

Formation of Necklace-Type Vortex System Upstream of a Gate Valve in Pipe Flow

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Abstract

A gate valve is one of the main elements of a circular pipeline, but the flow characteristics around the gate valve are hardly known. In this study, clarification of the flow field in front of the gate valve model in a pipe flow via flow visualization and PIV analysis was attempted. As a result, four kinds of steady necklace-type vortex systems, 2-vortex, 4-vortex, 6-vortex and 8-vortex systems, were clearly observed in a Reynolds number between 290 and 2130. In addition, the main vortex was observed in the Reynolds number range between 2130 and 4870 with difficulty. On this account, both the center position and vorticity in the main vortex are presented against Reynolds number.

Keywords

Pipe Flow, Gate Valve, Vortex Formation, Flow Visualization, PIV Analysis

1. Introduction

A gate valve has a feature that the pressure loss when fully opened is small and the valve opening degree can be finely adjusted. The gate valve is one of the main elements of a circular pipeline. However, the flow pasts a gate valve and the resistance characteristics of a gate valve have not been investigated sufficiently.

Koram and Sparrow (1978) and Sparrow *et al.* (1980) reported heat transfer and pressure drop characteristics induced by an unsymmetric blockage element installed into the circular pipe [1] [2]. Oguri (1991) and Yamada and Katoh (1993) studied a flow-meter using a segmental blockage element, such as a gate valve [3] [4]. Yamada *et al.* (2015) also investigated flow field and loss coefficient produced by a gate valve model installed in a circular pipe [5]. They first showed that one necklace-type vortex is formed in front and moves over the gate valve

model by using dye-method visualization. Recently, Alimonti (2014) reported an experimental characterization about pressure drop and flow rate of gate valves in vertical gas-liquid flows [6]. Lin *et al.* (2016) calculated influence of flashboard location on flow resistance properties and internal features of the gate valve model in rectangular pipes [7].

The flow resistance in the protrusion of various shapes installed into the pipe has been well studied. However, the flow field around a protrusion which is unaxisymmetric with circular pipe axis, e.g. a gate valve, in a circular pipe is not well-known. Particularly, excluding the study by Yamada *et al.*, the flow field in front of the protrusion has hardly been investigated [5].

Therefore, our interest was focused on the flow field in front of the gate valve model in circular pipes. Particularly, in this paper the feature of the necklace-type vortex (vortex system, vortex position, and vorticity) was investigated by flow visualization and PIV analysis against a wide Reynolds number.

2. Experimental Apparatus and Procedure

The measuring circular pipe employed in this experiment lies in a water channel flow which is 400 mm in width and 400 mm in depth. **Figure 1** shows the coordinate system and nomenclature in the circular pipe. The circular pipe is made of transparent acrylic with an internal diameter of 42 mm and a wall thickness of 4 mm. An inlet long ellipse nozzle is attached in the entrance of the pipe to smooth the inflow. The radius of curvature of the gate valve model is $D/2$ and the thickness is $t/D = 0.1$. The height ratio of the gate valve model height to the pipe diameter is $h/D = 0.6$. Therefore, the blockage ratio of the model front to the cross section is 0.5. The gate valve model was attached in the position of 1700 mm from the nozzle exit. In the experiment, fine nylon particles with an average particle size of 50 μm and a specific gravity of 1.03 were mixed in the water channel to visualize the flow. Then, the flow upstream of the gate valve model was irradiated by the laser light sheet, and was captured by using a high-speed camera. Conditions for shooting are shown in **Table 1**. The Reynolds number, $Re (= U_m \cdot D / \nu)$, was defined based on measuring the pipe diameter, D , and the averaged velocity, U_m , which was determined by using a flow-meter installed in the downstream of the measuring pipe. The mean velocity of the flow

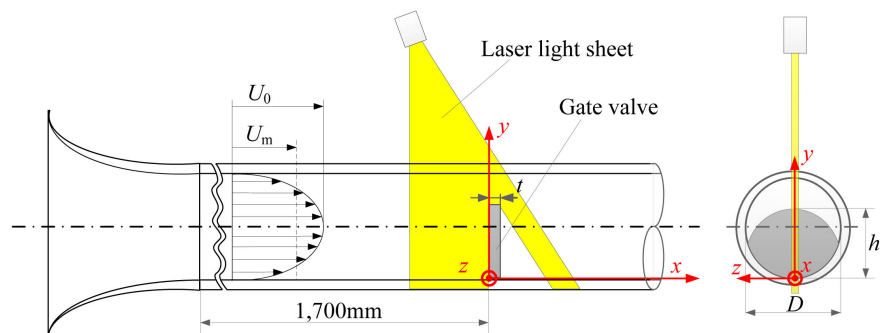


Figure 1. Experimental apparatus and nomenclatures.

Table 1. Conditions for shooting.

Re [-]	180	290	390	490	590	680	780	880	970	1460	1560 - 1850	2130 - 2460	4870	9740
Flame late [flame/s]		30			60		100	100			200		400	800
Resolution [pixel \times pixel]				1280 \times 1024							1280 \times 1024		1024 \times 768	640 \times 480
Number of flames [flame]	5400	1000	5400			1000			18,000	1000	18,000		31,346	80,162
Dissolution [mm/pixel]				0.05							0.05		0.07	0.10

field was calculated by a PIV analysis based on the correlation method. Furthermore, the template size for pattern matching was decided as 31 pixels \times 31 pixels. **Figure 2** shows the distribution of the mean velocity measured across the pipe without the gate valve model in each Reynolds number. Incidentally, uncertainty of velocity measured by the PIV in this research was about 6.5%, which was obtained by comparing Poiseuille flow velocity and the obtained velocity.

3. Experimental Results and Discussions

It is well known that necklace vortices are formed in front of a three-dimensional obstacle mounted on a wall. Surprisingly, various vortex systems to be similar with the necklace vortex systems shown by Nakahara and Yamada [8] were also confirmed upstream of the gate valve model in this experiment. Therefore, we named the clockwise vortices as V_1, V_2, V_3, V_4 upstream of the gate valve model, and called the counter clockwise vortices as V_0, V'_1, V'_2, V'_3 as shown in **Figure 3(d)**. Incidentally, by visualizing the dye behavior invading into one vortex tube, Yamada *et al.* showed that the vortex in the case of the gate valve model is almost equal with the main vortex in ordinary necklace vortices [5]. Therefore, we decided to call the vortices observed in this experiment a necklace-type vortex system.

3.1. Formation of Vortex System

Figure 3 shows the path lines image upstream of gate valve model in each Reynolds number. These path lines images were made by mutually superposing consecutive particle-images of 800. As shown in **Figure 3**, the steady necklace vortices were formed in the range of $Re \leq 2130$. In the case of $Re = 290$, the flow field was regarded as a 2-vortex system, because the number of the steady vortices having different signs was 2. Accordingly, the flow field was regarded as a 4-vortex system in $Re = 490$, as a 6-vortex system in $Re = 970$ and as an 8-vortex system in $Re = 2130$. In the range of $Re \geq 2460$, the flow field became more unsteady with increasing Reynolds number. Although, the center position of the main vortex V_1 in $Re = 2460$ and 4870 could be observed as well as the steady vortex system described above. Therefore, both formation and collapse of vortices may exist in the case of those Reynolds numbers. In the case of $Re = 9740$, it was difficult to confirm the formation of a time-averaged vortex system.

Figure 4 shows the variation of the steady vortex system against the Reynolds number. As mentioned above, the steady flow field varied from a 2-vortex to an

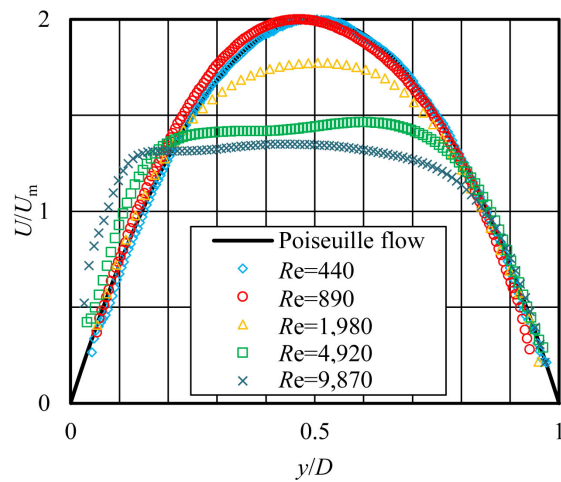


Figure 2. Velocity distribution in each Reynolds number without the gate valve model, measured in the position of 1700 mm downstream of the nozzle exit.

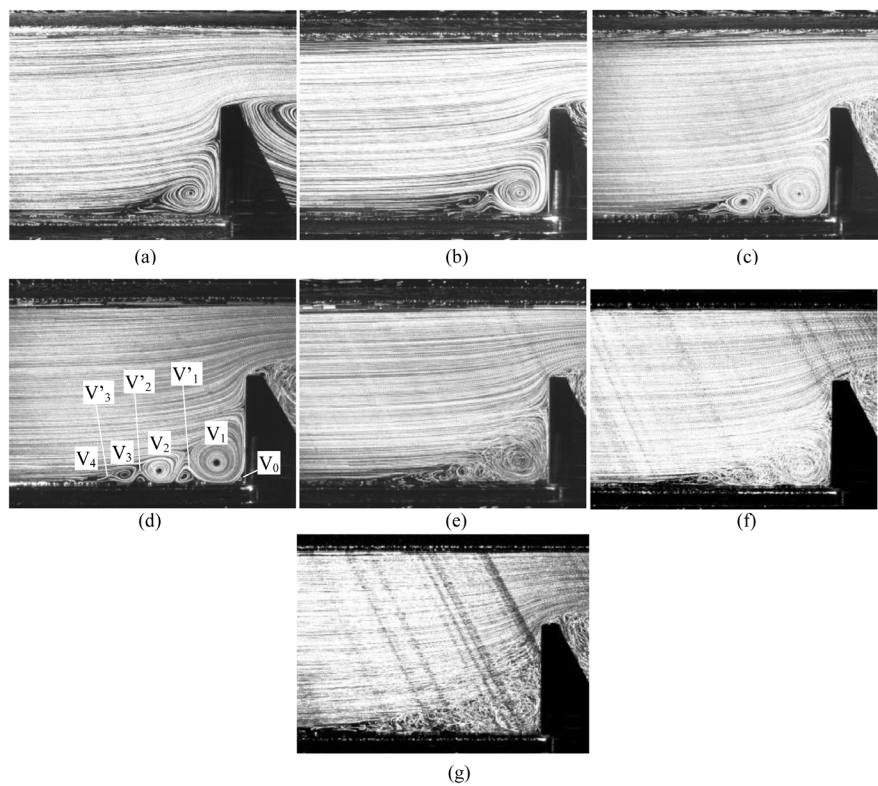


Figure 3. Visualization of necklace-type vortices by path lines: (a) $Re = 290$; (b) $Re = 490$; (c) $Re = 970$; (d) $Re = 2130$; (e) $Re = 2460$; (f) $Re = 4870$; and (g) $Re = 9740$.

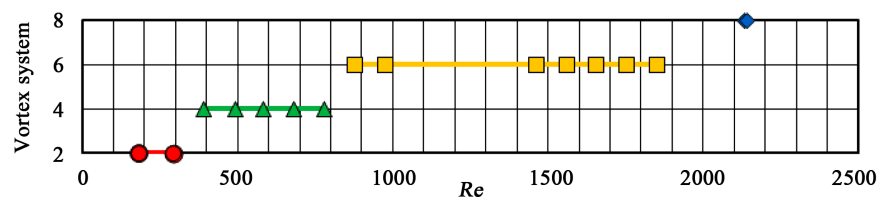


Figure 4. Classification of vortex system.

8-vortex system. The 2-vortex system existed between $Re = 180$ and 290 , the 4-vortex system existed between $Re = 390$ and 780 , the 6-vortex system existed between $Re = 880$ and 1850 , and the 8-vortex system existed in $Re = 2130$. Since the flow field was unsteady in $Re = 2460$, the range of Reynolds number in which the steady 8-vortex system appears is extremely small.

3.2. Characteristics of Vortex System

Figure 5 shows the ratio of the center point distance of the main necklace-type vortex, V_1 , to the circular pipe diameter, D . The x -direction distance from the gate valve model to the V_1 center point is defined as X_{V_1} , the height from the bottom wall of the circular pipe to the center point of the V_1 is defined as Y_{V_1} . The dashed line is the approximate line calculated by using the least squares method in the Reynolds number range drawn by the dashed line. X_{V_1}/D increased in the range of $Re \leq 500$, and gradually decreased, linearly, in the range of $Re > 500$. Y_{V_1}/D gradually decreased, linearly, until $Re = 4920$. Therefore, the center point of V_1 may gradually approach the gate valve model, and the scale of V_1 may gradually become smaller as Re increases. **Figure 6** shows the stagnation point height Y_s which is the distance from the circular pipe bottom wall to the stagnation point. Y_s/D increased until $Re = 1000$, and gradually decreased as Re increases. **Figure 7** shows the ratio of V_1 center height Y_{V_1} to the stagnation point height Y_s . Y_{V_1}/Y_s also gradually decreased with increasing Reynolds number. However, Y_{V_1}/Y_s might be regarded as a value of about 0.30 in the Reynolds number range between approximately 500 and 5000 .

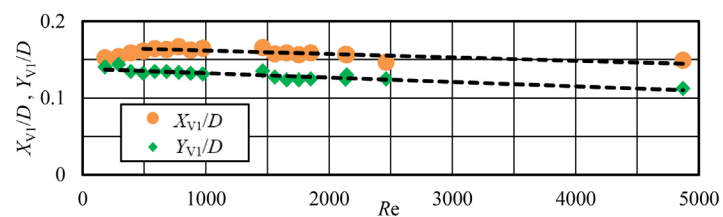


Figure 5. V_1 center point distance.

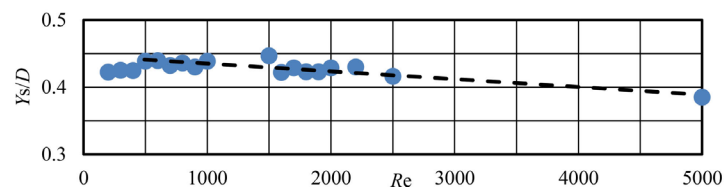


Figure 6. Stagnation point height.

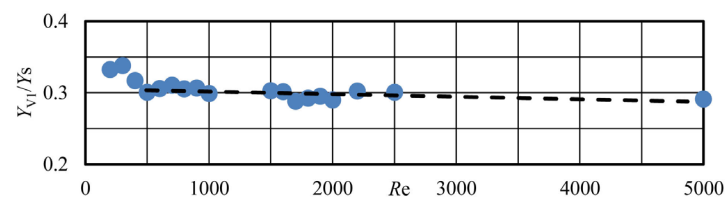


Figure 7. Ratio of Y_{V_1} to Y_s .

Figures 8(a)-(c) show the contours of relative vorticity obtained from time-averaged velocity data calculated by the PIV analysis. The negative value represents a clockwise rotation. In $Re = 970$, there was the vorticity contour corresponding with the 6-vortex system, though V_3 could not be confirmed clearly as shown in Figure 8(a). In $Re = 4870$, the presence of unsteady main vortex was clarified by the contour of time-averaged vorticity, as shown in Figure 8(b). In $Re = 9740$, the vortex formation could not be confirmed as well as the pass-lines image. However, there was a small negative vorticity observed in the turbulent region upstream of the gate valve model, as shown in Figure 8(c). Figure 9 shows the maximum relative vorticity in the V_1 center point. The relative vorticity increased in proportion to the Reynolds number. However, the relative vorticity in the main vortex center may be constant in the range of $Re > 2000$, because the maximum value of $(-D/U_m)\Omega$ in $Re = 4870$ was about 70 as shown in Figure 8(b).

4. Conclusions

The existence of the necklace-type vortex systems produced upstream of the gate valve model ($h/D = 0.6$) in the circular pipe was observed by using the flow visualization and PIV analysis. As a result, the following considerations about the characteristic of necklace-type vortices were gained:

1) Vortex systems were observed from two vortices to eight vortices in the range of $Re \leq 2130$. In the range of $Re \geq 2460$, unsteady necklace vortices were formed.

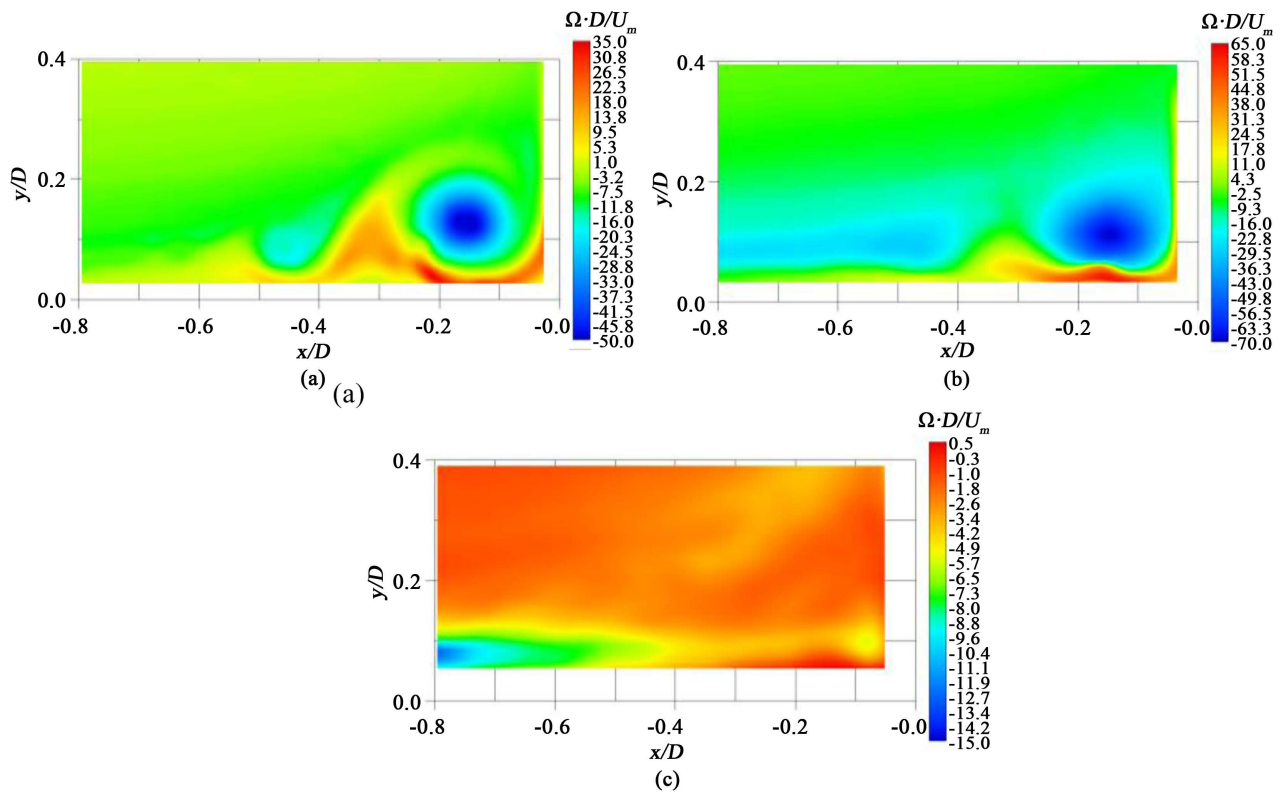


Figure 8. Contour of relative vorticity: (a) $Re = 970$, (b) $Re = 4870$, and (c) $Re = 9740$.

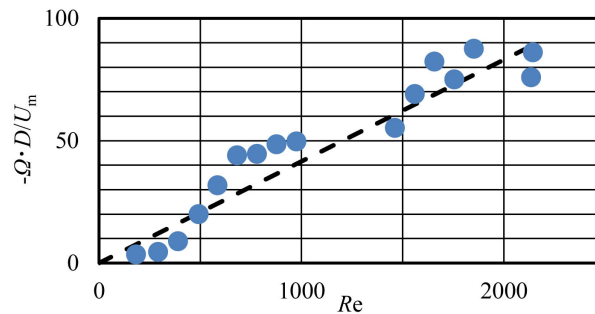


Figure 9. Vorticity distribution in V_1 center point.

2) As the steady necklace-type vortices in the upstream region of the gate valve model, formation of a 2-vortex system in $Re = 180 - 290$, a 4-vortex system in $Re = 390 - 780$, a 6-vortex system in $Re = 880 - 1850$, and an 8-vortex system in $Re = 2130$ occurred.

3) In the case of $Re > 500$, X_{V_1}/D and Y_{V_1}/D gradually decreased linearly with increasing Reynolds numbers. Therefore, the center position of V_1 approached the gate valve model as the Reynolds increased.

4) The relative vorticity at the center point of V_1 increased almost in proportion to the Reynolds number until about $Re = 2000$.

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Nomenclatures

- x : Distance measured from front surface of gate valve [m]
 y : Distance measured along asymmetry line of gate valve model from circular pipe bottom [m]
 u : x -direction velocity component [m/s]
 v : y -direction velocity component [m/s]
 U_m : Flow velocity averaged in cross-sectional area [m/s]
 U_0 : Maximum velocity in cross-sectional area [m/s]
 Re : Reynolds number ($= U_m \cdot D / \nu$)
 D : Diameter of circular pipe [m]
 t : Thickness of gate valve model [m]
 h : Height of gate valve model [m]
 X_{V_1} : x -direction distance from gate valve model to V_1 center point [m]
 Y_{V_1} : y -direction height from circular pipe wall bottom to V_1 center point [m]
 Y_s : y -direction height from circular pipe wall bottom to stagnation point [m]
 Ω : Vorticity $\left(= \frac{\partial v}{\partial x} - \frac{\partial u}{\partial y} \right)$ [1/s]
 ν : Kinematic viscosity [m²/s]