

Experimental Study on the Radiative Properties of Fly Ash in the Radiant Syngas Cooler of Gasifier

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Abstract

Radiant syngas cooler (RSC) is the key heat recovery equipment in coal gasification system. The syngas from gasifier carries large amount of slags in which the mass fraction of fly ash less than 100 µm is about 20%. Studying the optical properties of fly ash has high significance for the optimization of heat transfer calculation in RSC. A new experimental method was proposed to inversely calculate the radiative parameters of particles-"KBr transmittance-reflectance method". By measuring the "directional-hemispherical" reflectance and transmittance of fly ash particles by FTIR under the wavelength range of 0.55 - 1.65 µm, using the four-flux model to solve the radiative transfer equation and combing with Mie theory, the absorption and scattering efficiency of 22.7 μ m fly ash and optical constant (also known as complex refractive index, m =n + ik) of fly ash were inversely calculated. The results indicated that for fly ash with large size parameter, there was no obvious change of the absorption and scattering efficiency when the mass fraction of Fe₂O₃ was between 5.65% and 16.53%, which was well explained by Mie theory; The obtained optical constant was close to the results of KBr transmittance method.

Keywords

Radiant Syngas Cooler, Fly Ash, Radiative Properties, Absorption Efficiency, Scattering Efficiency, Optical Constant

1. Introduction

The syngas produced by various gasifiers contains about 10% to 20% calorific value which exists in the form of sensible heat. Usually, this part of the energy is not effectively used. For example, the high-temperature syngas in coal-water

slurry gasifier is directly cooled by chilling. The syngas temperature decreases from about 1400°C to less than 300°C, which causes huge energy loss. Radiant Syngas Cooler (RSC) is installed at the outlet of gasifier and plays a significant role in recovering this part of energy. The utilization of RSC can increase the power generation efficiency of Integrated Gasification Combined Cycle (IGCC) by 4 - 5 percents [1].

The syngas flowing into RSC carries a large amount of high-temperature slags, in which the mass fraction of particles less than 100 μ m is about 20%. Because of its small size and large number density, this part of fly ash has a significant effect of light scattering on the radiation transfer in RSC [2]. Therefore, the study of the optical properties of fly ash, including its absorption efficiency, scattering efficiency and optical constant, is important to the optimization of heat transfer in RSC.

The optical properties of fly ash are determined by chemical composition, size parameter x ($x = \pi D / \lambda$), surface condition and geometry [3]. In view of the radiative properties of fly ash, a lot of researches have been carried out mainly through the combination of calculation and experiment. Goodwin examined the optical constant of slags in the wavelength of 0.19 - 13 µm by measuring the the near normal reflectance and transmittance, which is widely accepted [4] [5]. Self and Ruan determined the optical constant by measuring KBr slabs that contain fly ash particles and then combining with Mie theory and K-K relation, but the extrapolation formula of the K-K relation will cause some deviations [6] [7] [8]. Meanwhile, the result of extinction coefficient k through this method is 10 - 100 times larger than that given by Goodwin. This is because particles have larger surface areas than bulk [9]. Yin and Liu obtained effective optical constant of fly ash based on the effective medium theory (EMT) of mean electromagnetic field [10]. Self compared the optical constant of slag from 300 K to 1900 K. It was found that the k value of some wavelength increased by nearly three times [6]. Mengüc and Wall used light scattering method to measure the optical constant of coal and fly ash respectively, but this method was difficult to apply [11] [12].

In order to eliminate the errors from the extrapolation formula of the K-K relation and reduce the effects of forward scattering in KBr transmittance method, a "KBr transmittance-reflectance method" was proposed in this paper based on [13] [14] [15] to obtain the optical constant of $3.21 \mu m$ fly ash particles and the absorption and scattering efficiency of 24.8 μm fly ash particles.

2. Theoretical Model

2.1. Lorenz-Mie Theory

Lorenz-Mie theory is a classical algorithm used to solve the interaction between spherical particles and plane electromagnetic waves. It gives an exact solution to the scattering problem of spherical particles with any size. When a light with wavelength of λ is incident on an isotropic homogeneous spherical particle, the extinction, scattering and absorption efficiency of the particle can be expressed by the following formula [16] [17]:

$$Q_{ext}(m,x) = \frac{2}{x^2} \sum_{n=1}^{\infty} (2n+1) \operatorname{Re}\{a_n + b_n\}$$
(1)

$$Q_{sca}(m,x) = \frac{2}{x^2} \sum_{n=1}^{\infty} (2n+1) \left[\left| a_n \right|^2 + \left| b_n \right|^2 \right]$$
(2)

$$Q_{abs}(m,x) = Q_{ext}(m,x) - Q_{sca}(m,x)$$
(3)

where x is size parameter; r is particle radius; a_n and b_n are called Mie scattering coefficients, which are calculated as follows:

$$a_{n} = \frac{\psi_{n}'(mx)\psi_{n}(x) - m\psi_{n}(mx)\psi_{n}'(x)}{\psi_{n}'(mx)\xi_{n}(x) - m\psi_{n}(mx)\xi_{n}'(x)}$$
(4)

$$b_{n} = \frac{m\psi_{n}'(mx)\psi_{n}(x) - \psi_{n}(mx)\psi_{n}'(x)}{m\psi_{n}'(mx)\xi_{n}(x) - \psi_{n}(mx)\xi_{n}'(x)}$$
(5)

where m = n + ik represents the optical constant; $\xi_n = \psi_n - i\eta_n$; ψ_n and η_n are the Bessel functions which follow the recurrence relation:

$$\psi_{n+1}(z) = \frac{2n+1}{z} \psi_n(z) - \psi_{n-1}(z)$$
(6)

$$\eta_{n+1}(z) = \frac{2n+1}{z} \eta_n(z) - \eta_{n-1}(z) \tag{7}$$

where,

$$\psi_{-1}(z) = \cos z, \ \psi_0(z) = \sin z$$
 (8)

$$\eta_{-1}(z) = -\sin z$$
, $\eta_0(z) = \cos z$ (9)

For dispersed particle system that satisfies the independent scattering condition, the scattering of particles has no effect on each other. The absorption and scattering coefficients of the particle system are the integral of the absorption and scattering efficiency by the particle size distribution, as follows:

1

$$\mu_{\lambda} = \int_0^\infty Q_{\mu} \frac{\pi D^2}{4} f(D) N dD \tag{10}$$

where μ_{λ} represents the absorption coefficient scattering κ_{λ} , scattering coefficient σ_{λ} , extinction coefficient σ_{λ} ; Q_{μ} represents the corresponding absorption, scattering and extinction efficiency; *N* denotes the number of particles per unit volume; f(D) is the normalized size distribution. For particles with same size, the relation is simplified as:

$$\mu_{\lambda} = \frac{\pi D^2}{4} N Q_{\mu} \tag{11}$$

Therefore, when the particle absorption, scattering coefficients and the size distribution are obtained from experiments, the absorption, scattering efficiency and optical constants of particles can be inversely calculated.

2.2. Four-Flux Model

The four-flux model is an approximate solution of radiative transfer equation to

determine the absorption and scattering coefficients of materials. In four-flux model, it is assumed that 1) there is no emission of the sample at room temperature; 2) only a collimated radiative flux is incident onto the front surface of the sample; 3) at any position z inside of the sample, there are four parts of energy: a collimated beam $I_c(z)$ propagating to positive z, a collimated beam $J_c(z)$ propagating to negative z, a diffuse beam $I_d(z)$ propagating to positive z, a diffuse beam $J_d(z)$ propagating to negative z [18] [19].

As shown in **Figure 1**, 0~L denotes the KBr slab that contains fly ash particles; ρ_{in} and ρ_{out} represent the internal and external reflectivity respectively which can be calculated by Fresnel equation [19]: $\rho_{in} = 0.6299$, $\rho_{out} = 0.1004$.

According to energy balance, the differential equations and boundary conditions can be established, see [20]. In this paper, the total reflectance R and transmittance T at two planes of 0 and L are derived under diffuse reflection boundary condition. The formulas are as follows:

$$R = \rho_{out} + (1 - \rho_{in})[C_2 + C_1 B + C_2 A + C_3 (1 - \beta) + C_4 (1 + \beta)]$$
(12)

$$T = (1 - \rho_{in})[C_1 e^{-\tau_1} + C_1 A e^{-\tau_1} + C_2 B e^{\tau_1} + C_3 (1 + \beta) e^{-2\beta\tau_2} + C_4 (1 - \beta) e^{2\beta\tau_2}]$$
(13)

The constants in the formulas are found to be:

$$C_{1} = \frac{1 - \rho_{out}}{1 - \rho_{in}^{2} e^{-2\tau_{1}}}$$
(14)

$$C_2 = \frac{(1 - \rho_{out})\rho_{in}e^{-2\tau_1}}{1 - \rho_{in}^2 e^{-2\tau_1}}$$
(15)



Figure 1. Illustration of four-flux model.

$$C_{3} = \frac{(\sigma_{1}\mu_{2}e^{2\beta\tau_{2}} - \sigma_{2}\mu_{1}e^{-\tau_{1}})C_{1} + (\sigma_{1}\mu_{1}e^{2\beta\tau_{2}} - \sigma_{2}\mu_{2}e^{\tau_{1}})C_{2}}{\sigma_{1}^{2}e^{2\beta\tau_{2}} - \sigma_{2}^{2}e^{-2\beta\tau_{2}}}$$
(16)

$$C_{4} = \frac{(\sigma_{1}\mu_{1}e^{-\tau_{1}} - \sigma_{2}\mu_{2}e^{-2\beta\tau_{2}})C_{1} + (\sigma_{1}\mu_{2}e^{\tau_{1}} - \sigma_{2}\mu_{1}e^{-2\beta\tau_{2}})C_{2}}{\sigma_{1}^{2}e^{2\beta\tau_{2}} - \sigma_{2}^{2}e^{-2\beta\tau_{2}}}$$
(17)

where,

$$\begin{aligned} \tau_1 &= (a+s)L \; ; \; \tau_2 = 0.5(M+N)L \; ; \; \mu_1 = \rho_{in}A - B \; ; \; \mu_2 = \rho_{in}B - A \; ; \\ M &= \varepsilon_d [a+(1-\zeta)s] ; \; N = \varepsilon_d (1-\zeta)s \; ; \; X = \varepsilon_c (1-\zeta)s \; ; \; Y = \varepsilon_c \zeta s \; ; \; T = a+s \; ; \\ \sigma_1 &= (1+\beta) - \rho_{in}(1-\beta) \; ; \; \sigma_2 = (1-\beta) - \rho_{in}(1+\beta) \\ A &= \frac{Y(M+T) + NX}{M^2 - T^2 - N^2} \; ; \; B = \frac{X(M-T) + NY}{M^2 - T^2 - N^2} \; ; \; \beta = \frac{\sqrt{M^2 - N^2}}{M+N} \; . \end{aligned}$$

where, *a* and *s* are the absorption and scattering coefficient respectively, and because KBr has no absorption in the infrared and partial visible spectrum, *a* and *s* are approximately treated as the absorption and scattering coefficient of the fly ash particles; *L* is the thickness of sample; ζ is the forward scattering ratio, which equals the energy scattered by a particle in the forward hemisphere over the total energy; ε is the average crossing parameter, which is defined by saying that, when the radiation light travels a length dz, the average path length is εdz [20]. For collimated light, $\varepsilon_c = 1$ and diffuse light is indicated by ε_d .

In order to make sure the accuracy of the four-flux model, the selection of ε_d and ζ is particularly important. Since the size distribution of particles can be controlled in experiment, ε_d and ζ are calculated under different size parameter *x* and *k* by Mie scattering theory, see **Figure 2**.

As shown in **Figure 2**, ε_d and ζ change little under different *k* values at the size parameter x < 1. However, at the size parameter 1 < x < 10, there is significant enhancement of forwarding scattering of particles, thus ε_d and ζ have sharp changes with different *k* values. As size parameter *x* increases larger than 10, ε_d and ζ reaches constants respectively, which are 1.05% and 95%. Because the particle sizes in experiments are 22.7 µm and 3.21 µm and the measuring wavelength is 0.55 - 1.65 µm, the size parameters are larger than 6. Thus in calculation, ε_d and ζ are chosen to be $\varepsilon_d = 1.1$ and $\zeta = 0.95$.

3. Experimental Procedures

3.1. Sample Preparation

The preparation of samples plays a crucial role in the experimental results. In the experiment, fully ground KBr was mixed with fly ash particles and then compressed into slab. The procedures of sample preparation are as follows: 1) Spectrum pure KBr pellets are ground into powder; 2) Fly ash and KBr are mixed with mass ratio 1:100; 3) The mixture was compressed using a tablet pressing machine under pressure 7 t/cm²; 4) Because KBr is deliquescent, infrared heating was used to ensure that the preparation of sample was in a dry environment.



Figure 2. Forward scattering ratio and average crossing parameter calculated by Mie theory.

3.2. Experimental Method

Measurement of the hemispherical-directional reflectance and transmittance spectra of free-standing KBr sample was performed at room temperature, which means the emission of the sample can be neglected. The experiments examined the wavelength range of 0.55 - 1.65 μ m using Fourier Transform Infrared Spectroscopy (FTIR). The experiment equipment illuminated hemispherical radiation onto sample slab. Then the effective radiation intensity of upper surface $I_{eff,1}$ and lower surface $I_{eff,2}$ were separately received by two FTIRs, see **Figure 3**. Since the radiation intensity from the hemispherical radiation source $I_{\lambda,source}$ was known, the reflectance R and transmittance T were readily calculated as



Figure 3. Illustration of experiment equipment (1 is a hemispherical radiation source, 2 is KBr slab).

 $R = I_{eff,1} / I_{\lambda,source}$, $T = I_{eff,2} / I_{\lambda,source}$. According to the reversibility of light, the hemispherical-directional reflectance R and transmittance T were equal to directional-hemispherical reflectance and transmittance that are required in the four-flux model. Based on the experiment data, the absorption, scattering coefficients of the fly ash system can be calculated and then the absorption, scattering efficiency and optical constant of single particle can be further retrieved.

4. Results and Discussion

4.1. Optical Constant of 3.21 µm Fly Ash Particle

There is multiple value problem when calculating optical constant of particles with large size parameter, which means a group of testing data (*R*, *T*) will get multiple values of (*n*, *k*). Thus, the optical constant of fly ash was retrieved from particles $\overline{D}_{43} = 3.21 \mu m$. The reflectance and transmittance spectra are displayed in **Figure 4**. The calculated optical constant is shown in **Figure 5**.

As shown in **Figure 5**, n value is essentially in agreement with the reference data which is between 1.5 and 1.6. The k value is similar to the results of KBr transmission method in reference [21], and is quite different from the result of slag in reference [4]. This is because particles have larger surface area than bulk materials, so that the measured k value of fly ash is larger than that of slag.

In the calculation of the heat transfer in RSC, the absorption, scattering coefficient and phase function of the fly ash particle system can be obtained according to the optical constant combining with suitable particle scattering model and particle size distribution, and the radiative transfer equation can be further solved.

4.2. Absorption, Scattering Efficiency of 22.7 µm Fly Ash Particle

In the experiment, the density of fly ash was $\rho = 2225 \text{kg/m}^3$; the thickness of



Figure 4. Reflectance and transmittance spectra of 3.21 µm fly ash.



Figure 5. Optical constant of 3.21 µm fly ash.



Figure 6. Absorption efficiency Q_a and scattering efficiency Q_s of 22.7 µm fly ash.

KBr sample was L = 1.1 mm; particle size was $\overline{D}_{43} = 22.7 \text{ }\mu\text{m}$. Five groups of controlled experiment were set up with the mass fraction of Fe₂O₃ ranging from 0.85% to 16.53%. The absorption and scattering efficiency calculated by genetic algorithm is shown in **Figure 6**.

It can be seen from **Figure 6** that when the mass fraction of Fe_2O_3 was between 5.65% and 16.53%, the change of Q_a and Q_s was not obvious and they concentrated around 0.9 and 1.1 respectively. Only when the mass fraction of Fe_2O_3 was reduced to 0.85%, Q_a and Q_s changed significantly: Q_a decreased to 0.3 - 0.4, while Q_s increased to 1.7 - 1.8.

Since Fe₂O₃ has strong absorption characteristic when the incident wavelength

is less than 4 µm [4], k is mainly influenced by the content of Fe₂O₃ and increases with the increase of Fe₂O₃, while the *n* value remains stable. Thus it is worth analyzing the results in **Figure 6** by comparing the change of Q_a and Q_s under different size parameter *x* and *k* values through Mie scattering theory, see **Figure 7**.

As shown in **Figure 7**, with the increase of size parameter *x*, the influence of *k* value on particle scattering and absorption efficiency gradually decreases; when *k* grows larger, the values of Q_a and Q_s coincide. In the experiment, when the mass fraction of Fe₂O₃ was relatively high, the *k* value became larger, so the change of Q_a and Q_s was not obvious as shown in **Figure 6**. In addition, it is



Figure 7. Direct calculation of absorption efficiency Q_a and scattering efficiency Q_s by Mie theory.

found that with the increase of the size parameter x, the scattering and absorption efficiency of the particles approach a constant respectively. And for materials with larger k value, the size parameter x is smaller when the absorption and scattering efficiency tends to be stable.

In the calculation of heat transfer in RSC, the absorption and scattering efficiency of large size parameter fly ash can be approximately determined as fixed values which are not affected by the variation of Fe_2O_3 .

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