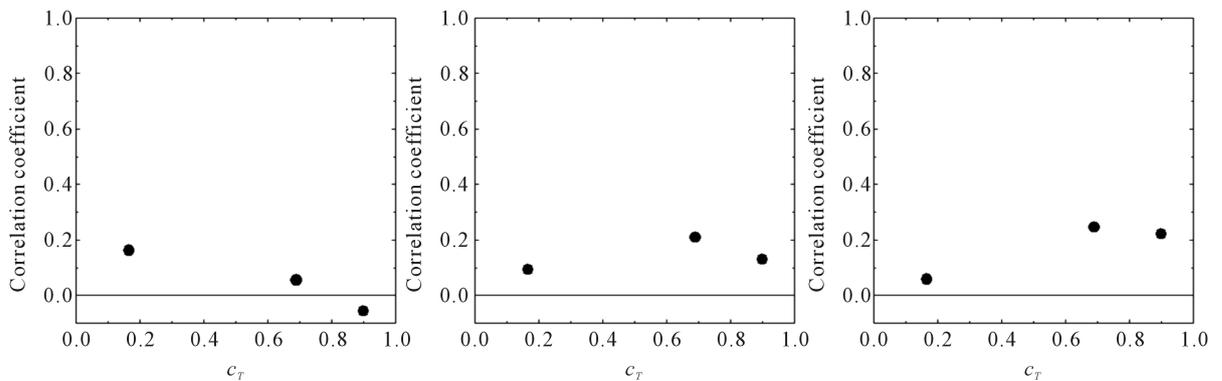


Figure 5. Correlation coefficients between non-dimensionalised u_d^{gi} and u_d^b on some isosurfaces of c_T with different Lewis numbers. From the left, case Ml, case Mm, and case Mh.

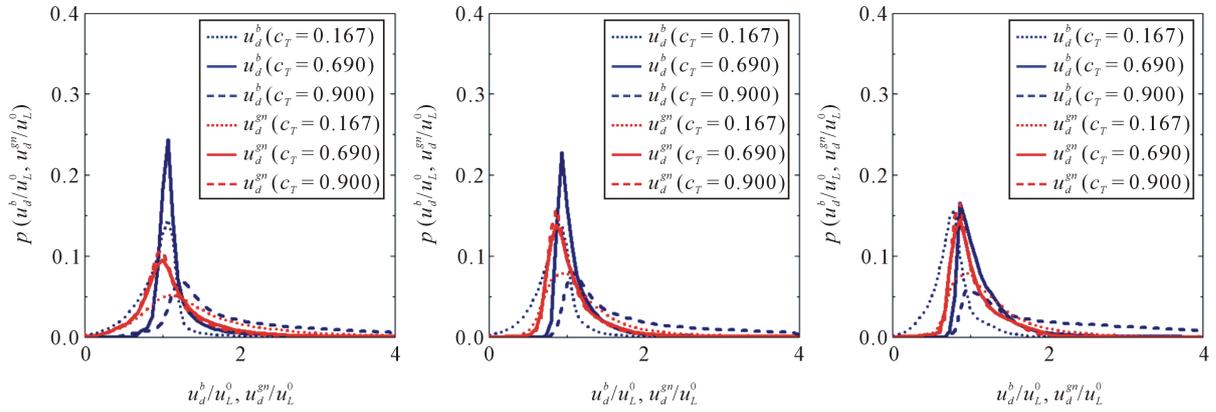


Figure 6. Pdfs of non-dimensionalised u_d^{gn} and u_d^b on some isosurfaces of c_T with different Lewis numbers. From the left, case MI, case Mm, and case Mh.

each isosurface of c_T in the different Lewis number cases are shown in **Figure 7**. The joint pdfs of u_d^{gn} with u_d^b in the isosurface of $c_T = 0.690$ had the largest probability density of the mode in the isosurfaces of c_T in each Lewis number case. In case MI, u_d^b was insensitive to u_d^{gn} in the isosurface of $c_T = 0.690$, and had no correlation with u_d^{gn} in other isosurfaces of c_T . In case Mm, Mh, u_d^{gn} had positive correlations with u_d^b in the isosurface of $c_T = 0.690$, and had indefinite but slightly positive correlations with u_d^b in other isosurfaces of c_T . The isosurface of $c_T = 0.690$ is where the temperature gradient indicates a maximum value, and thus where the dilation effect of the flame is strongest. u_d^{gn} had a clear correlation with u_d^b in the isosurface of $c_T = 0.690$ because the flame displacement speed is affected by the dilation effect of the flame [4]. The reason that u_d^b was insensitive to u_d^{gn} in the isosurface of $c_T = 0.690$ in case MI is considered to be the suppression of the dilation effect due to the predominance of the mass diffusion over the thermal diffusion in lower Lewis number than unity. The correlation coefficients of u_d^{gn} with u_d^b on each isosurface of c_T in the different Lewis number cases are shown in **Figure 8**. The correlation coefficient in the isosurface of $c_T = 0.690$ was highest and more than twice value in the case of u_d^{gi} in each Lewis number case. This means that u_d^{gn} involving the local flow velocity is more appropriate definition of the experimental flame displacement speed than u_d^{gi} involving the mean inflow velocity.

By comparing two kinds of experimental flame displacement speeds—involving the mean inflow velocity and the local flow velocity—with the numerical flame displacement speed, it was found that even if under the weak turbulence conditions in this study the local flow velocity is required to define the experimental flame displacement speed appropriately. However, the correlation coefficient which does not reach 0.6 is not so high, thus it is necessary to investigate the way to involve the local flow velocity in detail. Moreover, the fact—the correlation coefficient between the experimental and numerical flame displacement speeds is affected by Lewis number—means that the current experimental definition of the flame displacement speed is insufficient. It is also necessary to consider the way to incorporate the mass diffusion and the thermal diffusion into the definition of the experimental flame displacement speed.

4. Conclusion

The experimental measurement and analysis of the flame displacement speed were simulated using the DNS data of turbulent premixed flames with the different Lewis numbers, and the flame displacement speed obtained with simulating the experimental measurement and analysis was compared with the displacement speed numerically evaluated by the transport equation. The simulated experimental flame displacement speed involving the mean inflow velocity had no correlation with the numerical flame displacement speed, while the simulated displacement speed involving the local flow velocity had a clear correlation with the numerical displacement speed in the cases of higher Lewis number than unity. The correlation coefficient of the simulated displacement speed involving the local flow velocity with the numerical displacement speed had a maximum value on the isosurface of the reaction progress variable with the maximum temperature gradient where the dilation effect of the flame was strongest. Towards a more appropriate experimental flame displacement speed, it is necessary to

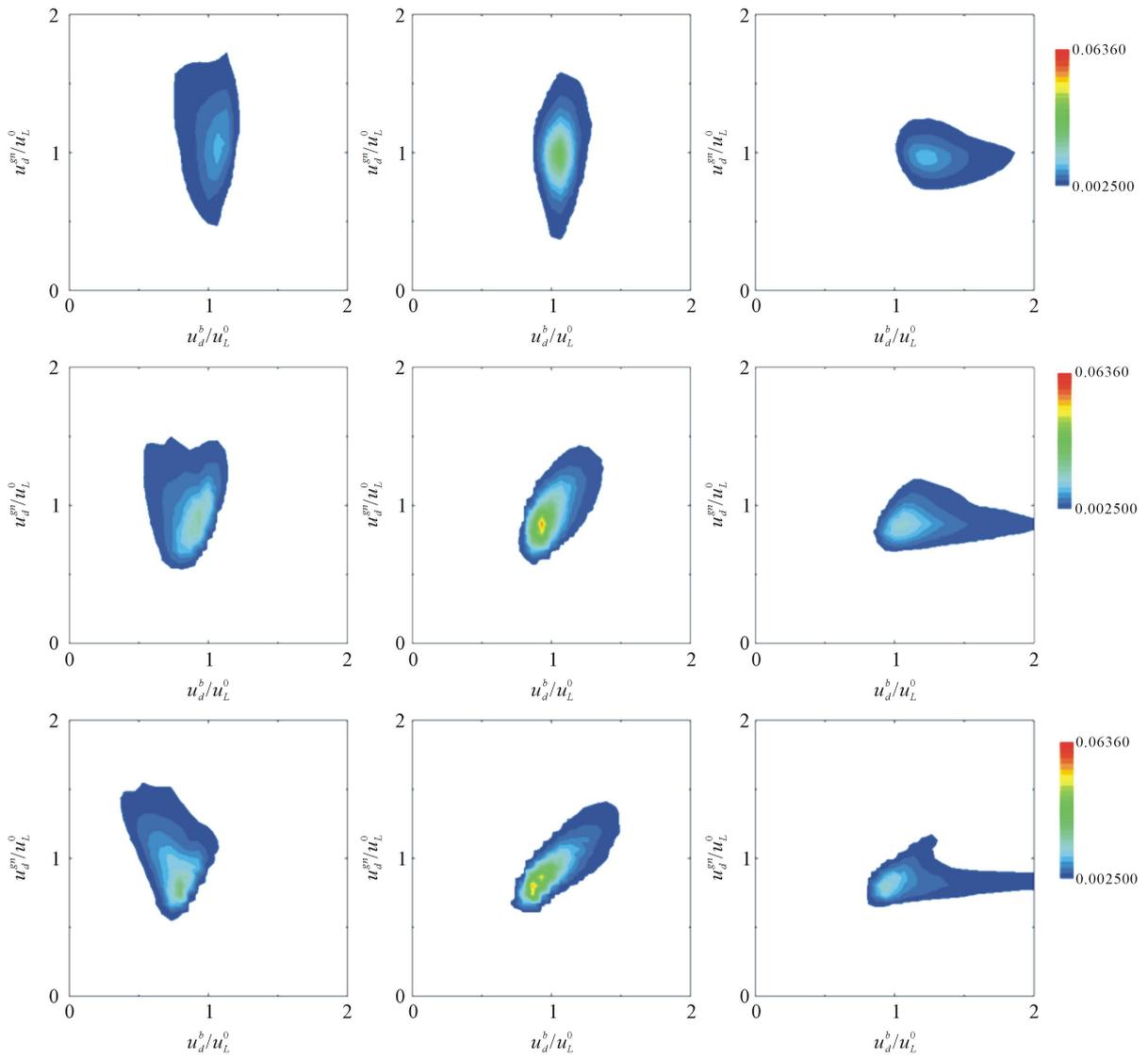


Figure 7. Joint pdfs between non-dimensionalised u_d^{gn} and u_d^b on some isosurfaces of c_T with different Lewis numbers. From the top, case Ml, case Mm, and case Mh, and from the left, $c_T = 0.167, 0.690, 0.900$.

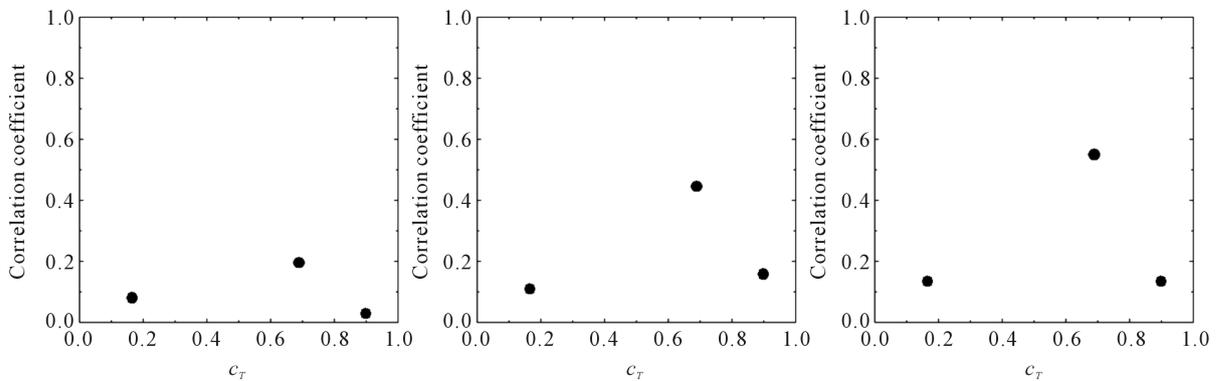


Figure 8. Correlation coefficients between non-dimensionalised u_d^{gn} and u_d^b on some isosurfaces of c_T with different Lewis numbers. From the left, case Ml, case Mm, and case Mh.

consider the treatment of the local flow velocity and the mass and thermal diffusions in the definition of the experimental displacement speed.

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Nomenclature

c_T	Reaction progress variable
Le	Lewis number
lt	Integral length scale
\mathbf{n}	Unit normal vector to a flame surface
Re_{lt}	Reynolds number based on integral length scale
Re_λ	Reynolds number based on Taylor microscale
T	Temperature
\mathbf{u}	Flow velocity vector
u'	Turbulence intensity
u_d^b	Flame displacement speed evaluated by the transport equation
u_d^{gi}	Flame displacement speed obtained in consideration of the mean inflow velocity on the upstream boundary
u_d^{gn}	Flame displacement speed obtained in consideration of the normal component of the local flow velocity
\bar{u}_m	Mean inflow velocity
u_L	Laminar burning velocity
u_T	Turbulent burning velocity
V	Total volume of the computation domain
Y	Mass fraction
α	Angle between \mathbf{u} and \mathbf{n}
Δt	Measurement time interval
$\Delta \mathbf{x}$	Displacement vector of a flame
δ_f	Flame thickness
λ	Taylor microscale
ρ	Density

Superscripts

0	Without flame stretch
t	At the time t
$t + \Delta t$	At the time $t + \Delta t$

Subscripts

a	In adiabatic condition
b	In burned product
u	In unburned mixture

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