

Thermodynamic and Dynamic of Chromium Biosorption by Pectic and Lignocellulosic Biowastes

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Abstract

Orange peel (OP) and rice husk (RH) were tested as low-cost biosorbents for Cr(III) removal from aqueous solutions. Dynamics of the biosorption process indicated that intraparticle mass transfer represents the rate-limiting step in the system that attained equilibrium at 120 min. While the OP sorbent material was capable of taking up 39.11 mg Cr(III)/g at the optimum pH 4.4, RH immobilized 3.20 mg Cr(III)/g at the optimum pH 3.0. The fitting of different sorption isotherms models resulted in the best fit with the Langmuir isotherm model. The mean free energy of the metal sorption process was in the range of 8-16 kJ/M. Abiotic Cr(VI) reduction was observed at various contact times and Cr-laden biomass was characterized by XPS, XAFS and EPR spectroscopy. These instrumental analyses confirmed that Cr(VI) removed from the solution was reduced and bound to the biomass as Cr(III). Results indicated that OP and RH materials are efficient biosorbents for eliminating Chromium from aqueous solutions.

Keywords: Chromium, Adsorption, Orange Peel, Rice Husk

1. Introduction

Chromium and its compounds are widely employed in industry [1] and Cr(III) is used as a tanning agent, resulting in severe groundwater contamination around tanneries [2,3]. Oxidation of polyuronic acids and pectin by hypervalent Chromium showed the presence of Cr(V), Cr(IV) and Cr(III)-saccharide complexes, with Cr(III)-pectin as an insoluble compound in the reaction media [4,5]. Following the treatment of Cr(VI) solution ($[\text{Cr(VI)}]_0 = 0.0176 \text{ M}$) with 1.0 g of D-polygalacturonic acid, only 10% of the total Cr ($\text{Cr}_T = \text{Cr(III)} + \text{Cr(VI)}$) remained in solution [5].

Different metal removal methods (ion exchange, chemical reduction and precipitation, reverse osmosis, phytoremediation, bioremediation, etc.) have been tested for detoxification of Chromium-laden wastewaters in the

recent years. However, these methods have high operating costs and problems in the disposal of the residual metal sludges. Biosorption techniques could use inexpensive sorbent materials as a feasible alternative for Chromium removal that features high efficiency, low operating costs with no adverse effects on the environment [6]. In recent years, several types of agricultural wastes such as sugarcane bagasse, grainless stalk of corn, etc. [7,8] have been applied with the aim of removing Chromium from wastewaters.

In this work, we study the behavior of biomaterials with different proportions of polyuronic acids when contacted with Chromium-containing wastewater. The study focused on easily obtainable waste materials such as orange peels (OP) and rice hulk (RH) which contain high proportions of pectin and lignin, respectively. XPS, XAS and EPR techniques were used to determine the oxida-

tion state of Chromium in the sorbent material, leading to establishing the mechanism of Chromium uptake/removal by OP and RH.

2. Experimental Section

2.1. Materials

The following analytical-grade reagents were used without purification: $K_2Cr_2O_7$, K_2CrO_4 , $Cr(NO_3)_3 \cdot 9H_2O$, Cr_2O_3 , Na_2CO_3 , $K_2S_2O_8$, $AgNO_3$, 1,5-diphenylcarbazine (DPC), and diphenylpicrylhydrazyl (dpph) (Sigma Grade). $Na[CrO(V)(ehba)_2] \cdot H_2O$ was synthesized [9].

OP was obtained from oranges harvested near the city of Rosario (Argentina) and RH came from a rice mill located in San Javier (Argentina). Both, OP and RH were washed with water, dried at 40°C for 12 h, powdered and sieved to retain the fraction of particles in the size range of 0.3–1.2 mm (OP) or 0.3–0.5 mm (RH), and were stored at room temperature in sealed polyethylene bags.

The reference solid compounds: oxidation state of Cr(VI) as K_2CrO_4 , Cr(V) as $Na[CrO(V)(ehba)_2] \cdot H_2O$, and Cr(III) as $Cr(NO_3)_3 \cdot 9H_2O$ and Cr_2O_3 .

2.2. Chromium Analysis

The $[Cr(VI)]$ was determined at 540 nm by using a double-beam UV-vis JASCO V-550 spectrophotometer after complexation with DPC [10]. $[Cr]_T = [Cr(VI)] + [Cr(III)]$ was determined by oxidizing Cr(III) to Cr(VI) using $K_2S_2O_8$ and $AgNO_3$ saturated solution as catalyst [11], prior to the DPC reaction. $[Cr(III)]$ was calculated as the difference between $[Cr]_T$ and $[Cr(VI)]$. The amount of Cr sorbed by the OP and RH biomass exposed to Cr(III) and Cr(VI) solutions was calculated from the difference between the initial chromium concentration of the control solutions and the final total Cr concentration in the respective supernatant solutions.

2.3. Spectroscopic Analysis

Cr-laden solid biomaterial samples were examined by EPR, XPS and XAS spectroscopy. The EPR spectra were derived on a Bruker ESP 300 E spectrometer at room temperature. XPS analyses were done with a SPECS system equipped with a hemispherical energy analyzer, a nine channeltron detector System and a double anode X-ray source. XAS experiments at the Cr K-edge (5989 eV) were carried out at beamline BL-9A with a ring energy of 2.5 GeV and a ring current of 450 mA. A double-crystal Si(111) monochromator was used, and the beam was focused using a pair of bent conical mirrors coated with Rh [12]. XAFS measurements were performed in a transmission mode for Cr-laden OP samples (Cr loading

4.9 wt%) and in fluorescence a mode for Cr-laden RH samples (Cr loading 0.71 wt%), respectively. The spectra of Cr-laden OP samples were recorded in transmission mode, with $N_2(30)$ -He(70) gas for the I_0 chamber and N_2 gas for the I chamber to monitor the incident and transmitted X-rays, respectively. On the other hand, the spectra of Cr-laden RH samples were collected in a fluorescence mode, using an argon-filled Lytle detector with a vanadium filter ($\mu t = 6$) for monitoring the fluorescent X-ray (I_f). The XANES spectra were measured with 0.35 eV steps and 1 s collecting time between 5980 and 6060 eV, while the EXAFS spectra were measured with 2.5 eV steps and 4 s (in transmission mode) or 8 s (in fluorescence mode) collecting time between 5500 and 7080 eV. XAFS data were analyzed with commercially available software (REX2000 program, Rigaku Co.). EXAFS analysis was performed as described in detail elsewhere [13]. The reference samples were used to compare their spectral shapes and to identify major Cr species on the biomaterial surface [14].

2.4. Batch Studies

2.4.1. Effect of pH, Contact Time and Biomass Dosage on Cr(III) Adsorption

Batch equilibrium sorption studies were carried out at $20.0 \pm 1.0^\circ C$. Biomaterials were suspended in Erlenmeyer flasks with an appropriate volume of work under constant stirring. $[Cr(III)]_0$ was 0.77 mM and 0.44 mM for OP and RH respectively. pH ranged from 0.2 to 5.2; pH was constantly controlled using a pH controller. A total amount of 5.0 g and 1.25 g of RH and OP, respectively, was used in these experiments. Time-based sorption uptake studies (process dynamics, including mass transfer and reaction) were carried out at $20.0 \pm 1^\circ C$, using a series of 150 mL Erlenmeyer flasks. For Cr(III) sorption by OP, 1.50 g was suspended in 75.0 mL of Cr(III) solution at pH 4.0. Cr(III) sorption by RH was performed using 5.0 g of sorbent suspended in 50.0 mL of Cr(III) solution at pH 3.0. Mixtures were magnetically stirred and samples withdrawn at different time intervals followed by centrifugal solids separation. Clear supernatants were analyzed for their Cr content. Separate controls were maintained for each period of time. All experiments were performed in triplicate for statistical purposes.

2.4.2. Adsorption Isotherms

Equilibrium sorption experiments were performed under optimum conditions derived using factorial design. The sorbent material (OP or RH) was exposed to varying concentrations of Cr(III) in Erlenmeyer flasks containing 75.0 mL or 50.0 mL of solution. The pH was adjusted to 4.4 or 3.0 for OP or RH, respectively. The biosorbent

dosage was 1.45 g and 5.65 g for OP and RH, respectively. The Cr(III) adsorption experiments were performed at $20.0 \pm 0.1^\circ\text{C}$. Mixtures were stirred for 120 min to reach equilibrium and then centrifuged. The supernatants were analyzed for their Cr content. All experiments were performed in triplicate for statistical purposes.

3. Results and Discussion

3.1. Cr-laden Biomaterials Spectroscopic Characterization

Characterization of the Chromium oxidation state on the surface of the biomaterial would establish if Cr(VI) adsorption-reduction mechanism contributes to its removal from the aqueous solution. Grainless stalk of corn (GLSC), an agricultural waste, was tested as a reference biomass for sorption and reduction of Cr(VI) [8]. The reduction took place mainly in the presence of solid biomaterial. High-resolution XPS of Cr-laden GLSC showed the presence of Cr(V) and Cr(III) at short contact time (**Figure 1(a)**) and only Cr(III) at prolonged contact time (**Figure 1(b)**).

The present experimental results support the conclusion of Park *et al.* [16] that the mechanism of Cr(VI) removal by GLSC is Cr(VI) sorption-coupled reduction to Cr(III) and partial complexation of Cr(III).

Figure 2 shows XPS spectra of Cr-laden OP. As can be seen in the high-resolution XPS spectrum of long-exposure Cr-laden OP, it was Cr(III) that became bound to the sorbent. While at short contact time, the amount of Cr sorbed by OP was below the XPS detection limit giving thus no discernible spectrum, at long contact times the amount of Cr sorbed was sufficient to produce an XPS spectrum with a Cr signal. Similarly, no chromium signal could be detected in the XPS spectrum of Cr-laden RH where Cr was still below the apparatus detection limit. The detection of intermediate states of Chromium for short contact times could be improved employing a more sensitive spectroscopic technique such as EPR. The EPR spectra are shown in **Figures 3** and **4**.

EPR spectra of Cr-laden OP and Cr-laden RH for different contact-time samples exhibit a sharp signal at $g_{\text{iso}} = 1.9788$ and $g_{\text{iso}} = 1.9785$, respectively, characteristic of Cr(V), superimposed on a broad signal (~ 600 G) at $g_{\text{iso}} \sim 2.00$, typical of Cr(III). The intensity of this broad signal increased for longer-contact time samples while the sharp Cr(V) signal diminished and finally disappeared, indicating thus that Cr(V) in these biosorbents was further reduced to Cr(III). The g_{iso} value of the Cr(V) EPR signal provides useful information on the nature and number of donor groups bound to Cr(V). The g_{iso} values 1.9788 and 1.9785 correspond to oxo-Cr(V) bound to

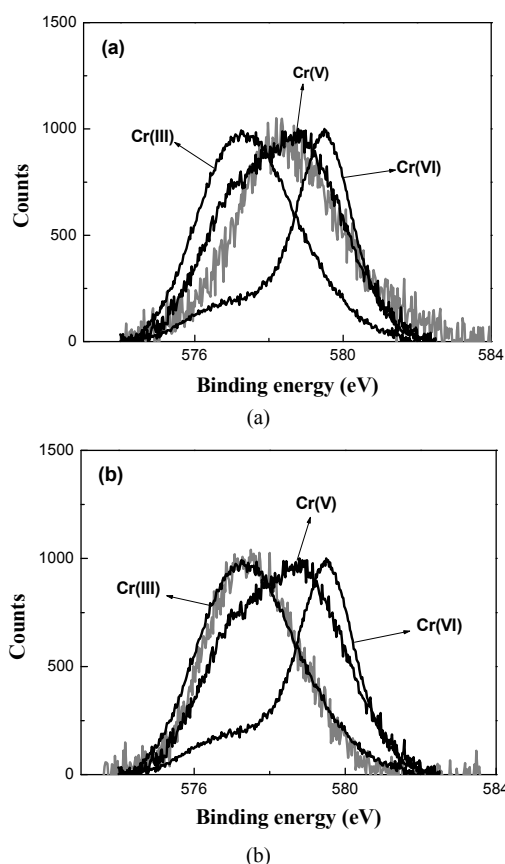


Figure 1. High-resolution XPS of Cr(VI)-laden GLSC. $\text{Mass}_{\text{GLSC}} = 0.3$ g; $V = 25.0$ mL; $\text{pH} = 0.9$; $[\text{Cr(VI)}] = 624$ mg/L; contact time: (a) 12 h; (b) 1 week.

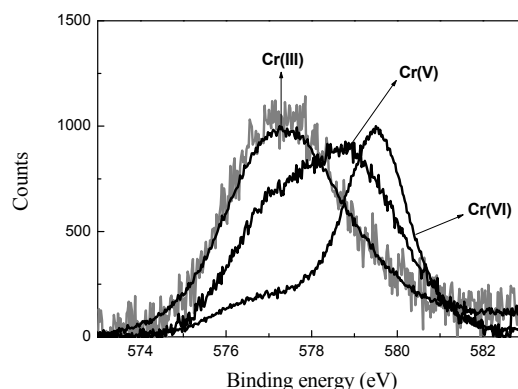


Figure 2. High-resolution XPS of Cr(VI)-laden OP. $\text{Mass}_{\text{OP}} = 0.3$ g; $V = 25$ mL; $\text{pH} = 2$; $[\text{Cr(VI)}] = 624$ mg/L; contact time: 1 week.

carboxylate and alcohol groups [17]. The detection of Cr(V) bound by OP and RH biomaterials reinforces the sorption-reduction model hypothesis for the removal of Cr(VI) by these biosorbents. In both sorbents exposed to Cr(VI), Cr(III) was the final species as can be seen in the EPR and XPS spectra.

XPS spectroscopy was also employed for detection of

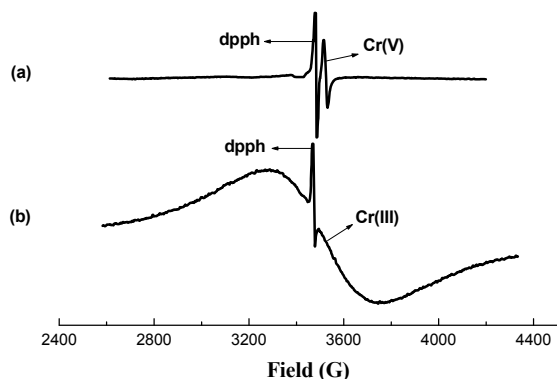


Figure 3. EPR spectra of Cr-laden OP at various contact time. $\text{Mass}_{\text{OP}} = 0.2 \text{ g}$; $V = 75 \text{ mL}$; $\text{pH} = 2.0$; $[\text{Cr(VI)}]_0 = 624 \text{ mg/L}$; contact time: (a) 12 hs; (b) 1 week.

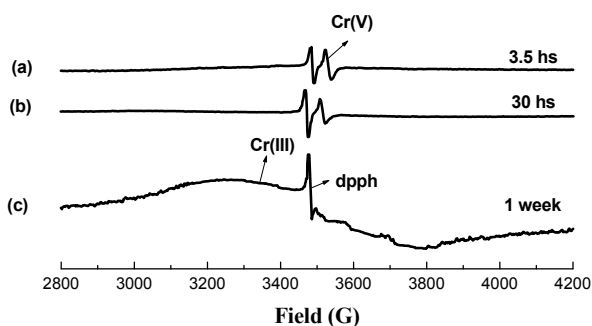


Figure 4. EPR spectra of Cr-laden RH at various contact time. $\text{Mass}_{\text{RH}} = 0.2 \text{ g}$; $V = 50 \text{ mL}$; $\text{pH} = 2.0$; $[\text{Cr(VI)}]_0 = 624 \text{ mg/L}$; contact time: (a) 3.5 hs; (b) 30 hs; (c) 1 week.

Cr(III) in metal-laden biomaterials and compared with a model complex Cr(III)-pectinate and Cr_2O_3 .

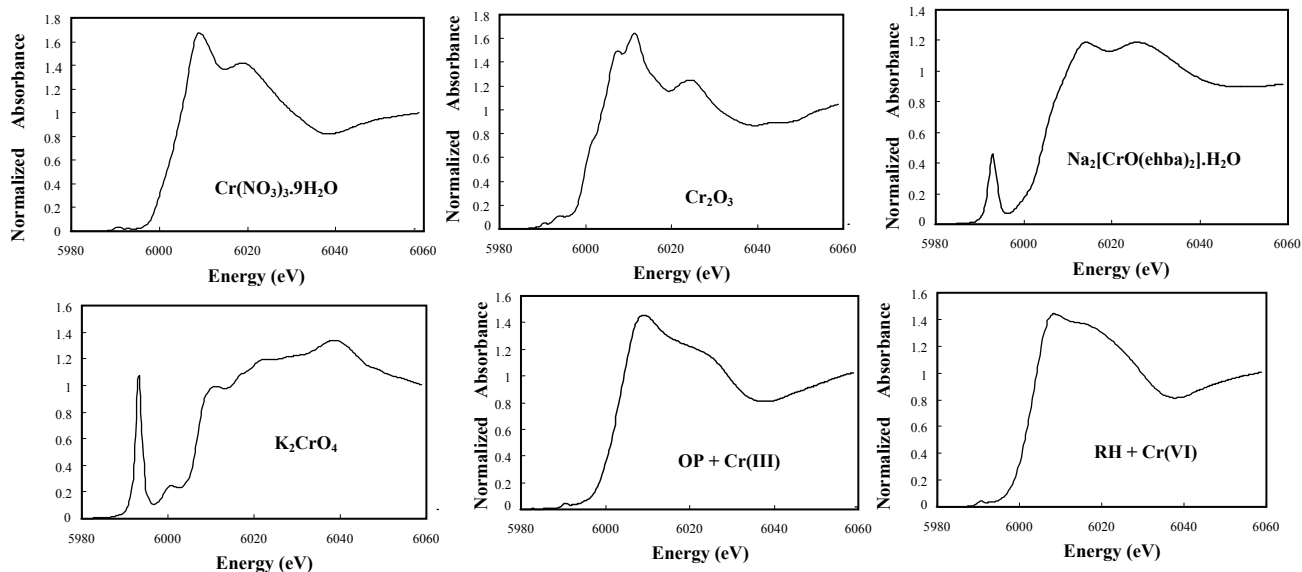


Figure 6. Cr K-edge XANES spectra of solid samples.

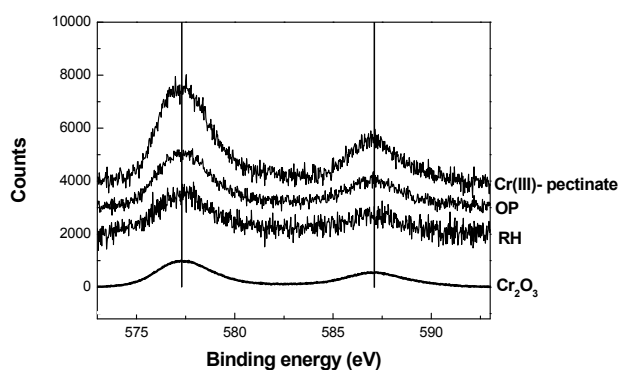


Figure 5. High-resolution XPS of Cr(III)-laden biomaterials. $\text{Mass}_{\text{biomaterial}} = 0.3 \text{ g}$; $V = 25 \text{ mL}$; $\text{pH} = 4$; $[\text{Cr(III)}] = 624 \text{ mg/L}$; contact time: 1 week.

High-resolution XPS spectra collected from the Cr2p core region indicated that there were significant contributions of the Cr bound to the biomaterials. **Figure 5** shows bands of Cr_2O_3 (576.8 and 586.7 eV). The spectra of all the Cr(III)-laden biomaterials (OP, RH) could well be matched with that of the Cr_2O_3 , similarly as with Cr(III)-pectinate. This fact indicates that Cr(III) is bound to oxygen atoms in the solid structures of the biosorbent. The XANES data were used to verify the oxidation state of the Cr(VI)- or Cr(III)-laden biomass. **Figure 6** shows the normalized Cr K-edge XANES spectra of reference compounds. The XANES data for Cr(III) standards show a small peak at 5990.5 eV, while those for Cr(V) and Cr(VI) show a pre-edge peak at 5993.0 and 5993.3 eV, respectively. The edge energy and the intensity of pre-edge absorbance decrease in the following order:

Cr(VI) > Cr(V) > Cr(III). The octahedral symmetry in XANES spectra of Cr(III) compounds is characterized by small resonances in the pre-edge region as signed to transitions of 1s electrons into antibonding orbitals with octahedral symmetry [18] whereas Cr(0) (body centered cubic) shows a broad pre-edge conduction band feature. The XANES data for K_2CrO_4 show the well-defined pre-edge peak from 5990 to 5997 eV [19], and for $Na[Cr(V)O(ehba)_2] \cdot H_2O$, the pre-edge peak position is consistent with that reported in the literature [20].

On the other hand, both Cr(III)-laden OP and Cr(VI)-laden RH samples do not show a pre-edge peak between 5990 and 5997 eV, and they have a small peak at 5990.5 eV, indicating the presence of Cr(III) binding in both biomaterials. It is also evident that Cr(III) is bound in the OP and Cr(VI) sorbed by the RH is completely reduced to Cr(III). This is quite consistent with the XPS and EPR results. EXAFS spectroscopy was employed to determine the local atomic structure of Cr in Cr(III)-laden OP and Cr(VI)-laden RH biomaterials. The experimental Fourier transform results are shown in Figure 7 and the curve-fitted values are given in Table 1.

For $Cr(NO_3)_3 \cdot 9H_2O$, the k^3 -weighted FT function gave a main peak centered at 1.60 Å which arises from first-shell oxygen back-scattering and another smaller peak centered at ~3.15 Å (phase-uncorrected). Three main peaks at 1.60, 2.52, and 3.31 Å (phase-uncorrected) could also be observed for the Cr_2O_3 compound, assigned to the first, second, and third shell contributions of a Cr(III) in an octahedral symmetry, respectively. For $Na[Cr(V)O(ehba)_2] \cdot H_2O$, a main peak is observed at 1.47

Å. The structure of the first coordination shell in the Cr(V) seems to be similar to that in the Cr(III). The Fourier transformed EXAFS spectra for the Cr(III)-laden OP and Cr(VI)-laden RH biomaterials were very similar to those for Cr(III) reference compound. This result means that the coordination environment of the chromium on the OP and RH biomaterials was also similar to that of Cr(III) compound, where Cr(III) is in an octahedral geometrical arrangement. The Cr-O bond distances were approximately the same lengths, which corresponds to the Cr-O bond lengths cited in the literature [18,21,22]. Cr(III)-laden OP sample showed the presence of the second and third peaks of Cr_2O_3 allowing thus a guess as to the formation of Chromium polynucleate species [23]. For the curve-fitting to determine the structural parameters, phase and amplitude functions for the absorbing and back-scatterer (Cr, O) pair were extracted from the filtering of the first peak of the EXAFS Fourier transform

Table 1. Cr K-edge EXAFS fitting results for reference samples and Cr-laden biomaterials.

Sample	Bond	CN	r (Å)	ΔE (eV)	σ (Å)	R (%)
Cr_2O_3	Cr-O	5.7	1.97	0.238	0.063	0.226
$Na[CrO(ehba)_2]$	Cr-O	2.4	1.91	-0.961	0.075	7.847
K_2CrO_4	Cr-O	3.8	1.66	1.089	0.066	1.931
OP + Cr(III)	Cr-O	6.1	1.97	-0.903	0.072	0.261
RH + Cr(VI)	Cr-O	5.2	1.96	-1.605	0.049	0.456

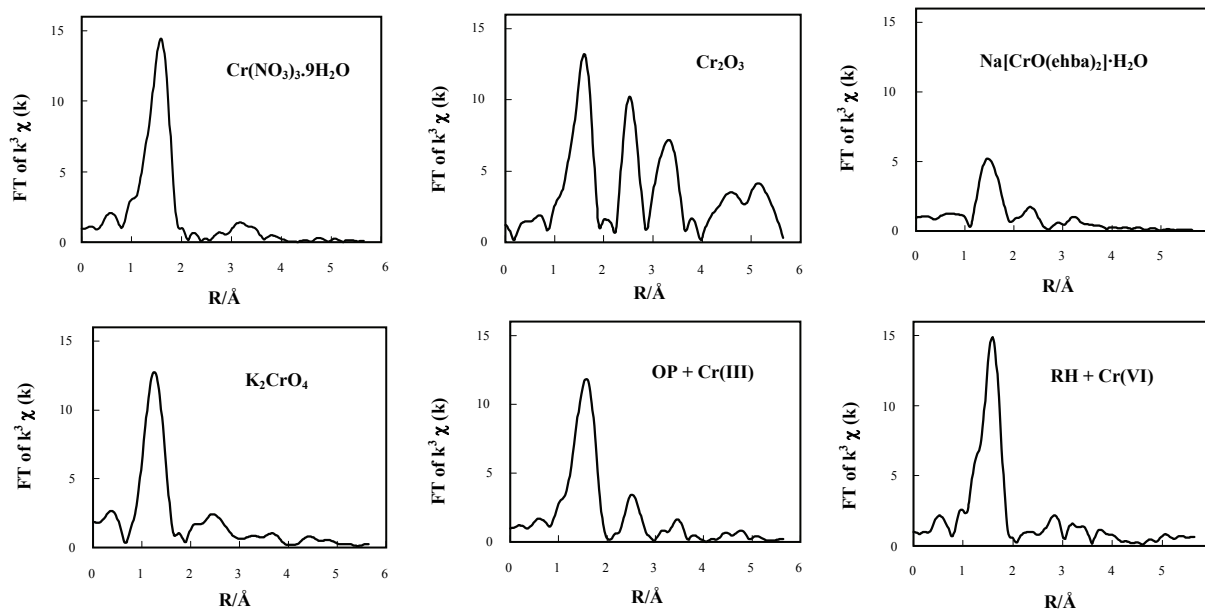


Figure 7. Fourier-transformed EXAFS spectra of solid samples.

of $\text{Cr}(\text{NO}_3)_3 \cdot 9\text{H}_2\text{O}$, where the chromium absorbing atom is surrounded by 6 oxygen atoms at the bond distance of 1.96 Å [21].

3.2. Effect of pH

The effect of pH, on the removal of Cr(III) by OP and RH is shown in **Figure 8**. The uptake of Cr(III) ion increased with increasing pH and OP biomaterial was more efficient in the removal. At $\text{pH} \leq 1.0$ there was a small adsorption, less than 7-25% for RH or OP respectively and Cr(III) removal yield increased up to 86-98% at pH 3.0-4.0 for OP. RH showed a capacity something smaller than OP for Cr(III) adsorption. In spite of employing four times biomass, only 78.0-85.0% was achieved at pH 3.0-4.0. At lower pH values, the higher $[\text{H}^+]$ effectively leads to fewer ligands being available for metal ions binding [24]. According to the pH dependence of this biosorption process, deprotonation of the carboxylic groups of uronic pectin moieties [4,5] might be involved. Increasing pH, surfaces becomes deprotonated, resulting in more ligand groups available for Cr(III) cations binding and electrostatic attraction available from carboxylate groups is likely enhanced. Thus, at high pH values where the $[\text{H}^+]$ is very low, carboxylic groups from OP and RH work as ion exchanger, where protons are released in the solution while metal ions are sorbed.

3.3. Sorption Process Dynamics

Reaction kinetics of the sorption process that is based on ion exchange is inherently very fast and studying it is experimentally difficult and inaccurate. With biosorbent particles involved that are “transparent” to ionic species, it is predominantly the intraparticle mass transfer that is observed externally and that represents the rate-limiting

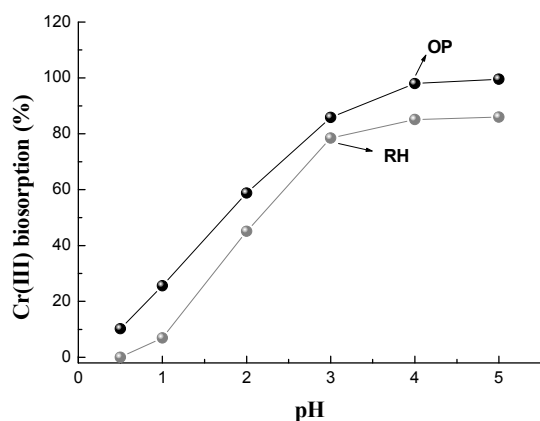


Figure 8. Effect of pH on the removal of Cr(III) by OP and RH. $T = 20^\circ\text{C}$; $V = 75.0 \text{ mL}$; $[\text{Cr}(\text{III})]_0 = 0.77 \text{ mM}$ (OP) and 0.44 mM (RH); mass = 5.0 g (OP) and 1.25 g (RH).

step. With easily accessible surface layers of the particles saturating first and fast, biosorption of Cr(III) onto OP and RH features two apparent steps, a fast initial sorption followed by a slower phase that reflects the penetration of sorbate into the particles. Correspondingly, the biosorption uptake increased sharply in the first 30 min, with more than 80% of Cr(III) taken up, and then continued increasing only at much slower rate. The sorption system equilibrium was reached in less than 120 min. A distinct two-step behavior has often been reported for metal ion biosorption. While Liu and Huang [25] attributed the two-step sorption characteristic to the heterogeneity of the surface binding sites on sorbents, Qin *et al.* [26] asserted that the fast initial sorption was the result of the fast transfer of metal ions to the surface of biomaterial, followed by a relatively slow uptake caused by the slow diffusion of metal ions into the intra-particle spaces of sorbents.

We tested of three kinetic models approach in order to establish the mechanism of Cr(III) adsorption onto OP/RH. Pseudo-first-order kinetic model (Lagergren [27]) is:

$$\frac{dq}{dt} = k_1 (q_e - q_t) \quad (1)$$

Pseudo-second-order kinetic expression (Ho [28]) is:

$$\frac{dq_t}{dt} = k_2 (q_e - q_t)^2 \quad (2)$$

k_1 (1/min) and k_2 (g/mg min) are the equilibrium rate constant of pseudo-first and pseudo-second order sorption respectively, and q_e and q_t are the amounts of solute sorbed per unit adsorbent at equilibrium (mg/g) and at time t , respectively.

Separating variables of (2), integrating and reordered one can obtain the following lineal expression:

$$\frac{t}{q_t} = \frac{1}{k_2 q_e^2} + \frac{t}{q_e} \quad (3)$$

The intraparticle diffusion model (Weber-Morris [29]) is:

$$q_t = k_{\text{dif}} t^{0.5} + C \quad (4)$$

where k_{dif} is the intraparticle diffusion rate constant and C can be obtained from the slope and intercept of the plot q_t vs. $t^{0.5}$.

The correlation coefficient (R^2) of pseudo-first-order (1), are nearly 0.86 (OP) and 0.54 (RH), and q_e calculated with (1) are lower than the experimental q_e . Therefore, the pseudo-first-order equation is not a good fit for Cr(III) adsorption on OP and RH.

The kinetic adsorption data were further fitted by the pseudo-second-order kinetic model, using (3). **Table 2** shows the experimental q_e , k_2 , R^2 values, and the calculated q_e values which agree perfectly with the experimental q_e values. Those results indicate that the rate-limiting step is a chemical sorption involving valance

Table 2. Kinetic parameters from pseudo-second-order for Cr(III) sorption.

Biomaterial	k_2 (g/mg min)	q_e (exp) (mg/g)	q_e (calc) (mg/g)	R^2
OP	0.14	0.83	0.88	0.9975
RH	2.26	0.40	0.42	0.9997

force through sharing between adsorbent and adsorbate.

The intraparticle diffusion kinetic model (4) provides information about the nature of the adsorption process [29]. A plot of q_t vs. $t^{0.5}$ for Cr(III) adsorption on OP and RH afforded two linear sections. A deviation of the straight line from the origin indicates that the intraparticle diffusion is not the only rate controlling step [30] and boundary layer diffusion controls the adsorption to some. If the regression of q_t vs. $t^{0.5}$ is linear and passes through the origin, intraparticle diffusion is the sole rate-controlling step [31]. The first straight portion was attributed to the fast mass transfer of sorbate molecules from the bulk solution to the sorbent surface and the second linear portion to the slower intraparticle diffusion into the biosorbent. Similar results were found for acid dye adsorption on activated palm ash [32].

Additionally, the kinetic model proposed by Boyd *et al.* [33] was applied to check that sorption proceeds via surface uptake followed by intra-particle diffusion:

$$F = 1 - \left(\frac{6}{\pi^2}\right) e^{-Bt} \quad (5)$$

where F is the fraction of solute adsorbed at different times t :

$$F = \left(\frac{q_t}{q_e}\right) \quad (6)$$

Bt , in (5), is a mathematical function of F which can be evaluated from each value of F as:

$$Bt = -0.4977 - \ln\left(1 - \frac{q_t}{q_e}\right) \quad (7)$$

Plot of Bt vs. t for both, OP and RH, are shown in **Figure 9** which are straight lines with R^2 of 0.9970 and 0.9921, respectively. The results suggest that intraparticle diffusion is not the sole rate controlling step because the plot does not pass through the origin. This is in agreement with the results obtained by using intraparticle diffusion model and, at the same time, indicating that the mechanism of metal adsorption by OP and RH is complex and both, external mass transport as well as intraparticle diffusion contribute to the rate determining step, being the rate limiting step the intraparticle transfer.

Value of rate constant B was calculated from the slope in **Figure 9** and used to calculate the effective diffusion coefficient, D_i (cm^2/s) employing the relationship:

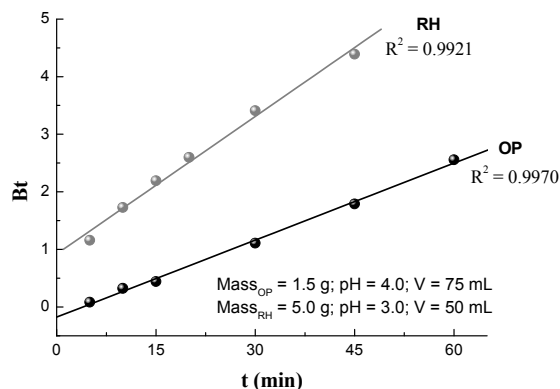


Figure 9. Boyd plot for Cr(III) sorption. $T = 20^\circ\text{C}$; $[\text{Cr(III)}]_0 = 0.385 \text{ mM}$ (OP) and 0.77 mM (RH).

$$B = \pi^2 \frac{D_i}{r^2} \quad (8)$$

where r represents the radius of the assumed spherical particle. The calculated D_i values for OP and RH were $9.5 \times 10^{-8} \text{ cm}^2/\text{s}$ and $5.9 \times 10^{-8} \text{ cm}^2/\text{s}$, respectively.

3.4. Adsorption Isotherms

Freundlich, Langmuir and Dubinin-Radushkevich (D-R) adsorption models were employed for describing the chromium biosorption behavior in the OP- and RH-Cr(III) systems.

Freundlich isotherm

$$q_e = K_f C_e^{1/n} \quad (9)$$

where C_e is equilibrium concentration of chromium in the bulk solution (mg/L), K_f and $1/n$ are Freundlich constants. Values of $1/n$ and K_f correspond to the adsorption intensity and maximum adsorption capacity, respectively. This empirical model can be applied to non-ideal adsorption on heterogeneous surfaces as well as multilayer adsorption. Relatively higher fractional values of $1/n$ ($0 < 1/n < 1$) indicate a fair validity of classical Freundlich isotherm over the entire concentration of Chromium [34].

Langmuir isotherm

$$q_e = \frac{q_m K_L C_e}{1 + K_L C_e} \quad (10)$$

where q_m is the monolayer adsorption capacity (mg/g) and K_L is the Langmuir constant related to the free energy of adsorption. High values of K_L are reflected by the step initial slope of a sorption isotherm and indicate a high affinity for the adsorbate.

The non-linear Freundlich and Langmuir isotherms for the uptake of Cr(III) on the OP and RH are presented in **Figures 10** and **11**. The solid curves represent the model fits in the wide range of concentrations. The corresponding Freundlich and Langmuir parameters together with

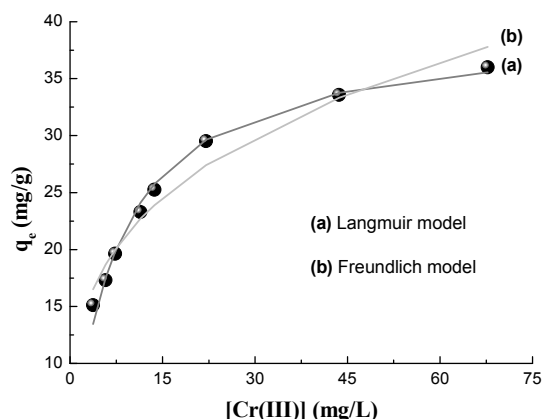


Figure 10. Adsorption isotherm for Cr(III) removal by OP. $Mass_{OP} = 1.45$ g; $T = 20^{\circ}C$; $pH = 4.4$; $V = 75$ mL; $[Cr(III)]_0 = 76.96 - 769.60$ mg/L; time contact = 120 min.

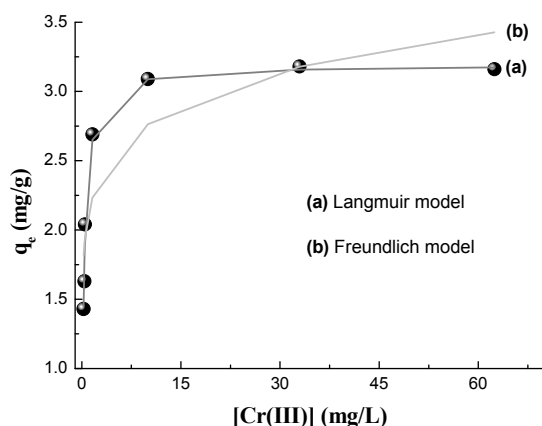


Figure 11. Adsorption isotherm for Cr(III) removal by RH. $Mass_{RH} = 5.65$ g; $pH = 3.0$; $T = 20^{\circ}C$; $V = 50$ mL; $[Cr(III)]_0 = 23.09 - 461.76$ mg/L; time contact = 120 min.

correlation coefficients are given in **Table 3**. In the given concentration range, the correlation coefficients showed that the Langmuir model fitted the experimental data better than the Freundlich model.

In previous studies [34,35], authors have suggested that using a dimensionless separation factor is suitable for evaluation of sorption data. For the Langmuir-type sorption process, the isotherm shape can be classified by a term R_L , dimensionless constant separation factor, which is defined as:

$$R_L = \frac{1}{1 + K_L C_0} \quad (11)$$

where C_0 is initial metal concentration. The parameter R_L indicates the shape of the isotherm accordingly: $R_L > 1$ unfavorable; $R_L = 1$ linear; $0 < R_L < 1$ favorable; $R_L = 0$ irreversible. The values of R_L were found to be less than 1 and greater than 0 for both biomaterials indicating a favorable adsorption for Cr(III) by the biomass.

Table 3. Langmuir and Freundlich constants and correlation coefficients for Cr(III) removal.

Biomaterial	Langmuir constants			Freundlich constants		
	q_m (mg/g)	K_L (L/mg)	R^2	K_f (mg/g)	$1/n$	R^2
OP	39.11	0.14	0.9902	11.30	0.29	0.9687
RH	3.20	2.98	0.9864	2.11	0.12	0.8173

D-R isotherm model [36]

$$\ln q_e = \ln q_M - \beta \varepsilon^2 \quad (12)$$

where q_M is maximum amount of ion that can be sorbed onto unit weight of sorbent (mol/g), β is a constant related to sorption energy (mol/kJ) and ε is the Polanyi potential:

$$\varepsilon = RT \ln \left(1 + \frac{1}{C_e} \right) \quad (13)$$

where R is gas constant (8.314×10^{-3} kJ/mol K) and T is absolute temperature expressed in K. Constant β (-3.7×10^{-9} mol²/J²) and q_m (9.60×10^{-4} mol/g) values were obtained from slope and intercept of the plot of $\ln q_e$ vs. ε^2 ($R^2 = 0.9891$), (10) and **Figure 12**. The mean sorption energy, E , which is the free energy mean of transference for 1 mol of solute from infinity (in solution) to the surface of biomaterial, can be calculated from:

$$E = \frac{1}{\sqrt{-2\beta}} \quad (14)$$

The obtained value of $E = 11.6$ kJ/mol, is in the expected range of 8–16 kJ/mol for ion exchange phenomena [36]. The correlation coefficient for RH was lower than OP system (0.9136) using D-R model with an estimate value of E of 16 kJ/mol.

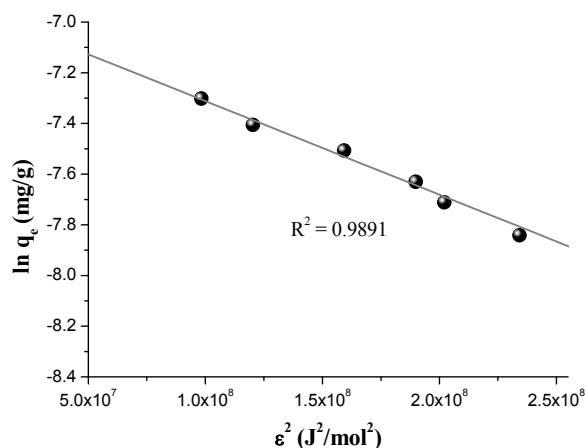


Figure 12. D-R isotherm plot for sorption Cr(III) onto OP. $Mass_{OP} = 1.45$ g; $T = 20^{\circ}C$; $pH = 4.4$; $V = 75$ mL; $[Cr(III)]_0 = 76.96 - 769.60$ mg/L; time contact = 120 min.

4. Conclusions

OP and RH agriculture biowaste materials were examined as possible low-cost sorbents for Cr(III) removal from aqueous solutions. Fitting of the intraparticle diffusion model indicated that intraparticle mass transfer resistance is likely the rate limiting phenomenon. The effective diffusion coefficient values for OP and RH were $9.5 \times 10^{-8} \text{ cm}^2/\text{s}$ and $5.9 \times 10^{-8} \text{ cm}^2/\text{s}$. Sorption dynamics data indicated that the time required to reach sorption equilibrium was approximately 120 min. Langmuir, Freundlich and Dubinin-Radushkevich sorption isotherm models were fitted to the experimentally derived biosorption isotherms. The isotherm data most accurately conformed to the Langmuir equation. The values obtained for q_m were 39.11 and 3.20 mg/g for Cr(III) adsorption by OP and RH, respectively. The mean free energy of metal sorption process calculated from D-R parameter and the Polanyi potential was found to be in the range of 8-16 kJ/mol indicating that the main mechanism governing the sorption process is most likely ion exchange. Abiotic Cr(VI) reduction by the biomass was performed with various contact times, and characteristics of the Cr-laden biomass were determined by spectroscopic studies that demonstrated that the Cr(VI) bound to the biomass was reduced to Cr(III). Results indicated that OP and RH are biomaterials quite effective in removing Chromium from aqueous solutions to drinking water standards.

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