Assessment Of Beneficiation Routes Of Tantalite Ores From Key Locations In Nigeria

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Abstract:

The beneficiation methods for some tantalite ores from selected deposits in Nigeria have been assessed through mineralogical and compositional analyses of the ores. Tantalite ores obtained from eight different well-known locations of the mineral in the country were analyzed with ¹⁰⁹Cd excitation source Energy Dispersive X-ray spectrometry using the emission-transmission method of quantification. The major minerals detected and quantified include TiO₂, MnO, Fe₂O₃, Ta₂O₅, Nb₂O₅, WO₃, Th and U. Impurity elements such as Hf, Zn, Zr, Co, Pb, Rb, and Y were also observed and evaluated. Our analyses further show that Ta₂O₅ in the ores ranged from a minimum concentration of about 8% in Otu to about 60% in the Egbe deposits, while the Nb₂O₅ concentrations in the ores ranged from about 20% to 37.5% with the highest coming from the Ofiki deposit. Based on these results and the work of other authors, we deduced that clean-up operations might be adequate for Ta extraction from most of the tantalite deposits in Nigeria. The consideration of simplicity and cost of process favours the direct dissolution of the ores in HF for the clean-up operations.

Keywords: Tantalite ores, Elemental Composition, EDXRF

INTRODUCTION

Nigeria is blessed with abundant mineral resources. These include vast deposits of coal, cassiterite, columbite, marble, limestone, clay, bitumen and tantalite. While some of these m inerals are currently m ined, several others have been identified to have huge potentials of being exploited in com mercial scale. The Federal Government of Nigeria is paying renewed attention to the solid m ineral sector; therefore, development activities in the sub-sector are expected to increase many-fold. Recent studies conducted by the Raw Materials Research and Developm ent Counc il (RMRDC) have show n that the need to develop capacity for processing of these m inerals into interm ediate products is the m ost important requirement of the solid mineral sector in the country [1].

The recovery of tantalite in Nigeria dates back to the 1940's as a by-product of cassiterite mining [2, 3]. Later, large t onnages of granite c ontaining about 0.26% Nb $_2O_5$ in urania pyrochlore (3.1% U $_3O_8$, 3.3% ThO $_2$, 37.5% Nb $_2O_5$ and 3.5% Ta $_2O_5$) were

identified. The reserves were however not confirmed. Primary deposits of huge economic value of the ore have now been reported in various parts of the country [4, 5, 6]. Indeed, Nigeria is currently rated to be the 7th largest producer of tantalum resources in the world [7]. The production in 2004 was estimated at 25 metric tons.

Tantalite is the most important mineral form of tantalum, a specialty m etal used mainly in the electronics industry for the m anufacture of capacitors and in several specialty alloy applications. The beneficiation of tantalite ores usually involves preconcentration, primary concentration and con centrate clean up. The choice of any or all of these processes would depend on the nature of the ore, p articularly the conten t of Ta_2O_5 in the o re r elative to its as sociated m inerals a nd im purities. Typica lly, mechanically mined ores contain less than 0.1%Ta 2O₅, and would ther efore essentially require enrichment through the three processes stated above. The concentration processes may be carried out by wet gravity, m agnetic or electrostatic m ethods or by flotation to produce concentrates containing up to 70% com bined Ta 2O5 and Nb 2O5 to m eet extraction requirem ents. However, th e universally em ploved m ethod for the concentration of tantalite ores is g ravity separation – the separation of two or m ore minerals as a result of differences in speci fic gravity and their m ovement in response to the force of gravity and one or m ore other forces [8, 9]. Other m ethods, when used, are employed in the final cleanup of gravity concentrates.

Furthermore, Burt [10] had noted that c oncentrates suitable for further processing to recover Ta are generally required to ex ceed 25% Ta $_2O_5$, with 50% combined Ta $_2O_5$ and Nb $_2O_5$. Primary ores with these Ta $_2O_5$ and Nb $_2O_5$ contents would only need clean-up operations for Ta extraction processes. The clean-up operation results in the rem oval of associated m inerals and im purity elem ents to a to lerable ex tent. Typica l assoc iated minerals include zircon, rutile, m onazite, cassiterite, ilm enite, garnet, uranium and thorium m inerals, beryl, spodum ene, tourm aline and, in som e cases, aquam arines and gold: light m inerals such as quartz and feld spar m ay also be present due to inefficient primary concentration.

A number of reports [11, 12] have give n the mineralogical composition of Ta-Nb ores obtained from a few locations in the m iddle belt region of Ni geria. However, the limitation of these previous wo rks is the failure to relate the results to an upgrading process for a value-added Nigerian tantalite.

The main objective of this work is to assess the appropriate beneficiation schemes by identifying the as sociated elements and impurity elements in sam ples obtained from notable tantalite deposits across Nigeria. The associated elements are known to contribute to the physical characteristics of the Tam ineral and thes e characteristics dictate the beneficiation methods. The outcom e of the work reported here would therefore provide critical information about the appropriate r outes for the beneficiation processes needed for value addition to the Nigerian tantalum industry.

MATERIALS AND METHODS

Eight sam ples were collected from differe nt notable deposits in Nigeria. The sources are Egbe, Komu, Nassarawa, Agunrege, Baba Ode, Ofiki, Igbo Ijaye and Otu. Six of the locations a re in Oyo Sta te in the S outh Western Nigeria; one location is in Kogi State while one is in Nassarawa State, both deposits located within the middle belt region of the country. The sam ples were obtained from miners in the study areas. The m iners employ manual methods of mining, in which the samples would have been upgraded to some extent by hand sorting. Measurem ents of the major constituents and trace elements were carried out using a ra dioisotope source Energy Disp ersive X-Ray Fluorescence (EDXRF) Spectrometer at the Centre for Energy Research and Training, Ahm adu Bello University, Zaria, Nigeria.

The samples were ground manually to powder with an agate m ortar and pestle to grain size of less than 125 μ m. Pellets of 19 mm diameter were prepared from 0.3 – 0.5g powder mixed with three drops of organic liquid binder and then pressed at 10 tons with a hydraulic press. Measurem ents were perform ed using an annular 25 m Ci ¹⁰⁹Cd as the excitation source, which em its Ag-K X-rays (22.1 keV) in which case all elem ents with lower characteristic excitation en ergies were accessible for detection in the samples. The system further consists of a Si(Li) detect or, with a resolution of 170 eV for the 5.90 keV line, coupled to a com puter controlled ADC -card. Further details about the system have been given elsewhere [11, 13,14].

Quantitative analy sis of the s amples was carr ied out us ing the Em ission-Transmission (E-T) m ethod, for which a num ber of quantification m ethods has been developed and applied [13 - 18]. These quantification m ethods provide different approaches to correct the matrix absorption as well as enhancem ent effects. In this work quantification was carried ou t using a m odified versi on of E-T m ethod [11, 19, 20], which involves the use of pure target m aterial (Mo) to measure the absorption factors in the sam ple. The Mo target serves as a source of m onochromatic X-rays, which are excited through the sample by prim ary radiation and then penetrate the sam ple on the way to the detector. In this way, the abso rption factor is experimentally determined. The program then uses the factor in the quantification of concentration of the elements. In addition, the contribution to the Mo-K peak in tensity by the Zr-K is subtracted for each sample. The spectra for the sam ples were collected for 3000s with the ¹⁰⁹Cd and the spectra were then evaluated using the AXIL-QXAS program [21]. It was noted that very light mineral associations of the Ta ores could not be determined due to the absence of an ⁵⁵Fe excitation source.

RESULTS AND DISCUSSION

The results of the m ineralogical analysis including a num ber of impurities/trace elements are shown in Tab le 1. The results show that the Egb e sam ple contains the highest Ta_2O_5 content at 59.58%. The Ta $_2O_5$ contents of Kom u, Nassarawa, Agunrege,

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Baba Ode, Ofiki, Igbo Ijaye and Otu ore samples are respectively 49.57%, 46.15%, 45.42%, 42.00%, 36.63%, 23.64% and 8.00%. The resu Its further showed that the samples also contain appreciable amounts of Nb₂O₅ and TiO₂. Other mineral ores/phases identified and quantified include MnO, Fe₂O₃, WO₃, Th and U. Impurities/trace elements such as Hf, Zn, Zr, Co, Pb, Rb, and Y were also determined.

	-8	
wa e	Ijaye	
3.81 1.64	.05 20.36 33.38	
±0.42 ±0.3	$0.33 \pm 0.58 \pm 0.67$	
0.03 5.80 6.69	0.10 3.46 0.74	
±0.17 ±0.13 ±0.1	$0.18 \pm 0.12 \pm 0.09$	
.51 10.69 7.37	.86 9.66 9.70	
±0.14 ±0.23 ±0.1	0.13 ±0.21 ±0.20	
9.57 46.15 45.4	6.63 23.64 8.00	
±0.54 ±0.52 ±0.4	$0.42 \pm 0.40 \pm 0.17$	
9.18 24.86 31.1	7.48 28.90 22.43	
±0.23 ±0.20 ±0.2	0.29 ±0.29 ±0.17	
.38 1.80 -	0.32 0.17	
=0.13 ±0.14	±0.09 ±0.05	
8.43 -		
±1.97		
0.26 0.31 0.18	.11 0.13 -	
=0.05 ±0.05 ±0.0	0.04 ±0.04	
0.22 0.09 -	.07	
=0.03 ±0.03	0.02	
0.12 0.26 0.15	.17 0.06 0.06	
±0.01 ±0.01 ±0.0	$0.01 \pm 0.01 \pm 0.01$	
70 1720 -	20	
±146 ±195	146	
20 ±47		
333 ±51 -		
0.03 0.15 0.02	.05 0.03 0.01	
0.37 0.65 0.42	.57 0.28 0.27	
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Table 1: Mineralogical Analysis of Tantalum Ore Samples From 8 Different Locations in Nigeria. A aumana Daha Offici

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The elem ental Ta content in the respective ore sam ples are 48.79%, 40.59%, 37.79%, 37.19%, 34.39%, 30%, 19.36% and 6.55% respectively for Egbe, Kom u, Nassarawa, Agunrege Baba Ode, Ofiki, Igbo Ijaye and Otu. An earlier work by Funtua [11] put the Ta content in the central pegmatite region around Jos, Nassarawa and Jama'a between 21 and about 30%. areas of central Nigeria at We note that this figure is somehow less than the Nassarawa ore found to be about 38% in the current investigation. The difference could probably be explained in terms of the diversity in the ore contents from site to site and from ore vein to ore vein.

In terms of beneficiation, the density of Ta-Nb minerals allows concentration with other heavy minerals by gravity methods; sluices, jigs, spirals and shaking tables are used in conjunction with screen sizing; other proc esses, when used, are employed in the final cleanup of gravity concentrates. Ta-Nb is separated from other heavy m inerals by a combination of high-tension electrostatic and high-intensity electrom agnetic m eans.

Eales

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Concentrates from Nigerian placer deposits, which ar e worked pr imarily for cassiterite, are dried and treated by m agnetic separators to r emove the m agnetic constituents: magnetite, ilmenite, columbite, monazite and magnetic cassiterite. The magnetic fraction is then re- treated to sepa rate the d ifferent minerals. Columbite, monazite and m agnetic cassiterite are weak ly magnetic. Columbite and magnetic cassiterite are separated on air flotation tables, whereas columbite and m onazite are s eparated e lectrostatically [2]. Classification, screening, and desliming ar e employed as adjuncts, depending on the composition of the ore. Treatment schemes vary from the most primitive hand methods to extremely com plex modern plants [22]. The liberation of values from waste must be carried out with care, since all tantalum minerals are friable, and, ac cording to Burt [10], concentration efficiency decreases with decreasing particle size.

Gravity p lant con centrate, grad ing approx imately 25% Ta ₂O₅ is g enerally upgraded to 50% in a clean-up plant. The Nb content in the ore is very im portant. Concentrates suitable for further processi ng to recover Ta are generally required to exceed 25% Ta₂O₅, with 50% combined Ta₂O₅ and Nb₂O₅ [10]. The ores below this level of $Ta_2O_5 - Nb_2O_5$ content need to be enriched by methods discussed above. The tantalum ores from Egbe, Komu, Nassarawa, Agunr ege, Baba Ode and Ofiki all have Ta $_{2}O_{5}$ -Nb₂O₅ combined content of about 70%, with the Ta₂O₅ contents of over 25%. Thus these up operations, without pre-concentration or ores can be subjected directly to cleanprimary concentration, for the rem oval of a ssociated minerals. Many of the ores m ay even be subjected to direct hydrom etallurgical extraction processes without going through clean-up operations. This is because their Ta 2O5 contents fall into categories for which technologies have specifically been developed as raw materials of different origins and grades [23], as shown in Table 2. The ore sample from Igbo Ijaye, which contains 23.64%Ta₂O₅ is rich enough for prim ary concentration, while the Otu ore sam ple, with 8%Ta₂O₅, would be enriched right from the pre-concentration stage (Table 3). These two ore samples were however found to have a high T iO_2 content of 20.36% and 33.38% respectively. Although the Otu figure is lower than that of a recently studied rutile sample [24], it would be appropriate to treat the ore pr imarily f or rutile r ecovery and then secondary recovery for tantalite and niobite.

Technology	Raw Material Input	%Ta/Ta ₂ O ₅
Pyrometallurgy	Low – Medium Grade Tin Slags	$2 - 10\% Ta_2O_5$
Chlorination	Alloys, Scraps	40-100%Ta
Hydrometallurgy	Natural Ores	20 - 40%Ta ₂ O ₅
	Synthetic Concentrates	20 - 40%Ta ₂ O ₅
	High Grade Tin Slags	>15%Ta ₂ O ₅

Table 2: Correlation between technology and raw material input [23]

The main associations of Ta $_2O_5$ in the ores under investigation apart from Nb $_2O_5$ and rutile are hematite, wolframite, uranium, cassiterite minerals as well as hafnium, zinc and zirconium elements with other trac e elements. We note that because T iO₂ and MnO are param agnetic and Fe $_2O_3$ is ferrom agnetic, they can be separated from the ore by magnetic separation, whereas electrostati c separation can be employed to rem ove cassiterite, hem atite, ilm enite, tan talite, n iobite and wolf ramite, which a re electrically

conducting, from the ore, leaving the non- conducting zirconium com pounds in the gangue. An earlier work by our group [25] had not been able to present the data shown in this work on the impurity/trace element contents of the ores. Most of these elements would go into the gangue during the elimination of the major constituents by the physical and subsequent chemical methods.

Table 3: Recommended beneficiation routes for different grades of Ta_2O_5 ores (Adapted from table provided by Burt, [10])

Ta ₂ O ₅ Content (%)	Sample Sources Content (%Ta ₂ O ₅)	Beneficiation Route
<10	Out (8.00)	Preconcentration (sizing, gravity
		separation
10 - 25	Igbo Ijaye (23.64)	Primary concentration (jigs and sluices)
		Hydraulic classification
		Stage treatment (spirals, shaking tables)
>25	Egbe (59.58), Komu (49.57,	Concentrate clean-up (floatation,
	Nassarawa (46.15), Agunrege	leaching, magnetic or electrostatic
	(45.42), Baba Ode (42.00), Ofiki	separation)
	(36.63)	

We note further that based on the characteristics of the ores analysed in this study. a prelim inary tre atment f or the samples would be fusion with K $_2CO_3$, which would separate Sn, Fe, Mn and TiO 2 from the earth acid s [26]. The approach in this case, is to fuse at red heat with threefold excess of K₂CO₃, dissolve the fused mass in water, filter, then precipitate the tantalum and niobium as the sodium salts. However, the num ber of steps and am ount of reagents required could make this process expensive. Gustion and Pilloton [26] observed that direct dissolution of ores in HF as a clean-up operation would not always produce adequate solution for separation by crystallization or liquid extraction. Thus an alternative route to eff ect a rough purification is to fuse them with caustic. The fused m ass would then be leached with water to remove excess c austic, Sn and W. The Ta and Nb, in the form of complex tantalates and niobates, are insoluble. An acid leach would then dissolve Fe, Mn, Alkalies, and alkaline earths, leaving as a residue a m ixture of the acids, T i, and traces of other contam inants. However, Gustion and Pilloton [26] showed that six add itional operations must be added to those required by direct HF dissolution in order to accomplish this. These are caustic fusion, crushing of the fusion mass, water leach, filtration of water-leach liquor, acid leach and filtration of acidleach liquor. The caustic fusion step is a hi gh-labour operation. Furth ermore, the labour requirements for each filtration step are about the same as for direct dis solution, so that filtration costs rise 100 -200% over the direct dissolution operation. Leaching in water requires about 50% as m uch labour as direct d issolution, but since leach ing in acid is comparable to direct d issolution the wet processing of the upgra ded ores altogether a direct dissolu requires about 100-150% m ore labour than tion operation. The consideration of simplicity and cost of proc ess therefore favours the direct dissolution of the ores in HF to dissolve Ta, Nb, Fe, Ti, Mn and W. In practice, the adv antages and disadvantages of caus tic fusion p rior to the HF leach m ust be carefully evaluated. The decision to use caustic fusion depends mainly on the type of ore that is treated and on the method of separation used. If chem ical a nd equilibria data were available for the

dissolution process, it m ight be possible to m aximize Ta and Nb dissolution with minimum dissolution of the gangue material.

Finally, it is appropriate to m ention here that depending on the country or region of exportation, som e Ta/Nb m inerals cannot be shipped out of their r country of origin because of their levels of radioactiv ity. The limits of allowed uranium and thorium oxide contents are $0.1 \ \%U_3O_8$ and 0.1%ThO $_2$ [27]. All the ore sam ples under investigation would not pass through such trans portation regulation for their U $_3O_8$ content while Egbe and Nassarawa sam ples would not pass through as a result of their ThO $_2$ content. This measure in principle could create a market problem for the tantalite ores originating from these Nigerian deposits. Where there are ready buyers because of the strategic importance of the end product, i.e. the tantalum metal/compounds, the crude ore is substantially reduced in value because of their radioactive contents. However, Krismer and Hoppe [28] have developed a process for the recovery of the non-radioactive m etal compounds from the ores containing com plexes of U and Th. The gangue can now be treated to recover uranium as an additional economic by-product [29].

CONCLUSION

The analysis of the tantalum ores from eight different notable deposits in Nigeria using EDXRF spectrom etry has shown that the Nigerian tantalum ores are of relatively high quality and can therefore be subjected to direct processing for tantalum products without the need for com plex and costly preconcentration procedures. The consideration of simplicity and cost of process favours the direct dissolution of the ores in HF. The simultaneous evaluation of rutile and niobium in the ores allows for the assessment of the suitability of the ores for prim ary/secondary recovery processes of rutile and niobium products. In addition, the XRF technique offers the possibility of determining other major constituents such as Fe, Mn, W , Th, U, Hf, Zn and Zr. The tantalite m ineral can be separated from the ore leaving the radioactive elements in the gangue, the secondary recovery of which is an added econom ic advantage. The knowledge of the presence of Co, Pb, Rb, and Y, as well as radioactive elements in the s amples would assis t in evaluating co-dissolved species as well as the development of appropriate beneficiation routes for value-addition to the mineral in Nigeria.

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