

Suppression of Pyrite Oxidation by Surface Silica Coating

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Abstract

The exposure of pyrite (FeS_2) to atmospheric conditions during mining activity causes a series of complex oxidation reactions, resulting to acid generation and the subsequent release of toxic heavy metals in the surrounding aquatic and terrestrial ecosystems. The produced acidic mine waters, known as acid mine drainage (AMD), constitute one the major environmental problems of both operating and abandoned mixed sulphide, coal and other mine sites where sulphidic minerals are encountered. A sustainable approach to the environmentally safe pyrite-bearing extractive waste management is related to the prevention of oxidation by developing artificial coatings on the pyrite surfaces. In this study, experiments performed to study the conditions of the silica coating formation on the FeS_2 particles contained in a pyrite concentrate are presented. Batch tests involving the treatment of pyrite samples with a coating solution, consisting of Na₂SiO₃, H₂O₂ and buffered pH, were performed under a liquid to solid ratio (L/S) 100 l/kg. The effect of parameters including SiO₂ concentration (5 - 50 mM), pH values (5.0 - 8.0) and contact time up to 24 hours, was investigated. Parameters examined to monitor the silica coating formation process include analysis of Fe, Si, SO_4^{2-} and H_2O_2 in the aqueous phase. Scanning electron microscopy with energy dispersive spectrometry (SEM/EDS) was used for the examination of the chemically modified surfaces of silica-treated pyrite samples.

Keywords

Acid Mine Drainage, Mine Wastes, Pyrite, Silica Coating

1. Introduction

Acid mine drainage (AMD) constitutes one of the most severe environmental problems of the mining industry. AMD which is a low-pH aqueous phase enriched primarily in iron (Fe) and sulfate anions, but also containing many metals and metalloids, such as lead (Pb), copper (Cu), zinc (Zn), manganese (Mn), nickel (Ni), cadmium (Cd), mercury (Hg) etc., depending on the mineralogy of the ore/waste. These acidic waters are produced by the oxidation of sulphide minerals, contained in the mine wastes and rocks, under the action of atmospheric air and water and catalyzed by the presence of bacteria. Singer & Stumm (1970) described the pyrite oxidation, which may occur via direct and indirect mechanisms, according to the following reactions:

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$$FeS_2 + 3.75O_2 + 3.5H_2O \rightarrow Fe(OH)_3 + 2SO_4^{2-} + 4H^+$$
 (1)

$$\text{FeS}_{2} + 14\text{Fe}^{3+} + 8\text{H}_{2}\text{O} \rightarrow 15\text{Fe}^{2+} + 2\text{SO}_{4}^{2-} + 16\text{H}^{+}$$
 (2)

Once generation of acidic waters commences, the sources of acidity may remain active for a long time after the mine closure. So, the effects of AMD can be both pernicious and far-reaching since contamination of surface and/or underground water can carry the pollution considerable distances from the mining area.

The acidic drainages are treated by conventional reclamation techniques, such as addition of alkaline materials (mainly, limestone and lime), covering with water to prevent oxygen access or formation of low permeability soil covers to minimize oxidizing agents transfer to the sulphides. Apart from the conventional prevention and remediation methods, an emerging and appealing technique for the inhibition of acid generation from sulphidic wastes involves the development of artificial coatings on sulphide grain surfaces (particularly on pyrite grains due to the abundance to all geological environments). This process is known as microencapsulation and was first described by Evangelou (1995a, 1995b), investigating the formation of phosphate coating on pyrite surfaces.

Other published studies refer to the establishment of coatings using inorganic materials, FeOOH (Huminicki & Rimstidt, 2009), silicates (Zhang & Evangelou, 1998; Evangelou, 2001) and magnesium and manganese compounds (Glover, 2007) and organic coatings such as humic acid and other organic ligands (Lalvani et al., 1996; Elsetinow et al., 2003; Kargbo et al., 2004).

The methodology, which was developed for the formation of silicic coating includes partial leaching/oxidetion of the sulphidic waste using a solution containing hydrogen peroxide (H_2O_2), a silica source and adjusted to pH 4.0 - 6.0 (Evangelou, 1996).

According to the study of Evangelou (2001), pyrite treatment with a solution consisting of H_2O_2 0.145 M, Si 0.0018 M, CH₃COONa 0.01 M, NaCl 0.1 M and adjusted to pH 6 at room temperature results in the formation of a silica coating composed of an inner layer of Fe³⁺ oxy-hydroxides and an outer layer of Si hydroxides. The coating process reduced by 85% the amount of oxidized pyrite compared to the control test. Bessho et al. (2011) performed batch-type tests and an effective silica coating was established on the pyrite surfaces, after treatment with a solution of Si concentration higher than 2500 mg/L and pH: 7.0.

However, coating technology needs further investigation. In this study, batch-type tests were performed in order to investigate the effect of pH and silica concentration on the formation of silica coating on the grains of a pyrite concentrate material.

2. Materials and Methods

A pyrite concentrate material assaying 50% S was used. The pyrite sample was screened and the selected fraction for the experiments was $(-125 + 75) \mu m$. The secondary oxidation products formed on the pyrite were removed by a pre-treatment procedure in which the selected fraction was washed with HCl 1 M for 24 hours (liquid to solid ratio, L/S = 20 l/kg), thereafter rinsed repeatedly with deionised water. The samples were then dried at 40°C for 24 hours and finally rinsed once with acetone. The purity of pyrite was confirmed by SEM/EDS and powder-XRD.

A series of batch-type tests were executed under atmospheric conditions ($T = 23^{\circ}C \pm 1^{\circ}C$) and the experimental conditions are presented in **Table 1**. Silica solution was prepared by dissolving pentahydrate sodium silicate (Na₂SiO₃*5H₂O) in deionized water and hydrochloric acid (HCl 3 N) was used to adjust pH to the selected

Parameter	Value
Size fraction (µm)	-125 + 75
H_2O_2 (mM)	100
SiO ₂ (mM)	5, 10, 25, 50
pH	5.0, 6.0, 7.0, 8.0
L/S (l/kg)	100
Duration (h)	0.5, 1, 2, 4, 6, 24

Table 1. Experimental conditions with the individual variables studied.

pH values. Sodium acetate (CH₃COONa) 0.2 M was used to buffer the coating solution to pH values 5.0 and 6.0, while THAM (tris-hydroxymethylaminomethane) 0.1 M was used to adjust to pH 7.0 and 8.0.

The experimental procedure involved the preparation of suspensions containing 0.9 g of pyrite and 90 mL of solution. The suspensions were placed for agitation on a rotary shaker (10 rpm) and removed for analyses after 0.5, 1, 2, 4, 6 and 24 hours. Each suspension was filtered through a 0.45 μ m pore size filter and the filtrate was analyzed for Fe, Si, SO₄ and H₂O₂. It is mentioned that the filtration of the suspensions buffered at pH 7.0 was performed using a filter paper with pore size 4 - 12 μ m due to their colloidal nature.

Iron and silicon concentrations in the aqueous phase was determined by means of Atomic Absorption Spectrophotometry (2100 Perkin Elmer). Sulfate concentrations were measured gravimetrically. The concentration of residual hydrogen peroxide in the aqueous phase was determined by volumetric titration with KMnO₄ 0.02 M. The surfaces of solid residues were examined and characterized by scanning electron microscopy with energy dispersive spectrometry (SEM/EDS).

3. Results and Discussion

3.1. Effect of pH and Silica Concentration

The concentration of dissolved Fe and sulphates in the solutions after treatment of the pyrite sample with the coating solution consisting of $H_2O_2 \ 0.1 \ M$, $SiO_2 \ 50 \ mM$ and adjusted to pH: $5.0 - 8.0 \ vs$. time is presented in **Figure 1(a)** and **Figure 1(b)**. As seen in **Figure 1(a)**, operation pH has a major effect on the dissolution of iron. The highest dissolution rate is observed at pH 5.0 with an almost linear kinetics, corresponding to the release of 0.28 mM of iron after 6 hours of treatment. Continuously increasing concentrations of iron in solution are also observed at pH 6.0 and 8.0, but the dissolution rates are lower and the final concentrations are 0.18 and 0.09 mM after 6 h of treatment. The best performance of the coating solution is observed at pH 7.0. At this pH, there is a slight mobilization of iron at the initial stages of treatment, not exceeding the level of 0.04 mM, but afterwards

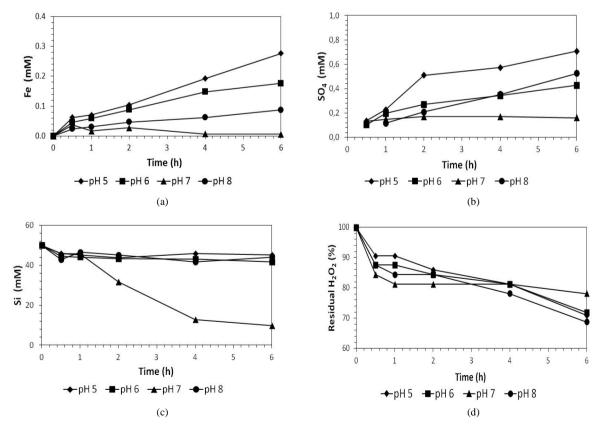


Figure 1. Concentration of dissolved (a) iron; (b) sulphates; (c) silicon and (d) % residual H_2O_2 in the aqueous phase vs. time at four operating pH values, 5.0, 6.0, 7.0, and 8.0. Initial Si 50 mM.

reprecipitation of iron occurred resulting in a final concentration lower than 0.004 mM.

The effect of pH on the oxidation of sulphates can be seen at **Figure 1(b)**. The highest oxidation is observed at the acidic pH 5.0, corresponding to 0.7 mM after 6 h. At pHs 6.0 and 8.0 the concentration of SO_4 in the solution after 6 h of treatment is 0.4 and 0.52 mM, respectively. At pH 7.0, the release of SO_4 in the aqueous phase is almost constant, varying between 0.15 - 0.17 mM, regardless of the treatment duration.

The evolution of Si is shown in **Figure 1(c)**. At the end of treatment tests, the concentration of Si was 45.5, 41.7 and 44.2 mM for the experiments executed under pH values 5.0, 6.0 and 8.0, indicating a very slight degree of precipitation compared to the initial Si concentration of 50 mM. On the contrary, the evolution of Si concentration at pH 7.0 suggests that a precipitation phenomenon occurs, resulting in a final concentration of Si after 6 h of treatment equal to 9.8 mM. According to several studies, Si concentration is strongly pH-depended and controlled by processes like polymerization, dissolution, absorption and precipitation (Alexander, 1954; Iler, 1979; Sjorberg, 1996). Our experimental data demonstrate that the higher removal of Si, i.e. 89% occur at pH 7.0 in accordance with the above studies. This may be attributed to the extensive silica polymerization, leading to the homogeneous nucleation of distinct SiO₂ phases on the oxidized pyrite surface.

Given that the higher removal of Si was associated with the lower level of dissolved iron, it may be deduced that silicic acid in the solution was associated with the iron hydroxides, leading to the formation of silica-iron(III) complexes on pyrite surfaces (Schenk & Weber, 1968; Herbillon & Vinh, 1969). The silicic acid association with hydrous ferric oxyhydroxides involves both absorption and polymerization processes and depends on the amount of H_4SiO_4 present at their surfaces, i.e. absorption as monomeric silicate on the surface, or via siloxane linkages (Si-O-Si) essentially polymerizing to form a separate silica phase (Swedlund & Webster, 1999; Swedlund et al., 2011). According to Schwertmann & Cornell (1991), the Fe³⁺ hydroxides formed through co-precipitation with silicates are amorphous and/or poorly crystalline and the transformation of amorphous iron precipitates to more crystalline phases is blocked by the absorption of silicate species.

The % residual H_2O_2 in the solution during treatment tests vs. time and pH is shown in **Figure 1(d)**. The residual hydrogen peroxide in the solutions decreased with time and after 6 h of treatment was corresponded to 69% - 78% of the initial amount. The consumption of the oxidizing agent does not correspond stoichiometrically to the amount of pyrite oxidation. It decomposes gradually and this reaction is mainly catalyzed by pyrite surfaces and dissolved iron ions in the solution, but also is catalyzed heterogeneously due to the presence of precipitated amorphous and/or poorly crystalline iron hydroxides (McKibben & Barnes, 1985; Lin & Gurol, 1998).

The experimental results obtained with the silica solutions of variable concentrations are shown in **Figure 2**. It is noted that all these experiments were carried out at pH 7.0. As seen in **Figure 2(a)**, when the treatment is conducted using the highest concentration of SiO₂ (50 mM), the concentration of dissolved Fe increases during the first 2 h and then decreases at the final value of 0.004 mM. During the treatment tests with SiO₂ 25 mM, the decrease of Fe concentration down to the value of 0.004 mM occurs only after 24 h of treatment, indicating a slower kinetics of precipitation. Iron precipitation was not observed during the two other experiments that were carried out with lower SiO₂ concentrations, i.e. 5 and 10 mM. Presumably, a longer treatment time is required for the appearance of precipitation process using these low SiO₂ levels.

The evolution of SO_4 concentrations during the treatment with variable SiO_2 concentration is shown in **Figure 2(b)**. It is evident that the oxidation of sulphur is higher as the SiO_2 concentration decreases. This is obviously related with the slower kinetics of formation of the silica coating at the lower SiO_2 concentrations. The variation of SiO_2 concentration during this experimental set is shown in **Figure 2(c)**. It is evident that the kinetics of SiO_2 removal from the aqueous phase depends greatly on the initial concentration of silica.

3.2. Characterization of Treated Pyrite Surfaces by SEM/EDS

SEM microphotographs of pyrite grains treated with 50 mM SiO₂ at pH 5.0, 7.0 and 8.0 are shown in **Figure 3**. Pyrite treated at pH 7.0 has a completely different surface morphology, which is due to the development of the $Fe(OH)_3$ -Si(OH)₄ coating.

EDS analyses of this grain indicated up to 16 wt% of Si and 12 wt% of O. Iron (52%) and sulphur (20%) measurements cannot be directly attributed to surface species due to the pyrite background. The presence of SiO₂ aggregates of approximately 5 μ m is also clear on the pyrite surface. Characteristic etch pits can be observed on the surface of pyrite grains treated at pH 5.0 and to a lesser extent at pH 8.0. According to the EDS analysis, grains at pH 5.0 have a very low content of Si, i.e. no more than 0.30 wt%. At pH 6.0 and 8.0, the concentration of Si was up to 5 wt%.

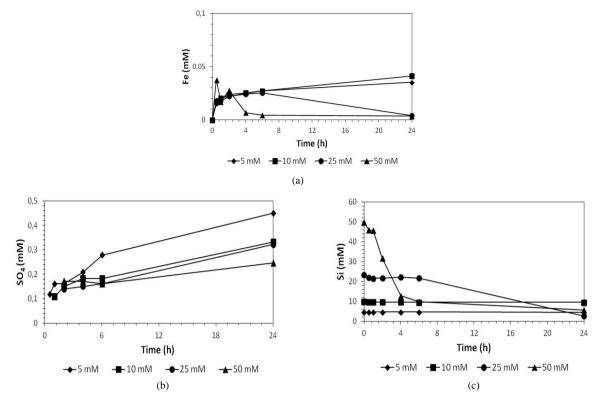
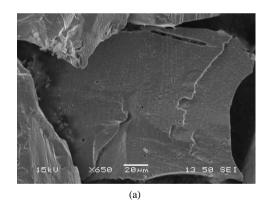
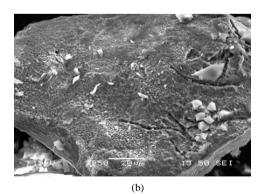


Figure 2. Concentration of dissolved (a) iron; (b) sulphates and (c) silicon vs. time for the pyrite treated with variable concentrations of Si, 5, 10, 25 and 50 mM at pH 7.0.





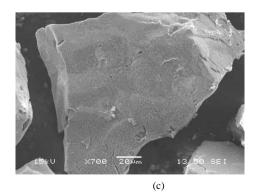


Figure 3. SEM microphotographs of the (-125 + 75) µm pyrite size fraction treated with a solution containing SiO₂ 50 mM buffered at pH (a) 5.0, (b) 7.0 and (c) 8.0.

Silicon concentration on the surfaces of pyrite grains treated with variable concentrations of SiO₂ at pH 7.0 was low, as indicated by EDS, i.e. up to 0.40 and 0.46 wt% for experiments carried out with solution of SiO₂ 5 and 10 mM, respectively, after 24 hours of treatment. A higher content of Si was measured, i.e. up to 2.0 wt%, when the treatment was conducted with SiO₂ 25 mM. SiO₂ aggregates of approximately 2 - 5 μ m are also obvious on pyrite surface.

4. Conclusion

Based on the results of this study, the following conclusions can be drawn: The treatment of the pyrite grains $(-125 + 75) \mu m$ with a solution consisting of H₂O₂ 0.1 M, SiO₂ 50 mM and buffered at pH 7.0 for 6 hours resulted in the formation of an extensive coating on the pyrite surface, containing up to 16 wt% of Si. The formation of this coating prevented pyrite oxidation, as demonstrated by the curves of iron and sulphates in the aqueous phase. The optimum pH for the development of surface coating is close to pH value 7.0. The kinetics of the process is greatly influence by the initial concentration of SiO₂. For instance, precipitation of SiO₂ is completed after 6 hours starting with 50 mM of SiO₂ and 24 hours with 25 mM SiO₂.

Experiments are ongoing to examine the stability of silica coatings under different conditions and evaluate their overall effectiveness in inhibiting pyrite oxidation.

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