

Titanasilsesquioxane-Alkylaluminum Catalyst System for Ethylene Polymerization

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Received August 4, 2012; revised September 8, 2012; accepted September 20, 2012

ABSTRACT

Homogeneous Ti (IV) complexes covalently anchored to Polyhedral Oligomeric Silsesquioxane (POSS) have been synthesized by the stoichiometric reaction between titanium (IV) alkoxide and (*iso*-Octyl)₇Si₇O₉(OH)₃. These catalyst precursors formulated as [Ti(OR)(*iso*-Octyl)₇Si₇O₁₂] were characterized by physicochemical and spectroscopic methods. These supported catalysts are found to be active in polymerization of ethylene at high temperatures in presence of ethylaluminum sesquichloride (Et₃Al₂Cl₃, EASC) as co-catalyst. The polyethylene obtained is generally linear, crystalline and display low molecular weight distribution. The microstructure of the polymer was analyzed by NMR and FT-IR spectroscopic methods which indicated a chain transfer reaction to aluminum. The unique molecular properties of PE formed has been compared with commercial micronized PE wax which find industrial applications in surface coating and ink formulations. The effect of reaction conditions on catalytic behaviour is described.

Keywords: POSS; Titanasilsesquioxane; Polyethylene; Ethylaluminum Sesquichloride; Polymer Microstructure

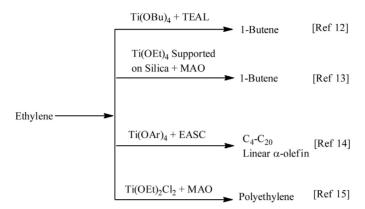
1. Introduction

Numerous catalysts have been developed, studied and commercialized for the production of polyolefins [1-4]. A large fraction of these catalysts, especially the industrially relevant ones, are heterogeneous systems prepared by the deposition of soluble complexes of Ti. Zr and Cr including metallocene precursors on high surface area supports such as silica and alumina [5]. The best choice of support for heterogeneous olefin polymerization catalyst is amorphous silica gel because it has a high surface area, good morphology, fragmentation properties and silanol functionalities to anchor the catalyst [6]. However, due to the heterogeneous nature of the catalysts the catalytic species are difficult to characterize and mechanisms of the catalyzed organic transformations and the nature of the metal-silica interactions remain unclear. This is due to the inherently very complicated atomic structure of the anchored silica surfaces. Improvement of this and alternative immobilization techniques, such as catalyst tethering [7,8] and grafting [9-11], remains therefore a topic of great interest.

The oxophilic alkoxide group has been considered as alternative for the ubiquitous Cp ligands. A few aliphatic and aromatic alkoxides of group (IV) metals have been employed for the oligomerization of ethylene in presence of alkylaluminum activators. As indicated in **Scheme 1** a majority of these lead to dimers or alpha olefins as the end products [12]. Some silica supported $Ti(OEt)_4$ complexes developed by Phillips in the eighties also showed dimerization activity for ethylene in presence of methyllalumoxane (MAO) co-catalyst [13]. In an earlier study, we had shown that bulky titanium aryloxide complexes were found to be selective towards the formation of linear α -olefins from ethylene in combination with ethylaluminum sesquichloride (Et₃Al₂Cl₃, EASC) as co-catalyst [14]. Due to the high tendency of β -hydride elimination associated with these catalysts preparation of high molecular weight polyethylene for industrial applications poses a challenge [15].

In recent years polyhedral oligomeric silsesquioxanes (POSS) have gained attention for its effective homogeneous mimic for zeolites as well as amorphous and mesoporous silica which contain surface silanol sites. POSS are a class of three dimensional oligomeric organosilicon compounds with cage like framework (ca. 1.5 - 2.0 nm) possessing different degrees of symmetry. Over the last decade or so these materials have evolved as alternative supports to silica surfaces for heterogenizing homogeneous catalysts [16-18]. The most common silsesquioxane systems include the cube-octameric clusters (*i.e.* R₈Si₈O₁₂) and incompletely condensed frameworks such as

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Scheme 1. Products of ethylene oligomerization by titanium alkoxide/aryloxide.

(c-C₆H₁₁)₇Si₇O₉(OH)₃ [19]. While a majority of Ti-POSS systems have been proven as highly active homogeneous catalyst system for the epoxidation of alkenes [20,21] systematic work on POSS based catalysts for making industrially important polyolefins is, however, lacking [22,23]. In order to explore this further we report herein the synthesis of a series of titanium alkoxide complexes tethered to a trisilanol POSS derivative such as (*iso*-Octyl)₇Si₇O₉(OH)₃. The supported titanium complexes were evaluated in polymerization of ethylene in combination with different alkylaluminum co-catalysts. The influence of reaction conditions on polymer properties has been described.

$$i ext{-Oct}$$
 $Si ext{OH}$
 $i ext{-Oct}$
 $O ext{OH}$
 $i ext{-Oct}$
 $O ext{OH}$
 $O ext{Si}$
 $O ext{Oct}$
 $O ext{I-Oct}$

iso-Octyl POSS trisilanol

2. Experimental

2.1. Materials

All reactions were carried out in an atmosphere of dry nitrogen in a dry box M-Braun (Unilab) or with the use of standard high vacuum Schlenk techniques. Toluene and *n*-pentane were dried over sodium-benzophenone ketyl and freshly distilled under nitrogen atmosphere prior to use and kept over molecular sieves (4A). Polymer grade ethylene (>99.95% purity) was used directly from a commercial plant, the pressure of which was adjusted with a two stage regulator. Alkylaluminum co-catalysts were purchased from Ethyl Corporation (Et₃Al, Et₃Al₂Cl₃) or Witco GmbH (MAO 10% in Tolu-

ene) and used without further purification. Titanium tetra*iso*propoxide, Titanium tetraethoxide, Titanium tetrapropoxide, Titanium tetrabutoxide and *iso*-octyl POSS triol [C₅₆H₁₁₉O₉Si₇(OH)₃] were obtained commercially (Aldrich) and were used as received.

2.2. Methods of Testing

Microanalysis was carried out on a Perkin Elmer C, H and N analyzer. The FT-IR spectra were recorded in Nujol on a Nicolet 6700 FT-IR (400 - 4000 cm⁻¹) spectrometer. For end group analysis the IR spectra were recorded by pressing the polyethylene powders into 0.5 mm thick pellets and scanning in the region between 800 -1400 cm⁻¹ with 0.5 cm⁻¹ resolution for 16 scans. ¹H NMR spectra of catalysts were recorded on a Varian 300 MHz instrument using C₆D₆ as solvent. ²⁹Si (79.5 MHz) NMR spectra were recorded in C₆D₆ solutions on a Brüker 400 MHz spectrometer at 25°C with a total of 10000 scans for each sample. The ${}^{13}\mathrm{C}$ NMR and ${}^{1}\mathrm{H}$ NMR spectra of polymer samples were recorded on an Ultrashield Brüker 400 MHz spectrometer at 110°C. The solutions were made up in o-dichlorobenzene-d₄. The number of scans performed for each spectrum was 512 or 2048 and 2048 or 6144 for ¹H and ¹³C NMR respectively. For the ¹H-NMR spectra the chemical shifts were referenced to residual H solvent shifts at 7.249. For the ¹³C NMR spectra the chemical shifts were referenced internally to the major backbone methylene carbon resonance which was taken to be 30.00 ppm. FAB mass spectral analysis of catalysts was carried out on a JEOL SX 102/DA - 600 mass spectrometer/data system using Argon/Xenon as the FAB gas, spectra recorded at room temperature. m-Nitrobenzyl alcohol was used as the matrix. The accelerated voltage was 10 kV. Molecular weights of polymer were determined by size exclusion chromatography. The high temperature gel permeation chromatographic (GPC) analysis of the polymers was carried out with Polymer Lab's PL-GPC 220 chromatograph. A set of three PL Gel Mixed B columns were used. 1,2,4

Trichlorobenzene was used as the mobile phase at 135°C. 0.0125% Irganox was added to the mobile phase before filtration. A sample preparation unit. PL-SP260, was used to dissolve and filter the samples at 135°C. 0.2% solutions were injected with the help of an auto sampler to record the chromatogram. Viscotek's Trisec conventional software was used to analyze the chromatograms. which were matched with polystyrene calibration curve. The following MHK constants were used to construct a universal calibration curve. For polystyrene, K = 1.2105 e^{-4} and a = 707; for PE, K = 4.055 e^{-4} and a = 725. Differential scanning calorimetry (DSC) was performed under continuous nitrogen purge on a Mettler-Toledo DSC 822 instrument from 30 to 200°C at a scan rate of 10°C/min. Indium was used to perform calibration of equipment. XRD measurements were carried out on a Brüker AXS model D8 advanced diffractometer. Scattering patterns were obtained with Ni filled CuKα radiation ($\lambda = 1.5406$ Å, generator voltage = 45 kV, current = 40 μA) in the reflection mode, as detected by a scintillation counter. Samples were pressed films approximately 400 μ thick and were scanned into 2θ ranges from 15° to 45° at a rate of 1°/min. Measurements were recorded at steps of 0.02°. Scanning electron micrographs (SEM) of powdered polymer samples were taken on a Jeol JFC 1100 instrument ion sputter water. They were observed in a Jeol 5600 CV scanning electron microscope in Hv mode at an operating voltage of 20 kV.

2.3. Catalyst Preparation

Catalysts **1-4** were synthesized by a modified literature procedure (**Scheme 2**) [20]. In a typical experiment a solution of 0.39 mmol (0.111 g) of $Ti(OPr^{i})_4$ in toluene (15 ml) was slowly added to 0.38 mmol (0.451 g) of the corresponding (iso-Octyl)₇Si₇O₉(OH)₃ ligand in toluene (15 ml) under nitrogen atmosphere and the mixture was heated at 100° C for 18 h. The solvent was carefully removed, the viscous gel washed with n-pentane and finally a yellow viscous complex was isolated, Yield 0.44 g, 78%.

Catalyst **1** ($C_{59}H_{126}O_{13}Si_7Ti$); Anal calcd. C, 55.01%; H, 9.86%; found: C, 55.18%; H, 9.55%. ¹H NMR (C_6D_6 , 25°C): 1.02 - 1.05 (42H, CH_2 -CH-(CH_3)₂ & 6H,

O-CH-(CH₃)₂), 1.10 - 1.13 (70H, (CH₂)₅-CH), 2.10 (7H, CH₂-CH-(CH₃)₂), 4.3 (1H, O-CH).

Catalyst **2** Yield = 0.28 gm, 72% ($C_{58}H_{124}O_{13}Si_7Ti$); Anal calcd. C, 54.66%; H, 9.82%; found: C, 54.73% H, 9.69%. ¹H NMR (C_6D_6 , 25°C): 1.02 - 1.06 (42H, CH₂-CH-(CH₃)₂ & 3H, O-CH₂-CH₃), 1.08 - 1.12 (70H, (CH₂)₅-CH), 2.20 (7H, CH₂-CH-(CH₃)₂), 3.62 (2H, O-CH₂).

Catalyst **3** Yield = 0.27 gm, 68% ($C_{59}H_{126}O_{13}Si_7Ti$); Anal calcd. C, 55.01%; H, 9.86%; found: C, 55.65%; H, 9.62%. ¹H NMR (C_6D_6 , 25°C): 1.02 - 1.06 (42H, CH₂-CH-(CH₃)₂ & 3H, O-CH₂-CH₂-CH₃), 1.11 - 1.14 (70H, (CH_2)₅-CH & 2H, O-CH₂-CH₂), 2.12 (7H, CH₂-CH-(CH₃)₂), 3.57 (2H, O-CH₂).

Catalyst **4** Yield = 0.24 gm, 74% ($C_{60}H_{128}O_{13}Si_{7}Ti$); Anal calcd. C, 55.32%; H, 9.92%; found: C, 54.95% H, 9.70%. ¹H NMR ($C_{6}D_{6}$, 25°C): 1.01 - 1.04 (42H, CH₂-CH-(CH₃)₂ & 3H, O-CH₂-CH₃), 1.10 - 1.15 (70H, (CH₂)₅-CH & 4H, (CH₂)₂-CH₃), 2.14 (7H, CH₂-CH-(CH₃)₂), 3.61 (2H, O-CH₂).

2.4. General Procedure of Ethylene Polymerization

Catalytic ethylene polymerization was carried out in a 100 ml stirred autoclave (Model 4593 Parr, USA) connected to a process controller (model 4871) and operated through the microprocessor controller (PC/PLC) using a customized Honeywell specview 32 software. Prior to polymerization, the reactor was heated to 150°C under nitrogen for 2 h and cooled to ambient temperature. In a typical experiment, catalyst 1 (2.2 mg, 1.7×10^{-6} mol) dissolved in toluene (20 ml) and EASC (0.247 g, 9.9 × 10⁻⁴ mol) in toluene (20 ml) were carefully charged into the reactor under a nitrogen blanket. The Al/Ti was kept at 500 (mol/mol) and the reactor temperature was increased to 100°C and then pressurized with ethylene to 300 psi. The reaction was terminated after 1 h. The reaction mixture was poured in acidic methanol (5% v/v) to precipitate the polymer. The precipitated white polyethylene powder was filtered, washed several times with methanol followed by acetone and finally dried under vacuum to a constant weight.

$$i\text{-Oct} \qquad i\text{-Oct} \qquad i\text{-Oct}$$

Scheme 2. Synthesis of compounds 1 - 4: $R = Pr^{i} 1$, Et 2, Pr 3, Bu 4.

3. Results and Discussion

3.1. Synthesis of Ti(IV) Complexes with (*iso*-Octyl)₇Si₇O₉(OH)₃ and Its Derivatives

The preparation of titanasilsesquioxane catalysts could be achieved by a stoichiometric reaction between titanium (IV) alkoxide and (*iso*-Octyl)₇Si₇O₉(OH)₃ ligand (alcohol exchange) in an appropriate solvent and separation of liberated alcohol by azeotropic/vacuum distillation [20,24]. The resulting catalysts 1 - 4 (**Scheme 2**) were employed for carrying out ethylene polymerization.

3.2. Catalyst Characterization

The reaction of Ti(OR)₄ and (iso-Octyl)₇Si₇O₉(OH)₃ ligand in toluene afforded yellow coloured viscous catalysts 1 - 4 which are soluble in aromatic solvents but only sparingly in aliphatic hydrocarbons. Catalysts 1 - 4 have been characterized by microanalysis, FTIR, UV-Visible, ¹H NMR, ²⁹Si NMR and FAB Mass spectra. In the FT-IR spectra of catalyst 1 no peaks were observed in the 3000 -3500 cm⁻¹ region indicating deprotonation of the (iso-Octyl)₇Si₇O₉(OH)₃ ligand. However, in the FT-IR of parent (iso-Octyl)₇Si₇O₉(OH)₃ ligand the band at 890 cm⁻¹ due to the bending mode of Si-OH stretching is replaced by a new peak at 928 cm⁻¹ assigned to the presence of Si-O-Ti vibration [25]. In the UV-Visible spectra of 1, an absorption peak was observed at 215 nm. This absorption is close to the 212 - 228 nm previously reported for Ti-silsesquioxane complexes and assigned to ligand to metal charge transfer (LMCT) transition involving four co-ordinated titanium bearing oxygen ligand

The ²⁹Si NMR spectrum of catalyst is particularly informative. In the ²⁹Si NMR spectra of (*i*-Octvl)₇Si₇O₉(OH)₃ multiplet signals were observed at $\delta = -58$, -67 and -68ppm (**Figure 1(a)**). The peak for Si-OH is observed at δ = -58 ppm. After complexation with titanium centre (Catalyst 1, Figure 1(b)) the absence of signal at $\delta = -58$ ppm was noted suggesting that the corner capping reaction as shown was successful. In the ¹H NMR spectra the set of multiplets at $\delta = 1.03 - 1.06$ ppm for -CH₃ protons, 1.09 - 1.13 ppm for -CH₂ protons and broad peak at 2.10 ppm for -CH protons of iso-Octyl group were observed. The signal at $\delta = 4.3$ ppm was observed for –CH protons of the *iso*-propyl group. Feher *et al.* reported the ¹H NMR of incompletely condensed silsesquioxane where in the Si–OH signal was observed in the region of $\delta = 6$ -6.9 ppm [26,27]. The absence of OH protons in $\delta = 6$ -6.9 ppm region in the catalysts 1 - 4 indicates complete deprotonation of the silanol and attachment to the titanium alkoxide. In the FAB mass spectra of catalyst 1, the prominent peak for ligand fragment [(iso-Octvl)₇Si₇O₉ (OH)₃] appeared at 1181 and a low intensity molecular ion peak was observed at 1289 corresponding to the Ti

(POSS) (OPrⁱ) species. In an earlier work Edelmann *et al.* and others showed that the reaction of Ti-tetraethoxide and cyclohexyl-POSS triol lead to dimeric complexes which were characterized by X-ray crystal structure analysis [20,28,29]. The concurrent formation of a dimeric compound such as (POSS-OOO)Ti-OPrⁱ-Ti (OOO-POSS) along with the mononuclear (POSS-OOO) Ti(OPrⁱ) was observed [16,29]. However, the synthetic method used in this work showed the formation of monomeric species only.

3.3. Catalytic Ethylene Polymerization

Unlike the regular polyethylene expected of a Ziegler type catalyst the present $(iso\text{-octyl})_7 \mathrm{Si}_7 \mathrm{O}_9(\mathrm{OH})_3$ supported Ti (IV) alkoxides produced unusually low molecular weights with the M_w in the 800 - 1500 range in all cases. Since the polydispersities are also quite narrow these PE resemble polyethylene waxes or oligomers within the C_{70} chain length. Synthetic PE wax is a class of commercial product that has specific end application. The results of ethylene polymerization using catalysts 1 - 4 are shown in **Table 1**. The polymerization was carried out under different conditions such as temperature, Al/Ti ratio, co-catalysts, solvents and ethylene pressure.

Initial examination of catalysts indicate that catalyst 1) containing an iso-propoxide group shows maximum activity while substitution of this pendant group by ethoxide 2), propoxide 3) or butoxide 4) results in considerable reduction in the polymer yields (Table 1, Entries 1 - 4, Figure 2). Apparently steric factors tend to significantly influence the polymerization activity of titanasilsesquioxane catalysts. It was found that the activity of catalysts 1-4 when activated by EASC followed the order 4(OBu) < 3(OPr) < $2(OEt) < 1(OPr^{i})$. This may be explained by the fact that the non-linear iso-propoxide allow better access to the titanium centre than that of linear alkoxy (ethoxy, propoxy and butoxy) groups indicating that accessibility to the Ti (IV) centre is a parameter influencing the overall activity [20]. The activity is predominantly dependent on the nature of the co-catalyst. Ethylaluminum sesquichloride was found to promote the ethylene polymerization. Other chlorinated alkylaluminum compounds such as ethylaluminum dichloride (EtAlCl₂) and diethylaluminum chloride (Et₂AlCl) are also active but catalyst productivity was slightly lower. In case of the conventional co-catalysts for polyolefin production such as Et₃Al and MAO only the latter showed moderate activity while Et₃Al is practically inactive (Table 2, Entry 5). Moreover, the presence of bulky iso-octyl group attached to silsesquioxane framework probably has a kinetic control on the reaction rate leading to oligomeric PE product (C_{70} carbon chain). This is in contrast to previous reports on ethylene polymerization on a cyclohexyl silsesquioxane based Ti-catalysts

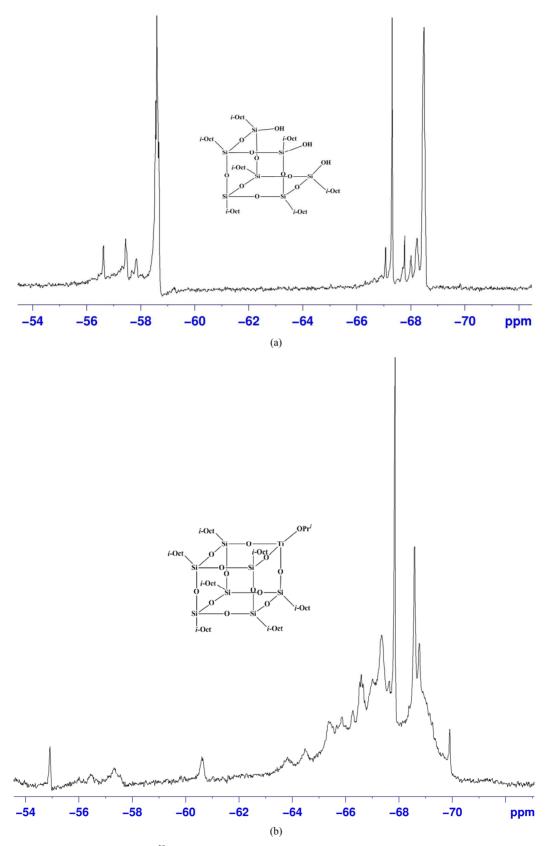


Figure 1. ²⁹Si NMR of (iso-octyl)₇Si₇O₉(OH)₃ (a) and catalyst 1(b).

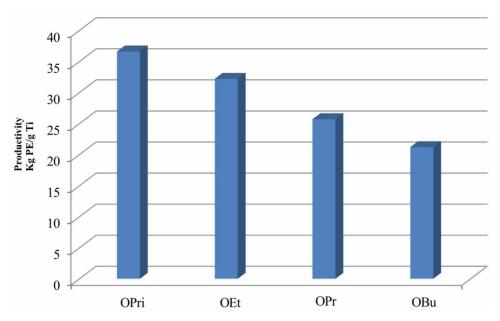


Figure 2. Influence of alkoxy group on ethylene polymerization.

Table 1. Ethylene polymerization with Titanasilsesquioxane-EASC system*.

Entry	Catalyst	Productivity Kg PE/g Ti	$M_{ m w}$	PDI	T _m (°C) —	% Crystallanity (X _c %)	
						XRD	DSC
1	1	36.6	1051	1.5	122	70.7	72.3
2	2	32.2	729	1.7	117	71.2	69.6
3	3	25.7	1146	1.6	121	72.6	73.1
4	4	21.2	927	1.7	119	70.8	69.4
5**	Ti(OEt) ₂ Cl ₂		1.3×10^6	1.8			

^{*}All reactions were carried out in a 100 mL SS reactor at 100°C and 300 psi ethylene pressure for 1 h, Al/Ti= 500 (mol/mol).
**[15].

Table 2. Effect of co-catalysts on ethylene polymerization at 100°C.

Entry	Co-catalyst*	Productivity Kg PE/g Ti	T _m (°C)
1	EASC	36.6	122
2	MAO	9.1	133
3	EADC	6.1	122
4	DEAC	2.2	124
5	TEAL	0.9	
6	TIBAO		

^{*}EADC = $EtAlCl_2$, $DEAC = Et_2AlCl$, TIBAO = Triisobutyldialumoxane, $EASC = Et_3Al_2Cl_3$, $TEAL = Et_3Al$, MAO = Methylalumoxane; Catalyst 1, $^PC_2H_4 = 300$ psi, Al/Ti = 500 (mol/mol).

which generally produced high molecular weight PE in presence of co-catalyst like B(C_6F_5)₃ or MAO [23]. Interestingly, the polyethylene obtained with these titanasilsesquioxane catalysts display narrow molecular weight distribution ($M_w/M_n=1.5$ - 1.7) and low molecular weights

corresponding to the C_{30} - C_{70} carbon nos.

Detailed studies on the effect of temperature were then carried out employing catalyst 1 and EASC as the co-catalyst. From the results summarized in **Table 3** it is evident that increasing the reaction temperature from

Table 3. Effect of temperature on polymerization*.

Entry	Temp (°C)	Productivity Kg PE/g Ti	T _m (°C)
1	100	36.6	122
2	50	19.0	123
3	27	3.9	121

*Catalyst 1-EASC, ${}^{P}C_{2}H_{4} = 300 \text{ psi}$, 1h, Al/Ti = 500 (mol/mol)

ambient to 100°C has marked effect on the catalyst activity (**Table 3**, Entries 1 and 3). Similarly the effect of ethylene pressure on polymerization was investigated and these results are compiled in **Table 4**. Applying higher pressure under similar conditions lead to an enhancement in productivity of up to 48% for an increase in ethylene pressure of 7 Kg/cm² (**Table 4**, Entries 1 and 2). Generally, a combination of higher Al/Ti ratio and a higher temperature lead to improvement in the productivity of the catalyst 36.6 Kg PE/g Ti (**Table 1**, Entry 1).

A brief examination of effects of different solvents (**Table 5**) indicated that chlorinated aromatic solvent such as chlorobenzene gave higher productivity (45.2 Kg PE/g Ti) than that observed for toluene (36.6 Kg PE/g Ti). However, other hydrocarbon solvent such as cyclohexane showed poor activity which is probably due to the low solubility of catalysts in this solvent.

To investigate further the properties of these polyethylene reported in **Table 1**, they were characterized by GPC. The GPC of this material also displays similar distribution in the low molecular weight region (**Figure 3**). The PE obtained with catalysts 1 - 4 display exceptionally low molecular weights ($M_{\rm w} = 729 - 1146$) and narrow PDI $(M_w/M_n = 1.5 - 1.7)$. As a benchmark for comparison of polymer properties with that obtained in this work a known sample of micronized polyethylene wax, MPP 635 powder, was used. The reference polyethylene sample is a micronized, high $T_{\rm m}$, crystalline form of polyethylene which was supplied by M/s Micro Powders, Inc., USA. The product had a $T_{\rm m}$ value of 125°C, a molecular weight of 2600, d (25°C) of 0.96, and a maximum particle size of 31 μ m. The values compare well with the $M_{\rm w}$ (2600) and polydispersity (PDI = 1.2) exhibited by the commercial polyethylene wax powder. In no case was high molecular weight PE ($\approx M_{\rm w} \ge 10^{\circ}$) obtained although these catalysts resemble typical Ziegler systems. The DSC (**Figure 4**) also reveals lower $T_{\rm m}$ (~120°C - 122°C) values than that observed for conventional HDPE or LDPE (128°C - 135°C). The intensity of the equatorial peaks in the X-ray diffractogram (**Figure 5**) for the 110 $(2\theta = 21.4^{\circ})$ and 200 $(2\theta = 23.9^{\circ})$ reflection planes for the experimental sample closely match the intensity of the

Table 4. Effect of pressure on ethylene polymerization*.

Entry	Pressure (psi)	Productivity Kg PE/g Ti	T _m (°C)
1	400	54.9	123
2	300	36.6	122
3	200	14.6	121

*Catalyst 1-EASC, 100°C, 1h, Al/Ti = 500 (mol/mol).

Table 5. Influence of solvent on polymerization*.

Entry	Solvent	Productivity Kg PE/g Ti	$T_{\rm m}(^{\circ}{\rm C})$
1	Toluene	36.6	122
2	Chlorobenzene	45.2	125
3	Cyclohexane	6.1	

*Catalyst 1-EASC, ${}^{P}C_{2}H_{4} = 300 \text{ psi}$, 1h, Al/Ti= 500 (mol/mol)

commercial sample and the pattern is indicative of orthorhombic crystallinity in these samples.

The crystalline nature of these polymers was estimated by integration of the X-ray diffraction peaks observed. A high degree of crystallinity was indicated in all cases, which was in the range of 69% - 76%. The polyethylene powders isolated after polymerization were generally observed to be fine particles ($<500~\mu m$) having uniform morphology as seen by scanning electron microscopy. A typical scanning electron micrograph (SEM) is reproduced in **Figure 6**. The morphology compares well with that of the commercial sample though the latter products are micronized (15 - 30 μ) by a separate process for end use. It is therefore possible to tailor the M_w and polydispersities of the polyethylene obtained by the titanasilsesquioxane-EASC catalyst system as per desired commercial application.

3.4. Polymer Microstructure

End group analysis of PE was made using ¹H NMR, ¹³C NMR and FT-IR spectroscopic methods. In the ¹H NMR spectra of PE a strong signal at 1.33 ppm was observed for the main chain methylene protons (–CH₂–CH₂–)_n. A signal of lower intensity at 0.90 ppm (**Figure 7**) was ascribed to the methyl end group protons (–CH₃). However, the intensity of the methyl proton is small due to the low concentration with respect to the main chain methylene protons. Likewise, in the olefinic region much weaker signal assigned to the vinyl chain end (CH₂ = CH–) at 4.9 - 5.0 ppm and vinylidene group (CH₂ = CH–) at 5.78 - 5.82 ppm were observed respectively. An additional very weak signal was observed at 3.56 - 3.59 ppm which is

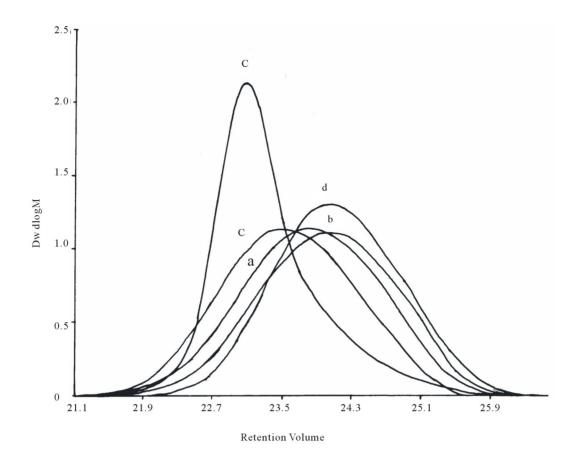


Figure 3. GPC of polyethylene Table 1: (a) entry 1, (b) entry 2, (c) entry 3, (d) entry 4 and (e) MPP - 635.

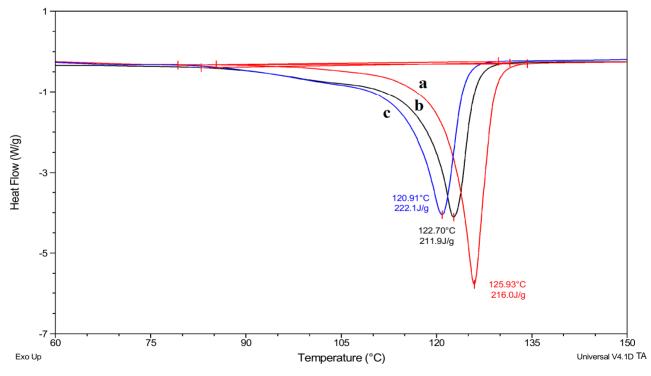


Figure 4. DSC of PEs MPP - 635: (a) Table 1, entry 1 (b) and entry 3 (c).

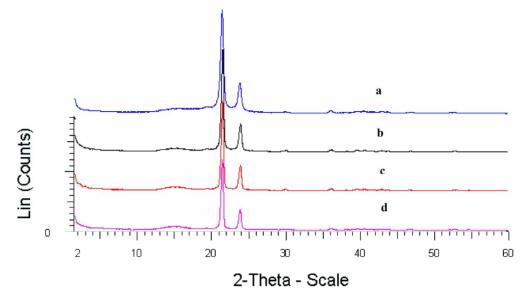


Figure 5. XRD of PEs: (a) MPP - 635, Table 1, entry 1 (b), entry 2 (c) and entry 3 (d).

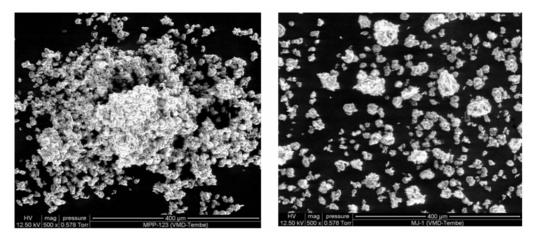


Figure 6. SEM of PEs MPP - 635 (Left) and Table 1, entry 1 (Right).

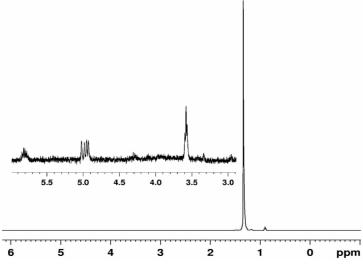


Figure 7. ¹H NMR of PE Table 1 and entry 1.

assigned to the presence of hydroxymethyl end group (-CH₂OH) in polyethylene, probably arising due to the transfer of active titanium centre to aluminum of EASC followed by exposure to oxygen to the resulting C-Al bonds during post reaction work up which converts to the hydroxy group (Equation (1)) [30,31]. These results suggest that obtained PE is a linear polymer.

$$\begin{array}{c} \operatorname{Et_2ClAl} - \operatorname{CH_2} - \operatorname{CH_2} - \operatorname{P} \\ \operatorname{Et_2Cl_2Al} - \operatorname{CH_2} - \operatorname{CH_2} - \operatorname{P} \end{array} \xrightarrow{\hspace{1cm} \operatorname{O_2/H_+}} \operatorname{HO} - \operatorname{CH_2} - \operatorname{CH_2} - \operatorname{P} \end{array} \tag{1}$$

The ¹³C NMR spectra (**Figure 8**) showed a strong signal at 30.0 ppm (B4) for the main chain methylene carbons ($-CH_2-CH_2$)_n of PE and the lower intensity signals at 14.08 ppm (B1) $-CH_3$, 22.87 ppm (B2) $\alpha-CH_2$, 32.17 ppm (B3) $\beta-CH_2$ which are ascribed to the chain ends

(Equation (2)) [32,33]. These results clearly support that synthesized PE is linear in nature.

As a benchmark for comparison, the ¹H NMR and ¹³C NMR spectra of commercial sample MPP - 635 were studied. In general, both ¹H and ¹³C NMR spectrum of MPP - 635 was similar to the spectra discussed above (**Figures 9** and **10**).

In the FT - IR spectrum of polyethylene vinyl peaks at 908 cm⁻¹ & 991 cm⁻¹ and vinylidene peak at 888 cm⁻¹ as well as an absorption band at 1050 cm⁻¹ attributed to the presence of hydroxy-methyl end group in polyethylene were clearly observed. Their presence was confirmed by ¹H NMR spectroscopy as discussed above [31,34]. In

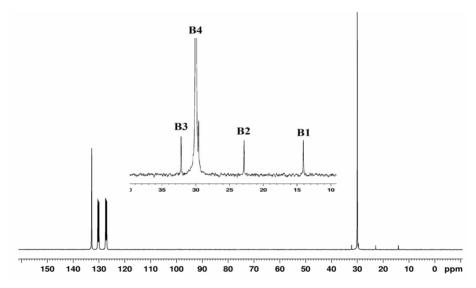


Figure 8. ¹³C NMR of PE Table 1 and entry 1.

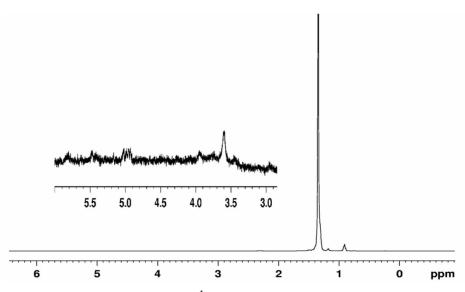


Figure 9. ¹H NMR of MPP - 635.

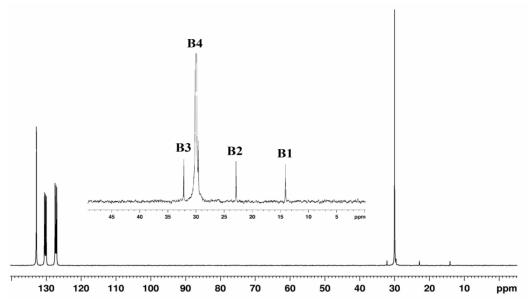


Figure 10. 13 C NMR of MPP - 635.

addition, the characteristic absorbance band at 1376 cm⁻¹ was assigned to the –CH₃ group of polyethylene. As a benchmark for the comparison of the polymer properties with those obtained in this study, commercial PE wax sample MPP - 635 was used. The ratio of unsaturated end group (vinyl) to saturated end group (methyl) of polyethylene was calculated as 0.96:1. The almost equal proportion (1:1) of these end groups supports the formation of linear polyethylene [35].

The obtained results showed that the synthesized polyethylenes possess linear structure and the presence of chain end groups indicate that chain transfer to aluminum is predominant in the catalytic reaction; the resultant polymer has low molecular weight with narrow PDI.

3.5. Reaction Mechanism

Treatment of mononuclear Ti(OR)₄ type alkoxides with alkylaluminum halides has been reported to yield active intermediates responsible for the polymerization of ethylene to low molecular weight products [36-39].

We believe that similar type of active species may be involved in the present titanasilsesquioxne system. Moreover, as EASC is derived from an equimolar mixture of EADC and DEAC [40], we have,

$$2Et_3Al_2Cl_3$$
 \bigcirc ($EtAlCl_2$), +(Et_2AlCl),

Since EASC can dissociate as Et₂AlCl and EtAlCl₂ in solution it is reasonable to expect the formation of two

types of catalytic species on interaction with titanasilsesquioxane catalyst.

The reduction of Ti (IV) in presence of EASC will generate catalytically active components. As shown in **Scheme 3** the active catalysts in polymerization need to retain monomeric four or five coordinate geometry to allow for olefin insertion and subsequent propagation/chain termination to aluminum alkyl. In the present titanasilsesquioxane catalytic system higher temperature tends to favour formation of active intermediates responsible for polymerization.

Based on this hypothesis it is possible to predict the pathway shown in **Scheme 3** for the formation of polyethylene. Though the structure of active intermediate is as yet unknown the mechanism leading to polyethylene is consistent with those reported previously for solution phase olefin polymerization using titanium alkoxides and aluminum alkyls [41,42] and cyclopentadienyl Ti-POSS complexes with MMAO [43]. Efforts are underway to investigate the detailed kinetics of this reaction.

4. Conclusion

Alkoxides of Titanium (IV) supported on polyhedral oligomeric silsesquioxane act as efficient catalysts in the presence of EASC as co-catalyst for the synthesis of specialty low-molecular weight PE with good productivities. The catalyst activity was significantly influenced by the reaction temperature and Al/Ti ratios. The physical properties exhibited by these linear polyethylenes such as low molecular weight, high crystallinity and narrow PDI suggest single-site catalytic behavior of these supported titanasilsesquioxane catalysts. The close resemblance of polymer properties to that of commercially important PE

Polyethylene

Scheme 3. Proposed mechanism of ethylene polymerization by titanasilsesquioxane catalyst system.

waxes holds promise for development of alternative catalysts for this process.

5. Acknowledgements

One of the authors (AMM) gratefully acknowledges the management of Reliance Industries Limited for use of its technical facility and the Head, Department of Applied Chemistry, S. V. National Institute of Technology of Surat for supporting this work. The authors also thank the Regional Sophisticated Instrumentation Centre, IIT

Mumbai and Central Drug Research Lab., Lucknow, for NMR and FAB mass spectral analysis.

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