# Evaluation for the Beneficiability of Yellow Silica Sands from the Overburden of Lignite Mine situated in Rajpardi district of Gujarat, India

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#### **ABSTRACT**

A representative feed sample of Yellow sand was wet-sieved in order to recover the desired fractions for glass making. The mass percentage of (-600 + 300)  $\mu$ m and (-300 + 125)  $\mu$ m fraction was found to be 44.2 and 55.8% (ratio 1:2.26). Hence, this ratio which satisfies the size specifications for glass making sand, was maintained for all the down stream processing studies. The chemical analysis of the 'wet sieved desired fractions for Yellow sand' (WSDFy) i.e., mixture of  $-600 + 300 \mu$ m and  $-300 + 125 \mu$ m fractions, showed that the material does not satisfy IS specifications since it still contains 0.41% iron. WSDFy analysed 95.8% silica, 0.41% Fe<sub>2</sub>O<sub>3</sub>, 0.25% TiO<sub>2</sub> and 0.3% Al<sub>2</sub>O<sub>3</sub>. In order to further value add WSDFy, the same was subjected to attrition followed by magnetic separation. Tests at optimum conditions gave a non-magnetic fraction (sand product) which analysed 98.5% silica with 0.08% Fe<sub>2</sub>O<sub>3</sub>, 0.05% TiO<sub>2</sub> and 0.2% LOI. This is found matching with IS specifications for Grade III sand only.

KEY WORDS: Yellow silica sand, Beneficiation, XRD, SEM, Magnetic separation.

# 1. INTRODUCTION

Silica bearing rocks and minerals such as quartz, quartzite, silica sand together with other varieties of silica like agate, amethyst, jasper, flint etc. are used in a host of industries such as glass, ceramics, foundries, ferro-alloys, abrasives, refractories, ornamentation etc. One of the

first to use silica sand is the glass industry. At least 4000 years ago, long before iron was smelted; glass-making was already a known craft. The oldest known specimens of glass was obtained from Babylon (2600 B. C.) and from Egypt (2500 B. C.). It could be conclusively proved that the glass-making was well established in these countries by around 1500 B. C. [1-4].

Silicon, the main constituent of silica does not occur in free state. But silicon compounds are abundantly available and constitute about 28% of the earth's crust. The range of silica raw materials occurring in nature is quite extensive. The silica, SiO<sub>2</sub>, occurs in different forms such as quartz, (crystalline); chalcedony, agate, flint and jasper (crptocrystalline), and opal (hydrous form); sandstone (sedimentary deposit composed of small grains of quartz); quartzite (metamorphosed derivative of sandstone) and silica sand (weathered sandstone or quartzite enriched in silica). The silica sand is an assemblage of individual silica grains in the size range up to 2mm. Sand can be formed in nature by natural weathering of sandstone and quartzite or mechanically by crushing a sandstone /quartzite or by a process of flotation whereby the various constituents in a pegmatite or kaolin mixture are separated.

The occurrence of silica sand in world is widespread and extensive. Good quality silica sand reserves are situated in UK, Germany, Belgium, France, Brazil etc. Silica sand is available almost in all the states of India. Important deposits are in Andhra Pradesh, Bihar, Goa, Gujarat, Haryana, Karnataka, Kerala, Madya Pradesh, Rajasthan, Tamil Nadu, Uttar Pradesh etc. Haryana is the leading producer followed by UP and Maharashtra. Silica sand also occurs in association with clays and quite often as admixture with siliceous or lignitic overburden.

The uses of silica sand depend on its mineralogy, chemistry and physical properties. It is mainly used for making glass and glass fibre, silicon carbide, sodium silicate, Portland cement, silicon alloys and metals, filter media in water treatment, sand paper and also for foundry sand, hydraulic fracturing, sand blasting, paint and a host of other applications. A major portion of silica sand produced is consumed by glass industry. Important types of glasses made are sheet, flat, bottle, wired and figured, vacuum, laboratory, fiber, shell, flint, ophthalmic, beads etc. There exist both physical and chemical specifications for each use. American Ceramic Society and US Bureau of Standards also give detailed chemical specifications for silica sand for making different types of glasses. After glass, perhaps, maximum standardization has been made for foundry applications. Silica sand is used in both foundry cores and moulds because of its resistance to thermal shocks. Physical properties of the sand is far more important here than the chemical. Silica content of 85% is used in iron castings while for steel foundries it should be minimum 95%. Silica particle size distribution and grain shape are very important for foundry application.

Impurities usually present in the silica sand are free and coated iron oxides, clay, titania and smaller amounts of sodium, potassium and calcium minerals. The iron, being the most detrimental impurity, can be reduced by a number of physical, physico-chemical or chemical

methods, the most appropriate method depends on the mineralogical forms and distribution of iron in the ore [5-8]. Upgrading of silica sand requires partial removal of iron, and other minerals which are detrimental to its end use. While much of the liberated impurities can be reduced or removed by physical operations such as size separation (screening), gravity separation (spiral concentration), magnetic separation etc., some times, physico-chemical (flotation) or even chemical methods (leaching etc.) are to be adopted for the effective removal of iron which may be in intimate association with the mineral quite often superficially. The aim of the investigation is to adopt simple, cost effective as well as environment-friendly processes and operations so that even a small/medium level entrepreneur can set up a beneficiation plant without much capital investment. So it was also decided to employ sieving (screening) and other physical operations as far as possible without going for chemical processing.

#### 2. MATERIALS AND METHODS

The investigation for proving the beneficiability of GMDC sands was initiated by blending the representative samples which were collected by the supplier of the sample (M/S Gujarat Mineral Development Corporation, Ahmedabad, India). The sand is the overburden of a lignite mine situated in the Rajpardi district of Gujarat. Each sample was prepared by thoroughly blending the material by 'centre displacement method' so as to obtain apparently a homogenous material. The 100 kgs of the sand was heaped at one spot and then the entire material was heaped on a second spot by shovelling (thus displacing the centre). This is repeated for 10 times (five heaps at each spot). By this, it is assumed that uniformity is achieved.

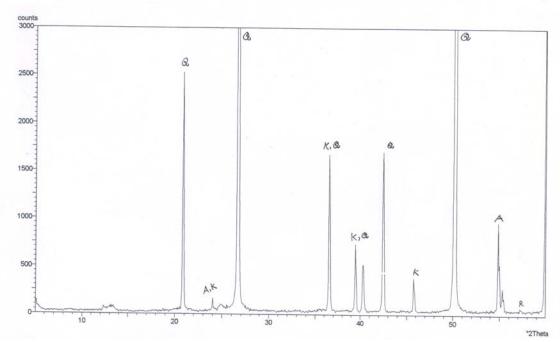
Standard wet chemical methods supported by instrumental analysis were adopted for determining the chemical constituents. The samples were analyzed for silica, alumina, loss on ignition and oxides of iron, titanium, calcium, sodium and potassium. Silica was estimated gravimetrically by volatilizing with hydrofluoric acid, alumina by complexometric (indirect EDTA) titration, iron and titanium by spectrophotometry and calcium, sodium and potassium by flame photometry.

X-ray diffraction (XRD) of the powder sample provides one of the easiest and semi quantitative methods of identifying the minerals present in clays. The powder XRD patterns were obtained on a diffractometer (Philips analytical) using Cu  $K_{\alpha}$  radiation operating at 40KV and 20mA on a diffraction range 5-60 $^{0}$  (2 $\theta$ ). Quartz minerals were observed using scanning electron microscope (SEM) for morphological studies. The grains were mounted on a SEM brass stub. The mounted quartz grains were coated with gold in a vacuum evaporator while the sample was being slowly rotated. Usually 15-20 grains were studied in detail and typical micrographs were taken by using JEOL JSM-5800 scanning electron microscope. The relative densities and relevant bulk densities of the feed and various intermediates and final products were determined by standard methods.

#### 3. RESULT AND DISCUSSION

#### 3.1. Characterization

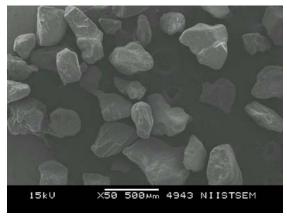
The bulk raw sample was blended to achieve maximum homogeneity. A small amount of Yellow sand sample was drawn from the blended bulk for determining their chemical constituents, mineral contents and physical properties. The presence of quartz, kaolinite, anatase and rutile was shown in the XRD pattern of the raw sample (Fig.1).



Q-Quartz, K- Kaolinite, A-Anatase, R- Rutile

Figure 1. XRD pattern of Yellow silica sand.

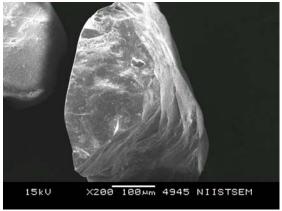
SEM studies reveal that the quartz grains are sub rounded marked by numerous surface pits, etch v'marks, irregular blocks. Weathered, triangular marks and fractured solution pits (Fig. 2) were created by mechanical abrasion and chemical processes.



15kU ×200 100mm 4944 NIISTSEM

a) Grains are sub rounded

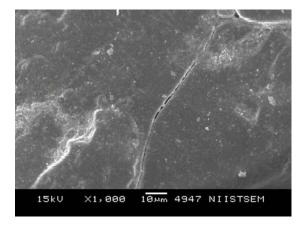
b) Sub-angular grain with conchoidal fracture.



15kU X388 50mm 4946 NIISTSEM

c) Weathered Quartz

(d) Grain showing triangular marks and impact marks and etch v's.



e) Fractured Quartz

Figure 2 Scanning Electron Micrographs of Yellow silica sand.

Chemical analysis was done initially to select the sample(s) based on their silica content before starting the beneficiation experiments (Table 1).

| Constituents     | Wt, % |  |
|------------------|-------|--|
| $\mathrm{SiO}_2$ | 91.5  |  |
| $Fe_2O_3$        | 1.4   |  |
| $TiO_2$          | 0.74  |  |
| $Al_2O_3$        | 4.22  |  |
| $Na_2O$          | 0.16  |  |
| $K_2O$           | 0.01  |  |
| CaO              | 0.6   |  |
| LOI              | 1.37  |  |

Table 1. Chemical analysis of raw Yellow silica sand.

Again at each stage of processing, the products were analyzed for the chemical constituents so that the extent of value addition or suitability of the beneficiation product with respect to standard specifications could be evaluated. The silica value of the raw yellow sand is 95.5% which is better than the White sand. The sample contained aluminium (corresponding to clay) again lesser than that of White sand. Similarly, iron, titania and LOI values were also lower than the White one. However, the yield of the desired fraction (DF  $\rightarrow$  -600 +125 $\mu$ m) is only 72.6% which is lower than the White sand. The sample cannot directly be used for any value added application.

#### 3.2 Laboratory Beneficiation Studies

Laboratory investigation studies were initiated after the completion of characterisation studies on the representative feed sample. BIS has put forth specifications for four grades of silica sand for glass making .The best grade known as Special grade should contain minimum 99% silica with maximum permissible level of 0.02% Fe<sub>2</sub>O<sub>3</sub> and 0.1% TiO<sub>2</sub> for a size fraction in between 600 and  $125\mu m$ . Others are Grade I, II or III in the decreasing order of purity.

# 3.2.1. Wet sieving and mixing of desired fractions (DF)

Wet sieving was carried out in tune with the requirements for glass making sand and hence the sieves selected were 1000, 600, 300 and 125µm. The data are given in Table 2.

Table 2. Wet sieve analysis of Yellow raw silica sand sample and chemical characterization of 'wet-sieved desired fractions' (WSDFy).

| Sie | eve Size, | %Wt. |         |                                |                  |           |                   |                  |      |      |
|-----|-----------|------|---------|--------------------------------|------------------|-----------|-------------------|------------------|------|------|
| μm  | 1         |      |         |                                |                  |           |                   |                  |      |      |
| +10 | 000       | 5.4  |         |                                |                  |           |                   |                  |      |      |
| -10 | 000, +600 | 16.5 |         |                                |                  |           |                   |                  |      |      |
| -60 | 0, +300   | 32.1 |         |                                |                  |           |                   |                  |      |      |
| -30 | 00, +125  | 40.5 |         |                                |                  |           |                   |                  |      |      |
| -12 | 2.5       | 5.5  |         |                                |                  |           |                   |                  |      |      |
|     |           | %Wt. | $SiO_2$ | Fe <sub>2</sub> O <sub>3</sub> | TiO <sub>2</sub> | $Al_2O_3$ | Na <sub>2</sub> O | K <sub>2</sub> O | CaO  | LOI  |
| WS  | SDFy      | 72.6 | 95.8    | 0.41                           | 0.25             | 0.3       | 0.007             | 0.004            | 0.04 | 0.33 |

The fraction above 600μm is coarse grits, which is about 21.9% of the feed sample and was removed since it is not suitable for glass making (This may be used for land filling). Similarly, the fraction below 125μm (~5.5% of feed sample) which contains mostly kaolin (clay mineral) is also rejected. The weight fraction of –600, +125μm 'cut' which is about 72.6% is the 'Desired Fraction' (DFy) as per the size specification. We shall denote it as 'WSDFy' since it is wet-sieved. In WSDFy, while -600, +300μm is 44.2%, the other fraction (-300, +125μm) is 55.8% which satisfies the IS specifications. Though the mass proportion as per the specification is satisfied, the chemical analysis (Table 2) showed that the material is not suitable for any glass making; hence WSDFy was subjected to further processing.

#### 3.2.2. Attrition

Since the combined iron was found to be mainly as coating on the surface of the sand grains, it was decided to go for attrition followed by magnetic separation. Attrition tests carried out in Netzsch mill, PE 075, which is a vertical cylindrical attritor jar fitted with a specially designed agitator. The mill was charged with 1.24 Kgs. of the attrition medium, viz., fused ceramic beads of 1-1.3 mm size and later on the material was added to the mill in slurry form. The agitator was switched on and was brought to the required rpm. The mill has got external cooling system for removing the heat generated during the attrition process. After completion of the set time, the total charge was taken out and the attrition media was separated from the slurry by sieving.

For the tests with Yellow silica sand, the agitator rpm was kept at 1150 so as to generate a small vortex at the centre of the attritor jar. Two variables were tried: 'slurry solid content' and the 'attrition time'. Solid loading was varied from 10 to 60%. Towards 55%, externally circulated cooling water of the attritor was getting heated up and at 60%, the contents did not move at all

due to high viscosity. Hence the optimum solid loading has been taken as 50%. Data are presented in Table 3.

Table 3. Influence of solid loading on attrition → impurity liberation and removal.

| Solid loading, Wt% | Non-magnetic product |                                 |                   |                                   |
|--------------------|----------------------|---------------------------------|-------------------|-----------------------------------|
|                    | %SiO <sub>2</sub>    | %Fe <sub>2</sub> O <sub>3</sub> | %TiO <sub>2</sub> |                                   |
| 15                 | 95.6                 | 0.290                           | 0.071             |                                   |
| 35                 | 95.9                 | 0.271                           | 0.069             |                                   |
| 45                 | 96.1                 | 0.263                           | 0.063             |                                   |
| 50                 | 96.7                 | 0.210                           | 0.052             |                                   |
| 55                 | 96.6                 | 0.213                           | 0.056             | <ul> <li>Cooling water</li> </ul> |
| 60                 | Could not            | subject to attriti              | _                 | ng heated up                      |

Fixed conditions: Media -1.24 Kg., Size-1-1.3mm fused ceramic beads;

Attrition time –10minutes, agitator rpm-1150

Magnetic separation: Magnetic field (equivalent current in Amp.) -3.2

Medium: Iron balls (diameter of 6.3 mm) -1.248 Kg.

(Total slurry volume – 250 ml)

Table 4. Influence of attrition time on impurity liberation and removal.

| Non-magnetic product |                                       |   |  |
|----------------------|---------------------------------------|---|--|
| %SiO <sub>2</sub>    | $%Fe_{2}O_{3}$                        | %TiO <sub>2</sub>   |  |
| 96.0                 | 0.290                                 | 0.040   |  |
| 96.7                 | 0.210                                 | 0.052   |  |
| 96.7                 | 0.209                                 | 0.050   |  |
| 97.8                 | 0.210                                 | 0.052   |  |
| 97.8                 | 0.207                                 | 0.053   |  |
|                      | %SiO <sub>2</sub> 96.0 96.7 96.7 97.8 | %SiO <sub>2</sub> %Fe <sub>2</sub> O <sub>3</sub> 96.0 0.290 96.7 0.210 96.7 0.209 97.8 0.210 |  |

Fixed conditions: Media -1.24 Kg., Size-1-1.3mm fused ceramic beads;

% Solids for attrition –50; agitator rpm-1150

Magnetic separation: Magnetic field (equivalent current in Amp.) -3.2

Medium: Iron balls (diameter of 6.3 mm) -1.248 Kg.

(Total slurry volume – 250 ml)

The attrition media was removed by sieving the product slurry using a  $600\mu m$  sieve. No sand was found along with the recovered media. The whole slurry was passed through a  $125\mu m$  sieve so as to remove the liberated iron impurities along with the over-ground (fine) sand. The

attrition resulted in size reduction of sand and attrition medium. The particle size distribution before and after attrition is presented in Table 5.

| Sieve Size, μm | %Wt.             |                 |  |
|----------------|------------------|-----------------|--|
|                | Before attrition | After attrition |  |
| -600, +300     | 44.2             | 43.0            |  |
| -300, +125     | 55.8             | 53.8            |  |
| -125           | Nil              | 03.2            |  |

Table 5. Particle size distribution before and after attrition.

It could be seen that about 3.2% of  $-125\mu m$  fraction was generated (w.r.t. WSDFy) which was removed by screening through 125 micron screen. The mass distribution between desired fractions (i.e., -600, +300 and-180, +125 $\mu m$ ) after attrition is slightly changed, however it does not affect the specifications.

As already stated above, attrition operation generates a sand fraction of about 3.2% below 125µm w.r.t. WSDFy. This is considered to be a loss since fraction below this size cannot be used for glass making. This is equivalent to 2.3% w.r.t. the raw sand sample. This includes the liberated iron and titanium minerals which is, relatively, a very small quantity. The grinding media loss has been estimated to be about 1.5%.

#### 3.2.3. Magnetic separation

A wet high intensity magnetic separator (WHIMS) which can generate an optimum magnetic field of 1.8 Tesla (18000 Gauss) at a maximum input current of ~3.2 Ampere was used for magnetic separation. The magnetic separation, which is integral with the attrition, was carried out using a Carpco machine which was operated on batch basis. The 'canister' (separating chamber) of the magnet was filled with the medium which, in the present case, is iron balls (1.248 Kg.) of about 6.3 mm in diameter (small size) and the magnetic field was generated by switching on the current. The dry sample was spread on the top of the medium and water was added manually and uniformly on the surface so that it wets the material and takes it through the voids among the balls. The water equivalent to 25% slurry was added initially. The liberated magnetic particles were caught by the iron balls and the sand slurry flows through the medium down to the collection pot unaffected by the field. Plain water was added into canister over the balls as wash water in order to dislodge the sand particles entrapped among the balls. The washings were collected along with the non-magnetics, i.e., product yellow sand. After the

product sand was collected, the magnetic field was switched off and the canister was flushed with water in order to dislodge the magnetics (iron impurities) from the medium. Later on, the balls were taken out and again washed to collect the final traces of the sticking iron particles. Both the materials were dried and weighed.

While WSDFy after attrition and magnetic separation at optimized conditions was found to satisfy Grade III specification for glass making, the iron content could not be reduced below 0.08%. Salient results of tests such as LOI and other chemical assays and size grading for the product yellow sand are given in Table 6.

Table 6. Comparison of Product Yellow sand with respect to 'Grade III' glass making sand.

#### (i) Chemical

| Chemicai                       |  |   |
|--------------------------------|--|---|
| Characteristics                | Product  | Grade III   |
| (% by mass)                    | Yellow   | specifications  |
|                                | sand   |   |
| Loss on ignition,              | 0.2  | 0.5   |
| Max.                           |  |   |
| Silica (as SiO <sub>2</sub> ), | 98.5   | 97  |
| Min.                           |  |   |
| Iron Oxide (as                 | 0.08   | 0.1   |
| $Fe_2O_3$ ), Max.              |  |   |
| Aluminium                      | 0.14   |   |
| Oxide (as                      |  |   |
| $Al_2O_3$ ), Max.              |  |   |
| Titanium                       | 0.05   |   |
| Dioxide ( as                   |  |   |
| TiO <sub>2</sub> ), Max.       |  |   |
| Manganese                      |  | To pass   |
| Oxide (as MnO)                 |  | the test  |
| Copper Oxide                   |  | To pass   |
| (as CuO)                       |  | the test  |
| Chromium                       |  | To pass   |
| Trioxide (as                   |  | the test  |
| $Cr_2O_3$                      |  |   |
|                                | Characteristics (% by mass)  Loss on ignition, Max.  Silica (as SiO <sub>2</sub> ), Min.  Iron Oxide (as Fe <sub>2</sub> O <sub>3</sub> ), Max.  Aluminium Oxide (as Al <sub>2</sub> O <sub>3</sub> ), Max.  Titanium Dioxide (as TiO <sub>2</sub> ), Max.  Manganese Oxide (as MnO) Copper Oxide (as CuO) Chromium Trioxide (as | Characteristics (% by mass) Yellow sand  Loss on ignition, 0.2  Max.  Silica (as SiO <sub>2</sub> ), 98.5  Min.  Iron Oxide (as 0.08  Fe <sub>2</sub> O <sub>3</sub> ), Max.  Aluminium 0.14  Oxide (as Al <sub>2</sub> O <sub>3</sub> ), Max.  Titanium 0.05  Dioxide (as TiO <sub>2</sub> ), Max.  Manganese Oxide (as MnO)  Copper Oxide (as CuO)  Chromium Trioxide (as |

# (ii) Size grading (Table 6 continued)

|                     | Product Yellow sand | IS Specifications for Grade III Glass making sand |
|---------------------|---------------------|---|
| Retained on         |                     |   |
| 1 mm IS sieve       | Nil                 | Nil   |
| Retained on 600     |                     |   |
| micron IS sieve,    |                     |   |
| % by mass, Max.     | Nil                 | 01.0  |
| Passing through 600 |                     |   |
| micron IS sieve,    |                     |   |
| but retained on 300 |                     |   |
| micron IS sieve,    |                     |   |
| % by mass, Max.     | 43                  | 50.0  |
| Passing through 300 |                     |   |
| micron IS sieve,    |                     |   |
| but retained on 125 |                     |   |
| micron IS sieve,    |                     |   |
| % by mass, Min.     | 53.8                | 50.0  |
| Passing through 125 |                     |   |
| micron IS sieve,    |                     |   |
| % by mass, Max.     | Nil                 | 05.0  |

In comparison with BIS specifications for Grade III glass making sand, the Product of beneficiation is 'Grade III glass making sand' while the coarse grit (+600 micron) can be taken as a byproduct.

# 3.3 Suggested beneficiation flow sheet for Yellow silica sand

Based on the laboratory processing studies conducted on the blended raw sand sample in order to establish the beneficiability of Yellow silica sand, a beneficiation flow sheet is suggested as follows.

The overburden sand is first wet-screened using a single deck vibrating screen having a 600  $\mu m$  screen. The oversize grits is collected separately to be used as a land fill while the undersize slurry is pumped to a second stage double deck vibrating screen fitted with 300 and 125  $\mu m$  screens. Both +300 and (-300 +125) fractions are taken together and this slurry after adjusting the pulp density is sent to attrition mills. The attrited sand slurry is screened using a vibrating screen fitted with 600  $\mu m$  screens in order to remove the attrition media. If required additional water can be added at this stage. The sand slurry is then passed through 125  $\mu m$  vibrating screen so as to remove the slimes which contains a major portion of the liberated iron and some broken attrition media as well as over-milled silica sand particles. The desired fraction (-600 +125 $\mu m$ ), after adjusting pulp density is pumped to wet high intensity magnetic separators to remove the remaining iron impurities. The non-magnetic slurry containing the desired silica sand fraction is collected and pumped to the hydrocyclones for first stage de-watering and finally to a spiral classifier for 2<sup>nd</sup> stage and final dewatering to obtain Grade III glass making sand as the principal product. The coarse grits from the 1<sup>st</sup> screen can form a by-product which can be used for land filling.

#### 4. CONCLUSIONS

The investigation was carried out on Yellow silica sand samples in order to evaluate their beneficiability for value addition. Initial characterization showed that the main impurities are iron and titania minerals in the sample. The results of beneficiation studies reveal that while wet sieving/screening removes majority of these contaminating minerals to give an intermediate product sand, attrition and magnetic separation is required to upgrade the same to grade III glass making sand. Coarse grits, (+600µm) can be considered as a by-product which can be used for landfill. Based on the laboratory study, beneficiation flow sheets have been suggested for the yellow silica sand samples.

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