

Photocatalytic Degradation of 2,6-Dichlorophenol in Aqueous Phase Using Titania as a Photocatalyst

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ABSTRACT

The paper includes the studies on photocatalytic degradation of 2,6-DCP in aqueous phase using titania (PC-105) as a photocatalyst. The degradation experiments were carried out by irradiating the aqueous suspensions of the model compound in the presence of photocatalysts under UV light. The rate of degradation was estimated from residual concentration spectrophotometrically. Various parameters affecting the degradation process viz. catalyst dose, pH, initial substrate concentration and time were investigated in order to obtain their optimum values. The maximum degradation of 2,6-DCP was achieved with 1.25 g/L catalyst dose at pH-4. The disappearance of 2,6-DCP obeyed pseudo-first order kinetics and the rate constant value was calculated to be $4.78 \times 10^{-4} \cdot s^{-1}$.

Keywords: Photocatalysis; Dichlorophenol; Titania; UV Light; Degradation

1. Introduction

Chlorophenols (CPs) constitute a particular group of priority toxic pollutants listed by the US EPA in the Clean Water Act [1-3] and by the European Decision 2455/ 2001/EC [4]. These pollutants are highly toxic and hardly biodegradable [5]. They are being introduced continuously into the aquatic environment as a result of several anthropogenic activities. CPs may be also generated as by-products during waste incineration, the bleaching of pulp with chlorine, and in the dechlorination of drinking water [6-9]. The variety, toxicity and persistence of CPs can directly present a threat to humans through contamination of drinking water supplies e.g. surface and ground water. They may produce disagreeable taste and odor to drinking water at concentrations below 0.1 µg/L [10] and adverse effects on the environment [11]. These contaminants are a major health concern because of their extremely high endocrine disrupting potency and genotoxicity. Consequently, considerable efforts have been devoted to develop a suitable purification method that can easily destroy these bio-recalcitrant contaminants. In recent years, the heterogeneous photocatalytic oxidation process employing TiO₂ and UV light has emerged as a promising method for the degradation of persistent organic pollutants and produces more biologically degradeable and less toxic substances [12,13]. This process is largely dependent upon the in-situ generation of hydroxyl radicals under ambient conditions which are capable of converting a wide spectrum of toxic organic compounds including the non-biodegradable ones into relatively innocuous end products such as CO₂ and H₂O. Ku and Hsieh [14] observed almost complete degradation of 2,4-dichlorophenol in aqueous solution under UV light in few hours of irradiation time and it was found that the degradation rate was influenced by the catalyst loading and pH of the solution. Bandara et al. [15] investigated the photocatalytic degradation of mono, di and trichlorophenols with TiO₂ and iron oxide aqueous suspensions and reported that the complete mineralization of chlorophenols was seen with TiO₂ whereas with iron oxide, only partial mineralization was observed. Antonaraki et al. [16] studied the photocatalytic degradation of all chlorophenols in the presence of H₂O₂ or polyoxometallate (POM) photocatalyst $PW_{12}O_{40}^{3-}$ under UV and visible light in aqueous phase. Saritha et al. [17] studied the degradation of 4-chloro-2-nitrophenol using different AOPs (UV, H2O2, UV/H2O2, Fenton, UV/Fenton and UV/TiO_2). The different parameters like pH, peroxide concentration, iron concentration and TiO₂ loading were varied to assess their effect on degradation. The degradation was estimated using COD reduction and compound reduction using spectrophotometeric methods which was further validated with HPLC studies. The order of degradation was: UV/Fenton > UV/Titania > UV/H₂O₂ > Fenton $> H_2O_2 > UV$. Information from various investigations suggests that the photocatalytic degradation of phenol and its chloro derivatives is mainly dependent upon the solution pH, catalyst type and dose, substrate

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type and concentration, light intensity etc. Therefore understanding the impacts of various parameters on the photocatalytic degradation efficiency is of paramount importance when choosing a sustainable, efficient technique for wastewater treatment.

Various reports have been reported dealing with the photodegradation of phenol and its chloro derivatives by employing metal oxide photocatalysts but only a few studies have been conducted for the degradation of 2,6-DCP. Therefore this paper aims to study the photo-catalytic degradation of 2,6-DCP using TiO₂ as a photo-catalyst. Further optimization of different process parameters has been carried out.

2. Experimental

2.1. Materials

Titanium PC-105 was gifted by Millennium Inorganic Chemicals, France and was used as received. 2,6-DCP was obtained from CDH chemicals. Double distilled water was used for preparation of various solutions. 1 M HCI or 1 M NaOH was used to adjust the desired pH.

2.2. Photocatalytic Reactor

The photochemical degradation experiments were performed in a batch reactor whose detail is given elsewhere [18]. The temperature was maintained constant throughout the reaction time. The spectra were taken with UVvis spectrophotometer (Shimadzu UV-2450 PC).

2.3. Procedure

A fixed amount of photocatalyst TiO_2 was added to 1000 mL of 25 mg/L solution of 2,6-DCP in each trial at defi-

nite pH. The suspension was subjected to irradiation under UV light for a fixed interval of time. The aqueous suspension was externally circulated through the reactor with the help of a pump. An aliquot was taken out at fixed time intervals and filtered through a Millipore syringe filter of $0.45 \,\mu m$.

Absorption spectra were recorded at $\lambda_{max} = 283$ nm. The rate of degradation was studied in terms of changes in absorption spectra at maximum wavelength. The percentage degradation was calculated as follows:

% Degradation =100 × $(C_0 - C)/C_0$, where C_0 = initial concentration of 2,6-DCP, C = concentration of compound after photoirradiation.

3. Results and Discussion

3.1. Photolysis/Photocatalytic Degradation of 2,6-DCP

The photocatalytic degradation of 2,6-DCP was investigated under three different experimental conditions: 1) UV alone 2) Dark + TiO₂ 3) UV + TiO₂. The concentration of 2,6-DCP in each solution was 25 mg/L. The results are given in **Figure 1**. 10% removal was achieved due to adsorption on TiO₂ as shown in figure and only 14% degradation was achieved when suspension was irradiated under UV light in the absence of TiO₂. However degradation under UV + TiO₂ was seen to be 52% after 30 minutes of irradiation.

3.2. Optimization of Process Parameters for the Photocatalytic Degradation of 2,6-DCP

To optimize the values of different operational parameters affecting the degradation, experiments were conducted by varying the catalyst dose (PC-105 TiO₂) from



Figure 1. Photolysis/photocatalytic degradation of 2,6-DCP at natural pH.

0.25 - 1.5 g/L, pH (3 - 11) and initial substrate concentration (5 - 100 mg/L).

3.2.1. Effect of Catalyst Dose

The experiments were performed by varying catalyst dose from 0.25 g/L to 1.5 g/L for substrate solutions of 25 mg/L at natural pH to determine the effect of catalyst loading on the degradation. The results are shown in **Figure 2**. Maximum degradation was seen with 1.25 g/L catalyst dose. Similar findings have been reported for the degradation of other pollutants [19]. The reason can be explained on the basis that optimum catalyst loading is found to be dependent on initial solute concentration because with the increase of catalyst dosage, total active surface area increases, hence availability of more active

sites on catalyst surface [20].

Therefore further studies were carried out using 1.25 g/L catalyst dose.

3.2.2. Effect of pH

As wastewater containing organic pollutants like chlorophenols and dyes is discharged at different pH; therefore it is very important to study the role of pH on degradation. To study the effect of pH on the degradation, experiments were carried out at various pH values, ranging from 3 - 11 for constant 2,6-DCP concentration (25 mg/L) and catalyst loading (1.25 g/L). **Figure 3** depicts the percentage degradation as a function of pH. It can be observed that the maximum rate of degradation was achieved at pH 4. The literature [21-23] suggests that TiO₂ surface



Figure 2. Effect of catalyst (TiO₂) dose on the photocatalytic degradation of 2,6-DCP.



Figure 3. Effect of pH on photocatalytic degradation of 2,6-DCP.

carries the net positive charge at low pH value (zpc for $TiO_2 \sim 6$), while the chlorophenols are primarily negatively and neutrally charged. Therefore, low pH values acilitates the adsorption of chlorophenols promoting their better photocatalytic degradation

3.2.3. Effect of Initial Concentration of 2,6-DCP

After optimizing the catalyst dose and pH conditions (catalyst dose 1.25 g/L and pH-4), the photocatalytic degradation of 2,6-DCP was carried out by varying the initial concentrations of 2,6-DCP from 5 - 100 mg/L in order to assess the appropriate amount of catalyst dose. As the initial concentration of the compound was increased, the rate of photodegradation decreased indicating for either to increase the catalyst dose or time span for the complete removal. Figure 4 shows the time dependent graphs of degradation of 2,6-DCP at different concentrations (5 - 100 mg/L). For solutions of 25 mg/L, almost 100% degradation was achieved within 90 minutes. For 50 mg/L of the 2,6-DCP solution, degradation was 54% in 90 minutes and it get further decreased on increasing the concentration of the substrate. It can be explained on the basis that as the initial concentration increases, more and more organic substances are adsorbed on the surface of TiO₂ but the intensity of light and illumination time are constant.

3.2.4. Kinetic Study

The kinetic analysis of disappearance of 2,6-DCP for an initial concentration of 25 mg/L under optimized conditions is shown in **Figure 5**. The results indicate that the photocatalytic degradation in aqueous TiO_2 can be



Figure 4. Effect of initial concentration of 2,6-DCP on degradation rate.



Figure 5. Kinetic analysis for 2,6-DCP.

described by the first order kinetic model, $\ln(C_0/C) = kt$, where C_0 is the initial concentration and C is the concentration at any time, t. The semi logarithmic plots of the concentration data gave a straight line. The correlation constant for the fitted line was calculated to be $R^2 = 0.96$. The rate constant was estimated to be $4.78 \times 10^{-4} \cdot s^{-1}$.

4. Conclusion

The chloro substituted phenol (2,6-DCP) was successfully degraded using TiO₂ based photocatalysis process under UV light. The disappearance reaction followed pseudo-first order kinetics. The initial rate of photodegradation increased with increase in catalyst dose upto an optimum loading. Further increase in catalyst dose showed no effect. Maximum photodegradation efficiency was obtained in acidic range with 1.25 g/L TiO₂ dose. As the initial concentration of the substrate was increased, the rate of degradation decreased.

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